

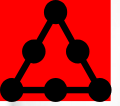
Fehr Solutions, LLC

Water Treatment Services and Consulting

BRINGING WATER TREATMENT IN HOUSE - MONITORING AND CONTROL STRATEGIES AND IMPROVED RESULTS AT NRG PHOENIX

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FEHR SOLUTIONS, LLC



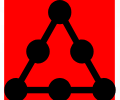
AGENDA

- A VERY BRIEF HISTORY OF COOLING WATER TREATMENT CHEMISTRY
- MOTIVATIONS FOR BRINGING CHEMISTRY IN HOUSE
- CHARTING A COURSE
 - IDENTIFYING THE CHALLENGES AND POTENTIAL PITFALLS
- IMPLEMENTATION
- FACILITY FEEDBACK



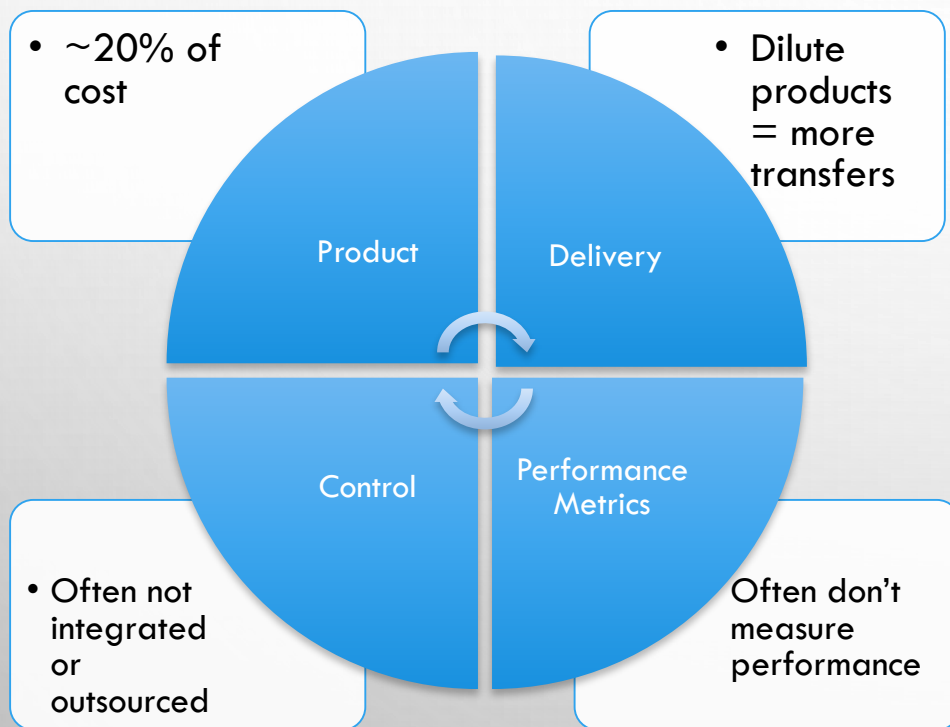
A VERY BRIEF HISTORY OF COOLING WATER TREATMENT CHEMISTRY

- INNOVATION (NEW MOLECULES) HAS DRAMATICALLY SLOWED DOWN OVER THE PAST 30 YEARS
 - WORK HORSE CHEMISTRY HASN'T CHANGED SIGNIFICANTLY FOR MOST CUSTOMERS THAT DISCHARGE TO A POTW
 - SCALE INHIBITORS (PBTC AND HEDP) - DEVELOPED IN THE 1970'S AND 1980'S
 - POLYMER (MULTIPLE – BUT GENERALLY FUNCTIONALLY EQUIVALENT) – DEVELOPED IN THE 1980'S AND 1990'S
 - YELLOW METAL CORROSION INHIBITOR - TOLYLTRIAZOLE/BENZOTRIAZOLE - DEVELOPED IN THE 1970'S
 - MILD STEEL CORROSION INHIBITORS - ZINC, PHOSPHATE, MOLYBDATE ,CARBOXYLATES - DEVELOPED IN THE 1970'S TO 1990'S.
 - PH CONTROL, NO PH CONTROL, SOFT WATER FEED.....DEPENDS ON SOURCE WATER
 - THESE CHEMISTRIES ARE THEN “BLENDED” TOGETHER TO FORM A PRODUCT DESIGNED TO TREAT A “TYPE” OF WATER
 - NO TECHNICAL BENEFIT TO BLENDING
 - RESULTS IN DILUTE PRODUCTS (SHIPPING MORE WATER)
 - MAKES IT DIFFICULT TO UNDERSTAND WHAT IS IN THE PRODUCT/RESULTS IN INEFFICIENT USE OF CHEMICALS



A VERY BRIEF HISTORY OF COOLING WATER TREATMENT CHEMISTRY

Components of a Standard Program

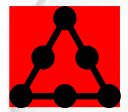


• PROS

- DON'T HAVE TO THINK ABOUT THE CHEMISTRY OR HANDLING ANYTHING
- LESS OPERATOR RESPONSIBILITY

• CONS

- PLANT HAS VERY LITTLE CONTROL OR "SAY" IN CHEMICALS SELECTED (TRUST)
- HARD TO UNDERSTAND COSTS



NRG PHOENIX

- 3 SEPARATE COOLING PLANTS WITH 40,000 TONS OF TOTAL CAPACITY
- 1 INTEGRATED COOLING LOOP WITH ICE STORAGE
 - APPROXIMATELY 3.5 MILLION GALLONS
- SERVING 38 CUSTOMERS IN 43 BUILDINGS



