



Considering District Energy Based on Residual Municipal Solid Waste Energy Plant

Case Study: Minneapolis
North Loop Development

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Overview

Hennepin Energy
Recovery Center
MSW Power Plant

Integrated District
Energy Master Planning

Downtown Minneapolis
North Loop





Existing WtE Plant - Downtown Minneapolis

Hennepin Energy Recovery Center (HERC)

- ▶ 365,000 tons/year of MSW.
- ▶ Steam Turbine 38.7 MW at 350,000 lbm/hr.
- ▶ Benefit: The facility helps meet the state's renewable energy goal of 25 percent of energy from renewable sources by 2025.
- ▶ Reduce the release of GHG emissions by about 255,000 metric ton/year.
- ▶ Use some low grade heat for snow melting the public plaza area.
- ▶ Interconnects with NRG district steam system.







Existing Infrastructure

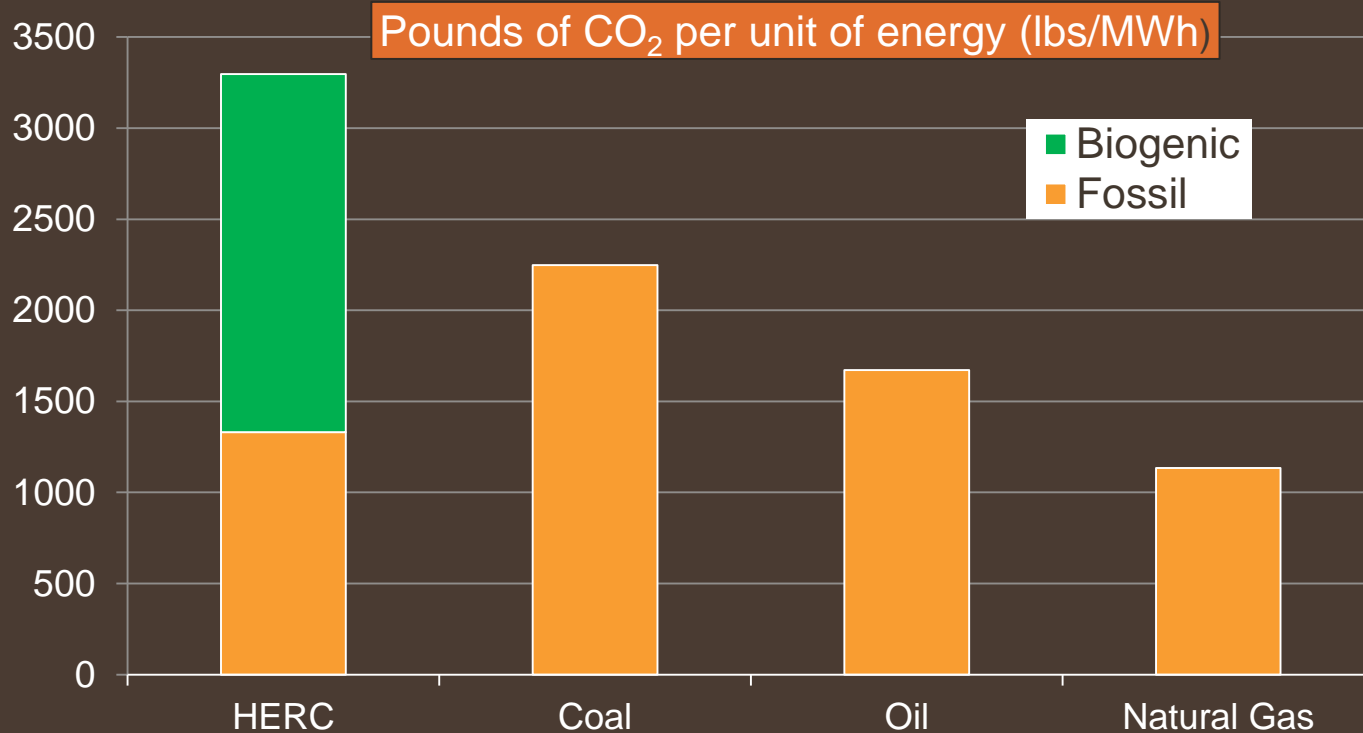


Existing Infrastructure





CO₂e Emissions of MSW vs Fossil Fuel





North Loop - Downtown Minneapolis

NORTH LOOP

Minneapolis' Fastest Growing Community:

- Target Field, Home of Minnesota Twins, and Timberwolves
- Planned Development for Commercial Office Buildings
- New and existing low rise apartments/condominiums



