

# CHP Design Considerations for Municipal Water Treatment Facilities

**Solar<sup>®</sup> Turbines**

*A Caterpillar Company*

**CleaverBrooks<sup>®</sup>**



# Learning Objectives

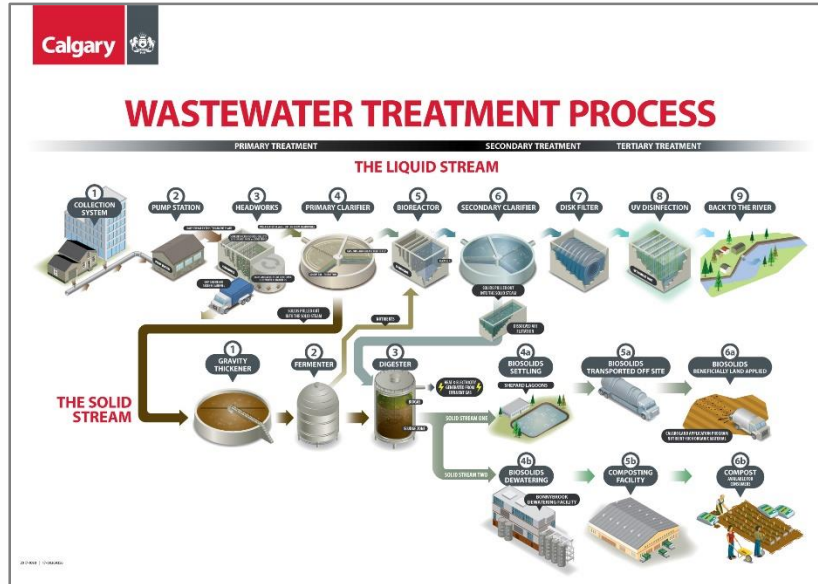
- Project Background
- Unique Concerns
- Gas Turbine Impact
- HRSG System Impact
  - HRSG Design
  - Economizer Design



# Project Background

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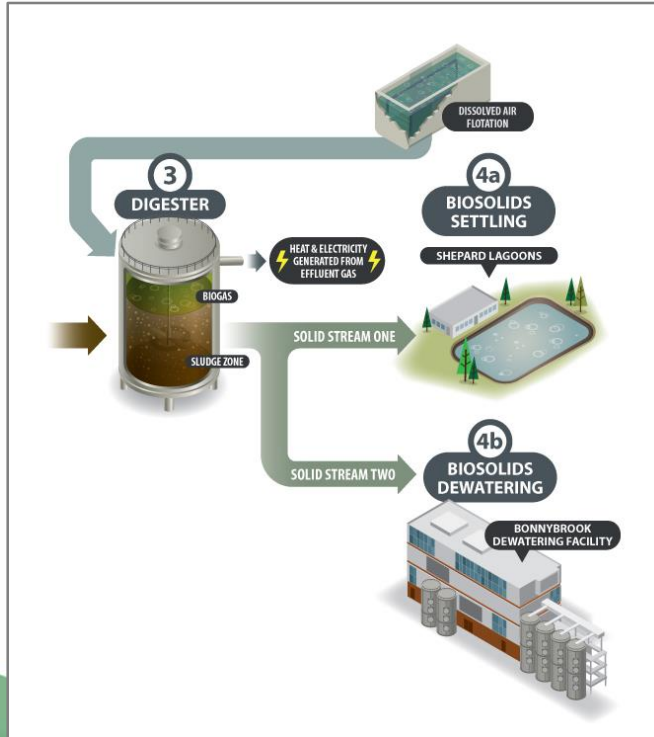
## Facility: Bonnybrook WWT Plant

- Calgary, Alberta, Canada
- World's largest cold-weather biological nutrient removal plant
- Expanding to meet a growing population now and in the future

# Project Background

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## Expanded Cogeneration Facility

- New Combustion Gas Turbine Generator (CTG)
- New HRSG
- New Steam Turbine Generator

