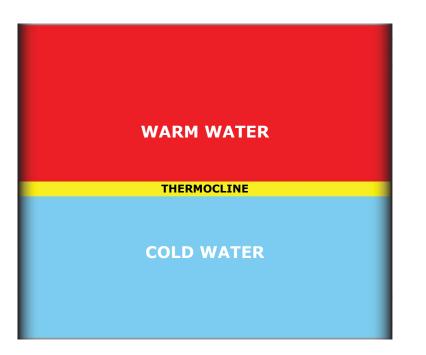


Key Design Elements

- 1. Pressure drop is low
- 2. Tank must be insulated to minimize losses
- 3. Must ensure stratification
- 4. Must minimize thermocline
 - Low Froude Number
 - Laminar flow through diffuser slots



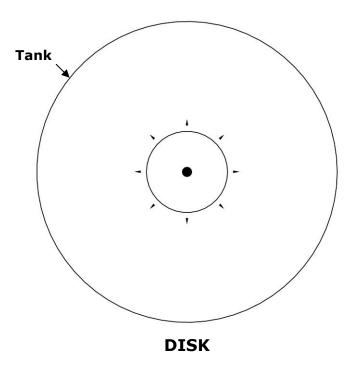
Thermal Storage Tank Stratification

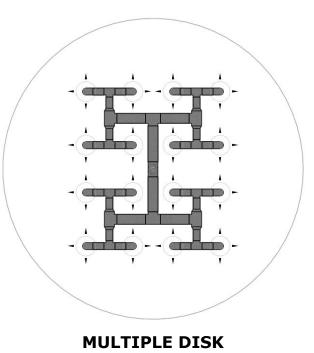






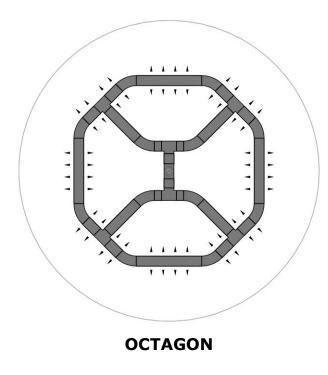
Water Diffuser Systems

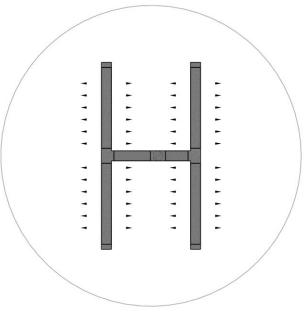






Water Diffuser Systems

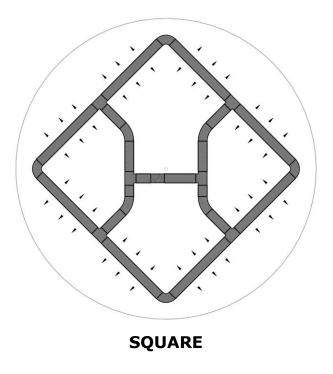


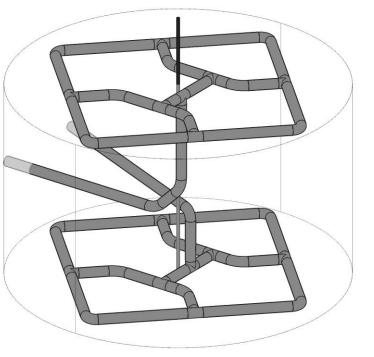


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Water Diffuser Systems

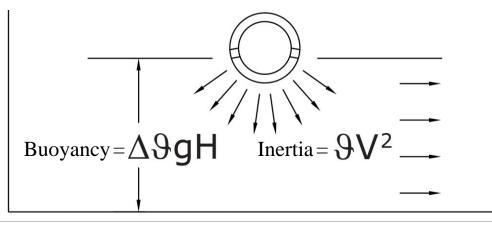






Froude Number

The Froude Number is the single most important design parameter in the design of the distribution system. It is the ratio of dynamic (inertial) forces to weight (buoyancy forces). A low Froude Number insures that the buoyancy forces predominate over inertia forces and allow the tank to be stratified.





Froude Number

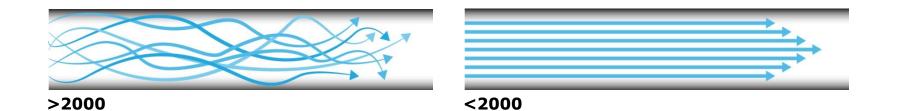
Q/L (gH³ x (∆୫/୬))¹/2

- Q/L = Volume flow rate per length of diffuser
 - **g** = Gravitational acceleration
 - H = Height of diffuser
- $\Delta \vartheta$ = Difference in water density = $\beta(T_{W} T_{C})$
 - ϑ = Density of inlet water



Reynolds Number

The Reynolds Number is the ratio of inertial forces to viscous forces. The critical Reynolds Number distinguishes between laminar or turbulent flow. A Reynolds number below 2000 is required to limit mixing action.