North Loop - Minneapolis



North Loop - Minneapolis





Aerial View Of The North Loop Area



District Energy Master Planning

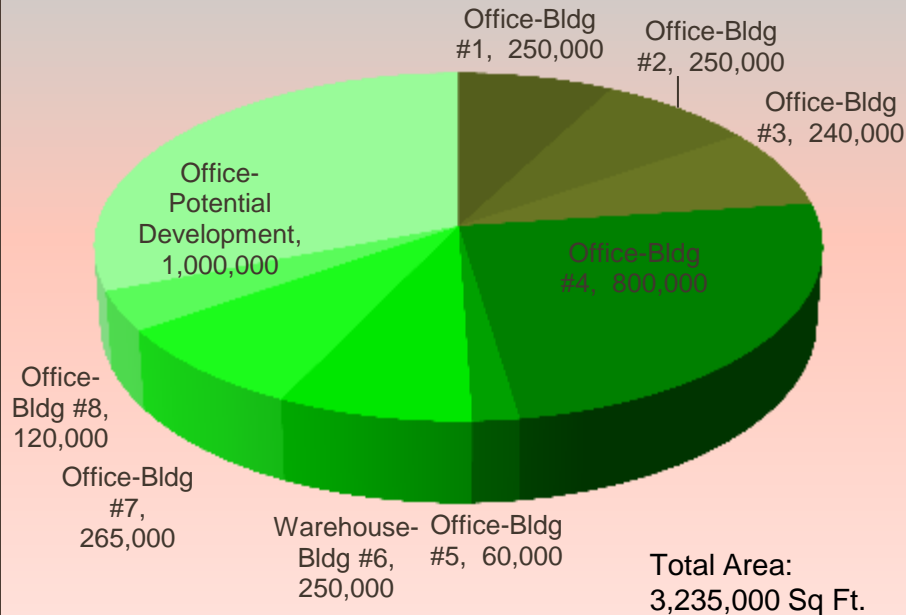
HGA Study

- ▶ MSW - Renewable Based Community District Energy
- ▶ Modern Low Temperature Hot Water Technology
- ▶ Cost Effective Phased Approach
- ▶ Phase 1 - Anchor Customers, 3-4 Buildings
- ▶ Phase 2 - Full Scale, 3 Million Square Feet
- ▶ Substantial CO₂e Reduction
- ▶ Reliable, Efficient, and Resilient



Building Space Projection

Potential Customer Base: Square Footage



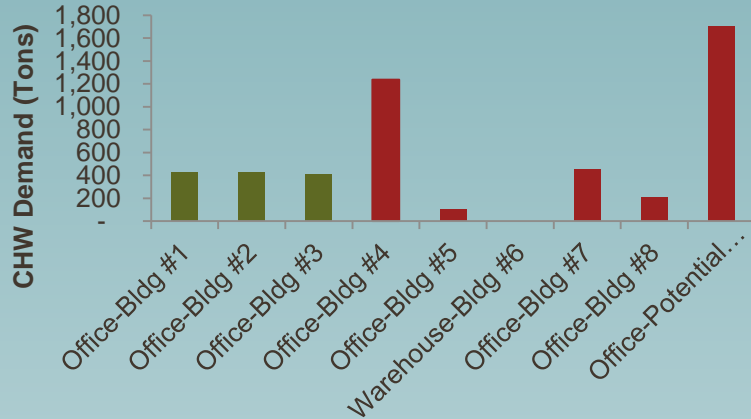
| Building Type/Usage | Phase 1(SF) | Phase 2(SF) | Total Space (SF) |
|------------------------------|----------------|------------------|------------------|
| Office-Bldg #1 | 250,000 | - | 250,000 |
| Office-Bldg #2 | 250,000 | - | 250,000 |
| Office-Bldg #3 | 240,000 | - | 240,000 |
| Office-Bldg #4 | | 800,000 | 800,000 |
| Office-Bldg #5 | - | 60,000 | 60,000 |
| Warehouse-Bldg #6 | - | 250,000 | 250,000 |
| Office-Bldg #7 | - | 265,000 | 265,000 |
| Office-Bldg #8 | - | 120,000 | 120,000 |
| Office-Potential Development | - | 1,000,000 | 1,000,000 |
| Total | 740,000 | 2,495,000 | 3,235,000 |

Account building space projection

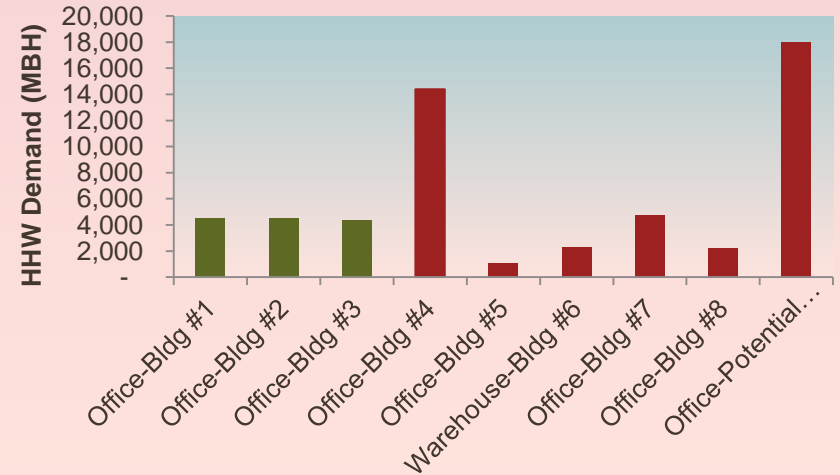
- By phased approach
- By building type - i.e. commercial, hotel, residential, office

Thermal Load Analysis

Diversified Chilled Water Demand



Diversified Hot Water Demand



Diversified Hot Water Demand (MBH)

Phase 1

13,320

Phase 2

42,660

Total

55,980

Diversified Chilled Water Demand (Tons)

