



# IDEA2021

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# ENVIRONMENTAL FOOTPRINT BENEFITS FROM BOILER WATER TREATMENT IMPROVEMENTS

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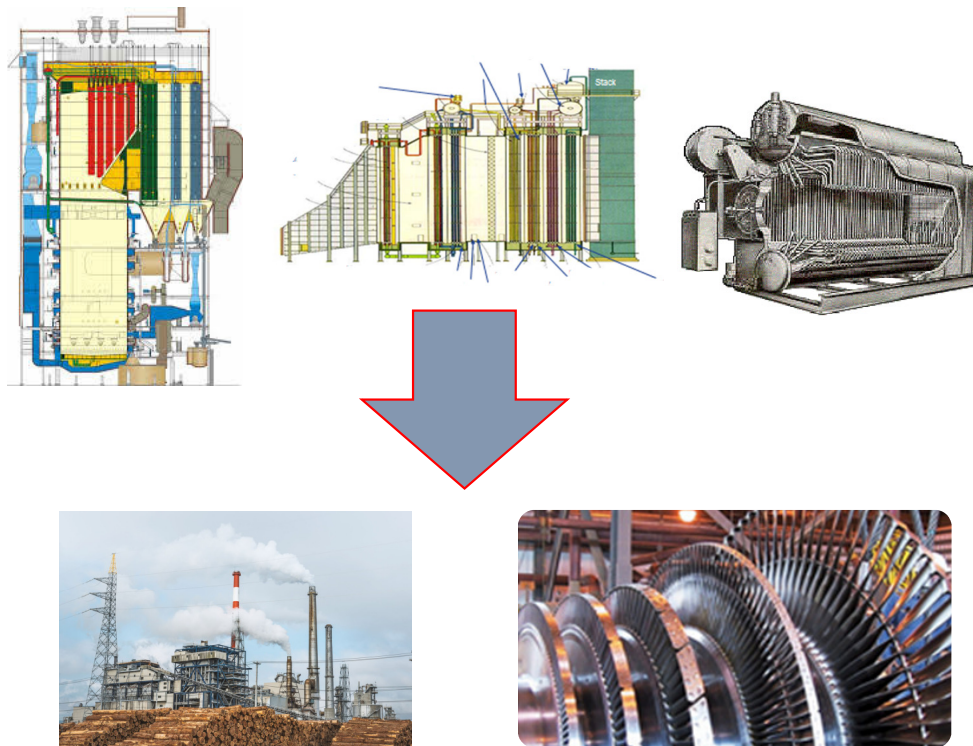
# AGENDA

- Purpose of boiler water treatment
- Plains Midstream Gas Plant Case Study
  - Overview of boiler system and design limitations
  - Environmental footprint boiler impact
  - Environmental and Economic benefits of boiler treatment optimization



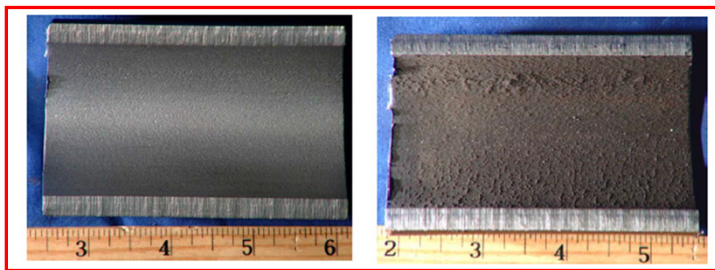
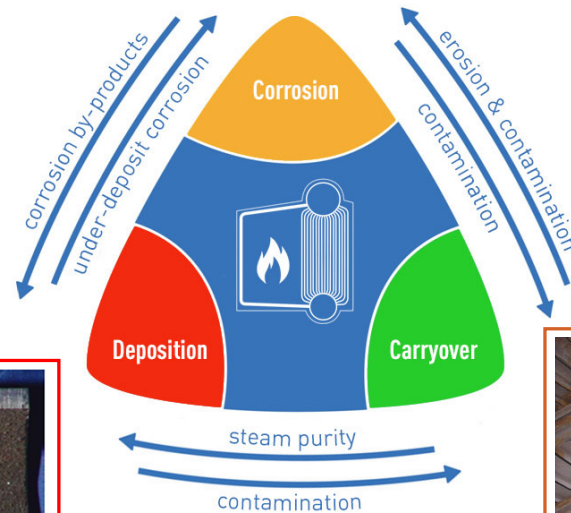
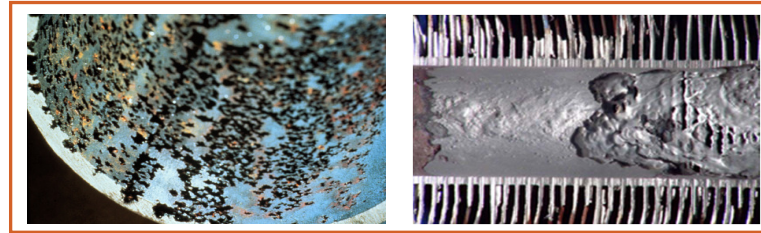
# Purpose of boiler water treatment

