



IDEA 2021

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ENVIRONMENTAL FOOTPRINT BENEFITS FROM BOILER WATER TREATMENT IMPROVEMENTS

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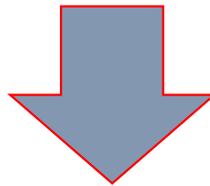
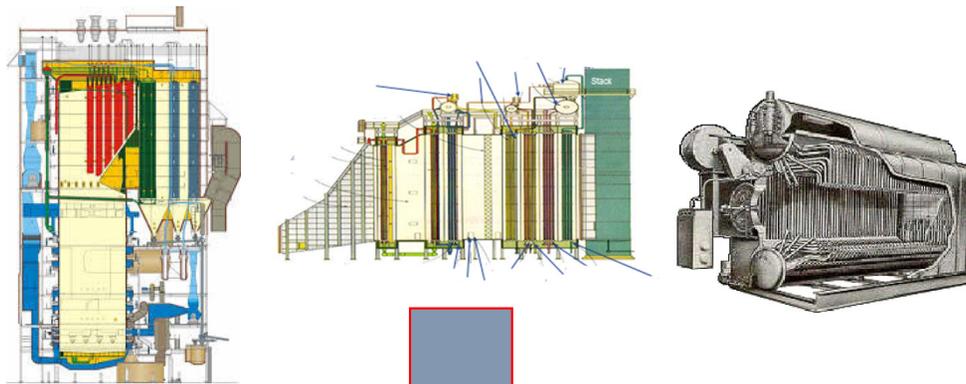


AGENDA

- Purpose of boiler water treatment
- Plains Midstream Gas Plant Case Study
 - Overview of boiler system and design limitations
 - Environmental footprint boiler impact
 - Environmental and Economic benefits of boiler treatment optimization

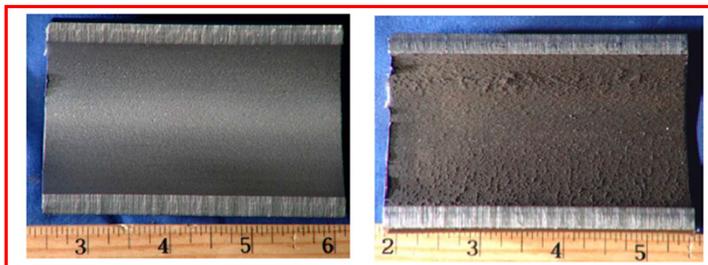
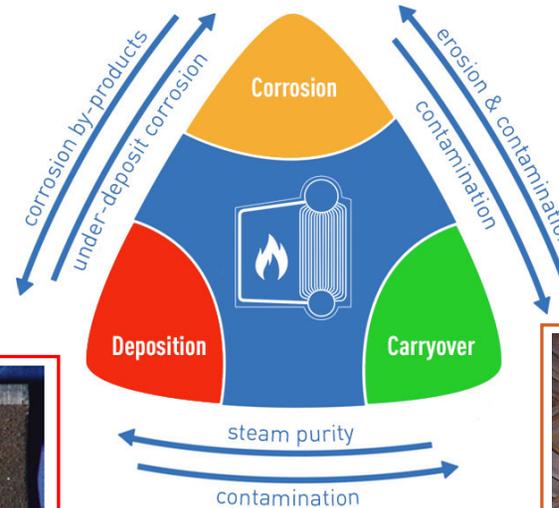
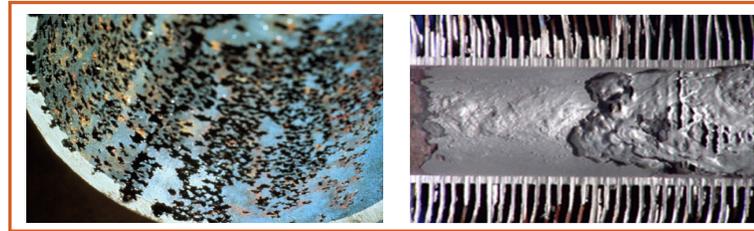
Purpose of boiler water treatment

