

# University of British Columbia (UBC) Case study: Use of Real-Time Hydraulic Modeling



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## BACKGROUND

This presentation is a **University of British Columbia case study** how UBC, based on **real-time distribution system hydraulic modeling**, gained **detailed control** of the operation, system optimization path, system expansion, system bottle necks, among others of their **hot water based district energy system**, to **monitor their CAD \$88 million investment**.

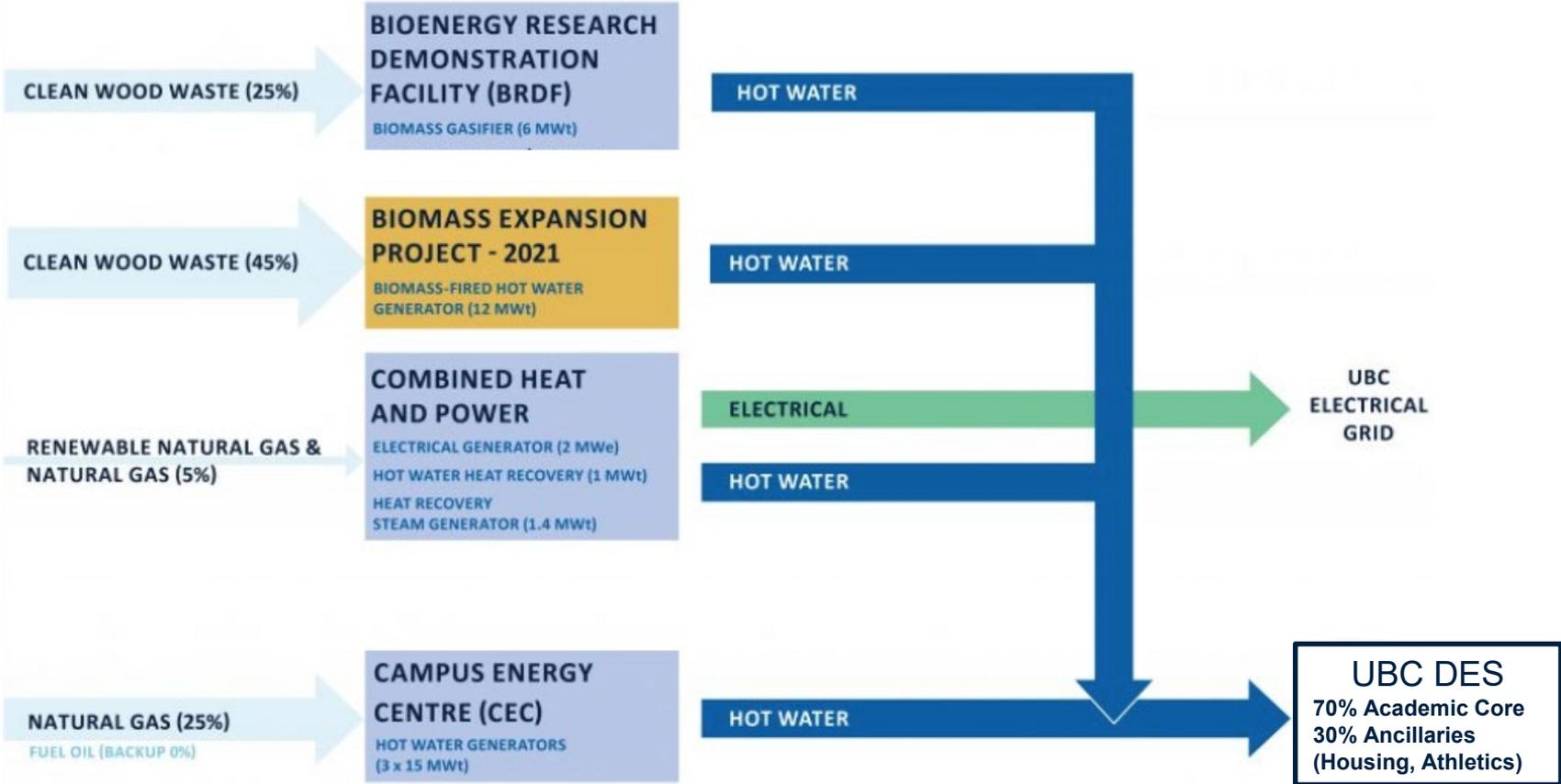
UBC transformed their district energy system to one of worlds leading medium temperature hot water system. Hydraulic modeling was a key component in this process and the real-time hydraulic modeling solution implemented in 2018 - in record time of just 3 months - has become **a strategic decision support tool**. Offline and Real-time hydraulic modeling is used for the day-to-day operational management, troubleshooting, engineering, planning for changes and additions of new buildings, distribution system piping and plant capacity.