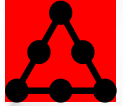
NRG Phoenix Downtown District Cooling System





WATER TREATMENT SITUATION – INCEPTION OF PLANT TO 2014

- OUTSOURCED WATER TREATMENT CHEMISTRY TO VARIETY OF 3RD PARTIES
 - IN THEORY THIS MEANT “LESS” OPERATOR INVOLVEMENT (LESS MANPOWER COMMITTED)
 - IN REALITY FOUND THAT LACK OF OWNERSHIP BY OPERATORS TRANSLATED TO NOT UNDERSTANDING WHAT WAS REALLY HAPPENING AND ULTIMATELY POOR PERFORMANCE
- MAINTENANCE COSTS WERE INCREASING
 - BASIN CLEANING/FILL CLEANING NECESSARY 2 TIMES A YEAR
 - PREMATURE FILL REPLACEMENT DUE TO SCALE FORMATION
 - ALGAE/BIOLOGICAL MATERIAL IN BASINS



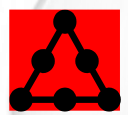
DECISION POINT

Path 1 – Choose a different supplier

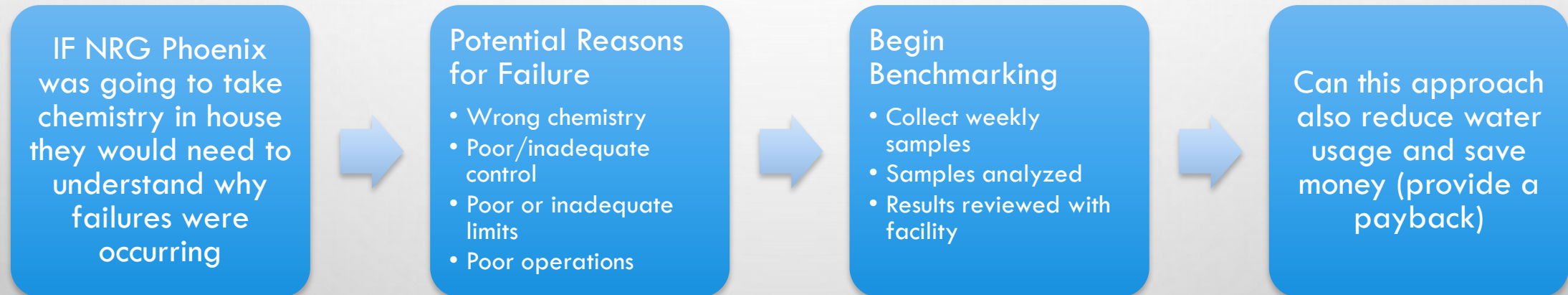
- Could improve situation
- Could be more of the same

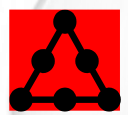
Path 2 – Take the water treatment chemistry entirely in house.

- What resources necessary internally to handle the potential increased Work load?
- Nobody to blame but the plant if it doesn't work (and of course the Consultant)



TAKING CHEMISTRY IN HOUSE

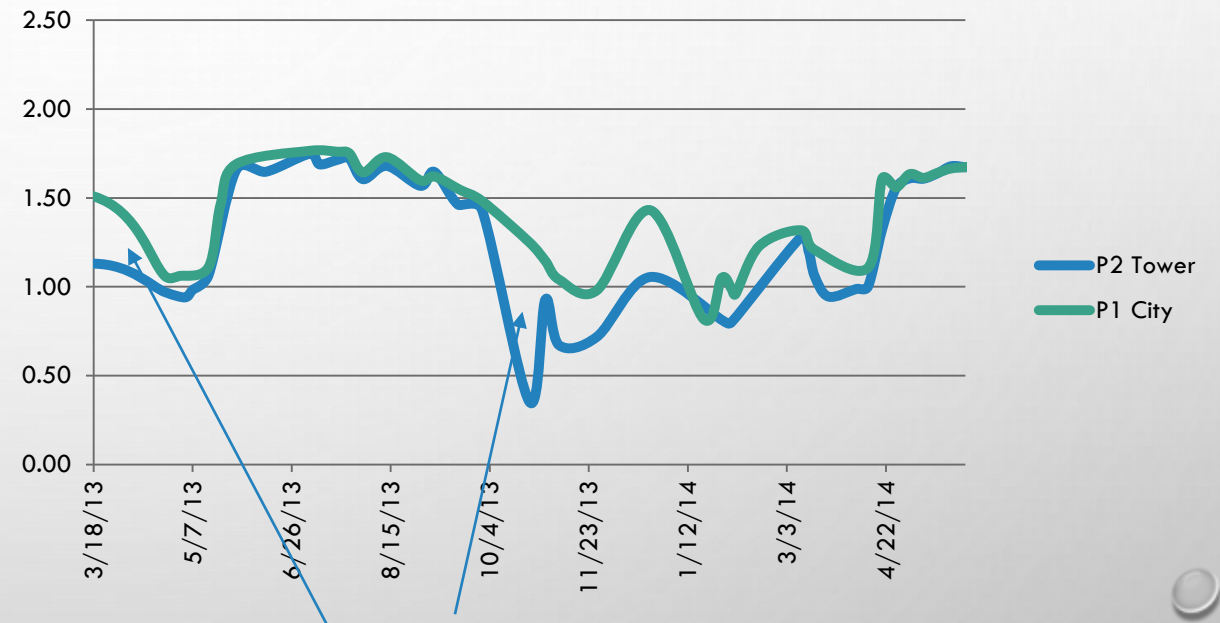




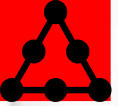
BENCHMARKING THE SYSTEM – THE SMOKING GUN

- PRIMARY METRICS (CHEMISTRY INDEPENDENT)
 - SCALE CONTROL METRIC - THE RATIO OF CA TO MG IN THE MAKE UP WATER SHOULD TRACK (WITHIN 5%) THE CA TO MG RATIO IN THE TOWER WATER.
 - MAGNESIUM IS NOT SENSITIVE TO PRECIPITATION UNDER NORMAL WATER CHEMISTRY AND CAN BE USED TO TRACK HOW MUCH CALCIUM SHOULD BE IN THE TOWER WATER IF SCALE FORMATION IS BEING CONTROLLED.

