

Design limitations that can justify the use of enhanced Ice-based Thermal Storage systems

Presented by: Thomas W. Brady

15 November 2016



CONSIDERATIONS THAT CAN LIMIT DESIGN

- 1. Spatial and Functional
 - a. Energy source availability and sufficiency
 - b. Availability of other resources (water, drainage, etc.)
 - c. Plant location driven
 - d. Design Working Pressure of Piping Systems
 - e. Distribution Piping System fluid velocity-density
- Cost Driven Factors
 - a. Land size
 - b. Building configuration (# of Floors, Roof size, column spacing, FL-FL height)
 - c. Technology selection
 - d. Number and capacity of individual chilling units (Unit cost, electric service)
- 3. Environmental / Regulatory
 - a. Refrigerant Selection
 - b. Efficiency standards
 - c. Sound limits



USING KAU CUP-2 AS A LOCAL EXAMPLE

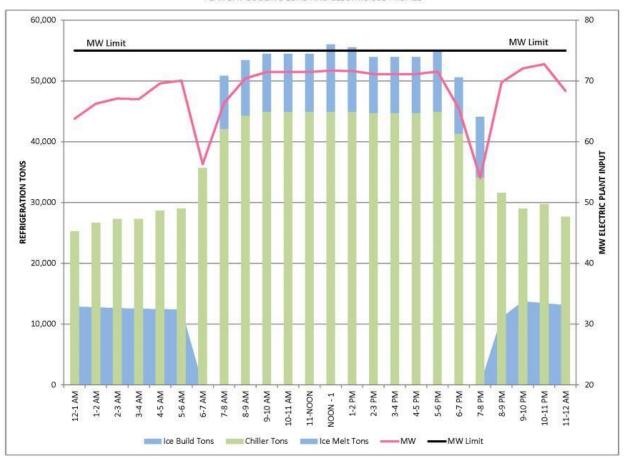


Energy source availability and sufficiency:

Electric power was available from the local utility but there were limits on the maximum commitment. A profile of the peak day cooling load and electric use is presented on the page 4 slide. This shows that using a cool storage system would allow approximately 15 MW to be eliminated for the CUP-2 electric service.



KAU CUP-2 PEAK DAY COOLING LOAD AND ELECTRIC USE PROFILE





USING KAU CUP-2 AS A LOCAL EXAMPLE

Availability of other resources (water, drainage, etc.):

A reliable source of water could not be established. This was not only true when design started in 2001 but it continues to be a fact. Since water was not available, air-cooled radiators had to be used to reject the heat from the chilling units. Due to the high ambient temperatures in Jeddah air cooled radiators require a minimum of 0.16 square meters of area at grade level for each ton of plant chilling capacity. This is slightly greater than the ground floor space required for all chiller units and related pumps and other plant equipment. A fraction of the air-cooled radiators required for CUP-2 are shown on slide 6.





Less than 50% of the required air-cooled radiators





USING KAU CUP-2 AS A LOCAL EXAMPLE

Design Working Pressure of Piping Systems:

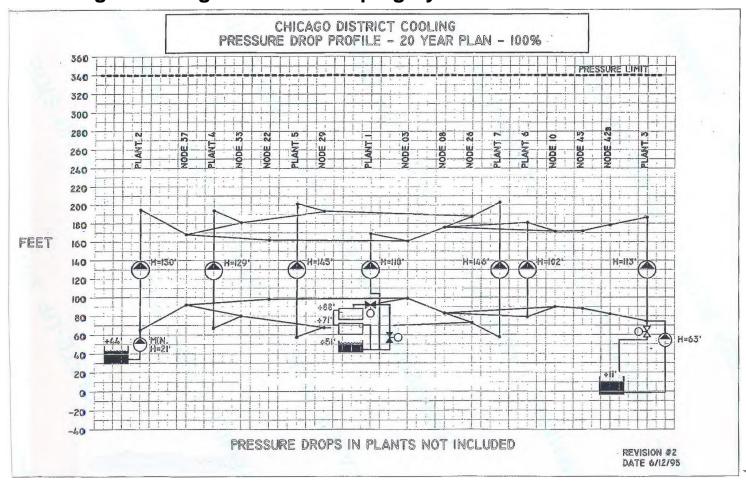
Sizing the piping for the distribution system must consider the cooling load and location of the customer buildings relative to the location of the cooling plants, as well as the general layout of the piping. One reason for this is to make certain that pressure of the water in any section of pipe, that is required to serve some number of buildings, does not exceed the design working pressure of that system, usually 150 PSI (1034 kPa).