- Steam generation to support production/operation



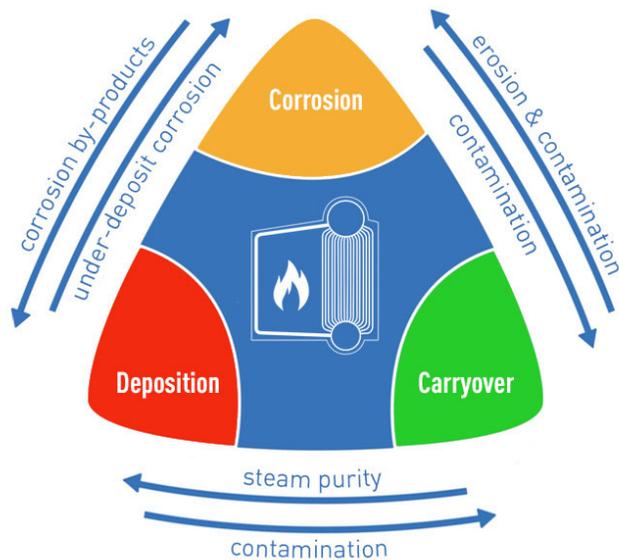
Purpose of boiler water treatment

- Asset protection:
 - Reliability



Purpose of boiler water treatment

INFRASTRUCTURE PROTECTION



INDUSTRY GUIDELINES

SUGGESTED WATER CHEMISTRY LIMITS
INDUSTRIAL WATERTUBE, HIGH DUTY,
PRIMARY FUEL FIRED, DRUM TYPE

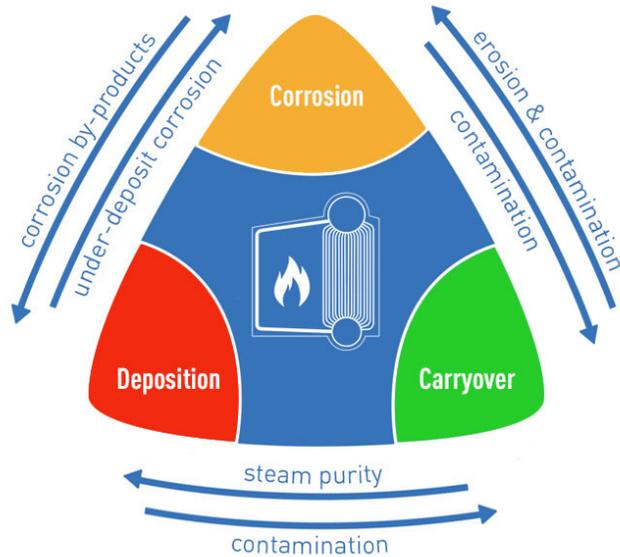
TABLE 1

Makeup water percentage: Up to 100% of feedwater
Conditions: Includes superheater, turbine drives, or process restriction on steam purity
Saturated steam purity target: See tabulated values below.