- Steam generation to support production/operation



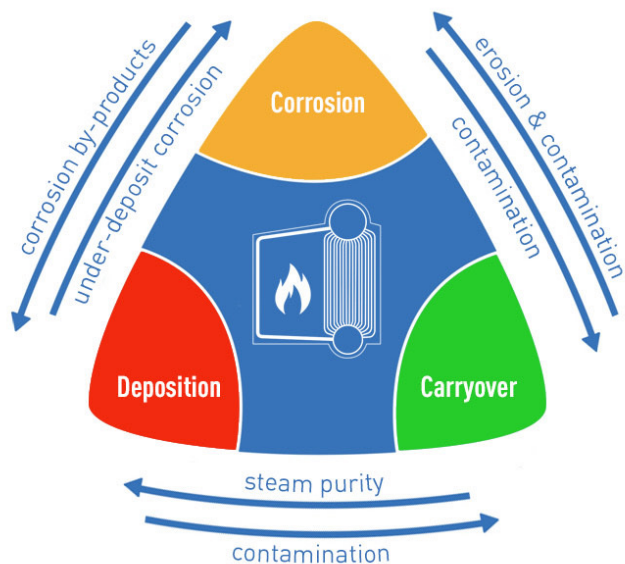
# Purpose of boiler water treatment

- Asset protection:
  - Reliability



# Purpose of boiler water treatment

## INFRASTRUCTURE PROTECTION



## INDUSTRY GUIDELINES

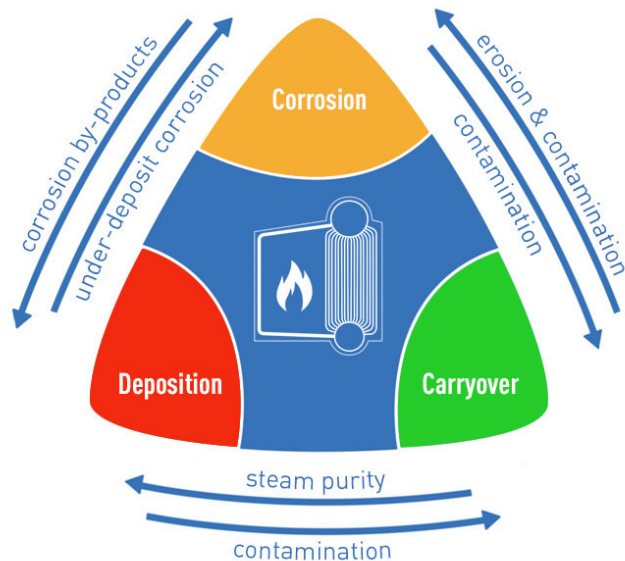
**TABLE 1**  
SUGGESTED WATER CHEMISTRY LIMITS  
INDUSTRIAL WATERTUBE, HIGH DUTY,  
PRIMARY FUEL FIRED, DRUM TYPE

Makeup water percentage: Up to 100% of feedwater  
Conditions: Includes superheater, turbine drives, or process restriction on steam purity  
Saturated steam purity target: See tabulated values below.