P2 Tower Ca to Mg Ratio



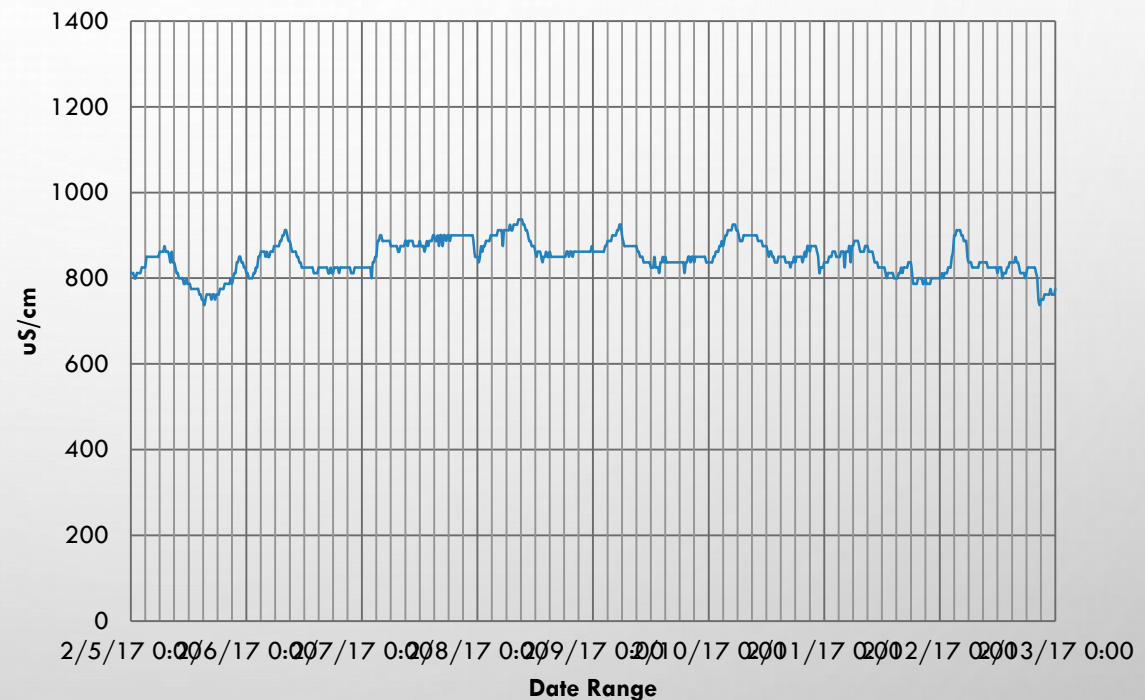
Scale formation
occurring

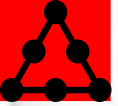


DETERMINING ROOT CAUSE OF SCALE FORMATION

- INVESTIGATION FOUND
 - PHOENIX CITY WATER CHANGES CONDUCTIVITY DRAMATICALLY – SOMETIMES HOURLY
 - SUMMER CAN SEE CONDUCTIVITY AS HIGH AS 1,800 MICRO SIEMENS
 - WINTER CAN SEE CONDUCTIVITY AS LOW AS 450 MICRO SIEMENS