The investment of the real-time hydraulic modeling solution has provided readily available information that has aided in decision making while avoiding professional fees, **paying itself back in less than 24 months**.

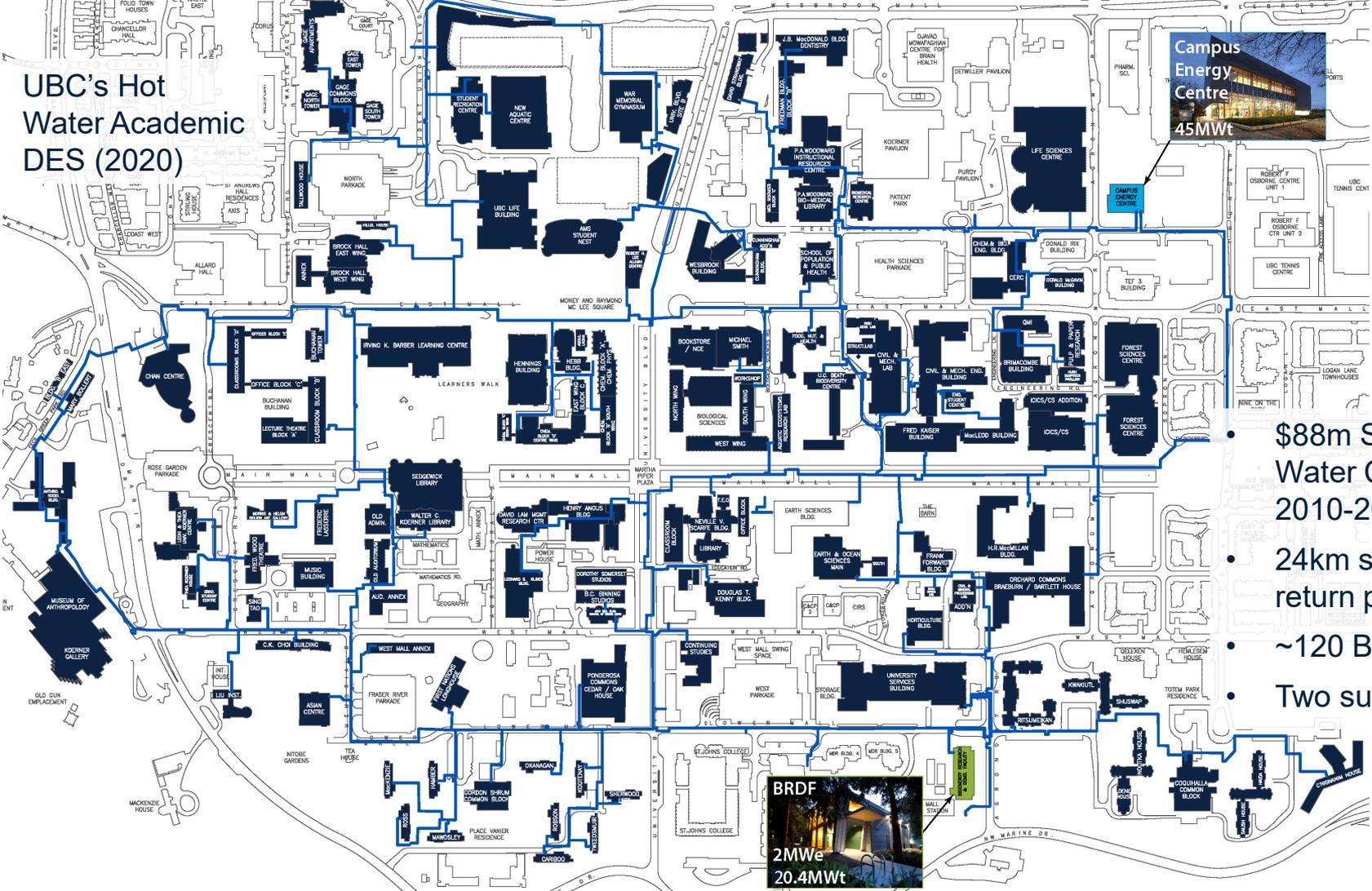
This presentation is a hands-on experience and includes **demo** to serve as an inspiration for all utilities interested in transforming their energy systems and to improve the efficiency of their energy systems.



