



IDEA 2015

Inspiring the Next
Generation

106th Annual Conference & Trade Show | Boston, MA | June 28 – July 1

Food Industry Waste to Energy Case Study





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Food Industry Waste to Energy Case Study

- ✓ Objectives
- ✓ Acknowledgements
- ✓ Existing Site Conditions
- ✓ Anaerobic Pretreatment
- ✓ Energy Recovery
- ✓ Project Execution
- ✓ Conclusions
- ✓ Questions



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CHP POWER GENERATION **FUELED** BY THE VERTICAL START-UP OF A 6.5MG ANAEROBIC REACTOR FOR INDUSTRIAL WASTEWATER PRETREATMENT IN THE FOOD SERVICE INDUSTRY

- ✓ Compliance with industrial pretreatment discharge limitations
- ✓ Elimination of off-site waste disposal
- ✓ Reduced energy & operating expenses for industrial pretreatment, energy generation, and heat recovery
- ✓ Use of design-build delivery method
- ✓ Securing of federal energy investment tax credit



Acknowledgements

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PROJECT TEAM



- * Daren Kaiser
- * Kyle Schilling
- * Brian Scott
- * Ray Holland



- * George Fertal
- * Shawn Veltman, PhD, PE, BCEE
- * J.S. Brown, PE

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Existing Site Conditions



General Mills, Murfreesboro, TN

- * Two operations on the same site
 - Pillsbury
 - Yoplait
- * Historical Perspective
 - 605,000 gallons per day of process wastewater with a COD of approximately 3,400 mg/L pre-treated on-site with an activated sludge treatment system (aerobic) with large energy requirements for aeration
 - Off-site disposal of concentrated Ag waste and yogurt whey at considerable expense
 - Discharge to City of Murfreesboro or to golf course irrigation under an industrial discharge permit
 - Large energy consumer (>10 MW electric, >18 MMBTU/hr gas)



Existing Waste Sources & Composition

- * Pillsbury Wastewater
 - 80,000 gpd; COD = 3,400 mg/L
- * Yoplait Wastewater
 - 525,000 gpd; COD = 3,400 mg/L
- * Ag waste
 - 24,000 gpd; COD = 57,500 mg/L
- * Greek Yogurt Whey
 - 80,000 gpd; COD = 70,000 mg/L
- * No sanitary waste admixture with process wastewater
- * Pretreatment Limits
 - 250 mg/L COD; 250 mg/L TSS; 20 mg/L Ammonia



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Anaerobic Pretreatment



Anaerobic Pretreatment

- * 1 MG equalization/re-acidification tank
- * 6.5 MG complete mix digester with an anaerobic DAF to separate the SRT and HRT (6-day HRT; 30-day SRT)
- * No supplemental heating
- * **Waste gas flare for expected biogas generation of up to 700 scfm**
- * Designed to treat the full wastewater flow
- * Related chemical feed systems for pH control, foam suppression, sludge conditioning and odor control
- * Aerobic reactor reconfigured for polishing



Pretreatment Results

- * Lowered overall sludge production
- * Average Effluent Quality
 - COD: 211 mg/L (250 mg/L)
 - TSS: 153 mg/L (250 mg/L)
 - Ammonia: 122 mg/L (20 mg/L)
- * **Gas Quantity & Quality**
 - **Average Flowrate: 450 scfm**
 - **Moisture Content: Saturated**
 - **CH₄ Content: 60-65%**
 - **H₂S: 400 ppmv (controlled by iron addition)**
 - **Total Siloxanes: <70 ppbv (very low)**

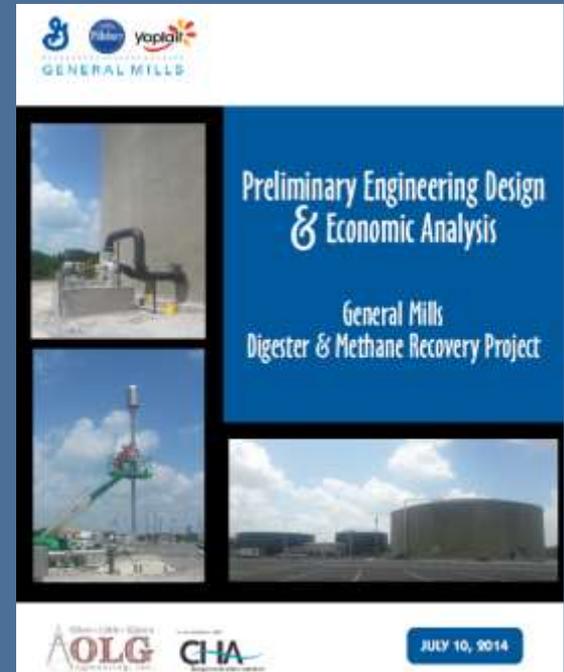
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Energy Recovery