Reynolds Number

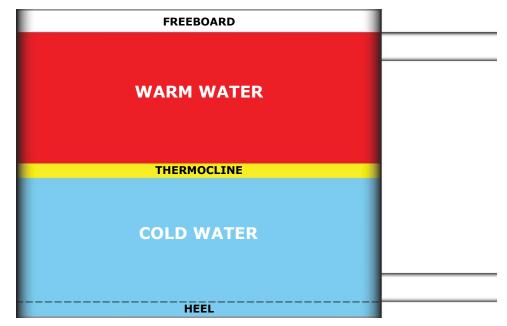
Q/L = Volume flow rate per unit length of diffuser υ = Kinematic viscosity

1)

L



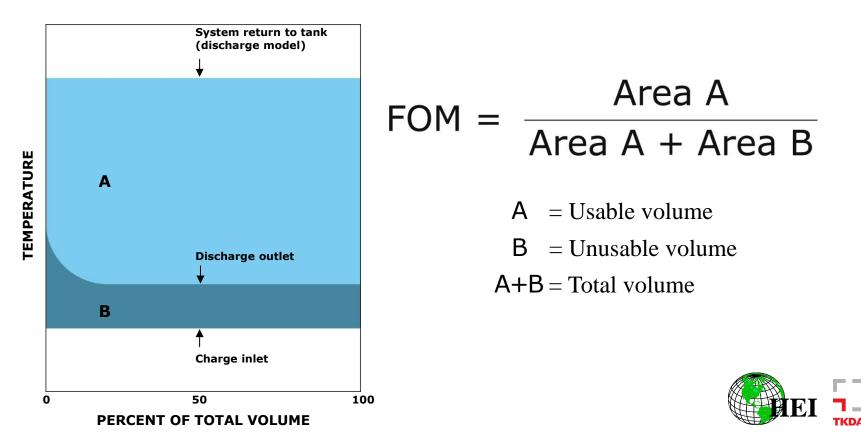
TES Capacity



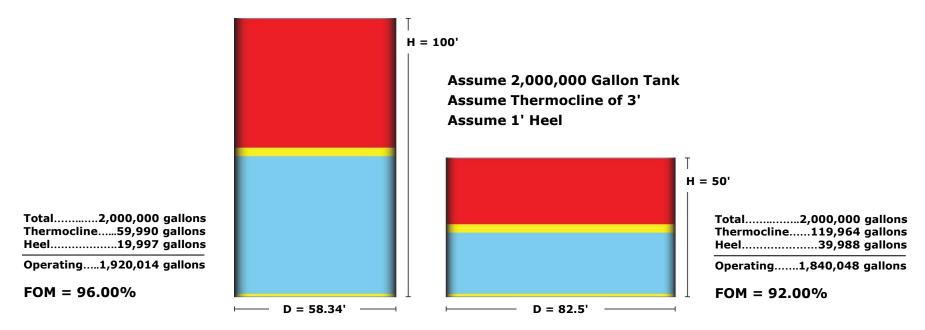
Net Storage Capacity = Total Capacity – (Freeboard + Thermocline + Heel)



Figure of Merit (FOM)



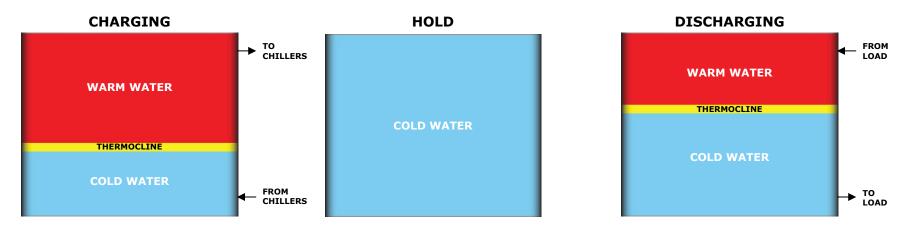
Tank Sizing: Effect of Tank Height to Diameter Ratio to Thermocline



Other factors concerning tank height to diameter: Site Foot Print (available space), Foundation considerations, Seismic, Tank economics, Insulation



Performance Test



During the Charging and Discharging, measure the following every 15 minutes:

- Flow Rate In
- Flow Rate Out
- Temperature of water going in
- Temperature of water going out

- Temperature at regular height intervals
- Pressure at inlet
- Pressure at outlet
- Ambient air temperature