# UBC DISTRICT ENERGY SYSTEM - 2021



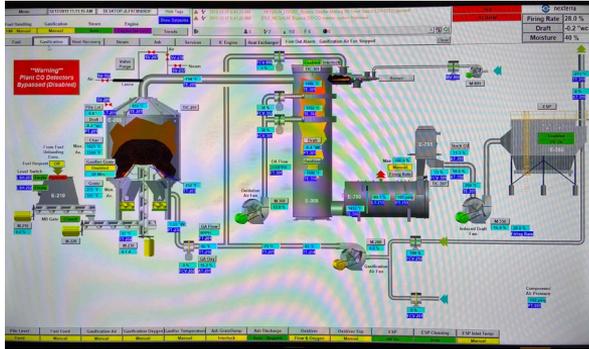
# UBC's Hot Water Academic DES (2020)



- \$88m Steam to Hot Water Conversion 2010-2017
- 24km supply and return piping
- ~120 Buildings
- Two supply plants



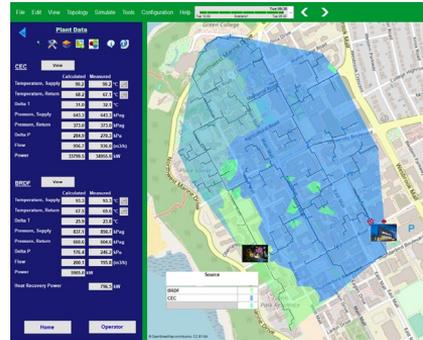
# HOW IS UBC MONITORING THIS \$88 MILLION INVESTMENT?



DES meters in all buildings trended alongside plant scada & field data collected and stored into a unified historian database for analytics.



Leak detection system



Termis real-time model





**Plant Data**



**CEC**

View

	Calculated	Measured	
Temperature, Supply	99.2	99.2	°C
Temperature, Return	68.2	67.1	°C
Delta T	31.0	32.1	°C
Pressure, Supply	643.3	643.3	kPag
Pressure, Return	373.0	373.0	kPag
Delta P	284.9	270.3	kPa
Flow	956.7	936.0	(m3/h)
Power	33799.5	34955.9	kW