Energy Recovery Evaluation

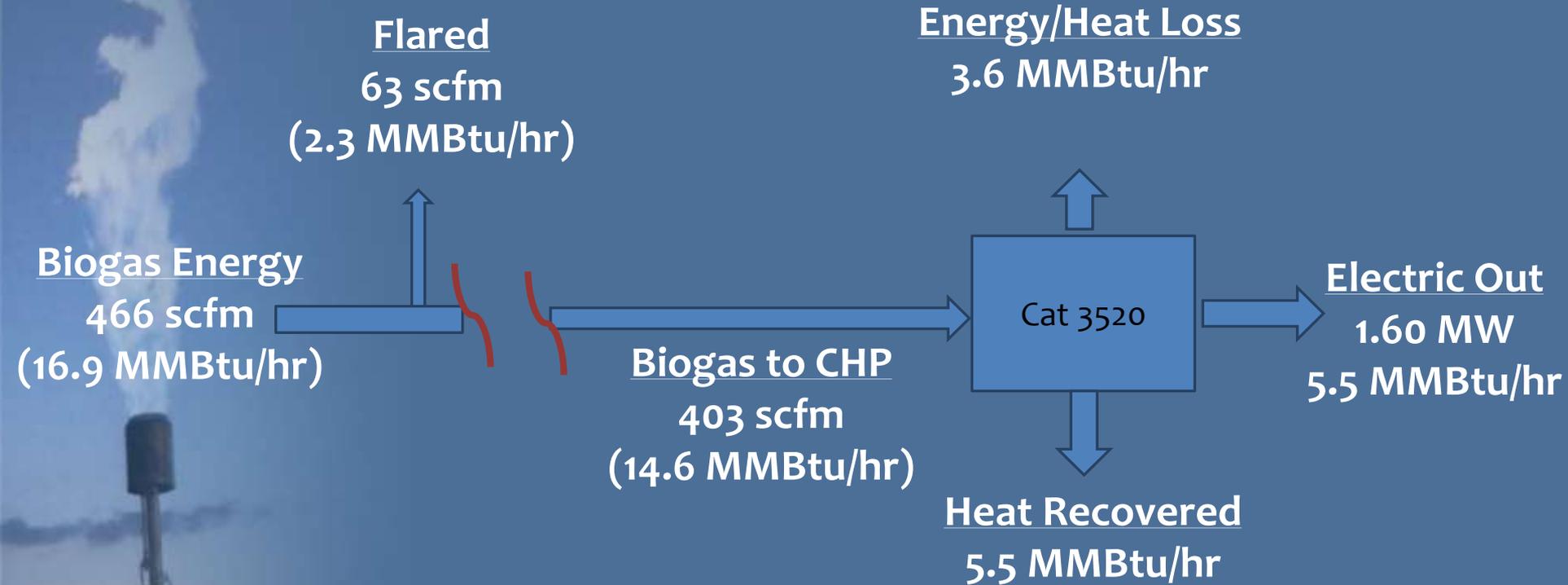
- * Based upon proof of gas asset
- * Alternatives considered
 - Direct Boiler Firing
 - Ice making
 - Electric generation using internal combustion engines with and without heat recovery
 - Grid sale of electric and net metering
- * Alternatives evaluated using economic model to determine IRR
- * A sensitivity analysis was performed to evaluate the impact of sensitive factors (electric rates, gas costs, ITC, heat recovery, on-line availability) on IRR



Energy Recovery Plan

- * Gas compression & drying at the digester site
- * Gas transmission line: \pm 3,200 ft.
- * A single containerized engine-generator with provisions for an additional unit; Options Included:
 - 1.6 MW electrical production with potential grid sale to TVA under renewables standard offer that includes sale of RECs
 - OR
 - 1.6 MW electrical production to off-set current site usage (Net Metering) and maintain the sale of RECs for GMI use at a later date
 - AND
 - Engine jacket, oil cooler, and exhaust gas heat recovery (5.5 MMBTU/hr) via an FDA approved plate & frame heat exchanger (transfer from engine cooling circuit to Yoplait HTHW (high temperature hot water system)
- * Excess biogas to flare or direct firing in a boiler for heat

