



# **DRY SORBENT INJECTION WITH HYDRATED LIME FOR ACID GAS CONTROL TO ACHIEVE REGULATORY COMPLIANCE WHILE BURNING VARIOUS COALS**

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# AGENDA

**Introduction**

**Proven, Versatile, Mature & Attractive Technology**

**Balance Of Plant Impacts & Improvement**

**Cost Effectiveness of Advanced Hydrate Limes**

**Applications and Case Studies**

**Discussion/Questions**

# Introduction

# Introduction

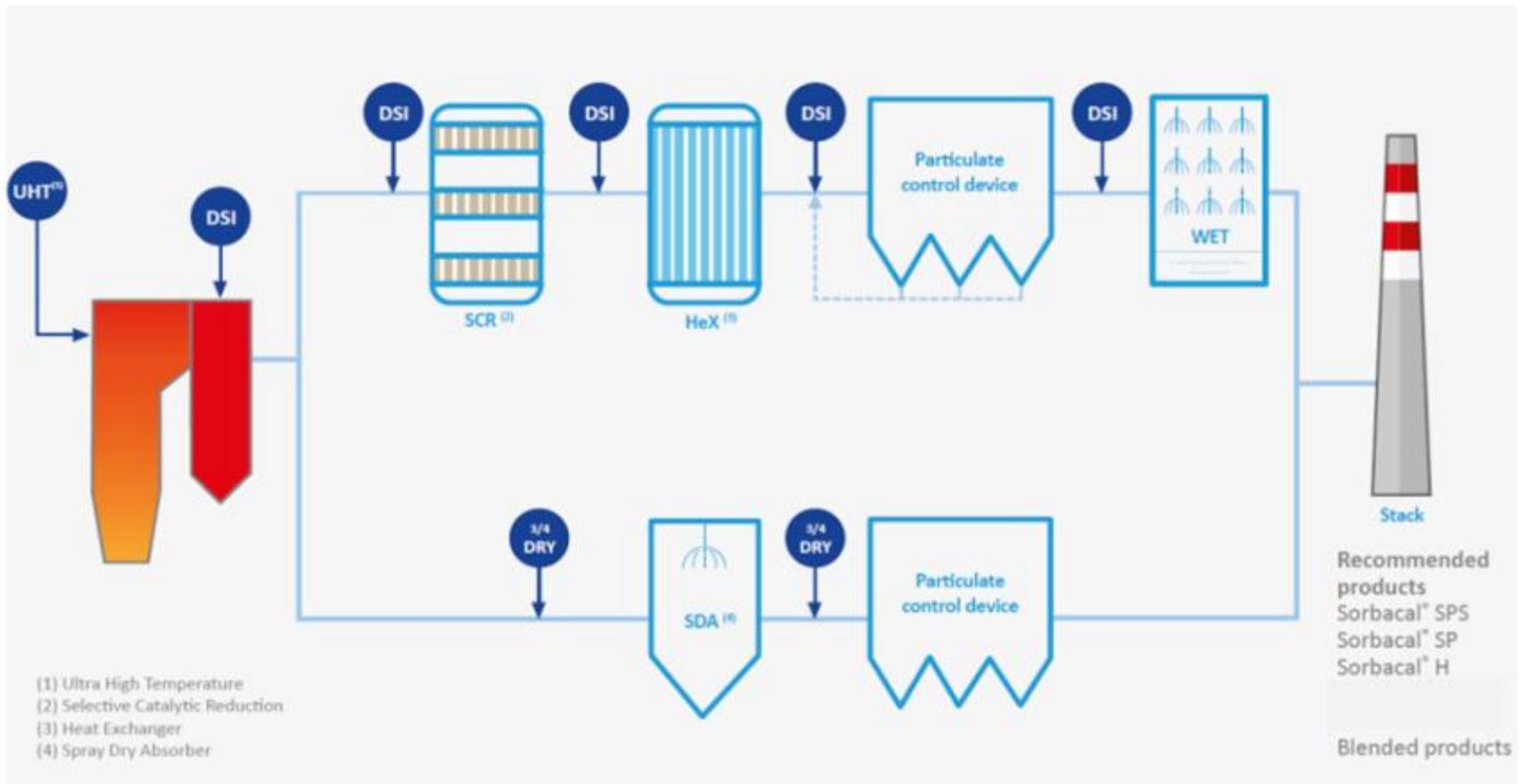
- > **Dry Sorbent Injection (DSI) is a technology of choice...**
  - > Low CapEx solution
  - > Easy retrofit – small installed foot print
  - > Flexible and customizable
- > **...that continues to evolve as an economical solution...**
  - > Improved equipment design based on years of operating experience
  - > Enhanced sorbents provide solutions for new applications and better cost to old ones
  - > Improved mixing technologies optimize operating costs/performance
- > **...providing solution for new and existing customers.**
  - > Regulatory compliance
  - > High removal performance capability of enhanced hydrated limes
  - > Likely the most economical solution for short life-cycle cost analysis
  - > Low by-product/CCR concerns/costs