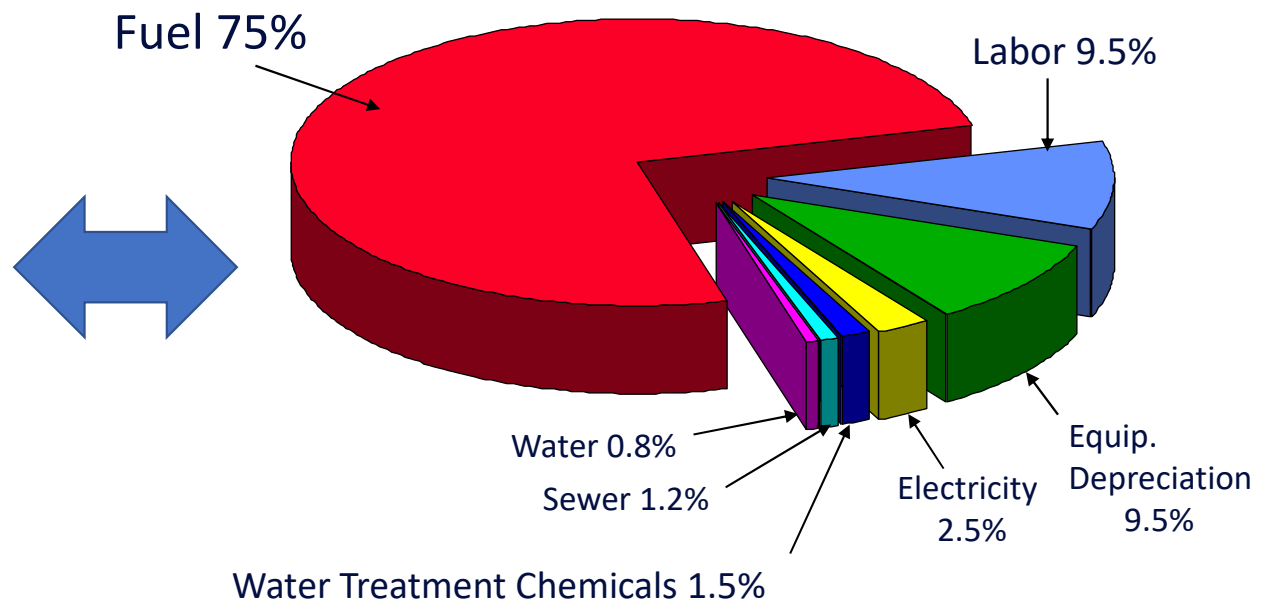
Drum Operating Pressure (1)(11)	psig 0-300 (MPa) (0-2.07)	301-450 (2.08-3.10)	451-600 (3.11-4.14)
<b>Feedwater(7)</b>			
Dissolved oxygen ppm (mg/l) $O_2$ -measured before chemical oxygen scavenger addition (8)	<0.007	<0.007	<0.007
Total iron ppm (mg/l) Fe	≤0.1	≤0.05	≤0.03
Total copper ppm (mg/l) Cu	≤0.05	≤0.025	≤0.02
Total Hardness ppm	≤0.3	≤0.3	≤0.2
pH @ 25°C	8.3-10.0	8.3-10.0	8.3-10.0
Chemicals for preboiler system protection	NS	NS	NS
Nonvolatile TOC ppm (mg/l) C (6)	<1	<1	<0.5
Oily matter ppm (mg/l)	<1	<1	<0.5
<b>Boiler Water</b>			
silica ppm (mg/l) $SiO_2$	≤150	≤90	≤40
Total alkalinity ppm (mg/l)*	<700(3)	<600(3)	<500(3)
Free OH alkalinity ppm (mg/l)* (2)	NS	NS	NS
Specific conductance (12) $\mu mhos/cm$ ( $\mu S/cm$ ) 25°C without neutralization	5400-1100(5)	4600-900(5)	3800-800(5)
<b>Total Dissolved Solids in Steam (9)</b>			
TDS (maximum) ppm (mg/l)	1.0-0.2	1.0-0.2	1.0-0.2