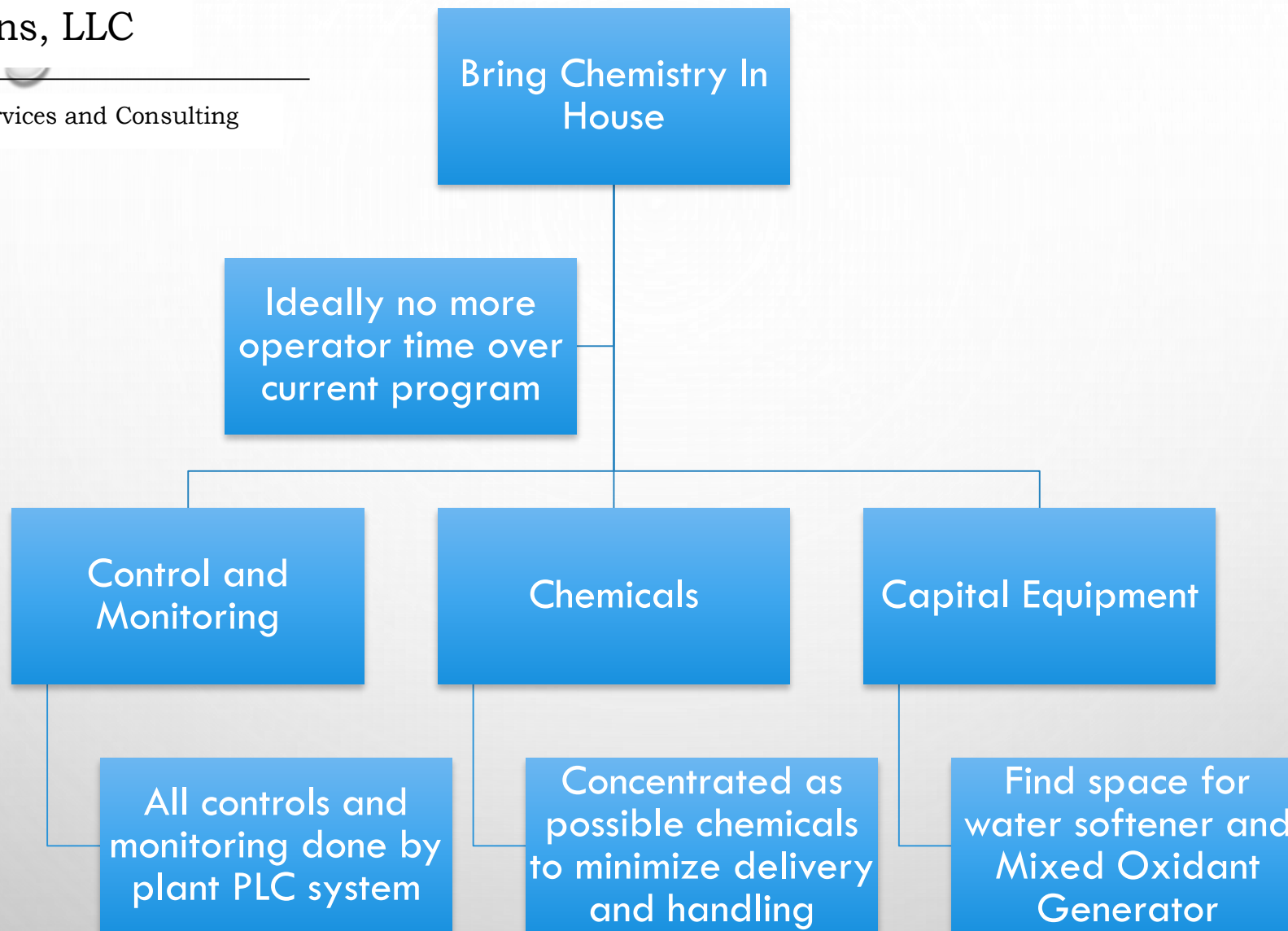
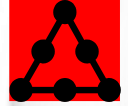
Plant 1 Make up Water Conductivity - 8 Days





HOW CAN THIS BE SOLVED?

- CONSIDERED THE THREE MOST COMMON METHODS
 - MONITOR INCOMING CONDUCTIVITY AND ADJUST BLOWDOWN SET POINT BASED ON CHANGES
 - WON'T RESULT IN SUBSTANTIAL WATER SAVINGS BUT WILL PREVENT GROSS SCALE FORMATION
 - FEED ACID TO CONTROL PH
 - PLANT HAD DONE THIS PREVIOUSLY
 - ISSUES WITH LEAKS
 - PLANT 2 IS UNDER THE CONVENTION CENTER - ANY CHEMICAL DELIVERY IS CHALLENGING
 - SOFTEN WATER TO REMOVE CALCIUM AND MAGNESIUM
 - CAPITAL INVESTMENT – BUT ALLOWS FOR HIGHER OVERALL CYCLES OF CONCENTRATION
 - SAFER VERSUS ACID HANDLING
 - **THIS APPROACH WAS SELECTED BECAUSE IT GAVE THE BEST PAYBACK COUPLED WITH THE LEAST OVERALL RISK**





SCALE AND CORROSION CONTROL CHEMICALS

- CONSULTANT SPECIFIED CHEMISTRY DURING TRANSITION AND WHEN ON SOFT WATER
 - DURING TRANSITION - CALCIUM CARBONATE INHIBITION PRIMARY CONCERN (PBTC – 10 PPM POLYMER – 10 PPM)
 - AFTER TRANSITION – MILD STEEL CORROSION PRIMARY CONCERN (PBTC – 5 PPM, POLYMER – 10 PPM, HYDROXYL PHOSPHONO ACETIC ACID – 2 PPM, PYRO PHOSPHATE – 2 TO 4 PPM)
 - TOLYLTRIAZOLE USED DURING BOTH PERIODS FOR COPPER CORROSION CONTROL (1 TO 3 PPM)