Energy Balance



Future Biogas to second engine-generator or direct boiler firing

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Project Execution



Pillsbury

Yoplait

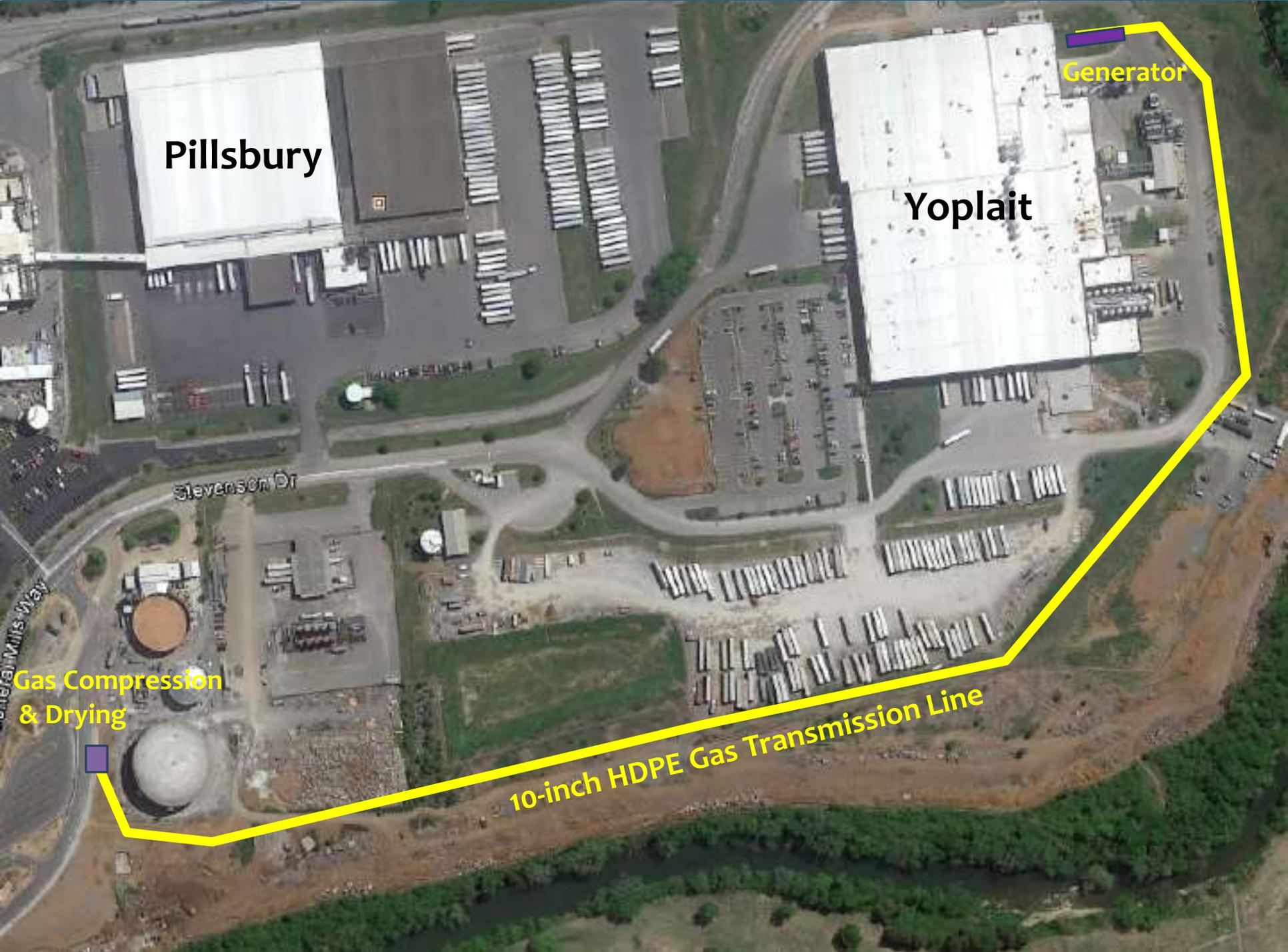
Generator

**Gas Compression
& Drying**

10-inch HDPE Gas Transmission Line

Stevenson Dr

Wendell Mills Way



Gas Compression & Cleanup



General Equipment Arrangement:

- 2 – 50 HP 700 SCFM Centrifugal Blowers
- 1 – Biogas Demister / Particle Filter
- 1 – 700 SCFM Dual Core Heat Exchanger
- 1 – 2 HP 700 SCFM After Cooler
- 1 – 20T Air Cooled Glycol Chiller
- 1 – Gas Analyzer

Engine Generator



General Equipment Arrangement:

- 1.6 MW CAT 3520 Containerized Engine-Generator
- 5.5 MMBTU/Hr (519GPM) Heat Recovery Loop

HTHW Heat Recovery



Equipment Arrangement:

- 5.5 MMBTU/Hr Heat Recovery Loop
 - 1 – FDA compliant Plate & Frame HEX
 - 2 – 20 HP Circulating Pumps

Current Status

- * Corporate approval of \$7.7 million digester and \$5.4 million energy recovery facilities secured late 2014.
 - 30% ITC of approximately \$4 million - a major factor in the economic evaluation
- * Permitting (with TVA through Murfreesboro Electric Cooperative & Tennessee DEC) completed
- * Design-Build Delivery Approach Selected
 - 100% design completed January 2015
 - Construction 95% complete with first power exported on 5/27/2015 (Placed in Service; **27 weeks from NTP**)
 - System Training completed
 - Completing punch list items
 - Full power production July 2015

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Conclusions



Conclusions

- ✓ Greater than 10% of power produced by Waste to Energy CHP plant
- ✓ Reduction of more than 10% of natural gas usage through heat recovery
- ✓ Reduction in 95,000 liters of diesel fuel annually
- ✓ 35 million gallons of water returned to watershed
- ✓ 2000 acres of farmland returned to normal ag use
- ✓ Reduction of 10,000 tons of CO₂ emissions
- ✓ In compliance with all regulatory standards
- ✓ Federal ITC approved
- ✓ 23.4% IRR; 4 year payback

Questions

Contacts

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