# Purpose of boiler water treatment

## INFRASTRUCTURE PROTECTION



## COST OF OPERATION & ENVIRONMENTAL FOOTPRINT



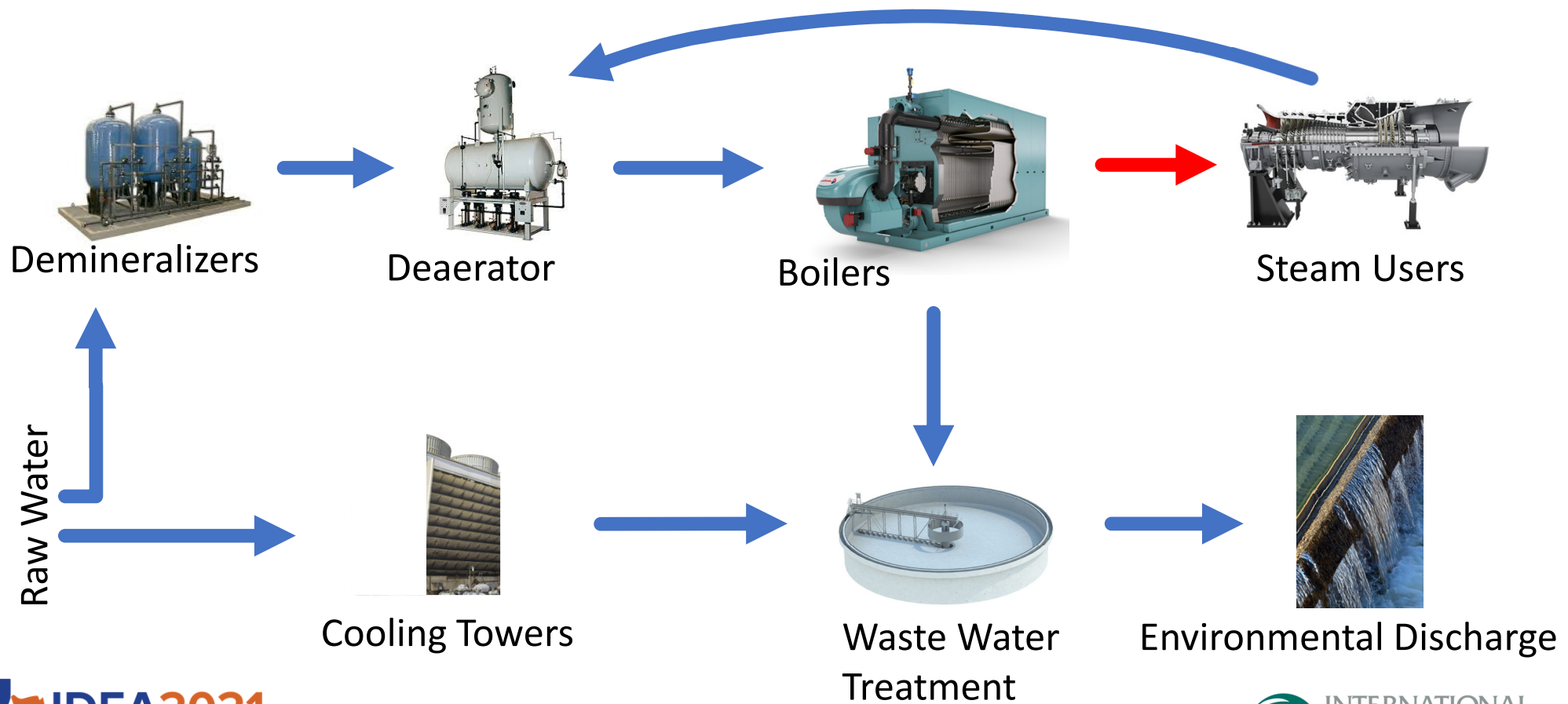
# Plains Midstream Case Study

## Empress, AB



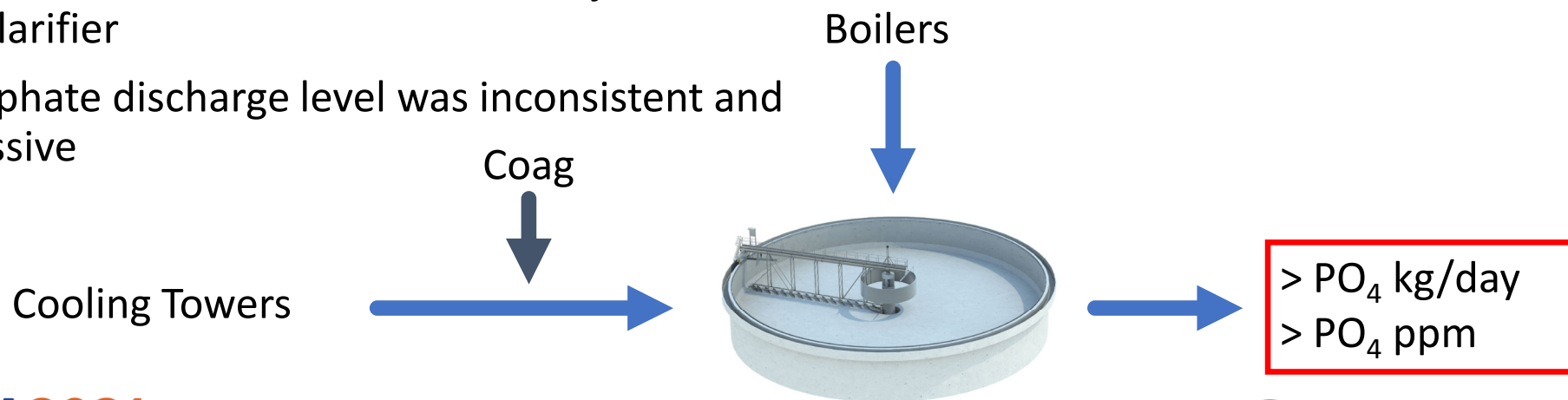


# Overview of Plains Midstream boiler system



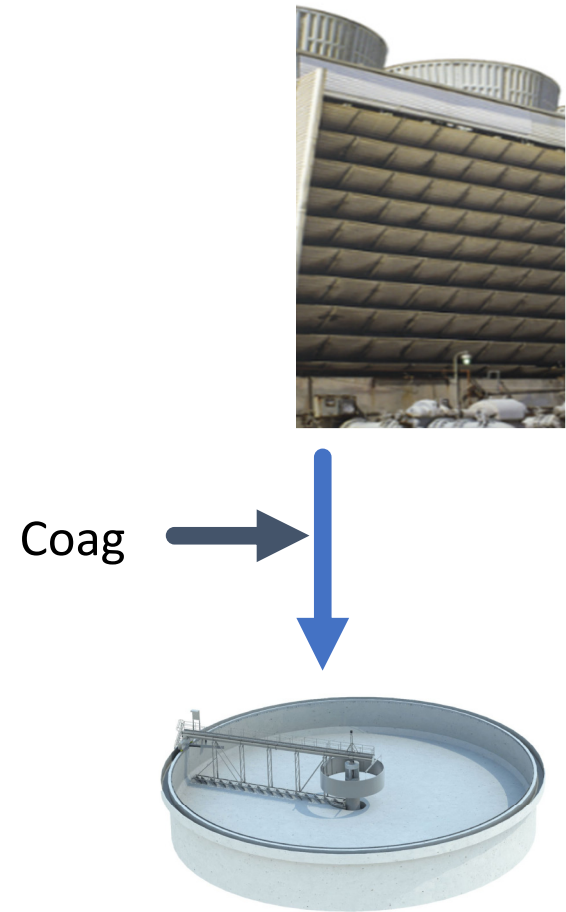
# Waste Water Treatment

- Waste Water from Cooling Tower and Boiler blowdowns
- Limited treatment space and reaction time
- Coagulant injected to the Cooling Tower blowdown
- Boiler blowdown is untreated until injection to the clarifier