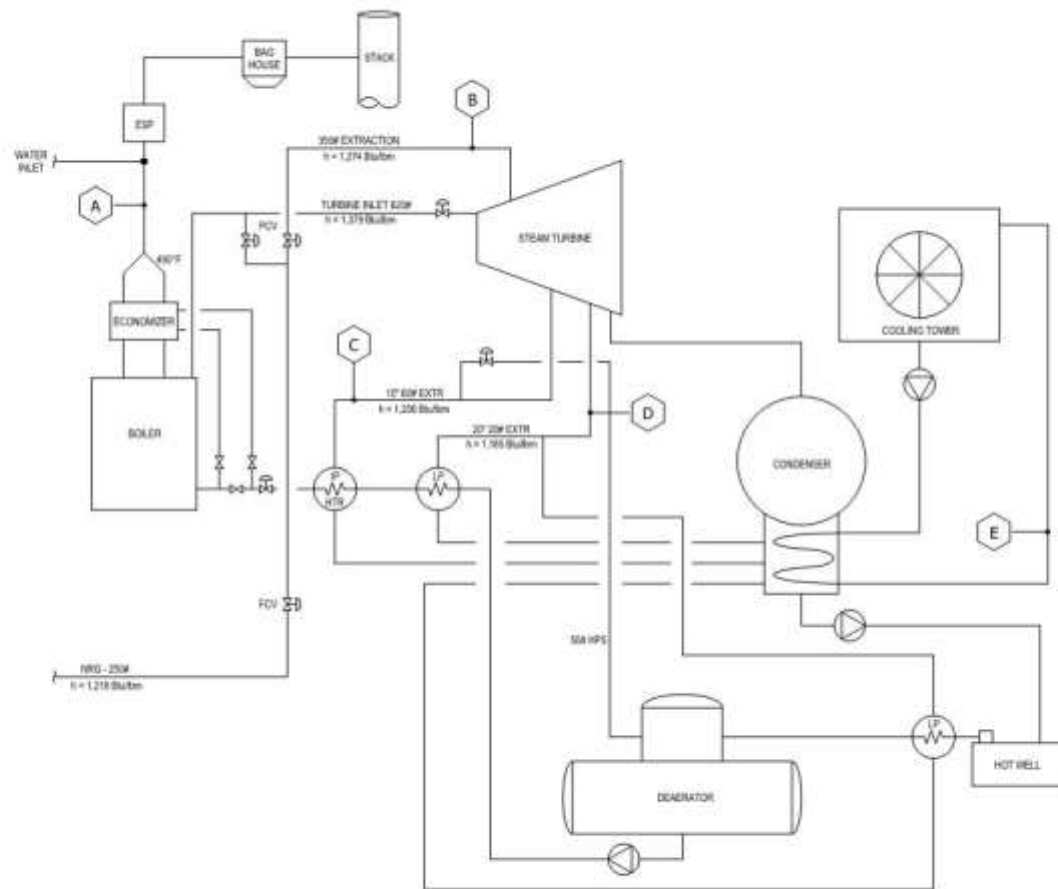
1,258

3,693

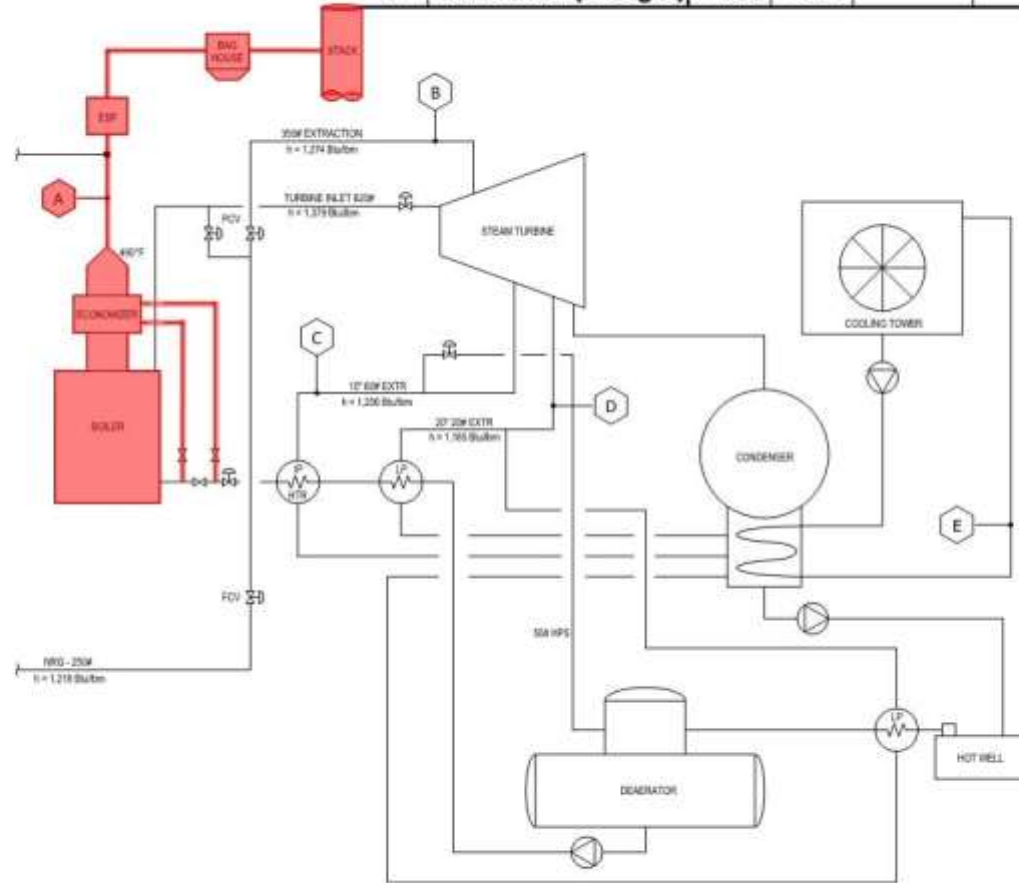
4,951

Account realistic building consumer load assessment

- Account for diversification



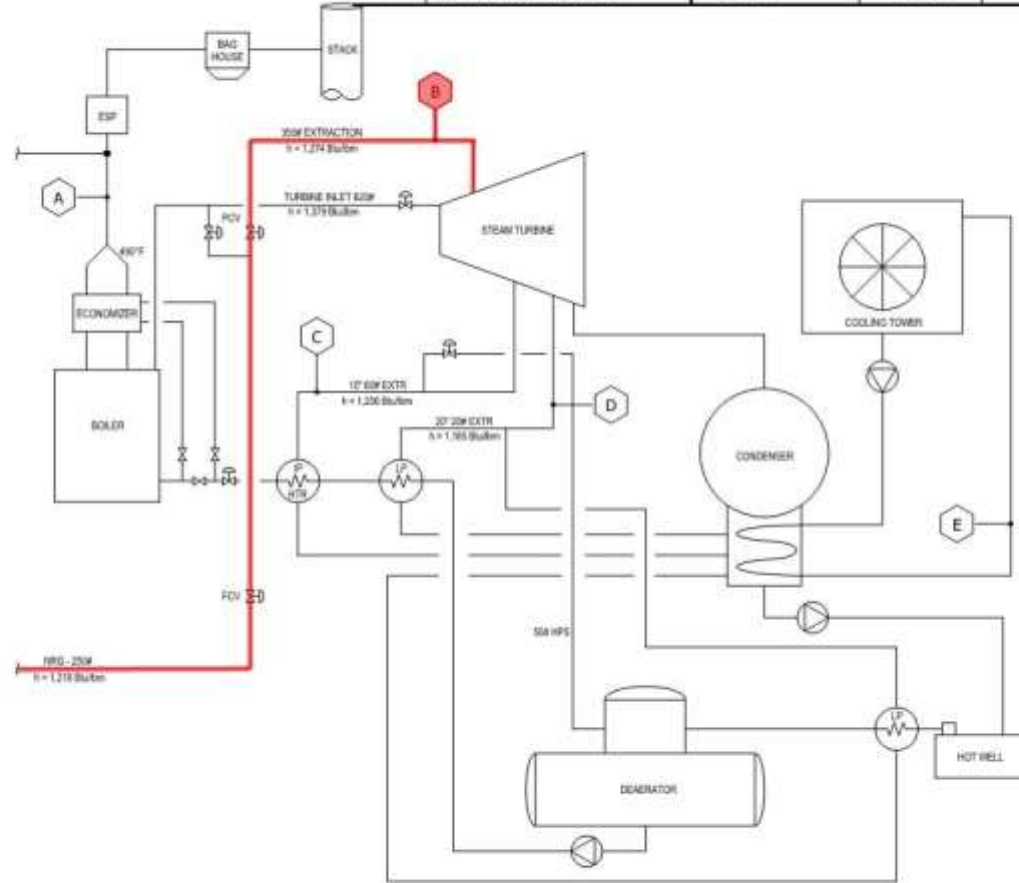
- Waste Heat
- Reduces water Use
- Available Space in Breeching and Plant
- Before Emission Controls
- Available Energy Fluctuates over Time



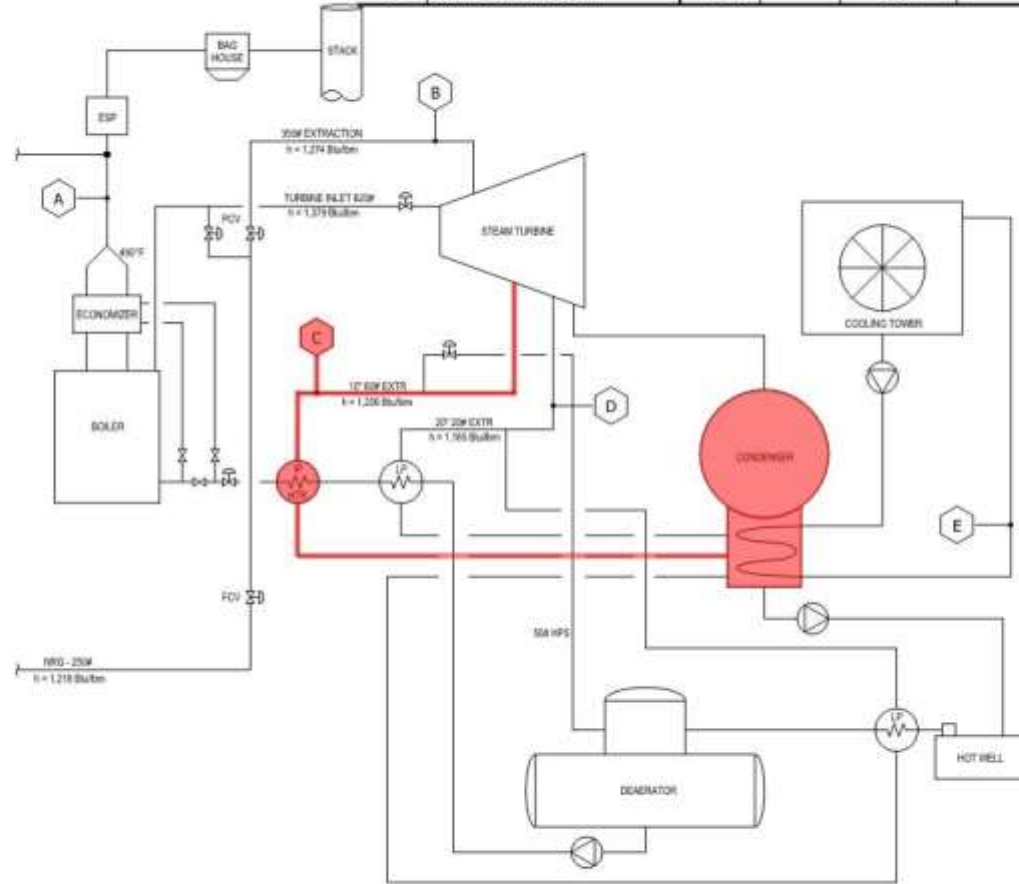
| Recovery Point | | Temperature (°F) | | Pressure (psig) | Maximum Mass Flow Rate (lbm/hr) | Design MMBtu/H Available |
|----------------|-----------------------|------------------|-----|-----------------|---------------------------------|--------------------------|
| A | Economizer (Flue gas) | 400 | 270 | | 456,000 | 19.0 |

- Largest Available Source
- Existing Export Contract
- Greatest impact on Electrical Generation

| | Recovery Point | Temperature (°F) | Pressure (psig) | Maximum Mass Flow Rate (lbm/hr) | Design MMBtu/h Available |
|---|-----------------|------------------|-----------------|---------------------------------|--------------------------|
| B | 350# Extraction | 539 | 350 | 90,000 | 106.7 |