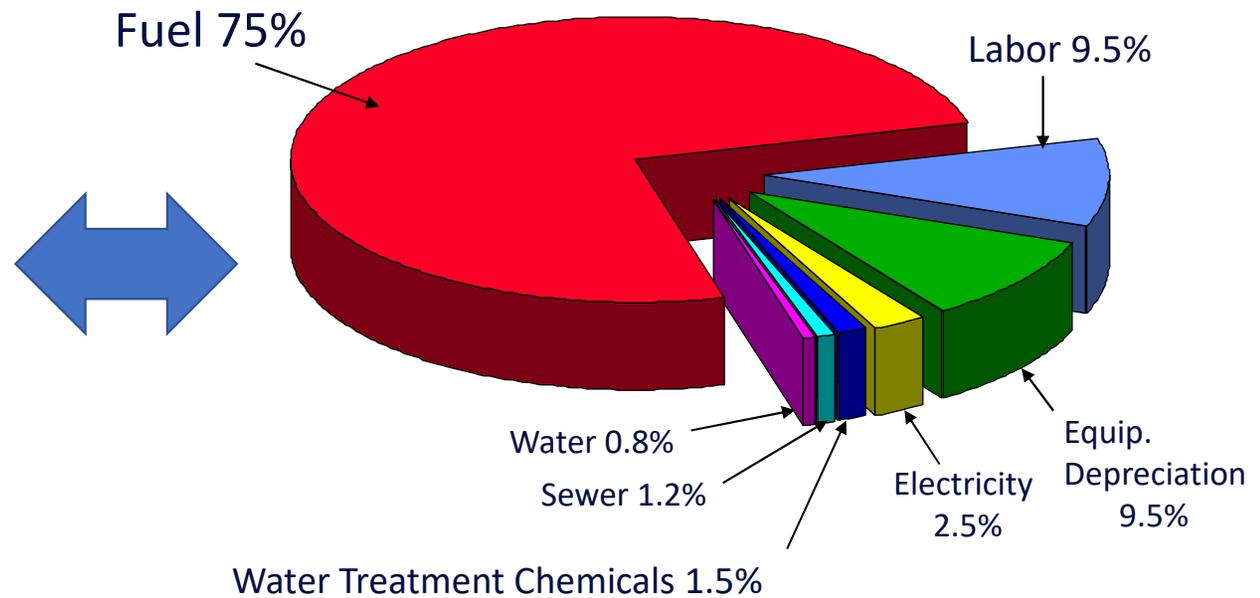
Drum Operating Pressure (1)(11)	psig 0-300 (MPa) (0-2.07)	301-450 (2.08-3.10)	451-600 (3.11-4.14)
Feedwater(7)			
Dissolved oxygen ppm (mg/l) O ₂ -measured before chemical oxygen scavenger addition (8)	<0.007	<0.007	<0.007
Total iron ppm (mg/l) Fe	≤0.1	≤0.05	≤0.03
Total copper ppm (mg/l) Cu	≤0.05	≤0.025	≤0.02
Total Hardness ppm	≤0.3	≤0.3	≤0.2
pH @ 25°C	8.3-10.0	8.3-10.0	8.3-10.0
Chemicals for preboiler system protection	NS	NS	NS
Nonvolatile TOC ppm (mg/l) C (6)	<1	<1	<0.5
Oily matter ppm (mg/l)	<1	<1	<0.5
Boiler Water			
silica ppm (mg/l) SiO ₂	≤150	≤90	≤40
Total alkalinity ppm (mg/l)*	<700(3)	<600(3)	<500(3)
Free OH alkalinity ppm (mg/l)* (2)	NS	NS	NS
Specific conductance (12) μmhos/cm (μS/cm) 25°C without neutralization	5400-1100(5)	4600-900(5)	3800-800(5)
Total Dissolved Solids in Steam (9)			
TDS (maximum) ppm (mg/l)	1.0-0.2	1.0-0.2	1.0-0.2