- Phosphate discharge level was inconsistent and excessive



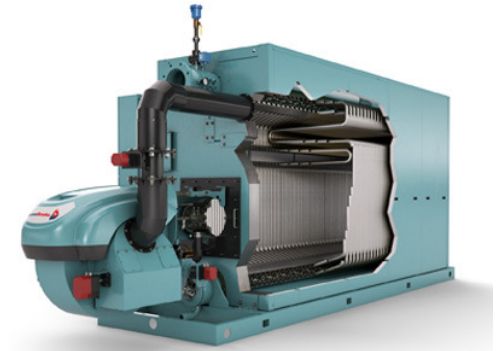
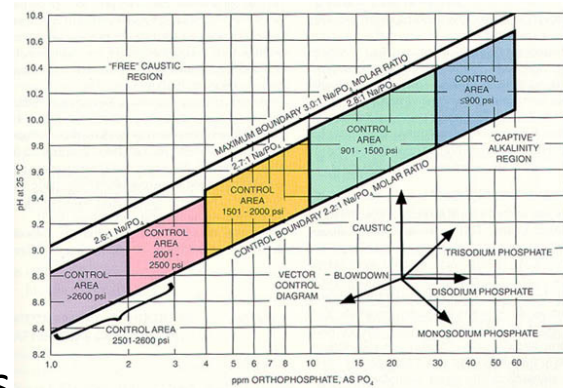
# Cooling Towers

- Phosphate is a common corrosion inhibitor for open recirculating cooling systems
- Levels of 5-15 ppm  $\text{PO}_4$  are typical depending on pH and hardness levels
- Non-phosphate Cooling Tower chemistries have been newly introduced by SUEZ and others to address phosphate discharge regulations, but was not available at that time.
- Coagulant treatment was optimized for Cooling Tower phosphate removal, so it was not the main source of phosphate “leakage”.