**BRDF**

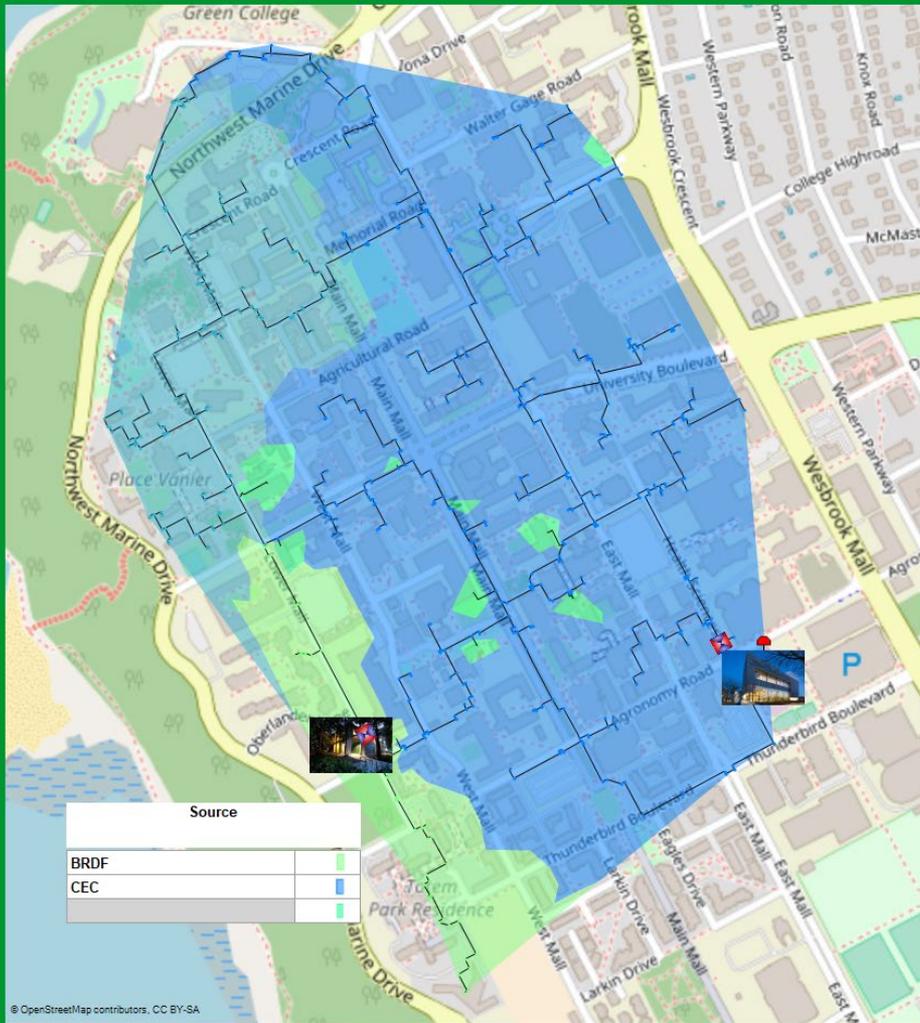
View

	Calculated	Measured	
Temperature, Supply	93.3	93.3	°C
Temperature, Return	67.5	69.6	°C
Delta T	25.9	23.8	°C
Pressure, Supply	837.1	850.7	kPag
Pressure, Return	660.6	604.6	kPag
Delta P	176.4	246.2	kPa
Flow	200.1	195.8	(m3/h)
Power	5905.0		kW