Purpose of boiler water treatment

INFRASTRUCTURE PROTECTION



COST OF OPERATION & ENVIRONMENTAL FOOTPRINT

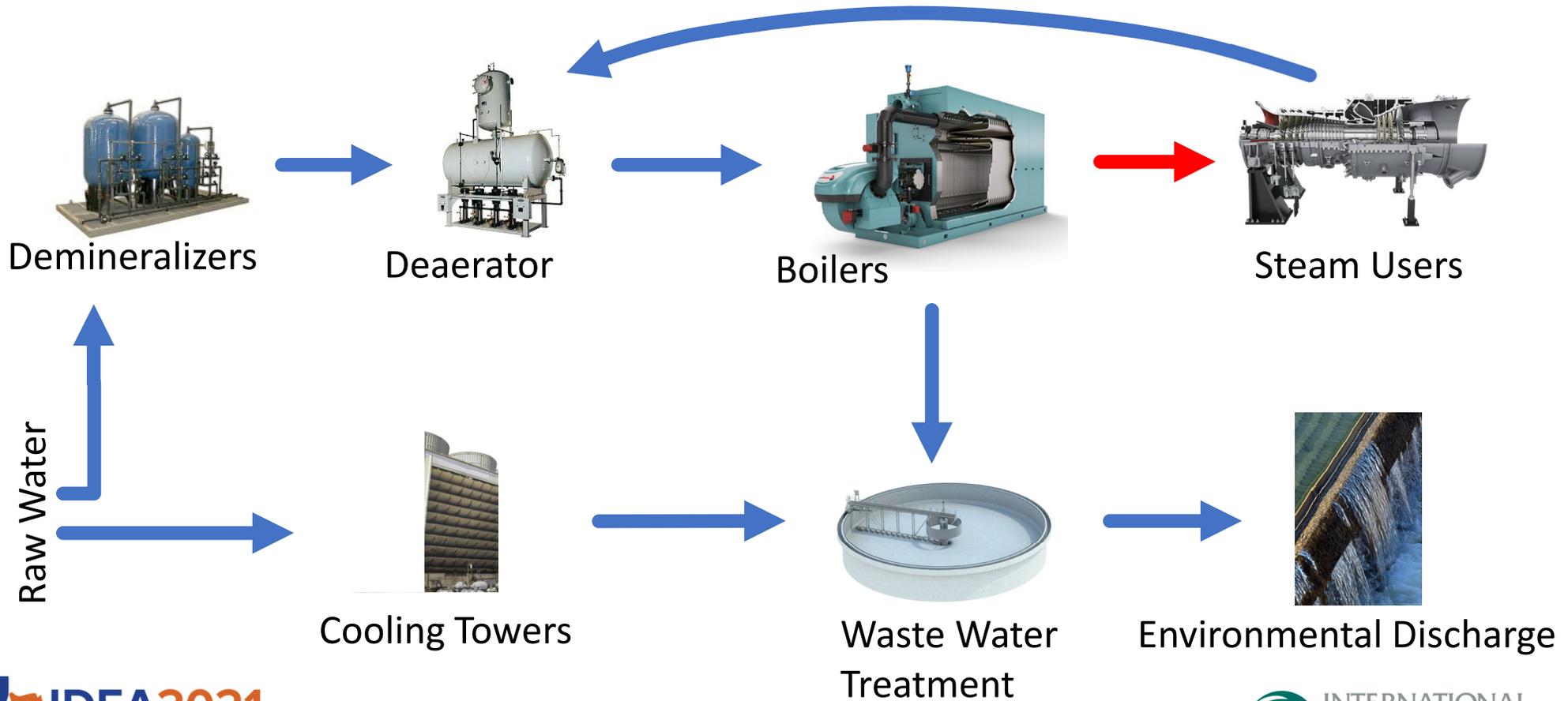


Plains Midstream Case Study

Empress, AB

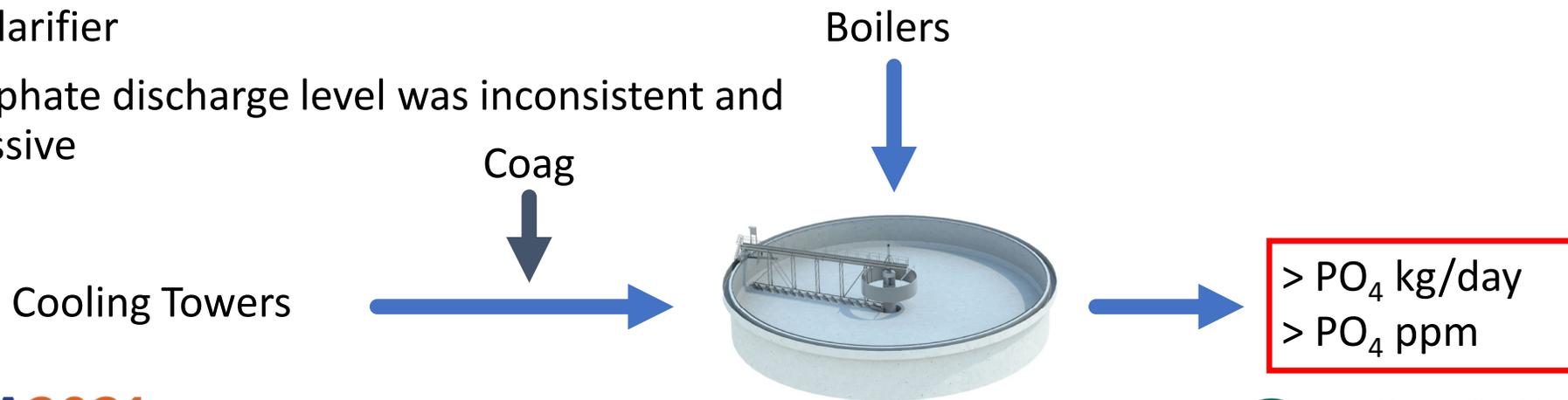


Overview of Plains Midstream boiler system



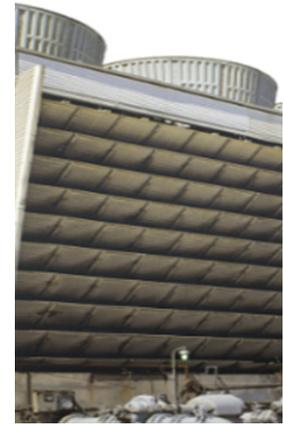
Waste Water Treatment

- Waste Water from Cooling Tower and Boiler blowdowns
- Limited treatment space and reaction time
- Coagulant injected to the Cooling Tower blowdown
- Boiler blowdown is untreated until injection to the clarifier
- Phosphate discharge level was inconsistent and excessive

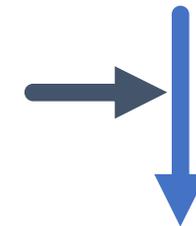


Cooling Towers

- Phosphate is a common corrosion inhibitor for open recirculating cooling systems
- Levels of 5-15 ppm PO_4 are typical depending on pH and hardness levels