The graphic on slide # 8 depicts the considerations that should be understood.

Delivering the cooling load at a larger temperature differential, by lowering the supply temperature, is a tool that a designer has to reduce system flow rate, which has a positive affect upon the pipe sizing and pressurization requirements.

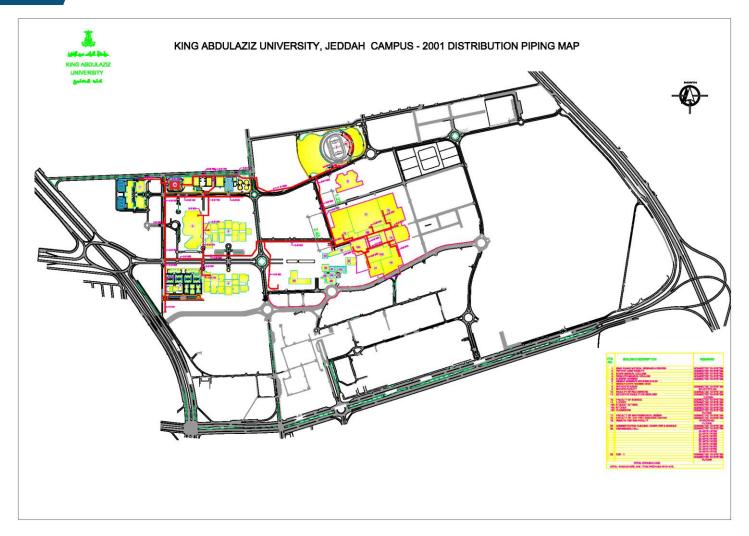


USING KAU CUP-2 AS A LOCAL EXAMPLE **Design Working Pressure of Piping Systems:**