# Boiler Treatment

- 1 MMkg/day of steam @ 400 psig
- 15-25 ppm  $\text{PO}_4$  in the boiler water
- Coordinated pH/ $\text{PO}_4$  treatment was applied due to demineralized feedwater
- Below 900 psig, Coordinated pH/ $\text{PO}_4$  is not warranted due to lower localized heat flux. Phosphate then neither acts as a pH stabilizer nor a precipitation aid
- Conversion to patented all-polymer terpolymer solubilizing technology
- From daily batch making and manual blowdown to automated neat chemical treatment



from



Phosphate  
batch

to



Neat  
Terpolymer



# Boiler Treatment

- Erratic treatment and blowdown made for an average of 43 Cycles of Concentration
- Operational Boiler Water Chemistry guidelines on demineralized water would easily allow 65-75 Cycles



## The impact of increased Cycles of Concentration:

1)  $\% \text{Blowdown} = 1 / \text{CoC}$

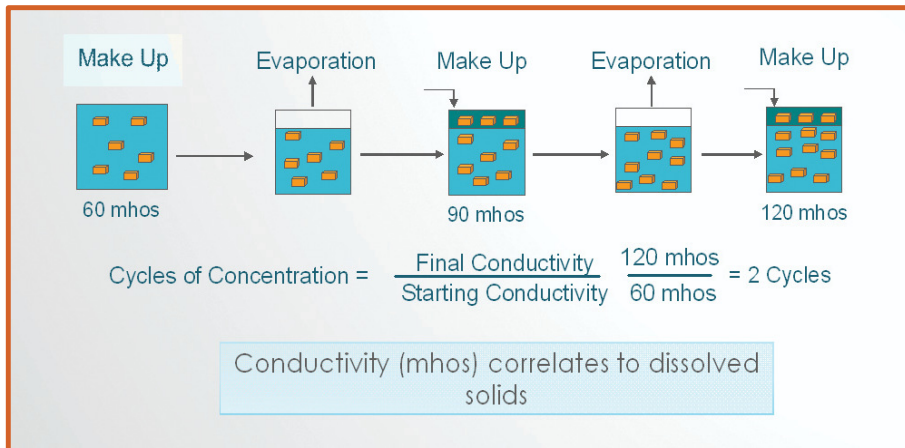
$$= 1 / 43 = 2.3\% \text{ BD}$$

$$= 1 / 75 = 1.3\% \text{ BD}$$

↓ 45%

2)  $\text{Blowdown} = \text{BFW} - \text{Steam}$

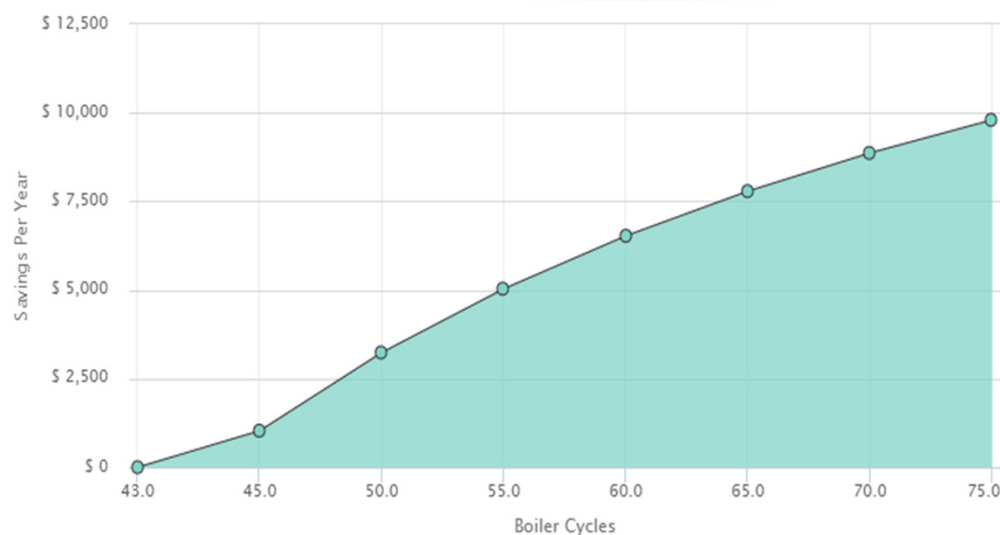
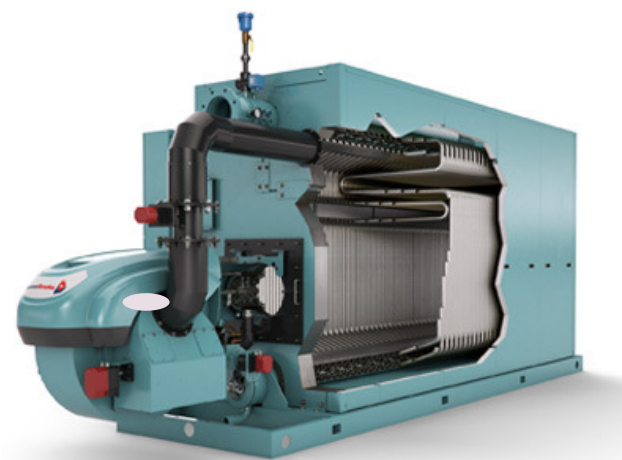
3)  $E_{\text{STEAM}} = E_{\text{MU}} + E_{\text{COND}} + E_{\text{BW}}$



# Boiler Treatment

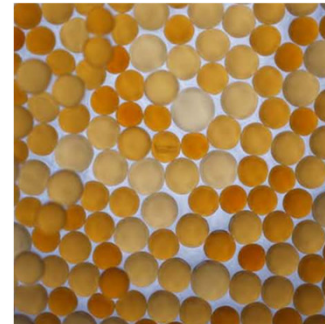
- Improvements in chemical treatment, dosage, monitoring and control, as well as application of operational best practices (blowdown control) generated:

- Chemical savings  
= \$18,980/year
- Fuel savings  
= \$10,000/yr
- Reduction in fresh water  
↓ 1,000,000 USG/year
- CO<sub>2</sub> emission reduction  
↓ 200 Ton CO<sub>2</sub>/year