- Non-phosphate Cooling Tower chemistries have been newly introduced by SUEZ and others to address phosphate discharge regulations, but was not available at that time.
- Coagulant treatment was optimized for Cooling Tower phosphate removal, so it was not the main source of phosphate “leakage”.

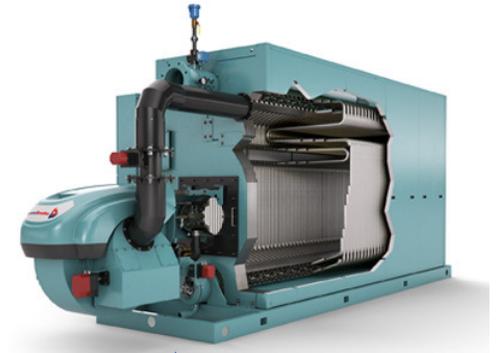
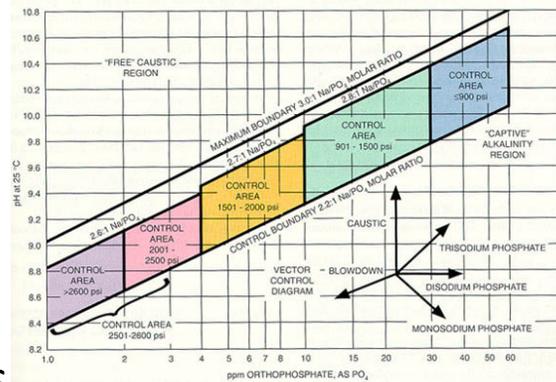


Coag



Boiler Treatment

- 1 MMkg/day of steam @ 400 psig
- 15-25 ppm PO_4 in the boiler water
- Coordinated pH/ PO_4 treatment was applied due to demineralized feedwater
- Below 900 psig, Coordinated pH/ PO_4 is not warranted due to lower localized heat flux. Phosphate then neither acts as a pH stabilizer nor a precipitation aid
- Conversion to patented all-polymer terpolymer solubilizing technology
- From daily batch making and manual blowdown to automated neat chemical treatment