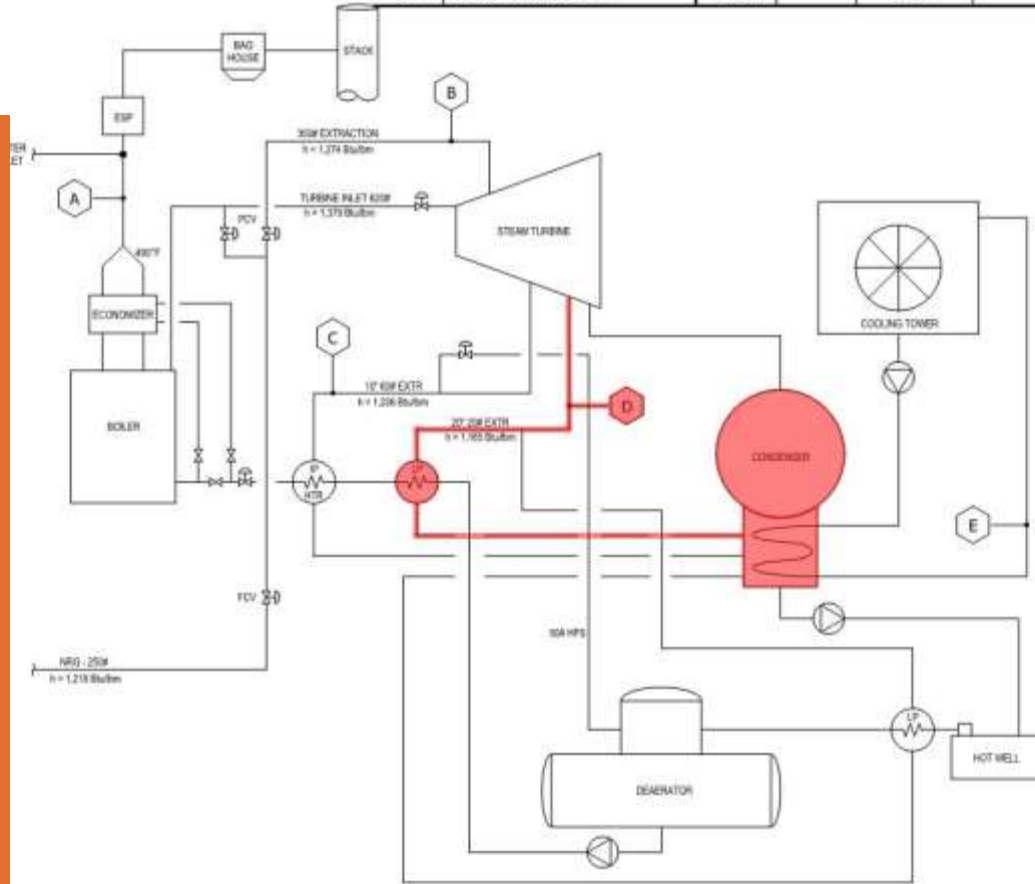


- Less Impact on Electrical Generation
- Existing port
- Current Loads:
 - Feedwater Preheat
 - Deaerator



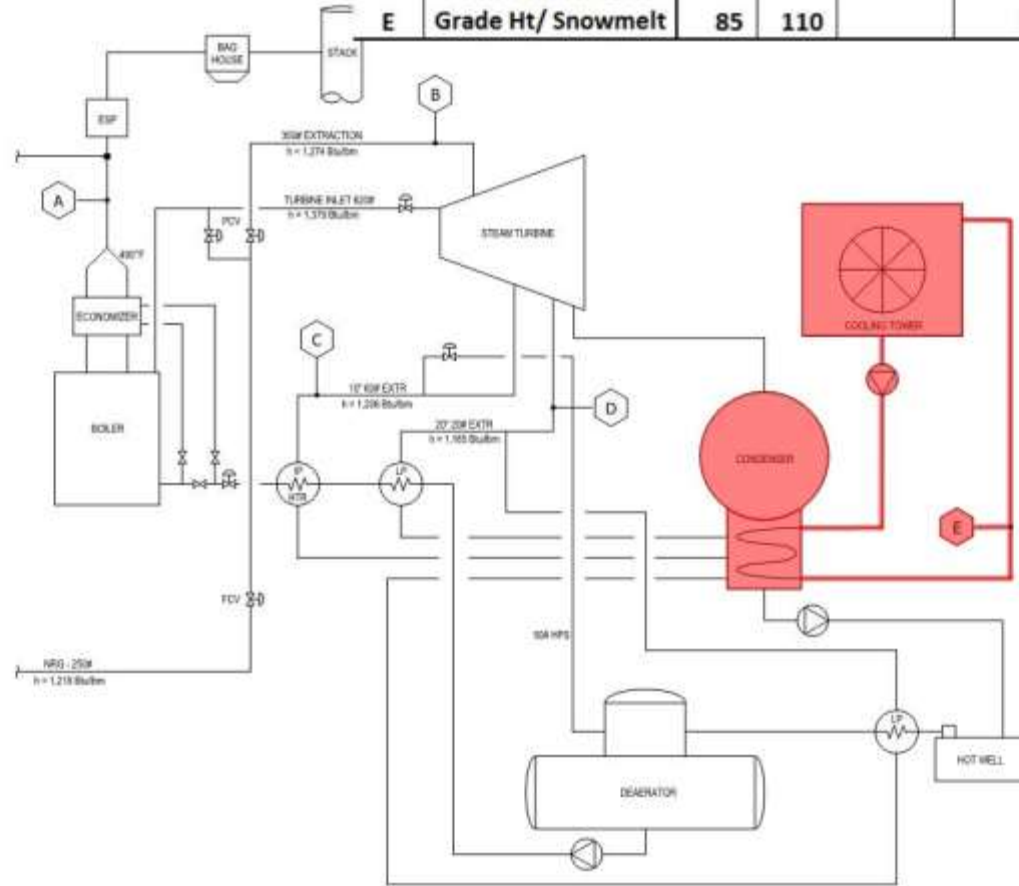
| | Recovery Point | Temperature (°F) | Pressure (psig) | Maximum Mass Flow Rate (lbm/hr) | Design MMBtu/Hr Available |
|---|----------------|------------------|-----------------|---------------------------------|---------------------------|
| C | 60# Extraction | 350 | 60 | 64,000 | 60.7 |