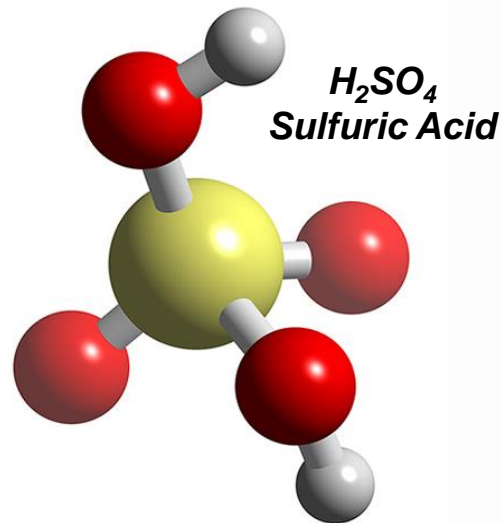
# Unique Concerns

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- Raw Digester Gas can contain as much as 5000 PPM of  $H_2S$
- System includes a biological  $H_2S$  scrubber but its reliability has proven to be questionable
- Combustion of this fuel in the CTG can result in a  $SO_2$  content in the HRSG flue gas as high as 266 ppm
- The sulfur acid dew point of this flue gas will be approximately  $285^{\circ}F$





# CHP System

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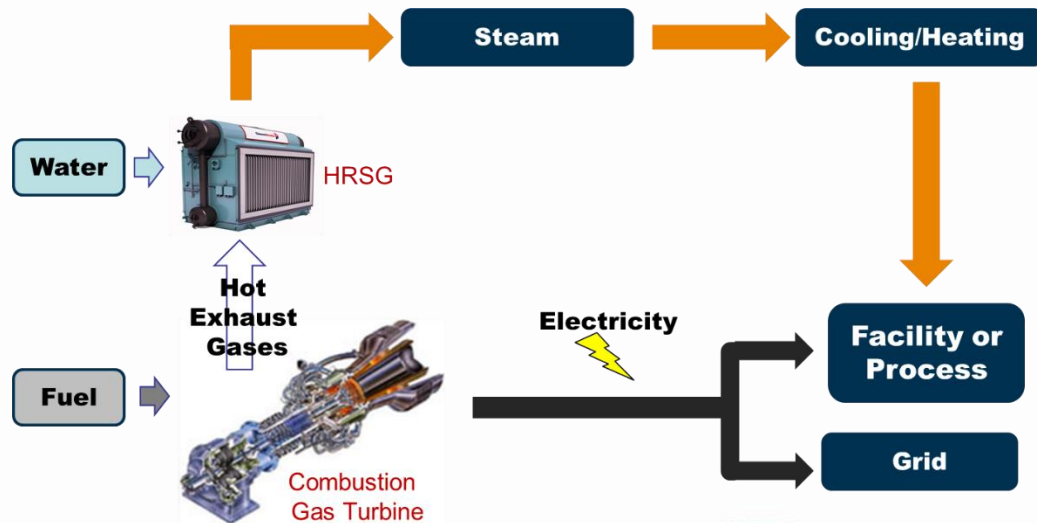


## Key Components

- Solar Centaur 50 CTG firing natural gas & digester gas blend to produce 4.5 MW of electricity
- HRSG to generate 23,000 lbs/hr of steam at 350 psig

## Key Design Considerations

- Combined heat & power generation and efficiency
- Fuel flexibility
- Steam production including process and cogeneration
- Life expectancy