**Proven, Versatile, Mature & Attractive**

## Proven Technology

- > **Hundreds of DSI systems installed in the United States**
  - > Widely installed in the coal-fired Utility Sector
  - > Growing penetration in the Industrial Sector
  - > Considerable interest from the Industrial Boiler Sector
    - > IB MACT applications
    - > Comfortably achieving compliance levels
- > **Versatility**
  - > Broad application: CFB, PC-fired, Stoker
  - > 20MW to 800MW applications
  - > Control Hydrogen Chloride (HCl) ...plus, SO<sub>3</sub> HF and SO<sub>2</sub>

# Versatile Technology



# Mature Technology

## > Pioneered in the late 1980's and early 1990s

- > DOE National Energy Technology Laboratory (NETL) began studying "DSI with calcium sorbents"
- > Response to the compliance challenge from CAAA of 1990
- > Duct injection of hydrated lime for SO<sub>2</sub> control
- > First systems were crude, material-handling approaches to a chemical application problem

## > Second-Gen Systems

- > Early 2000's – Hydrated lime for SO<sub>3</sub> control
  - > e.g., TVA Widows Creek
  - > Corrosion control, plume mitigation, acid deposition, enhanced PM control Dilute-phase conveyance with a more sophisticated destitution

## > Current State of the Art

### Air Island

Optimized dilute-phase conveyance  
Dehumidifiers - Aftercoolers

### Material Storage Island

Advanced multi-stage LIW  
Precise feeds  
Feed forward-feed back logic  
Flow enhancing technologies

### Delivery and Distribution

Engineered manifolds  
Modelled lance placement  
Installed diagnostics  
In-duct Static Mixers (low dP)

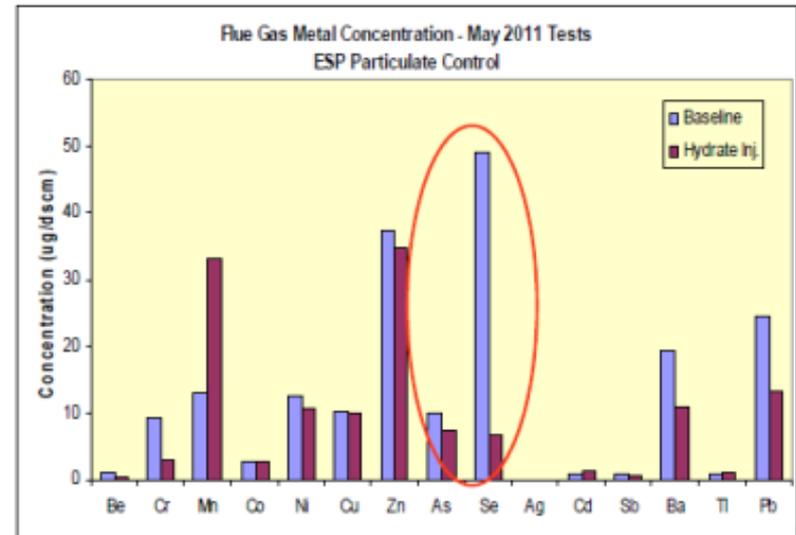
## Attractive Technology

> **Low Capital Cost**

> **Small Footprint**

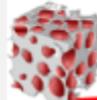
> **Broad Co-Benefits**

- > Heat rate reduction through lower Air Heater (AH) deposition
- > Lower AH outlet temps facilitate better electrostatic precipitator (ESP) operations
- > Vapor-phase trace metal collection
- > Greater fuel flexibility
- > Enhance Mercury (Hg) capture effectiveness