- **Least Impact on Electrical Generation**
- **Existing port**
- **Best Pressure**
- **Current Loads:**
 - **Feedwater Preheat**
 - **Air Preheat**



| | Recovery Point | Temperature (°F) | Pressure (psig) | Maximum Mass Flow Rate (lbm/hr) | Design MMBtu/Hr Available |
|---|----------------|------------------|-----------------|---------------------------------|---------------------------|
| D | 20# Extraction | 251 | 20 | 32,000 | 31.0 |

- **Waste Heat- No Impact on Electric Generation**
- **Largest Source**
- **Good for Heat Pump Loop**
- **Low Grade Heat**
- **Largest Piping required for District Energy**
- **Current Loads:**
 - **Snowmelt**



| Recovery Point | | Temperature (°F) | | Pressure (psig) | Maximum Mass Flow Rate (lbm/hr) | Design MMBtu/Hr Available |
|----------------|------------------------------------|------------------|-----|-----------------|---------------------------------|---------------------------|
| E | Cond Water -Low Grade Ht/ Snowmelt | 85 | 110 | | 182,117 | 273.0 |

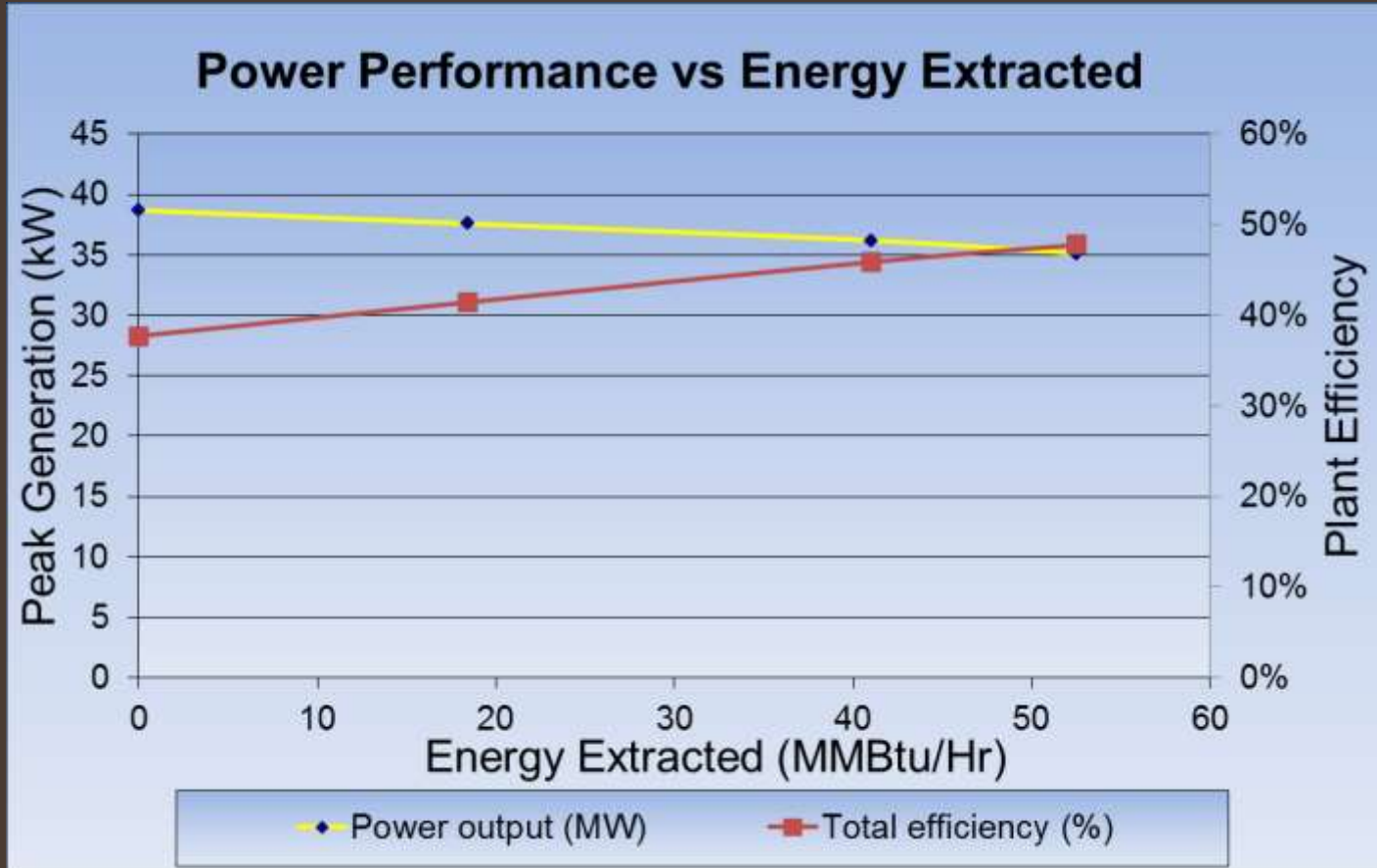
| Recovery Point | | Temperature (°F) | | Pressure (psig) | Maximum Mass Flow Rate (lbm/hr) | Design MMBtu/Hr Available | Existing Diversified Flow (lbm/hr) | Existing Diversified MMBtu /Hr Available |
|----------------|------------------------------------|------------------|-----|-----------------|--|---------------------------|------------------------------------|--|
| Turbine Inlet | | 750 | | 620 | 350,000 | 147.0 | 300,000 | |
| A | Economizer (Flue gas) | 400 | 270 | | 456,000 | 19.0 | 390,857 | 6.9 |
| B | 350# Extraction | 539 | | 350 | 90,000 | 106.7 | 25,000 | 57.1 |
| C | 60# Extraction | 350 | | 60 | 64,000 | 60.7 | 53,500 | 1.4 |
| D | 20# Extraction | 251 | | 20 | 32,000 | 31.0 | 26,500 | 1.0 |
| E | Cond Water -Low Grade Ht/ Snowmelt | 85 | 110 | | 182,117 | 273.0 | - | 258.0 |
| F | Blowdown | 180 | 110 | | 7,000 | 0.5 | 6,000 | 0.4 |
| | | | | | Total Available (MMBTU/HR) | | | 324.8 |
| | | | | | Extraction Energy Available (MMBTU/HR) | | | 59.5 |