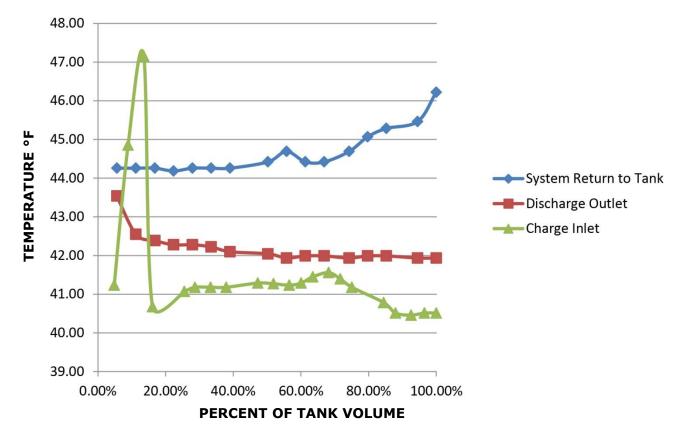


Abu Dhabi Results

Location	Abu Dhabi UAE						
Owner	ABU DHABI Industrial						
General Contractor	Drake and Skull						
Tank Contractor	Petron						
Diffuser Type	TKDA H Shape- Slotte	d Pipe					
			F	Results			
			Average	Min	Max		
Parameter	Units	Design	Actual	Actual	Actual		
Capacity	Ton Hours	15,00	0				
Peak Charge Rate	gpm	4,48	4380	4320	4426		
Peak Discharge Charge Rate	e gpm	4,48	3602	2792	5249		
Chilled Water Supply	Deg. F	4	41.52	40.46	47.16		
Warm Water Returned	Deg. F	5	6 44.65	44.19	46.22		
Temperature Differential	Deg. F	1	6 2.46	0.72	4.28		
Maximum Heat Gain	% in 24 Hours	1.0	% 1.44				
Ambient Outside Temp	Deg. F	13	115				
Maximum Head Loss	psi		3 1				
Tank Diameter	ft	72.1	8				
Tank Height	ft	49.2	2				
Height to Overflow	ft	48.7	2				
Capacity	Gallons	1,506,37	4				
FOM	Percent	90.00	%				



Abu Dhabi Graph



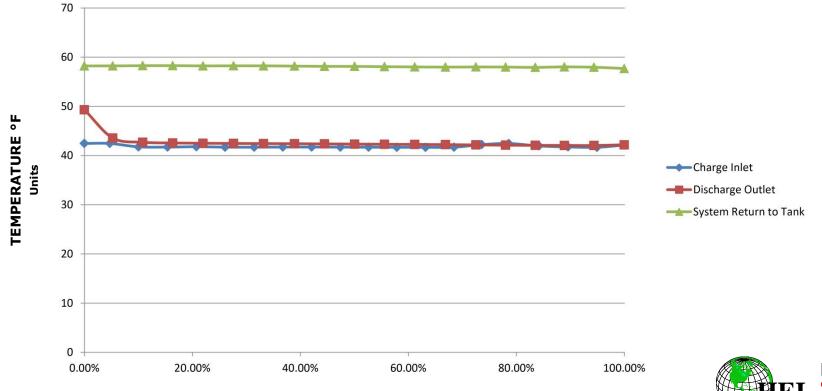


Stanford TES 2011 Results

Location	Stanford, CA					
Owner	Stanford University					
General Contractor	Whiting Turner					
Tank Contractor	Pacific Tank and Construction					
Diffuser Type	KDA Patented Polygonal (square)					
			Results			
				Average	Min	Max
Parameter	Units	Design		Actual	Actual	Actual
Capacity	Ton Hours	45,0	00			
Peak Charge Rate	gpm	14,1	98	14,016	13,185	15,458
Peak Discharge Charge Rate	e gpm	14,1	98	14,252	13,280	14,684
Chilled Water Supply	Deg. F		42	41.85	41.67	42.45
Warm Water Returned	Deg. F		58	58.09	57.69	58.27
Temperature Differential	Deg. F		16	15.71	14.66	15.97
Maximum Heat Gain	% in 24 Hours	2.0	%	0.00%		
Ambient Outside Temp	Deg. F	1	00	65		
Maximum Head Loss	psi		3	0.79		
Tank Diameter	ft	1	00			
Tank Height	ft	82	2.5			
Height to Overflow	ft		75			
Capacity	Gallons	4,399,7	39			
FOM	Percent	92.00)%			



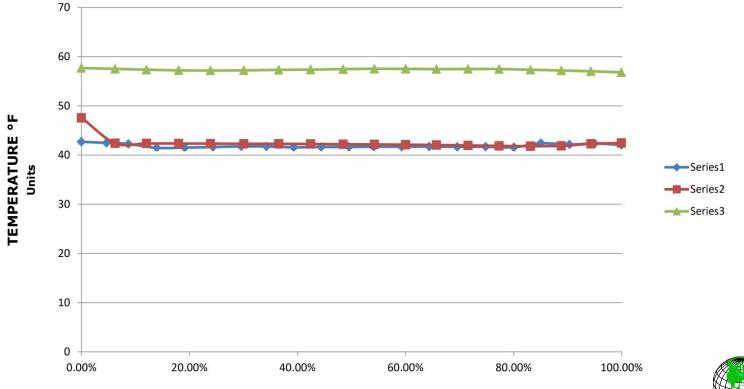
Stanford TES 2011 Graph



PERCENT OF TANK VOLUME

τκdδ

Stanford TES 2012 Graph



PERCENT OF TANK VOLUME