from



Phosphate batch

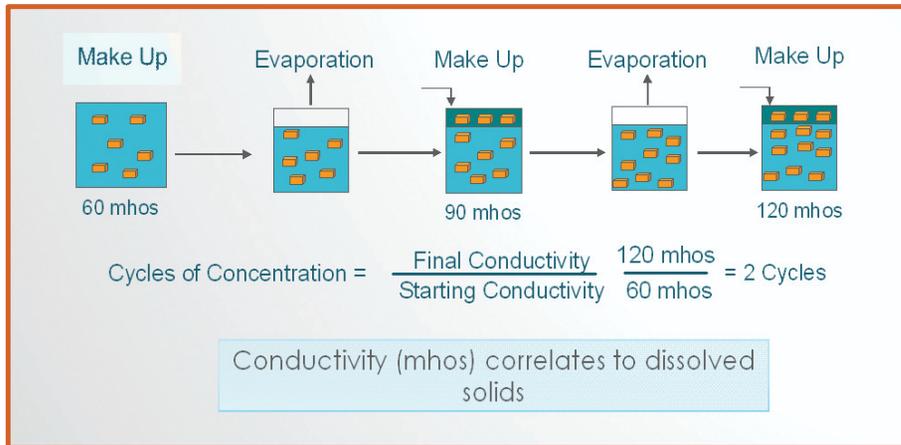
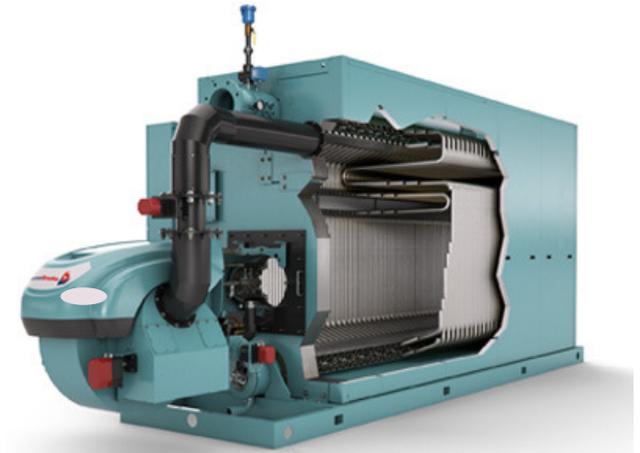
to



Neat Terpolymer

Boiler Treatment

- Erratic treatment and blowdown made for an average of 43 Cycles of Concentration
- Operational Boiler Water Chemistry guidelines on demineralized water would easily allow 65-75 Cycles



The impact of increased Cycles of Concentration:

1)
$$\% \text{Blowdown} = 1 / \text{CoC}$$

$= 1 / 43 = 2.3\% \text{ BD}$
 $= 1 / 75 = 1.3\% \text{ BD}$

↓ 45%

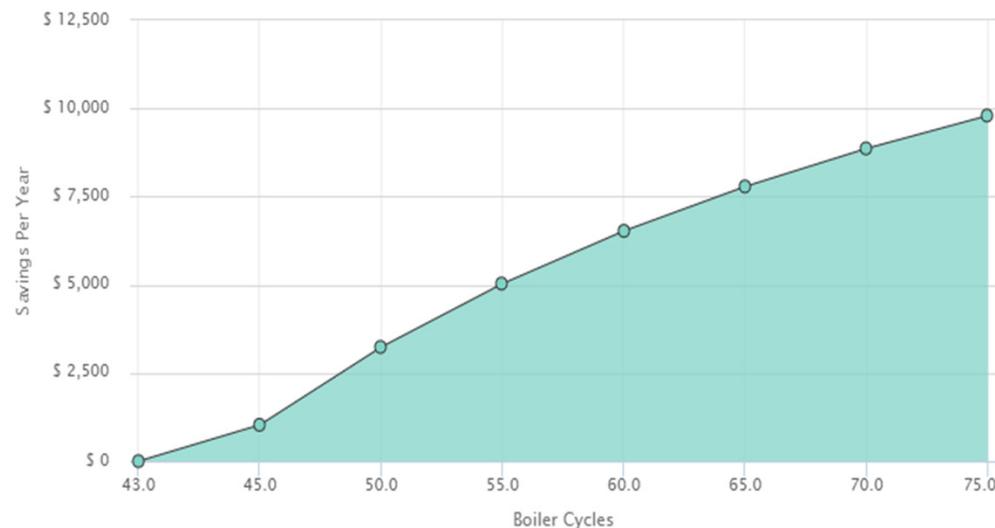
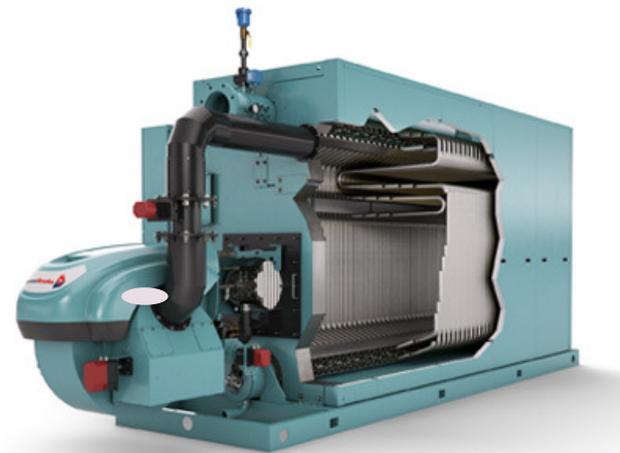
2)
$$\text{Blowdown} = \text{BFW} - \text{Steam}$$

3)
$$E_{\text{STEAM}} = E_{\text{MU}} + E_{\text{COND}} + E_{\text{BW}}$$

Boiler Treatment

- Improvements in chemical treatment, dosage, monitoring and control, as well as application of operational best practices (blowdown control) generated:

- **Chemical savings**
= \$18,980/year
- **Fuel savings**
= \$10,000/yr
- **Reduction in fresh water**
↓ 1,000,000 USG/year
- **CO₂ emission reduction**
↓ 200 Ton CO₂/year