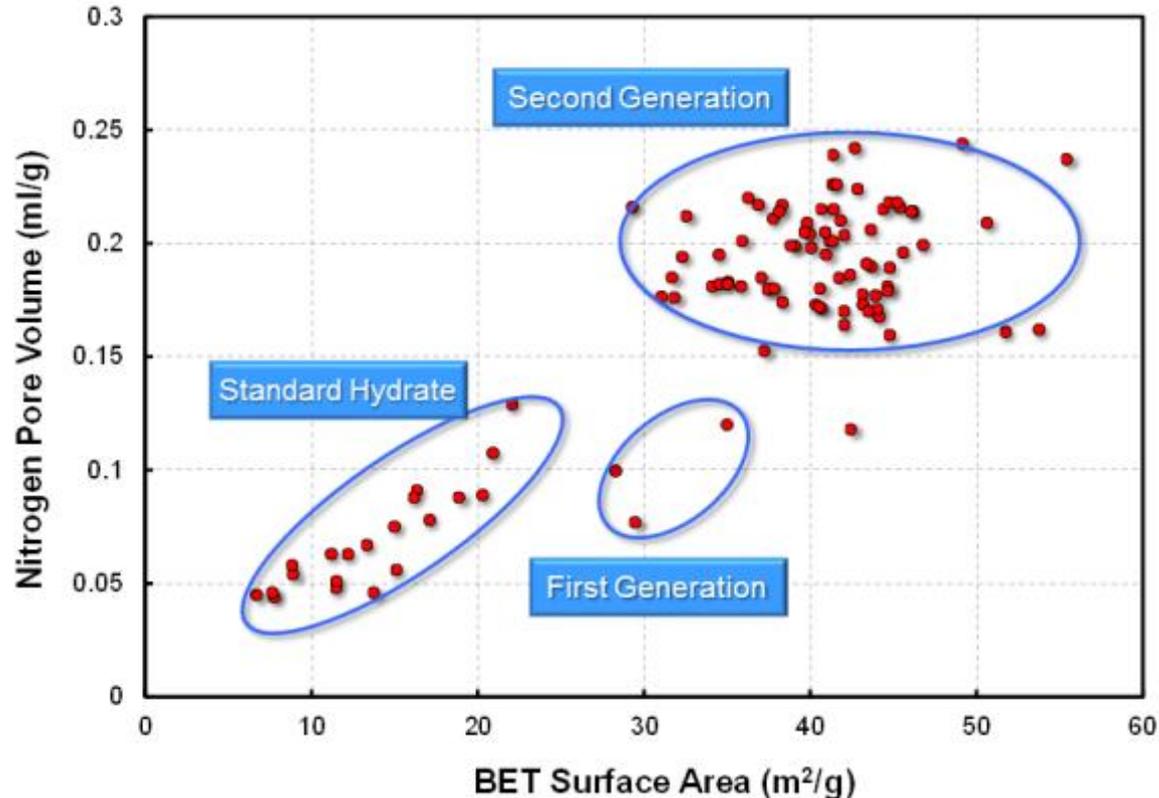
## Enhanced Hydrated Lime

- > Hydrate lime suppliers have pursued numerous products enhancement to improve performance
  - > Improved reactivity
  - > Increased chemical utilization
  - > Physical modification
  - > Surface additives

Sorbent	Standard Hydrated Lime	Sorbacal® H	Sorbacal® SP	Sorbacal® SPS	Units
Figure					-
Typical Available Ca(OH) <sub>2</sub>	92 – 95	93	93	93	%
Typical Surface Area	14 – 18	> 20	~40	~40	m <sup>2</sup> /g
Typical Pore Volume	~0.07	0.08	~0.20	~0.20	cm <sup>3</sup> /g