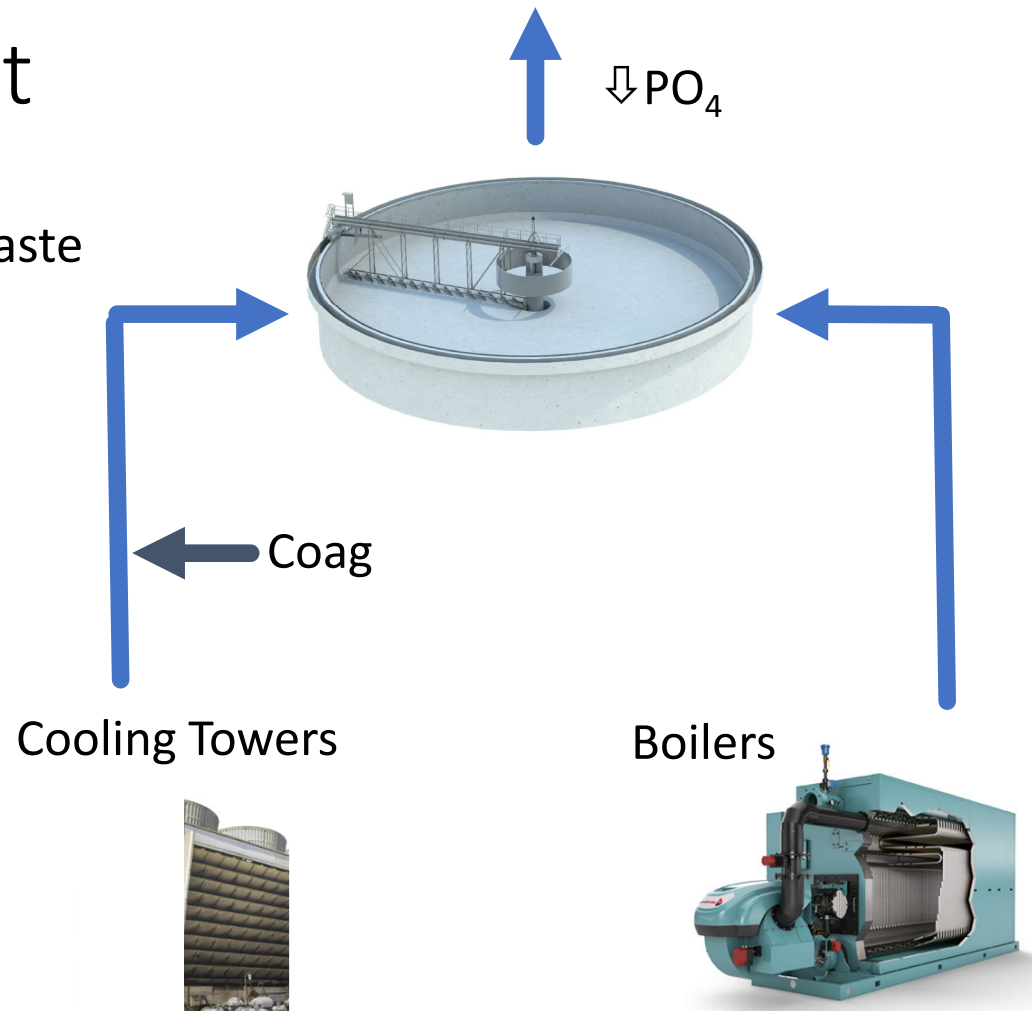
# Boiler Pretreatment

- Reductions in fresh water demineralization requirement reduced regenerations frequency on the cation and anion, which translated to:
  - 52 fewer regenerations per year
  - Acid and caustic regenerant savings = \$11,250/yr
  - Reduction in regeneration water  
↓ 100,000 USG/year



# Waste Water Treatment

- Elimination of phosphate-based boiler treatment resulted in reduced load to waste water:
- **Phosphate discharged**
  - ↓ 200 kg/yr
  - ↓ 1 ppm as  $\text{PO}_4$
- **Savings in coagulant**
  - = \$11,900/year
- Eliminated the need for waste water system redesign
- Eliminated the risk of discharge limit violation