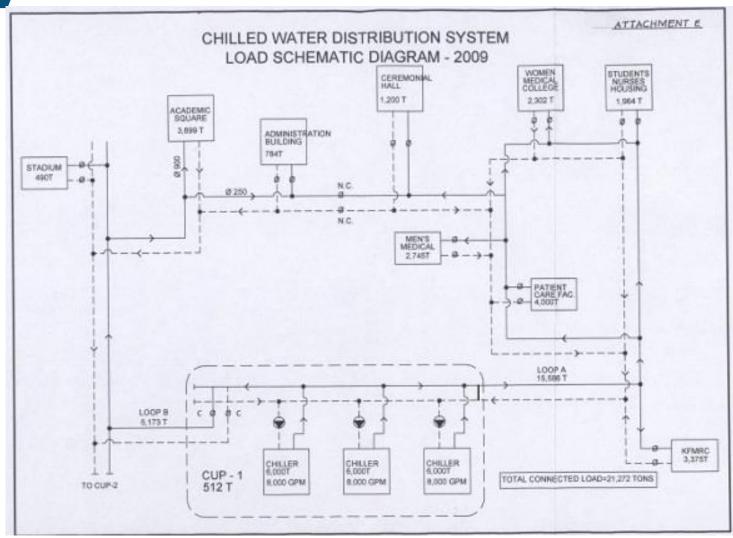


KAU 2001 CAMPUS MAP – 13,000RT

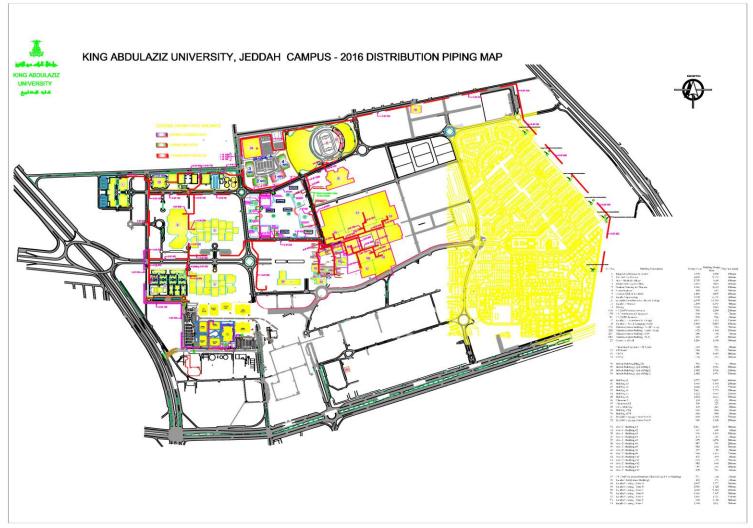




KAU 1996 to 2015 DISTRIBUTION SYSTEM



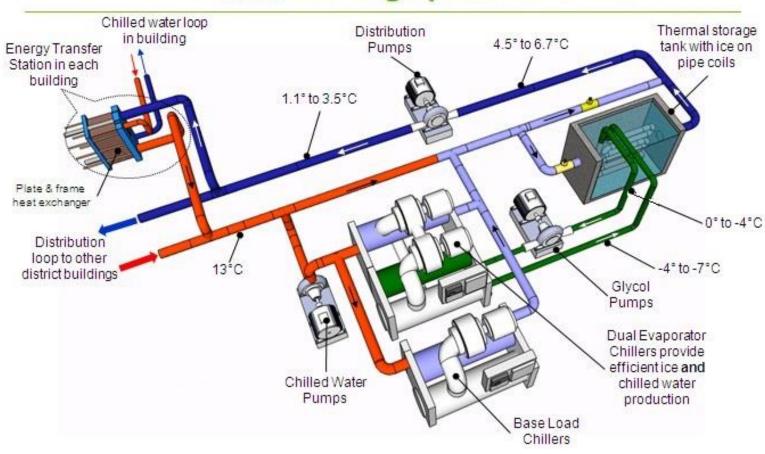
KAU 2016 CAMPUS MAP – 86,000 RT





KAU CUP-2

KAU Cooling System overview



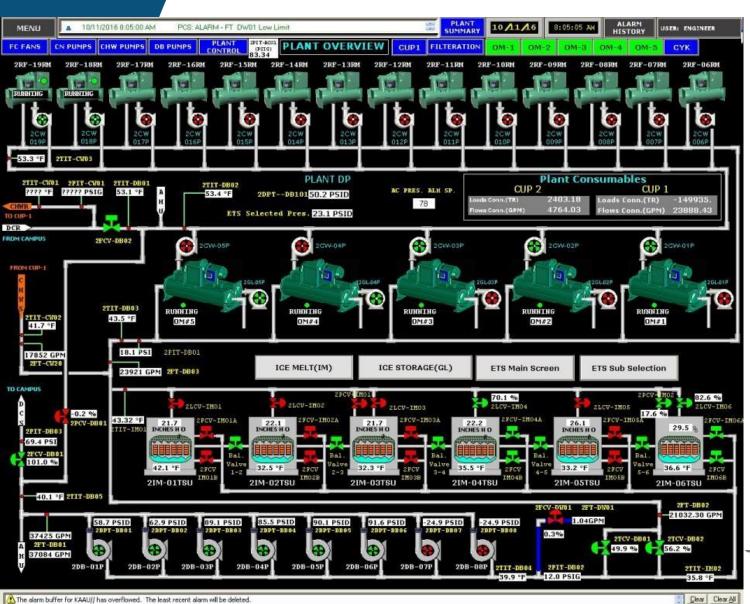


KAU CUP-2 Ice-Based Thermal storage

One of six compartments of galvanized pipe coils used to generate and store 126,720 ton-hours of thermal energy. Total construction volume = 7.4ton-hours per m^3 .