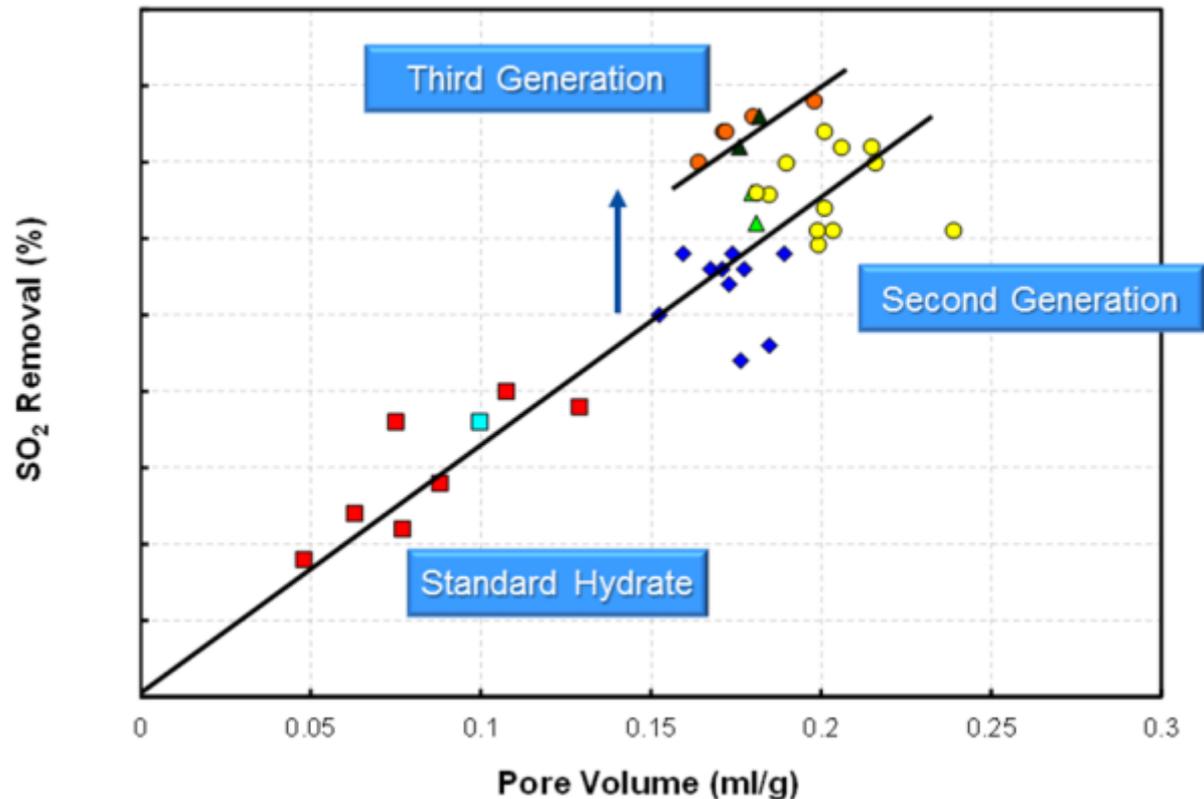
# Reactivity Property Relationships

## > Surface Area and Pore Volume Product Development



# Evolution of High Performance Products

## > Surface Area and Pore Volume Product Development



## Balance of Plant Impact/Improvements

## Balance of Plant

- > **Reduced O&M on downstream equipment**
  - > Reduced corrosion
  - > Reduced fouling

**Protect Equipment and Ductwork** - corrosion protection

**Maintain AH cleanliness** - lower dP thru condensable removal

**Improved Operating Costs** – heat rate improvement

Lower heat rate means less coal burned and lower CO<sub>2</sub> emissions  
1 lb coal ~ 2.5 lb of CO<sub>2</sub> emitted

# Improved Cost Effectiveness with Enhanced Hydrated Limes

## Cost Effectiveness

- > **Greater sorbent efficacy means less sorbent consumed for equal performance**
  - > Better \$USD/lb of acid gas removed
  - > Higher chemical utilizations
  - > Lower stoichiometric ratios
  - > Lower mass injection ratios
  
- > **Lower mass loading means**
  - > Less wear and tear on particulate control devices
  - > Lower ash/CCR volumes to dispose of or manage
  - > Lower truck/delivery traffic
  - > Lower incidences of system maintenance

## Cost Effectiveness

- > **Greater sorbent efficacy means less sorbent consumed for equal performance**
  - > Better \$USD/lb of acid gas removed
  - > Higher chemical utilizations
  - > Lower NSRs
  - > Lower mass injection ratios