BIOLOGICAL CONTROL CHEMICALS

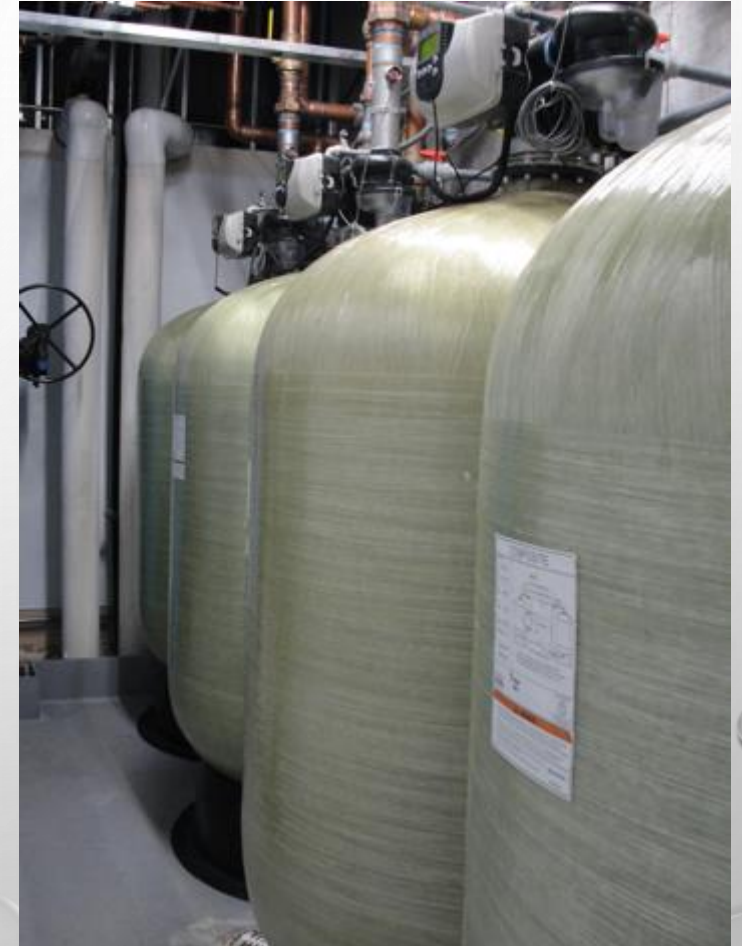
- MOST BIOCIDES ARE ALREADY SOLD AS CONCENTRATED AS POSSIBLE
 - BLEACH (12.5%)
 - STABILIZED BROMINE (12%)
 - BROMINE DONORS (SOLID TABLETS)
- THESE REQUIRE EXTENSIVE HANDLING AND ARE AMONG THE MOST HAZARDOUS OF CHEMICALS
- ALTERNATIVE IS TO GENERATE BIOCIDES ON-SITE USING SODIUM CHLORIDE (NaCl) AS THE PRECURSOR.
 - THIS ELECTROLYTIC PROCESS GENERATES A DILUTE SOLUTION OF BLEACH (0.45%) AND HYDROGEN PEROXIDE
 - MIOX MANUFACTURERS UNIT
 - A SEPARATE TALK DETAILING THIS UNIT WILL ALSO BE GIVEN
- THE SITE CAN GENERATE 30 LBS OF CHLORINE PER DAY.
 - HAVE FOUND THAT THEY ONLY NEED TO GENERATE 6 TO 20 LBS PER DAY TO MAINTAIN 0.5 TO 1.0 PPM FAC IN TOWER SYSTEM

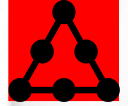




CAPITAL - WATER SOFTENERS

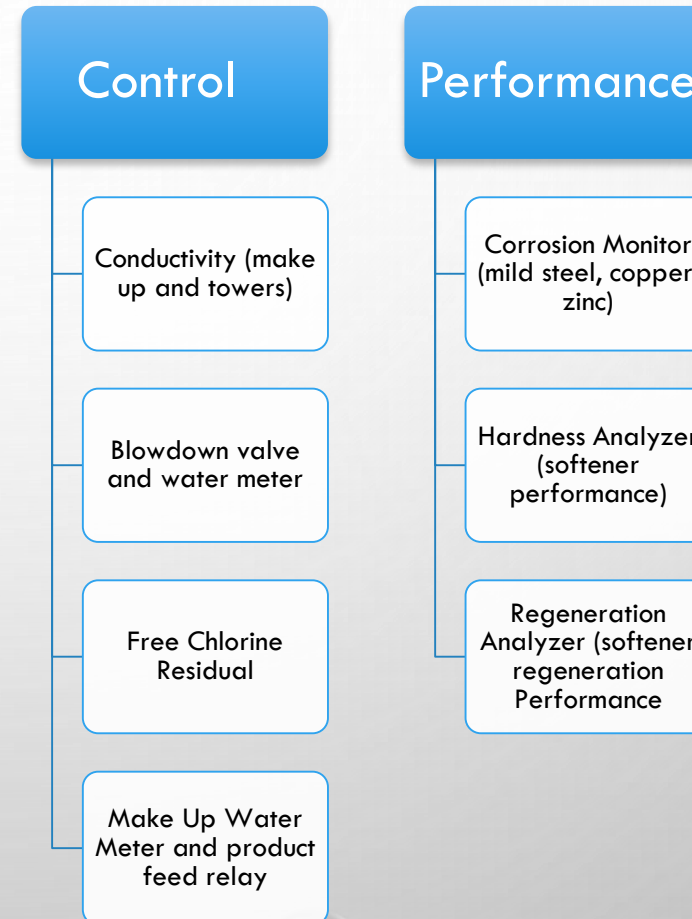
- THE BASIC EQUATION FOR SCALE FORMATION IS
 - $\text{Ca}^{+2} + \text{CO}_3^{2-} \rightarrow \text{CaCO}_3$
 - REMOVING THE CALCIUM (BY EXCHANGING FOR SODIUM) REMOVES ABILITY TO FORM SCALE
 - FOR OUR APPLICATION A WATER SOFTENER SYSTEM WAS MOST ECONOMICAL
 - SIZING
 - PLANT MAKE UP RATE MAXIMUM IS 650 GPM
 - THREE TANKS CAN HANDLE THIS FLOW WHILE THE FOURTH ONE REGENERATES
 - ~ 60 CUBIC FEET OF RESIN PER VESSEL. EACH VESSEL CAN FLOW AT A MAXIMUM OF 250 GPM
 - SALT USAGE
 - PLANT 2 USES APPROXIMATELY 300 TONS OF SALT PER YEAR WHILE PLANT 1 AND 3 USE 120 TONS PER YEAR.
 - COST OF SALT IS \$200/TON
 - BULK DELIVERY IS \$140/TON BUT REQUIRES BRINE SILOS WHICH ARE DIFFICULT TO HIDE IN DOWNTOWN PHOENIX