Heat Recovery Power 796.5 kW

Home

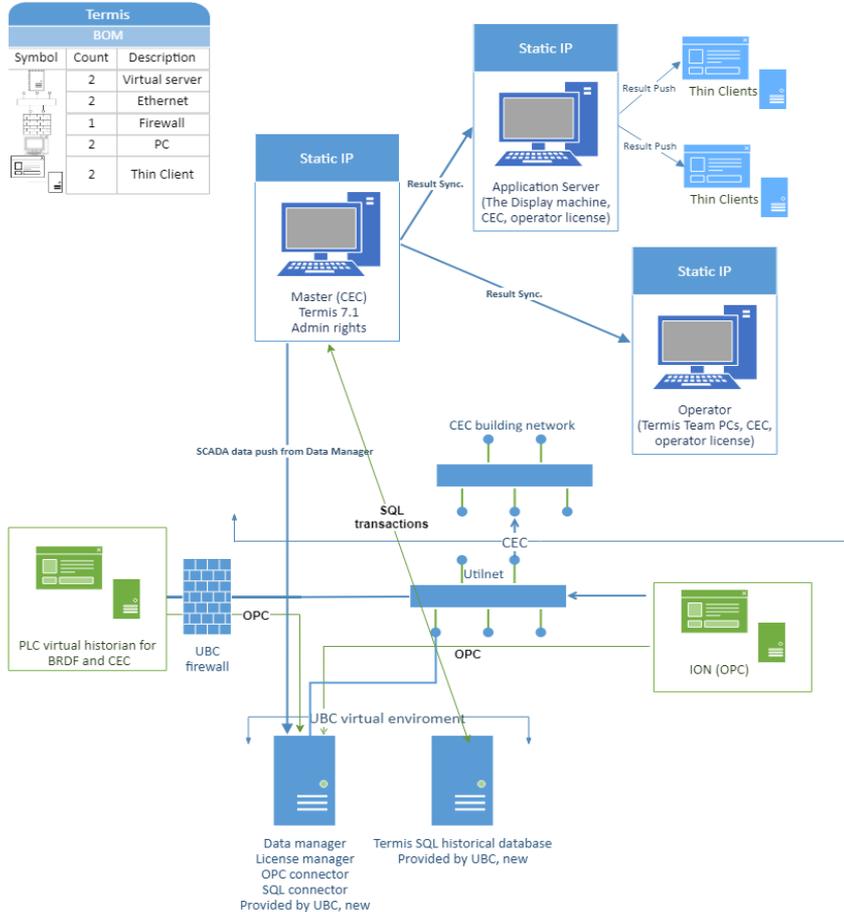
Operator



Source	
BRDF	<div style="width: 10px; height: 10px; background-color: green; border: 1px solid black;"></div>
CEC	<div style="width: 10px; height: 10px; background-color: blue; border: 1px solid black;"></div>



# TERMIS IMPLEMENTATION



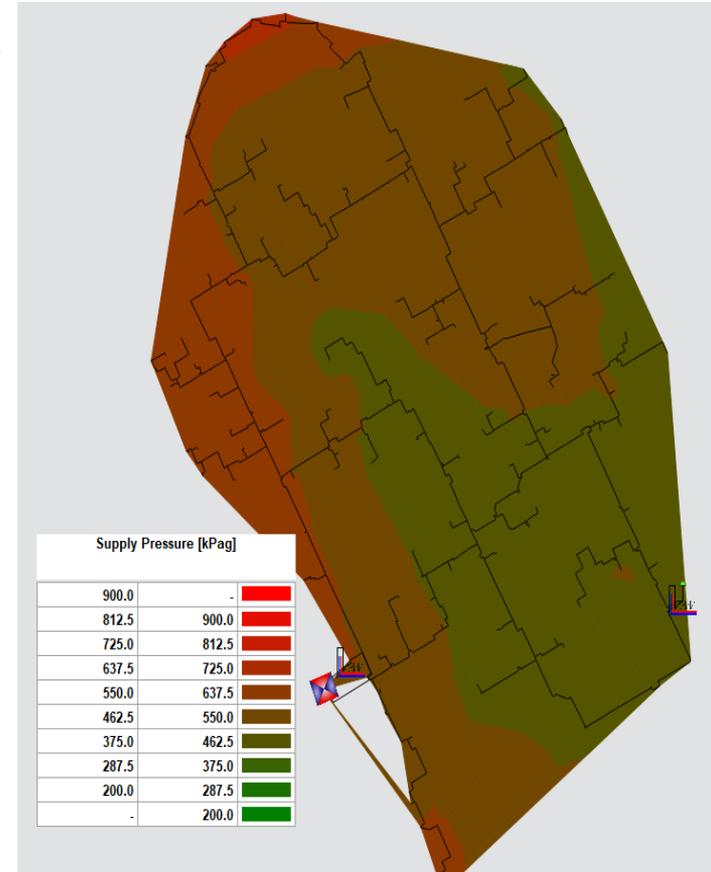
- Spring of 2018 - 3 months
- High level of buy-in and support from all levels
- IT resources
- Required an all around effort to integrate plant and building data into the Termis background databases
- IT resources
- Staff training on data administration as well as model use
- Ongoing model & data management, IT infrastructure upgrades, ongoing calibration to reflect reality



# MODELING – WHAT AND WHY

Industry preferred District Energy management software which models the whole district system (plant, piping, consumer)

- Hydraulic and thermal model that performs calculations of flow, pressures, losses, temperatures, velocities, gradients for every single pipe
  - Developed in Denmark and implemented worldwide
  - Both offline and real-time configurations
  - Provides ability to observe and manage performance of the whole system
  - “Eyes” on your whole district energy system
  - SI units
- **Planning and Design**
  - **Optimization & Efficiency**
  - **Operational & KPI tracking**