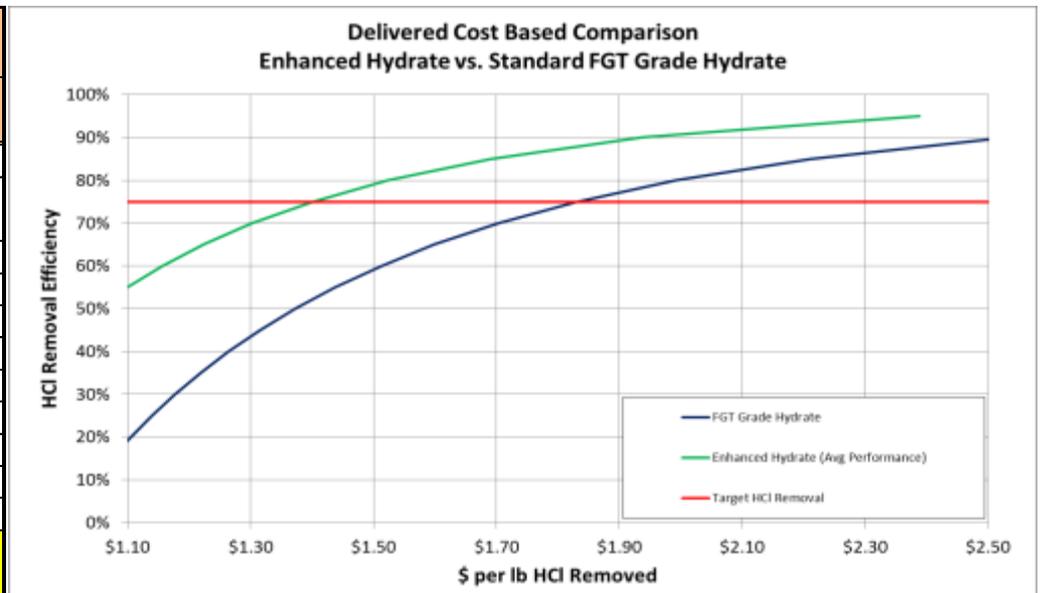
**Hydrated Lime is a Value Choice not a Price Decision**

- > **Lower mass loading means**
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# Cost Effectiveness

> A recent University procurement example...

Sorbent	Enhanced Hydrate	Standard Hydrate	
	Avg Performance	Base	
Delivered Price	\$246.05	\$193.00	per Ton
Improvement in Performance	40%	0%	
Usage	450	750	Tons
Operating Hours	5,760	5,760	Hours
Average Usage	0.078	0.130	Tons/Hour
Average Inlet HCl	40	40	ppmv
Target HCl	10	10	ppmv
Target HCl Removal	75%	75%	
HCl Removed	13.7	13.7	lb/hr
Delivered Sorbent Cost	\$19.22	\$25.13	per Hour
<b>Delivered Sorbent Cost per lb HCl Removed</b>	<b>\$1.40</b>	<b>\$1.83</b>	<b>per lb HCl Removed</b>