| Recovery Point | | Temperature (°F) | | Pressure (psig) | Maximum Mass Flow Rate (lbm/hr) | Design MMBtu/Hr Available | Existing Diversified Flow (lbm/hr) | Existing Diversified MMBtu /Hr Available |
|----------------|------------------------------------|------------------|-----|-----------------|--|---------------------------|------------------------------------|--|
| Turbine Inlet | | 750 | | 620 | 350,000 | 147.0 | 300,000 | |
| A | Economizer (Flue gas) | 400 | 270 | | 456,000 | 19.0 | 390,857 | 6.9 |
| B | 350# Extraction | 539 | | 350 | 90,000 | 106.7 | 5,000 | 78.9 |
| C | 60# Extraction | 350 | | 60 | 64,000 | 60.7 | 40,200 | 15.2 |
| D | 20# Extraction | 251 | | 20 | 32,000 | 31.0 | 13,300 | 15.2 |
| E | Cond Water -Low Grade Ht/ Snowmelt | 85 | 110 | | 182,117 | 273.0 | - | 258.0 |
| F | Blowdown | 180 | 110 | | 7,000 | 0.5 | 6,000 | 0.4 |
| | | | | | Total Available (MMBTU/HR) | | | 374.6 |
| | | | | | Extraction Energy Available (MMBTU/HR) | | | 109.3 |

Plant Efficiency & Derate at Steam Extraction

| Extraction (Mlbs/hr) | Extraction (MMBtu/hr) | Power output (MW) | Total efficiency (%) | Th Energy Cost (\$/MMBtu) Based on Lost Electrical Revenue (\$/MWH) | |
|--|--------------------------|-------------------------|----------------------------|--|----------|
| - | - | 38.70 | 38% | \$ 30.00 | \$ 60.00 |
| 19.00 | 18.42 | 37.59 | 41% | \$ 1.81 | \$ 3.62 |
| 42.80 | 41.00 | 36.20 | 46% | \$ 1.83 | \$ 3.65 |
| 56.00 | 52.50 | 35.11 | 48% | \$ 2.05 | \$ 4.10 |
| 99.80 | 90.65 | 38.70 | 54% | \$ 2.39 | \$ 3.98 |
| Waste Heat Recovery from Condenser Water | | | | | |
| - | 52.50 | 38.70 | 51% | \$ - | \$ - |

Plant Efficiency & Derate at Steam Extraction



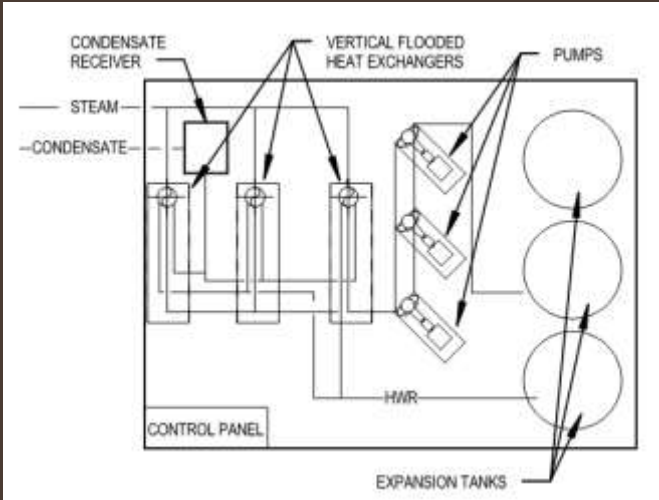
Thermal Piping Network - Anchor Customer-Phase 1



Thermal Piping Network - Full Build-out-Phase 2



Capital Expenditure - Heating System

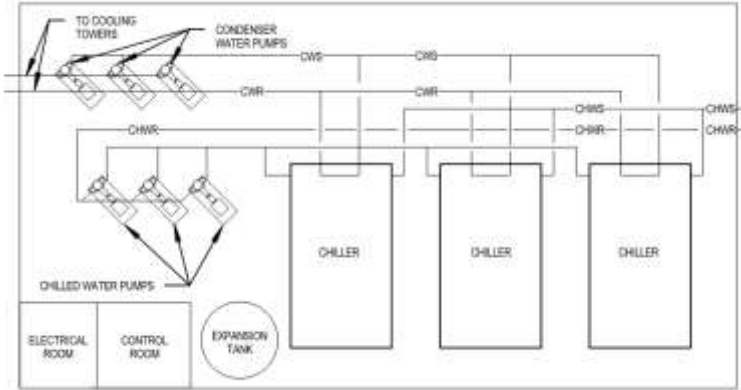


| | Existing HERC Plant-Mech Room | Parking Ramp C | |
|---|-------------------------------------|--------------------|--------------------|
| Heating System | Plant #1 | Plant #2 | Total |
| New Heating Plant | \$564,400 | \$564,400 | \$1,128,800 |
| Plant piping | \$250,000 | \$0 | \$250,000 |
| Plant Building Site | \$0 | \$300,000 | \$300,000 |
| Contractors Gen. Cond.Fee/Bond/Insurance | \$90,300 | \$224,700 | \$315,000 |
| Est. Design Fee | \$81,400 | \$98,000 | \$179,400 |
| Contingency-15% | \$147,915 | \$178,065 | \$325,980 |
| SUBTOTAL Plant Cost | \$1,134,015 | \$1,365,165 | \$2,499,180 |
| Distribution Piping: | | | |
| Buried Steam Piping System | \$0 | \$1,532,000 | \$1,532,000 |
| Buried HHW piping | \$235,500 | \$174,000 | \$409,500 |
| SUBTOTAL Buried Piping | \$235,500 | \$1,706,000 | \$1,941,500 |
| | | | |
| GRAND TOTAL | \$1,369,515 | \$3,071,165 | \$4,440,680 |
| | | | |
| Building Interface* | \$379,260 | \$193,500 | \$572,760 |