MONITORING AND CONTROL

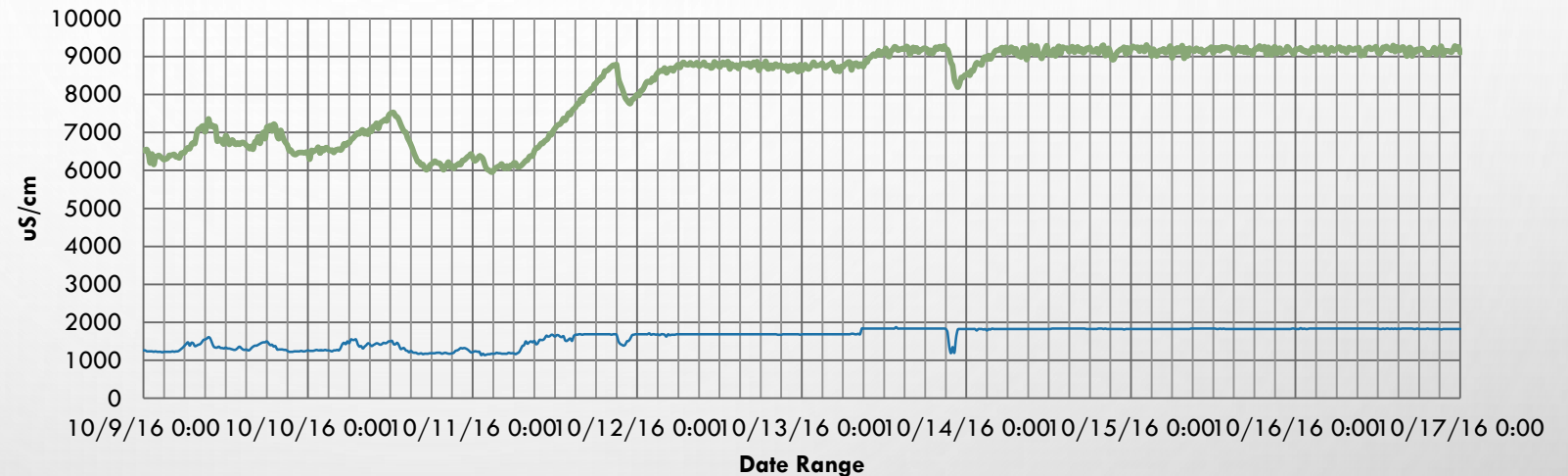
- IT IS COMMON TO UTILIZE A SINGLE CONTROLLER TO CONTROL WATER TREATMENT CHEMISTRY HOWEVER IT WAS CRITICAL TO HAVE THE DATA, ALARMS AND CONTROLS IN ONE PLACE FOR THE OPERATORS.
- THESE CONTROLLERS DID NOT FIT OUR NEEDS IN TERMS OF NUMBER OF INPUTS/OUTPUTS AND ABILITY FOR OPERATORS TO EASILY CONTROL



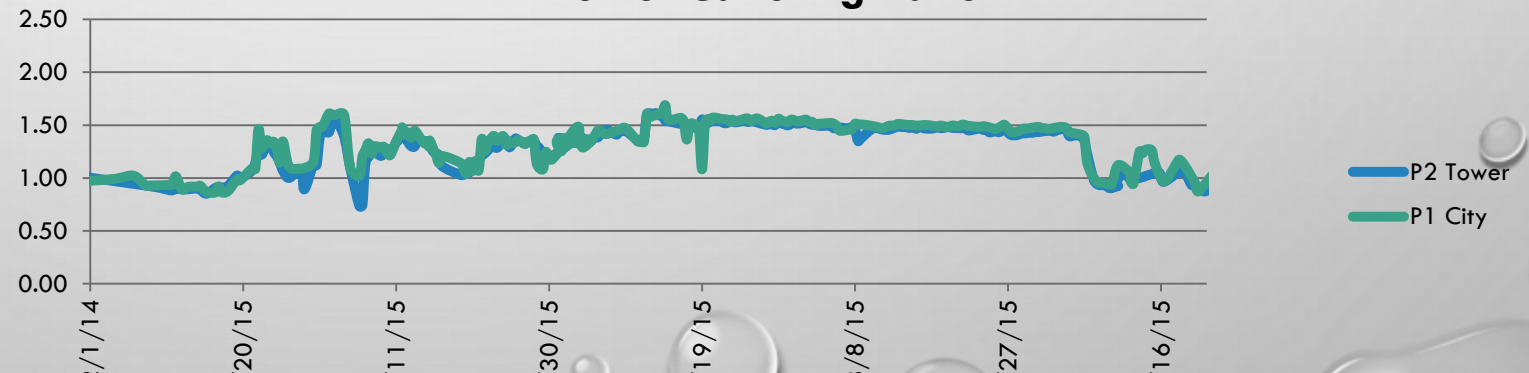
MONITORING AND CONTROL PROCESS – DID WE CORRECT SCALE FORMATION?