KAU CUP-2 Primary Control Screen





KAU CUP-2 Automation System

The plant automation system features adaptive control algorithms that optimize

- 1. The use of thermal storage each day, and
- Distribution pump sequences that allow reliable and effective control of 2 variable speed pumps in parallel with 6 constant speed pumps.
- 3. Uses the relatively high daily range in dry bulb temperature to generate icebased thermal storage during the nighttime hours.



KAU CUP-2 Automation System

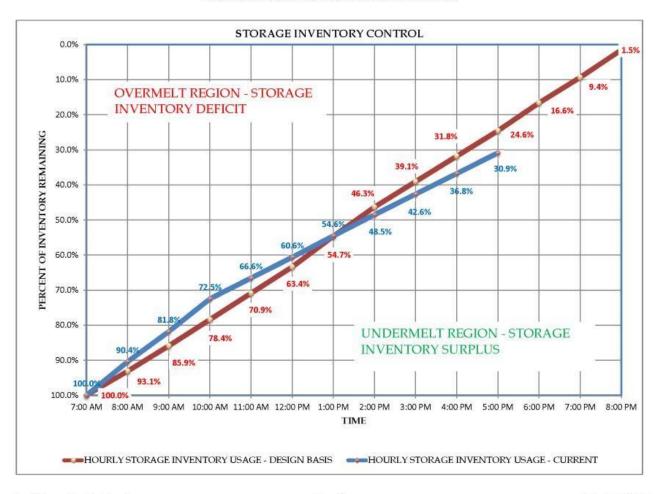
Inputs to Thermal Storage System Control Algorithms

	zimai otorage oystem oom	a or Algorithms
Cooling Load Inputs	Chiller System Input	Storage System Input
Current instantaneous cooling load	Number and capacity of available chiller units	Installed Thermal Storage Inventory (Tonhours)
The average cooling load over the past 2 hour time period	Current instantaneous water chilling output from CUP-1	Storage Inventory at 7am this day (Tonhours)
Time of day	Current instantaneous water chilling output from CUP-2	Current Storage Inventory in (Ton-hours)
Outside air temperature		Current Storage Inventory usage percentage [Current Storage Inventory / Storage Inventory at 7am].
"Design Basis" Cooling load profile		"Design Basis" storage inventory percentage for current time period
The "Design Basis" rate of change cooling load factors (7am through 8pm)		Anticipated storage inventory percentage in 1 hour.
Anticipated cooling load for the next hour [Rate of Change Load Factor x Average Cooling Load for Last 2 Hours]		Current Inventory percentage surplus or deficit
Hours that mode D is expected to be engaged (normally 7am to 8pm)		Current Inventory Ton-hour surplus or deficit



KAU CUP-2 Automation System

KING ABDULAZIZ UNIVERSITY - CUP II



- Use 34.0°F to 36.0°F chilled water supply temperature to increase return temperature from ETS and reduce distribution flow rates by over 30%. This can reduce pipe sizes for any planned piping or reduce pumping electrical input by about 40%. Provides flexibility when adding pipe runs to newly constructed buildings.
- 2. Use thermal energy storage, either ice-based or chilled water, along with adaptive use algorithms to reduce the electric power used during day time peak hours, and reduce the size of electric transformer that serve the plant.
- 3. Reduce construction costs by using a combination of constant speed and variable speed pumps to serve the distribution system.
- 4. Use the greater flexibility and more efficient chiller units that have become available since the KAU project to reduce the construction cost of ice-based thermal storage and improve the efficiency of both types of thermal storage.