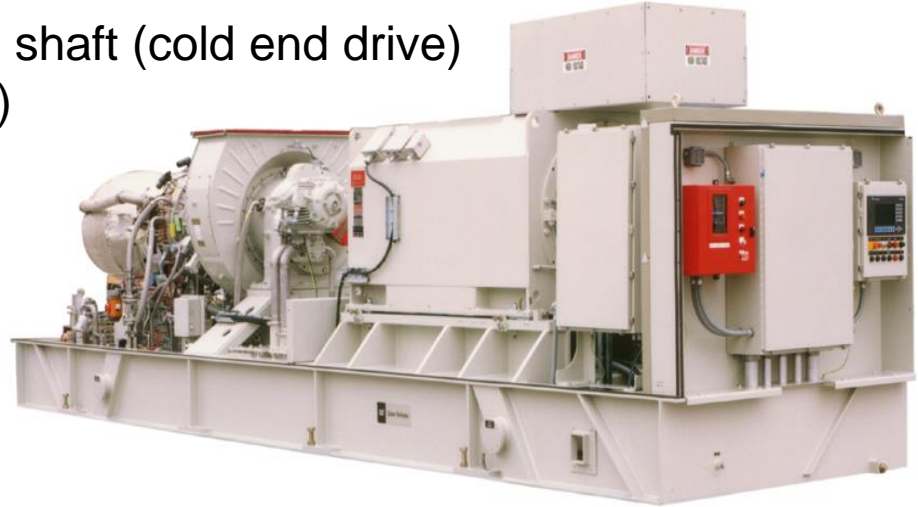
# CTG Package

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- Solar Centaur 50 (4.5 MW ISO) single shaft (cold end drive) combustion turbine generator (4.16kV)
- Industrial turbine
- Sound attenuating (85 dB) weather proof package in CSA certified single lift module
- On skid controls, fuel system, and ancillary equipment
- Integral fire suppression system



# CTG Concerns

- Wide & varying fuel gas composition
- Blending fuel from 100% natural gas (1000 BTU/scfm) to 100% digester gas (550 BTU/scfm)
- Startup on 100% digester gas (no other torch fuel)
- Fuel bound sulfur ( $\text{H}_2\text{S}$ ) up to 5,000 ppm
- Fuel carbon ( $\text{CO}_2$ ) composition up to 40%
- Potential for high levels of siloxanes in fuel
- High ambient air particulate matter (dust) levels
- Very cold ambient air temperatures (less than  $-30^\circ \text{C}$ )





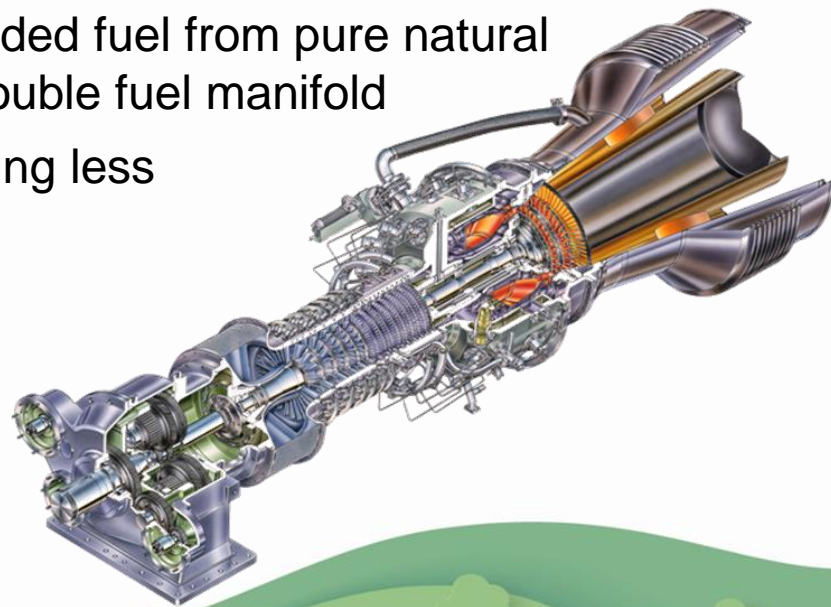
# CTG Combustion

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- Wide fuel suitability for combustion of blended fuel from pure natural gas to pure digester gas (low BTU) with double fuel manifold
- Conventional dry emission system producing less than 46 ppm on pure (100%) digester gas
- Able to startup on pure (100%) digester gas without pilot torch boost fuel
- Capable of handling fuel bound sulfur concentrations between 3,000 and 5,000 ppm without impact on lifespan



# CTG Accessories

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- Siloxane removal system (provided by owner)
- Self cleaning updraft combustion air filter system for extreme cold weather application
- Package ventilation barrier filters for dusty environment
- Package heaters for extreme cold weather startup
- Oil/air lube oil cooler & VFD for extreme cold weather operation