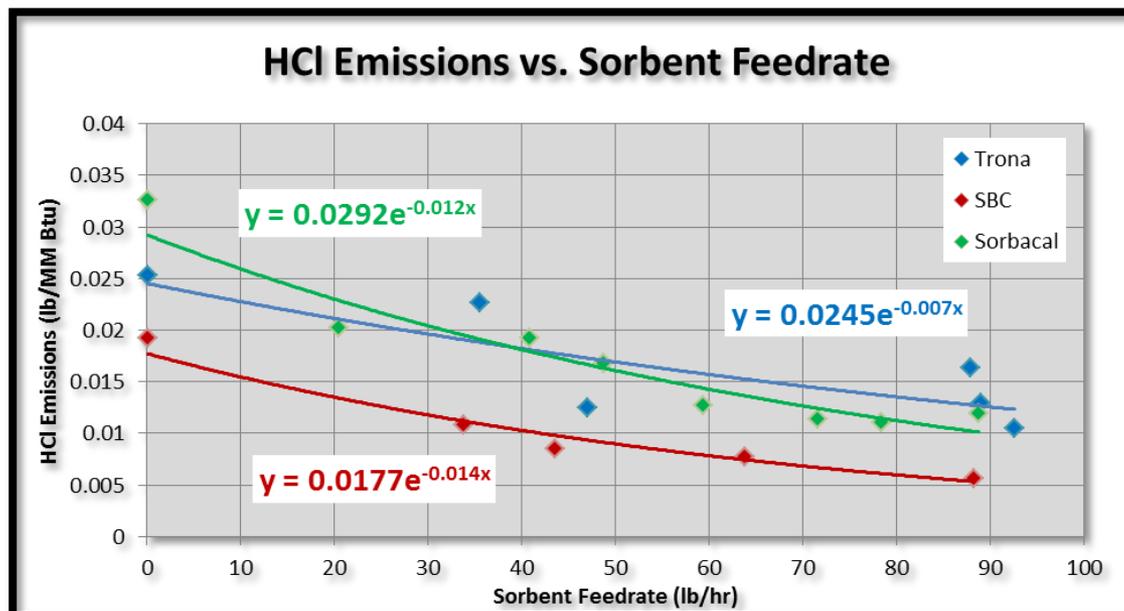


**Hydrated Lime is a Value Choice not a Price Decision**

## Case Studies

## Case Study #1

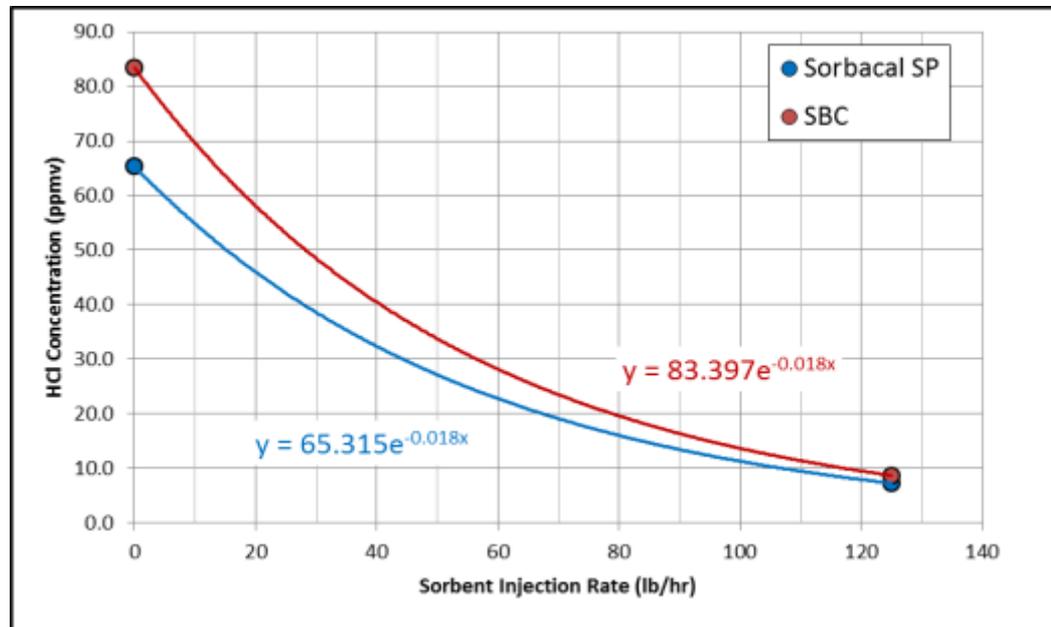
- > **Biomass-fired boiler – HCl control study**
  - > Three sorbents were tested: enhanced hydrate, trona and SBC
  - > Injection at the BHF inlet: 350-375F
  - > Enhanced hydrate was within 15% of the relative performance of SBC & twice as effective as trona