* To be negotiated with the potential customers



Capital Expenditure - Cooling System



| Cooling System | Existing HERC Plant #1 | Plant #2 | Total |
|-------------------------------------|------------------------|------------------|--------------------|
| | Phase 1 | Phase 1 | |
| Cooling Plant | \$1,820,600 | \$0 | \$1,820,600 |
| Cooling Towers | \$400,000 | \$0 | \$400,000 |
| Electric Equipment, Wiring | \$300,000 | \$0 | \$300,000 |
| Plant Building Site | \$0 | \$0 | \$0 |
| Plant Piping | \$350,000 | \$0 | \$350,000 |
| Contractors | | | |
| Gen.Cond.- Fee/Bond/Insurance | \$403,300 | \$0 | \$403,300 |
| Design Fee | \$294,700 | \$0 | \$294,700 |
| Contingency-15% | \$535,290 | \$0 | \$535,290 |
| SUBTOTAL | \$4,103,890 | \$0 | \$4,103,890 |
| Distribution Piping: | | | |
| Buried Chilled Water Piping Network | \$329,500 | \$914,500 | \$1,244,000 |
| SUBTOTAL | \$329,500 | \$914,500 | \$1,244,000 |
| | | | |
| GRAND TOTAL | \$4,433,390 | \$914,500 | \$5,347,890 |
| | | | |
| Building Interface* | \$624,750 | \$318,750 | \$943,500 |



Phase 1 Heating System Summary Cost

| | |
|--------------------------|-------------|
| Heating Plant | \$2,499,000 |
| Distribution Piping | \$1,941,000 |
| Building Interconnection | \$0 |
| Subtotal | \$4,440,000 |

Operating Assumption

| | |
|---------------------|-----------|
| Heating Maintenance | \$12,654 |
| Incremental Labor | \$30,000 |
| Total Annual Admin | \$7,500 |
| Fuel Cost | \$121,978 |
| Capital Recovery | \$368,558 |
| Total Fixed Cost | \$418,712 |
| Variable Cost | \$121,978 |

District Hot Water Heating Pricing Structure

| | |
|--|---------|
| Connected Bldg Square Footage | 740,000 |
| Peak Diversified Demand (MMBtu/hr/Sqft) | 18 |
| Peak Diversified Heating Capacity (MMBtu/hr) | 13.32 |
| Equivalent Full Load Hours | 1800 |
| Annual Heating Consumption (MMBtu) | 23,976 |
| Demand Charge (\$ per MMBtu/hour-month) | 2620 |
| Variable Charge (\$ per MMBtu) | 5.09 |
| Availability | 93% |
| Boiler Efficiency | 80% |
| MSW Fuel (\$/MMBtu) | 4.00 |
| Heating Unit Cost (\$/MMBtu/hr) | 21 |



Phase 1 Cooling System Summary Cost

| District Cooling Pricing Structure | |
|--------------------------------------|-----------|
| Peak Cooling Demand (ton/sq.ft.) | 575 |
| Peak Cooling Capacity (ton) | 1287 |
| Equivalent Full Load Hours | 900 |
| Cooling Plant Efficiency (Kw/Ton) | 0.70 |
| Electrical Price (\$/KWh) | 0.08 |
| Annual Cooling Consumption (ton-hr) | 1,158,261 |
| Demand Charge (\$ per ton per month) | 27 |
| Variable charge (\$ per ton-Hr) | 0.09 |
| Cooling unit cost (\$/ton-hr) | 0.45 |

| Capital Cost | Phase 1 |
|---------------------|--------------|
| Cooling Plant | \$ 4,103,000 |
| Distribution Piping | \$ 1,244,000 |
| Building | \$ - |
| Subtotal | \$ 5,347,000 |

| Operating Assumption | Cost(\$) |
|------------------------------|----------|
| Capital Recovery | 341,457 |
| Electricity | 64,863 |
| Water and Sewer, Chemical | 40,539 |
| Subtotal Cooling Consumption | 105,402 |
| Subtotal Cooling Demand | 411,131 |



Financial Projection- Phase 1

| Building Conventional System Pricing | |
|---|-----------------|
| Average Heating+Cooling Cost (\$/Sft)- 20 | 1.85 |
| | |
| District Thermal Pricing | |
| Average Heating + Cooling Cost (\$/SF)- | 1.75 |
| | |
| Returns | |
| IRR | 5.01% |
| District Heating and Cooling Savings | |
| Average Over 20 yrs | 4% |
| Cumulative | \$ 1,805,000.00 |

| Financing | |
|-------------------------|--------|
| Equity | 10% |
| Debt Amount (1000\$) | 10,049 |
| Interest Rate | 5.00% |
| Capital Recovery Factor | 7.095% |
| Term | 25 |



Financial Projections - Phase 1

Potential Changes to Revenues

- ▶ Reduced Direct Electric Revenue \$72K-\$158K
- ▶ Thermal Revenues \$480K-\$800K
- ▶ Additional O&M Costs \$10-\$30K
- ▶ Reduced Water Costs \$22-\$50K
- ▶ Other Potential Revenue streams
 - ▶ ,
 - ▶ Carbon Credits



Major Benefits & Opportunities



- Improved Plant Efficiency- improves with added customers.
- Reduced water use and discharge.
- Reduces fossil fuel use
- Renewable Energy.
- Lower City Carbon Footprint relative to conventional equipment.
- Current PPA expires in three years.
- Urban area with potential rapid development.
- Interconnect with NRG district steam system

Challenges



- Timing and uncertainty among the developers for the anchor customers.
- New Building on Independent System.
- Area development vs building development.
- Back-up sources - permitting for on-site heating generation.
- Rate structure between steam and hot water.