# HRSG System

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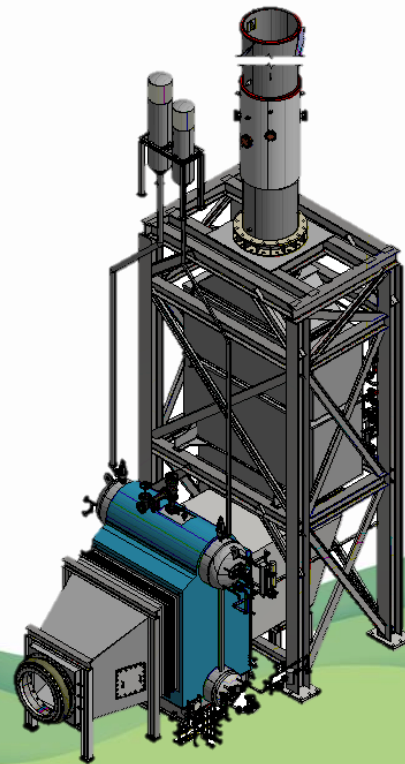


## Key Components

- Ductwork
- Boiler
- Economizer
- Stack

## Key Design Concerns

- Cold End Corrosion
- Flue Gas Migration



# HRSG System

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## Boiler System

- Simple Design
- Saturated Steam
- Maximize Heat Transfer

## Key Design Concerns

- Cold End Corrosion (NOT A CONCERN)
- Flue Gas Migration (A CONCERN)



# HRSG System

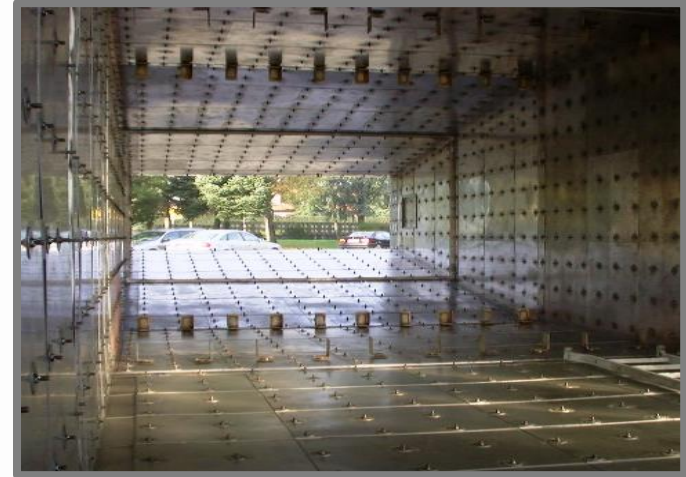
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## Internal Casing / Floating Liner:

Risk is migration of sulfur laden flue gas into gaps in the internal liner and eventually cooling and forming acid in the walls of the boiler.



# HRSG System

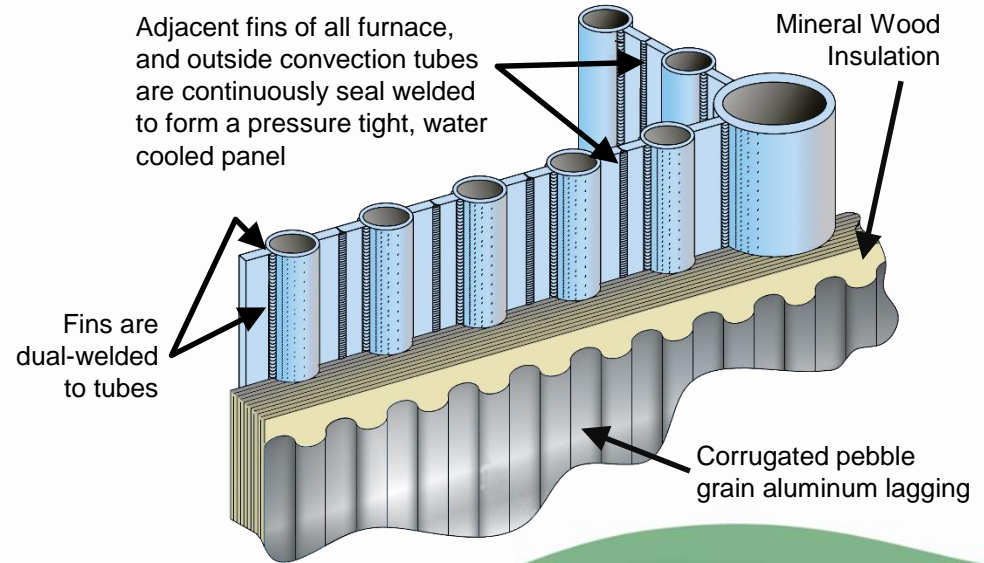
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## Design Solution:

Membrane wall construction in the boiler. No longer possible for flue gas migration through the walls of the unit.





# HRSG System

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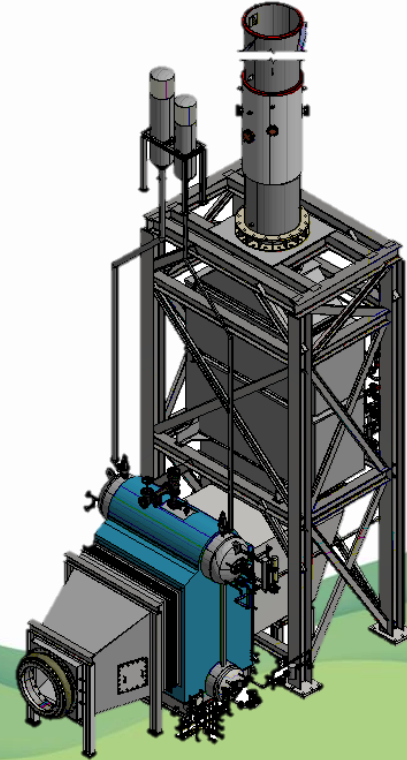


## Key Components

- Ductwork
- Boiler
- **Economizer**
- Stack

## Key Design Concerns

- **Cold End Corrosion**
- Flue Gas Migration



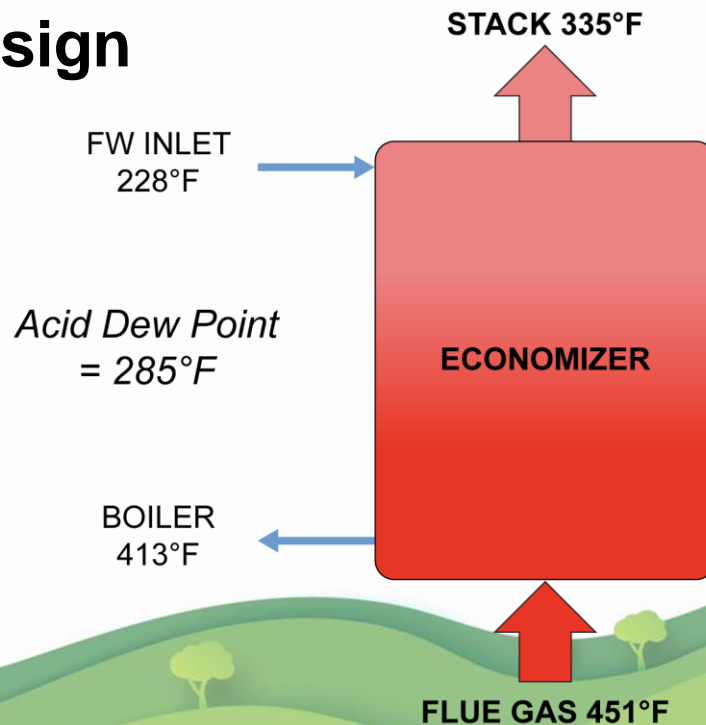
# HRSG System

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## Traditional Design



# HRSG System

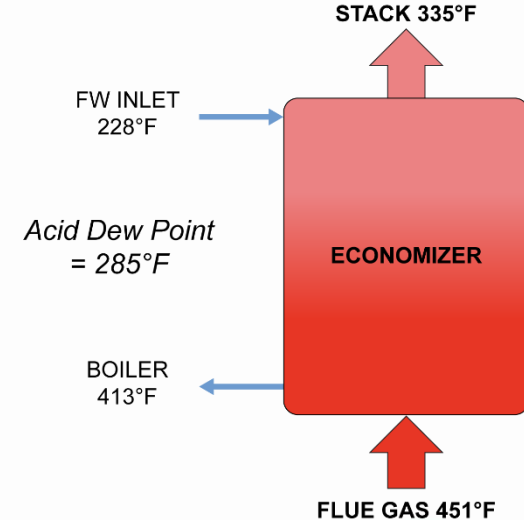
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## Possible Solutions

- Disposable economizer?
- Disposable portion of economizer?
- Materials?