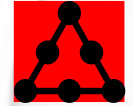
- CONTROL TOWER CONDUCTIVITY BASED ON A MULTIPLIER OF INCOMING WATER CONDUCTIVITY
 - ACCOUNTS AND CORRECTS FOR CHANGES IN INCOMING WATER CONDUCTIVITY AND PREVENTS LONG TERM OVER AND UNDER-CYCLING

Plant 2 Make up versus Tower Conductivity - 8 Days



P2 Tower Ca to Mg Ratio





OPERATOR SCREEN

Tower Make up
Section –insures
they don't use
too little water
per cell

Tower Blowdown
Section –note we
have both valve
position and
blowdown flow. If
valve is supposed
to be open and
there is no flow
then valve issue

Plant 2 Chemical System Control

Tower Make-Up Summary

	Value	Setpoint
Tower Basin Level	7.2 in.wc	6.8 in.wc
Tower MakeUp Flow	91.4 GPM	600 GPM
Towers Req. Make-up Flow/Tower	8	75 GPM
Total Tower Make-Up	This Month: 3132.8 kgal Last Month: 7999.8 kgal	
Tower MakeUp Valve Man Control	Auto	Off
Tower Make-Up Valve	Command: 11.7 % PID Calc: 11.8 %	Position: 10.6 %
Tower MakeUp Conductivity	912 uS/cm	
Tower Fill Valve Min. Flow Setpt	120.0 GPM	

Chemical Control Summary

	Value	On Stpt	Off Stpt
MIOX Injection Solenoid	On	0.65 ppm	0.70 ppm
Belcor 585 Pump (1)	S/S	Time Stpt	Gal Stpt
PBTC Pump (2)	On	12 Sec	500 Gal
Azole 50% Pump (3)	On	25 Sec	500 Gal
Tetra 60% Pump (4)	On	20 Sec	500 Gal

Tower Blow Down Summary

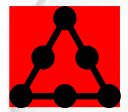
	Value	Setpoint
Tower Blowdown Flow	0.0 GPM	
Total Tower Blow-Down	This Month: 312.7 kgal Last Month: 709.1 kgal	
CDW Conductivity	6447 uS/cm	6474 uS/cm
CDW Conductivity Setpt Settings	Multi: 7.0 Deadband: 50 uS/cm	
Tower Blow-Down Valve Man Cntrl	Auto	Off
Tower Blow-Down Valve	Command: Off	Position: Closed

Alarm Control Summary

Alarm Description	Value	Lo Alarm	Hi Alarm
CDW Free Chlorine	0.613	0.30 ppm	1.20 ppm
CDW Corrosion Imb	0.025 mpy		21.0 mpy
CDW Corrosion	0.050 mpy		21.0 mpy
DCHW Corrosion Imb	0.000 mpy		21.0 mpy
DCHW Corrosion	0.000 mpy		21.0 mpy
DCHW pH Level	8.588 pH	7.5 pH	9.5 pH
DCHW Glycol Level	0.2 ppb		100.0 ppb
Mazzei Injector DP	14.8 PSI	5.0 PSI	
Floor Water Detection	Off		Alarm Reset
DCHW Circ Pump	On	Iso Valves	On
P2 MBOX CWS Temp	77.5 °F	45.0 °F	85.0 °F
Hardness Analyzer	Off		Soft Water