Application: AHRI 400 Version 15.1

Customer : Mr. Tom Brady

Project : Dubai

Item : HX-1 Date : 9/13/2016

Model: AC	14L-FG		
		Hot Side	Cold Side
Fluid		Water	Water
Volume flow rate	GPM	2686.0	2681.2
Inlet temperature	°F	58.0	40.0
Outlet temperature	°F	42.0	56.0
Pressure drop	psi	9.88	9.92
Heat exchanged	kBtu/h	21600	
Mean temperature differe	nce °F	2.0	
Surface area	ft²	11741	
Density	lb/ft³	62.4	62.4
Specific heat	Btu/lb,°F	1.00	1.00
Thermal conductivity	Btu/ft,h,°F	0.339	0.338
Viscosity	cP	1.16	1.20

Plate material / Thickness		ALLOY 304 / 0.40 mm	
Sealing material		NBRP	NBRP
Connection material		Stainless steel	Stainless steel
Connection locations		S1 -> S2	S4 <- S3
Connection diameter	in	14	14
Pressure vessel code		AS	ME
Design Temperature	°F	150.0	150.0
Design pressure	psi	150.0	150.0
Liquid volume	ft ³	47.987	47.987
Overall length x width x height	in	158 x 4	5 x 126
Net weight, empty / operating	lb	18100	/ 24000

- Heat Exchangers and cooling coils can be selected with no change in performance within the building but allowing higher return temperature to the DC plant.
- Since the sizing criteria for the heat exchanger (LMTD) is higher the price is lower.





Application: AHRI 400 Version 15.1

Customer : Mr. Tom Brady

Project : Dubai

Item : HX-2 Date : 9/13/2016

item	Qty	Description	Price
HX-1	1	AQ14L-FG, with (507) ALLOY 304 plates with NBRP CLIP-ON gaskets.	\$128,000.00
HX-2	1	AQ14L-FG, with (475) ALLOY 304 plates with NBRP CLIP-ON gaskets.	\$122,600.00

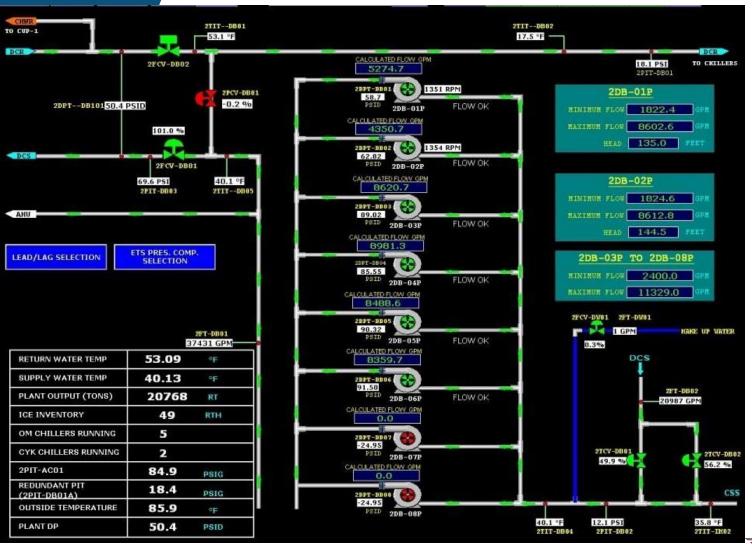
Oty Description

Model: AQ14	L-FG		
		Hot Side	Cold Side
Fluid		Water	Water
Volume flow rate	GPM	2158.0 60.0	1864.1 36.0
Inlet temperature	°F		
Outlet temperature	°F	40.1	59.0
Pressure drop	psi	7.49	5.72
Heat exchanged	kBtu/h	21	000
Mean temperature difference	°F	2.2 10997	
Surface area	ft²		
Density	lb/ft³	62.4	62.4
Specific heat	Btu/lb,°F	1.00	1.00
Thermal conductivity	Btu/ft,h,°F	0.341	0.340
Viscosity	cР	1.13	1.14
Plate material / Thickness		ALLOY 304 / 0.40 mm	
Sealing material		NBRP	NBRP
Connection material		Stainless steel	Stainless stee
Connection locations		S1-> S2	S4 <- S3
Connection diameter	in	14	14
Pressure vessel code		ASME	
Design Temperature	°F	150.0	150.0
Design pressure	psi	150.0	150.0
Liquid volume	ft ³	44.986	44.986
Overall length x width x height	5.7	158 x 45 x 126	
Net weight, empty / operating	lb	17600 / 23100	