## Case Study #2

### > CFB boiler – HCl control study

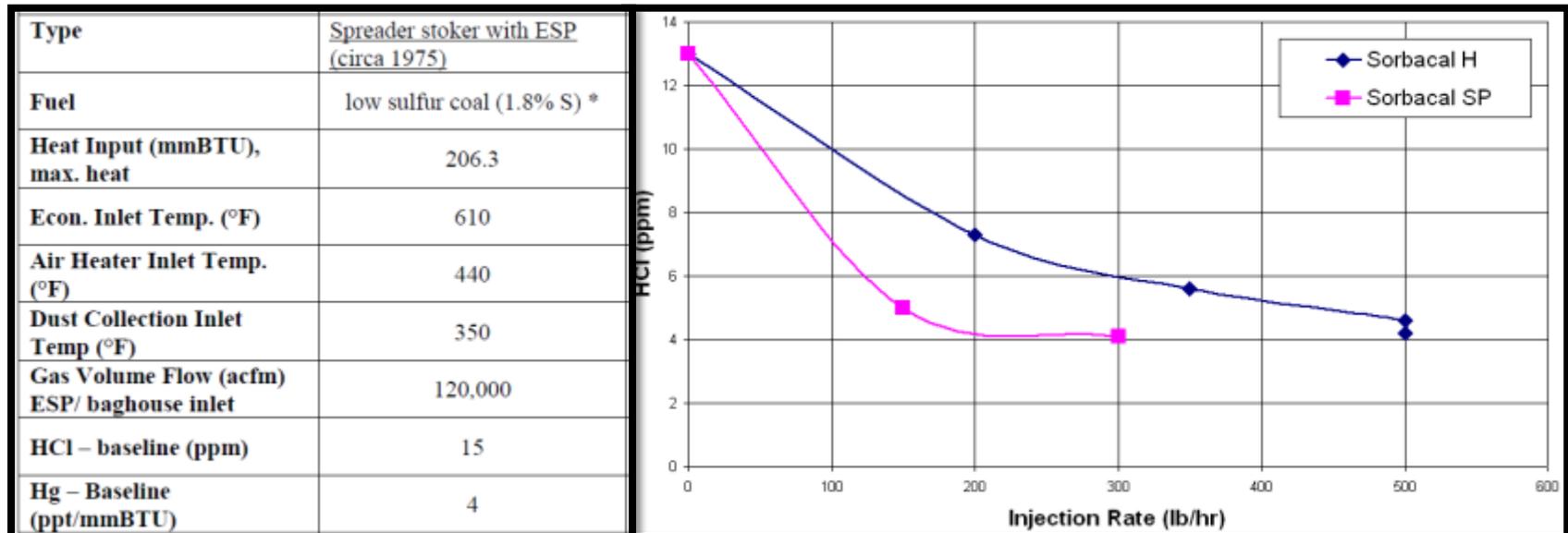
- > Enhanced hydrate and SBC were tested
- > Injection at the BHF inlet: 350-375F
- > Enhanced hydrate performed similarly to SBC



## Case Study #3

### > Stoker boiler – HCl control study

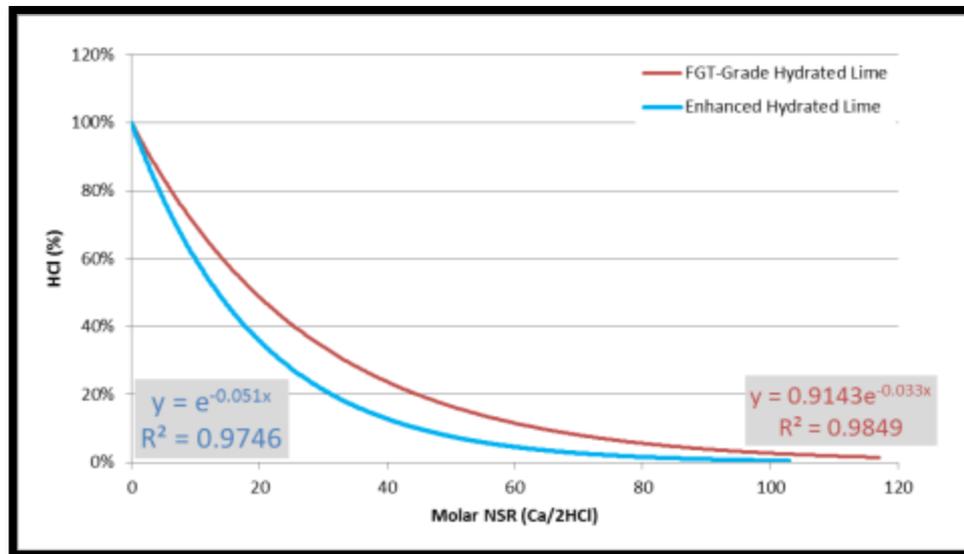
- > Two enhanced hydrates were tested
- > Injection immediately upstream of the AH: 440F
- > Enhanced hydrate performed similarly to SBC