Chemical Control
- based on make
up flow rates or
free chlorine
analyzer

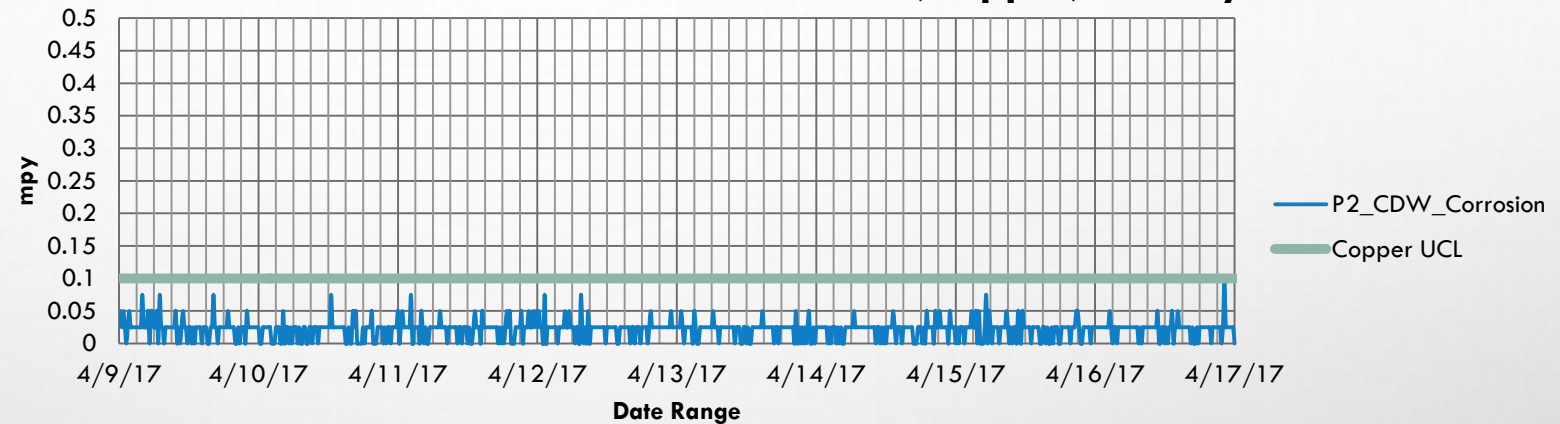
System alarms
and performance
alarms



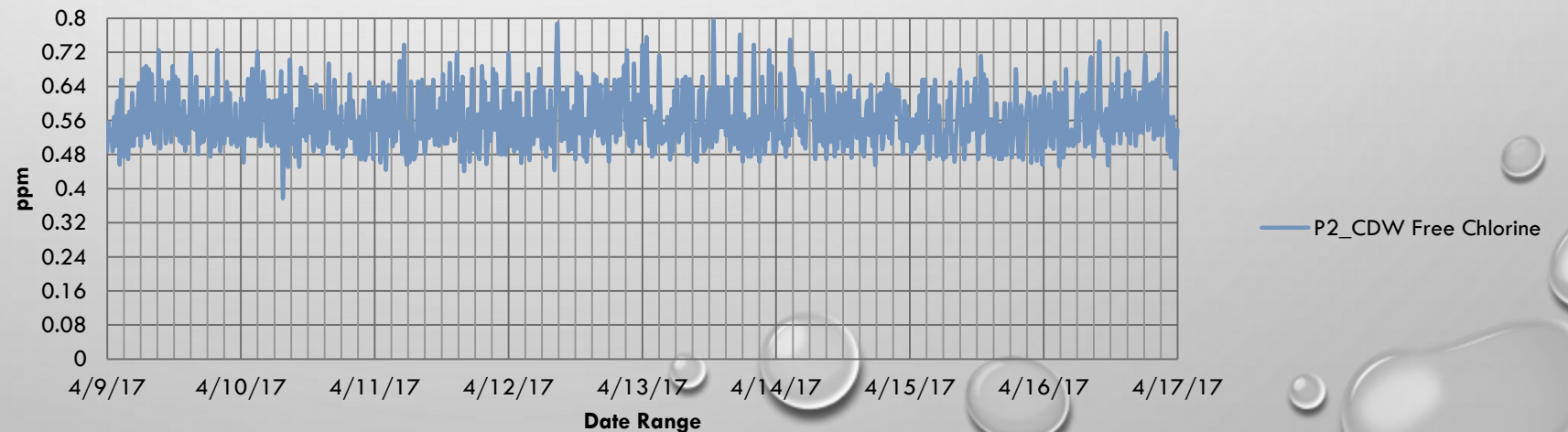
- THIS ALLOWS
US TO
MONITOR
PERFORMANCE
AND FOR
MANAGEMENT
REVIEW

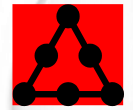
OUTPUT AND TRENDING

Plant 2 General Corrosion Rate (Copper) - 8 Days



Plant 2 Free Chlorine Level - 8 Days

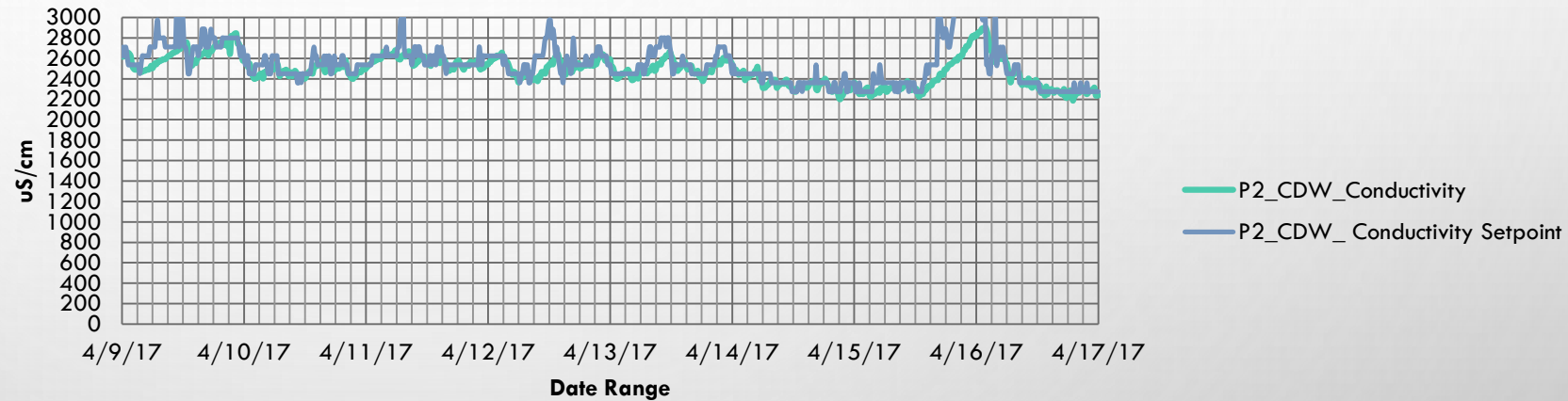


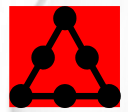


OUTPUT AND TRENDING

- IN ADDITION WE GET INFORMATION ON NUMBER OF REGENERATIONS AND REGENERANT USAGE
- OTHER DIAGNOSTIC FEATURES ARE INCLUDED

Plant 2 Tower Conductivity versus Set Point - 8 Days





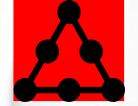
SUSTAINABILITY

- IMPLEMENTATION OF THIS PROGRAM RESULTED IN THE FOLLOWING
 - 3,500 TO 8,500 LBS OF BIOCIDES NOT DELIVERED
 - 3,500 LBS OF SCALE AND CORROSION INHIBITOR (ALL WATER) NOT BEING DELIVERED
 - 37.5 MILLION GALLONS OF WATER SAVED PER YEAR



ECONOMICS

- THE PAYBACK FOR THE PROJECT AVERAGED OVER ALL THREE PLANTS (SOFTENERS, MIOX, CONTROLS) IS BETWEEN 2.5 TO 3.0 YEARS AND INCLUDES:
 - CHEMICAL SAVINGS
 - WATER SAVINGS
 - REDUCED MAINTENANCE COSTS (THIRD PARTY TOWER CLEANING)



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PLANT PERSPECTIVE/QUESTIONS