LMTD for higher temperature return heat exchanger is 2.2. The heat transfer surface and the price for the heat exchanger are both lower. Note that the average water temperature at a cooling coil in the building is the same 50.0°F.

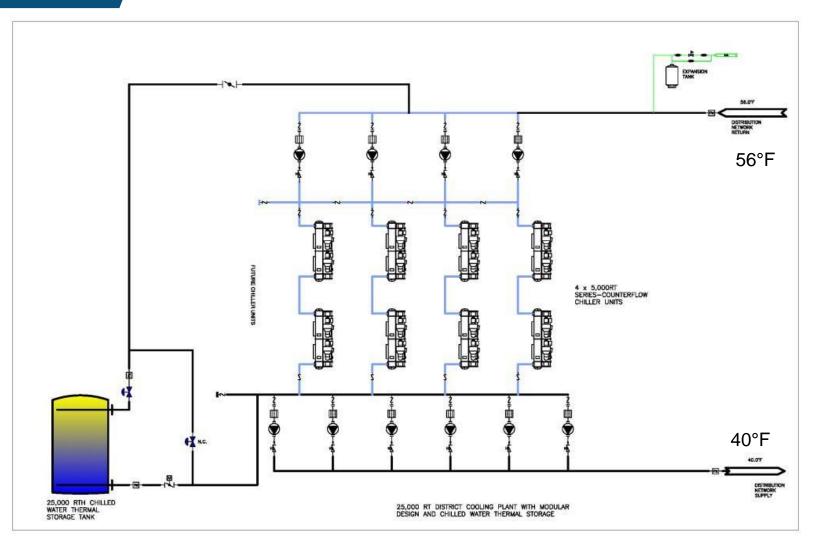


Drice



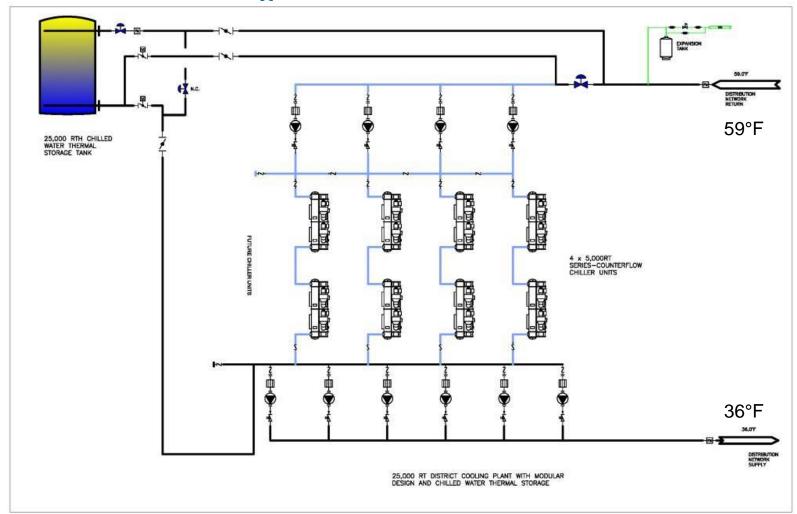
Combining variable speed and constant speed pumps has been done successfully for decades. Care must be taken to include the proper operating and limit safeguards. With the cost of MV VFDs the extra time spent in design is well worth the effort.

UAE DC Design with CHW Thermal Storage





Reduced Temperature Design with CHW Thermal Storage





Conclusion

THANK YOU