- Feedwater recirculation?
- Must increase the feedwater temperature
  - Increase the DA pressure?



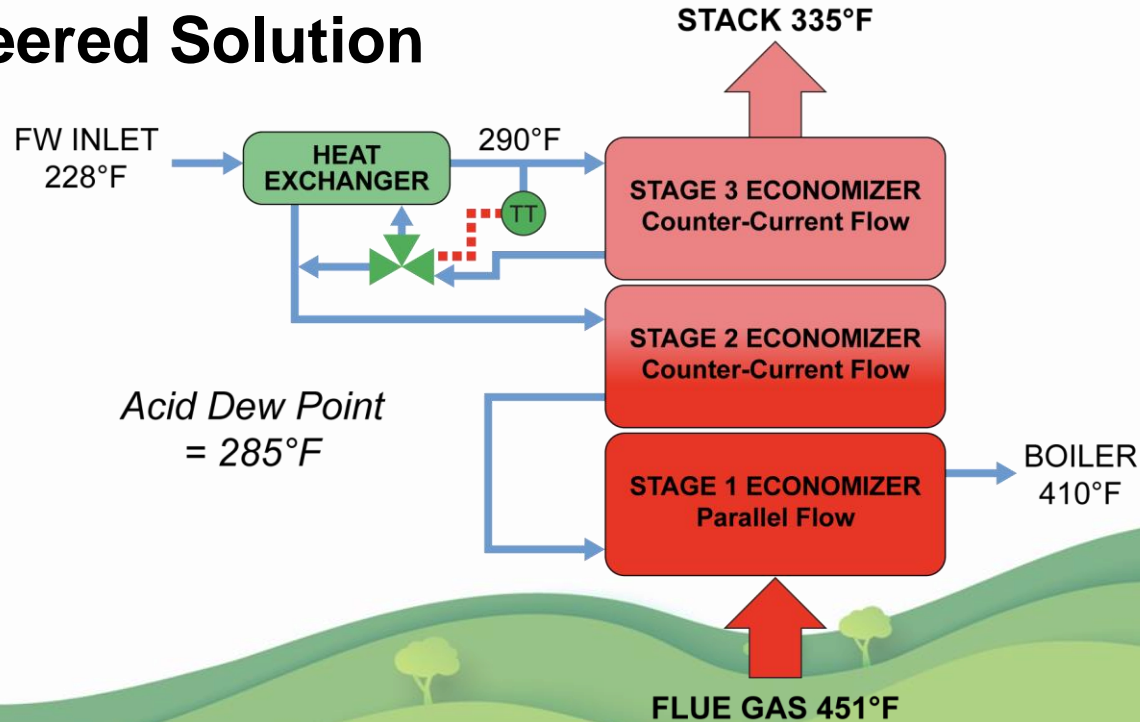
# HRSG System

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## Engineered Solution



# Summary

Meet unique needs with a unique engineered system.

Nitrogen – Oxygen – Iron - Argon

|   |   |   |  |
|---|---|---|--|
| <div>7</div> <div>14.007</div> <div>N</div> <div>NITROGEN</div> | <div>8</div> <div>15.999</div> <div>O</div> <div>OXYGEN</div> | <div>26</div> <div>55.845</div> <div>Fe</div> <div>IRON</div> | <div>18</div> <div>39.948</div> <div>Ar</div> <div>ARGON</div> |
|---|---|---|--|



# Any Questions

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