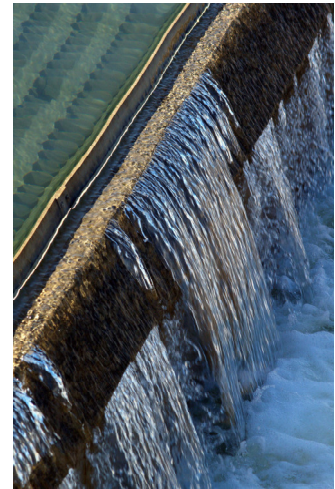
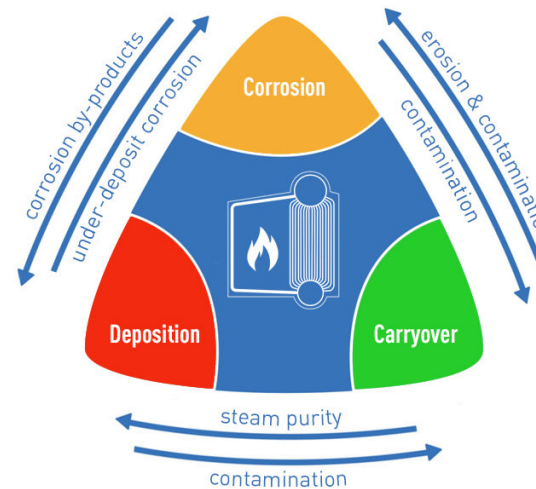
# Conclusions – Environmental and Economic Benefits

- A project to overhaul the boiler treatment to remove stress on the waste water system provided multiple environmental footprint benefits:

While providing a safer, more efficient and more reliable operation, at a lower cost:

- Phosphate discharged  
↓ 200 kg/yr  
↓ 1 ppm as  $\text{PO}_4$
- Fresh water usage  
↓ 1,1 MMUSG/yr
- $\text{CO}_2$  emission reduction  
↓ 200 ton  $\text{CO}_2$ /yr

- **OPERATIONAL SAVINGS**  
**\$51,850/YEAR**



# Thank You!



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SUEZ Water Technologies & Solutions**



# Q&A