## Case Study #4

### > Stoker boiler – HCl control study

- > Enhanced hydrate and FGT-Grade Hydrate were evaluated
- > Injection at the AH outlet/RAFF inlet
- > Enhanced hydrate performed roughly 30% better than std hydrate



Gas temp = 540°F  
 H<sub>2</sub>O in wet gas, % by wt. = 11.75%  
 SO<sub>2</sub>-to-HCl ratio (lb/lb) = 92.6

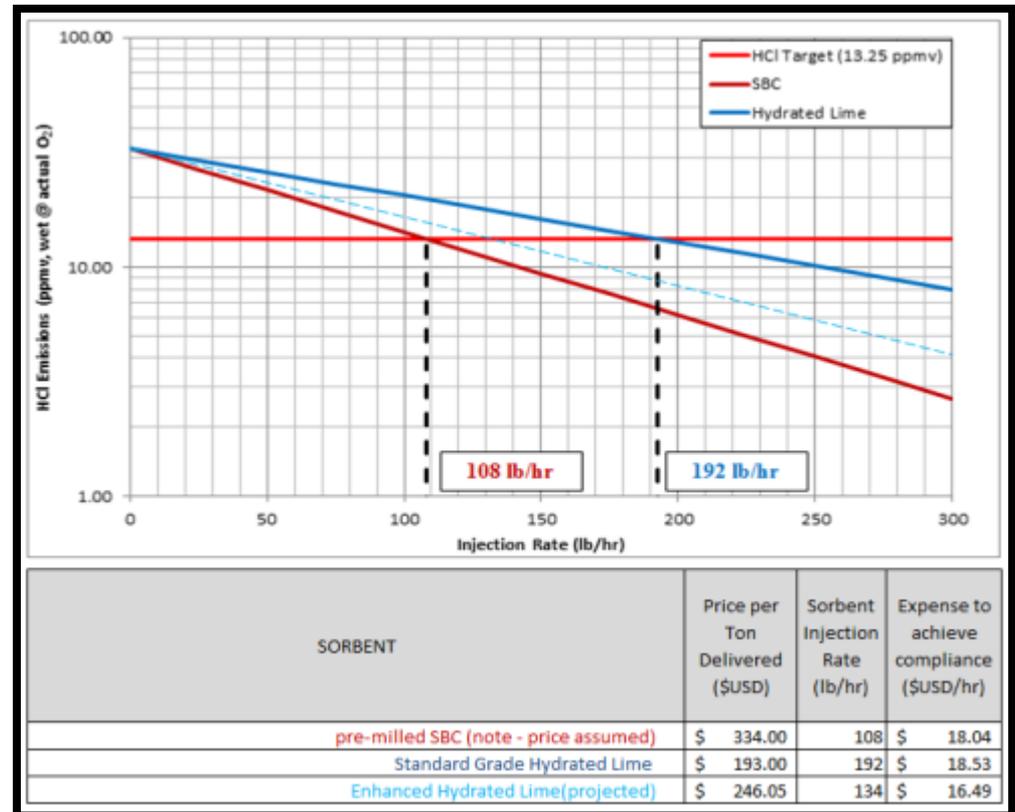
# Case Study #5

## > PC Wall-fired boiler – HCl control study

> Standard hydrate and pre-milled SBC were tested

> Injection upstream of the fabric filter post air pre-heater @ 360 F

> Substantial cost differential between the sorbents.



## Summary

- > **Dry Sorbent Injection (DSI) is a broadly implemented acid gas control technology**
- > **The higher efficacy of enhanced hydrated limes means:**
  - > Reduced O&M due to reduced corrosion and fouling
  - > Lower ash/CCR generation rates
  - > Improved operating cost
  - > Greater assurance of obtaining compliance goals
- > **Enhanced hydrated lime is a for cost-effective choice for acid gas control**

**Hydrated Lime is a Value Choice not a Price Decision**



## Discussion/Questions?

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