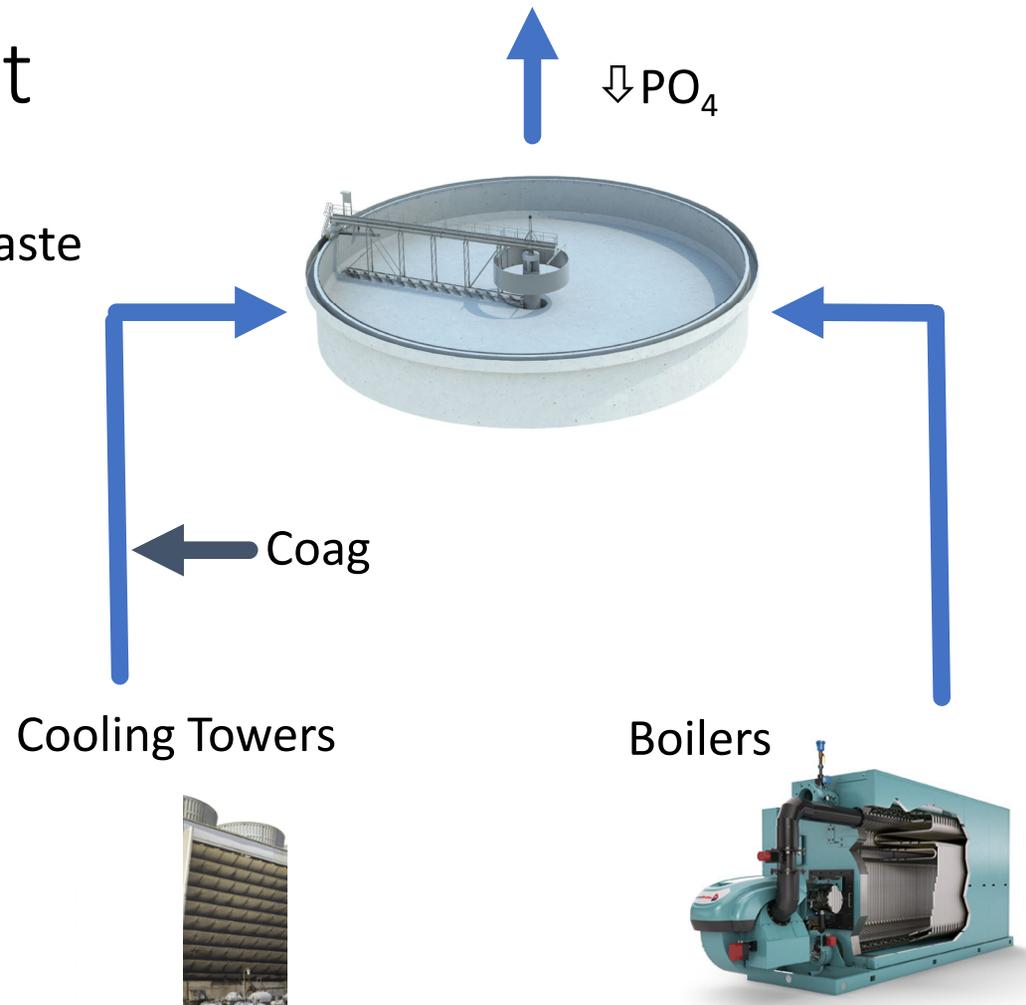
Boiler Pretreatment

- Reductions in fresh water demineralization requirement reduced regenerations frequency on the cation and anion, which translated to:
 - 52 fewer regenerations per year
 - Acid and caustic regenerant savings = \$11,250/yr
 - Reduction in regeneration water ↓ 100,000 USG/year



Waste Water Treatment

- Elimination of phosphate-based boiler treatment resulted in reduced load to waste water:
 - **Phosphate discharged**
 - ↓ 200 kg/yr
 - ↓ 1 ppm as PO_4
 - **Savings in coagulant**
= \$11,900/year
- Eliminated the need for waste water system redesign
- Eliminated the risk of discharge limit violation



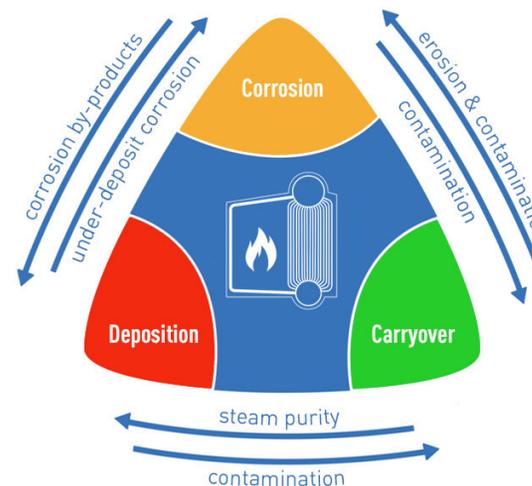
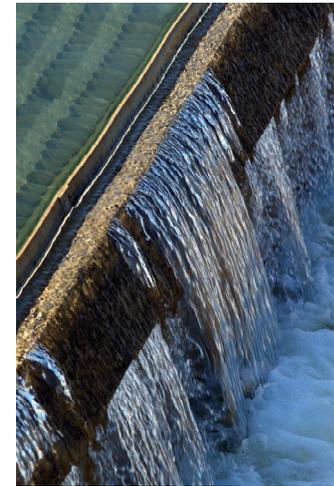
Conclusions – Environmental and Economic Benefits

- A project to overhaul the boiler treatment to remove stress on the waste water system provided multiple environmental footprint benefits:

- Phosphate discharged
 - ↓ 200 kg/yr
 - ↓ 1 ppm as PO₄
- Fresh water usage
 - ↓ 1,1 MMUSG/yr
- CO₂ emission reduction
 - ↓ 200 ton co₂/yr

While providing a safer, more efficient and more reliable operation, at a lower cost:

- **OPERATIONAL SAVINGS**
\$51,850/YEAR



Thank You!



**Gregoire Poirier Richer &
Stephanie Enslin
SUEZ Water Technologies & Solutions**



Q&A