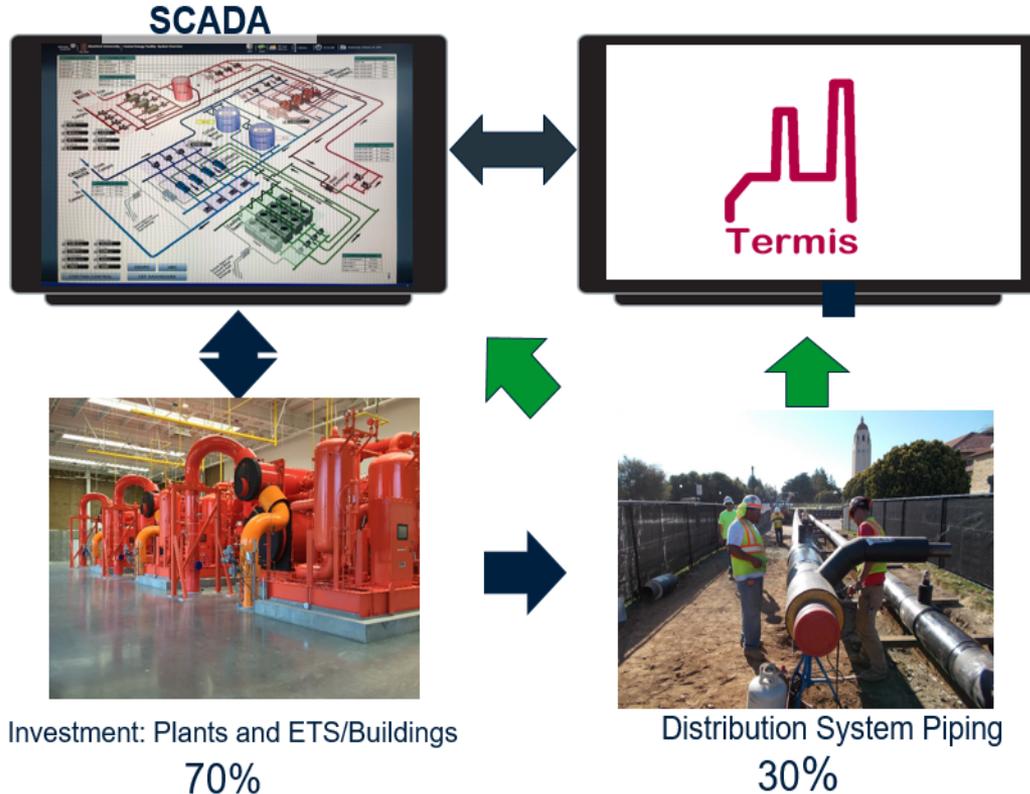


# Real-Time Dynamic Modeling versus Static Modeling

Elimination of the "black hole syndrome" and guess work

Scalable solution starting simple and adding functionality on a solid platform:

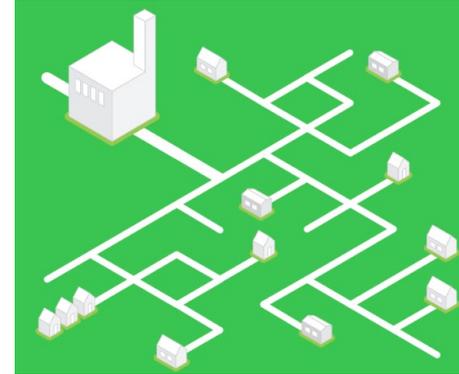
1. Static: How it should work
  1. Limited to a specific point in time
  2. Post analyses labor intensive
2. Real Time: Facts-Calibration
  1. Control Room and Field Operations monitoring and diagnostics
  2. Immediate Optimization of pressures, flows, temperature, losses, and equipment wear and tear
3. Cost



# BENEFITS OF REAL-TIME MODELING

## Planning and Design

- Decision Support Information to the management, operation, maintenance, planning, design and commissioning of thermal energy networks
- Pipe sizing for new network extensions / buildings
- Design pipes, pumps, valves
- Evaluation of control schemes “As-Is” and planned changes
- Plan outages and valving off parts of the system
- Perform “What-if” scenarios – Feasibility studies, Energy Master Plan



# BENEFITS OF REAL-TIME MODELING

## Optimization & Efficiency

- Optimize pressure, temperature, flow, velocity
- Identify areas of high pressure/heat loss in the network
- Load forecasting and Demand analysis
- Supply and return pressure and temp optimization
- Electricity and thermal optimization

## Operation Monitoring

- Detect abnormalities in operation
- Measurement & meter validation
- Track KPIs such as system thermal losses etc



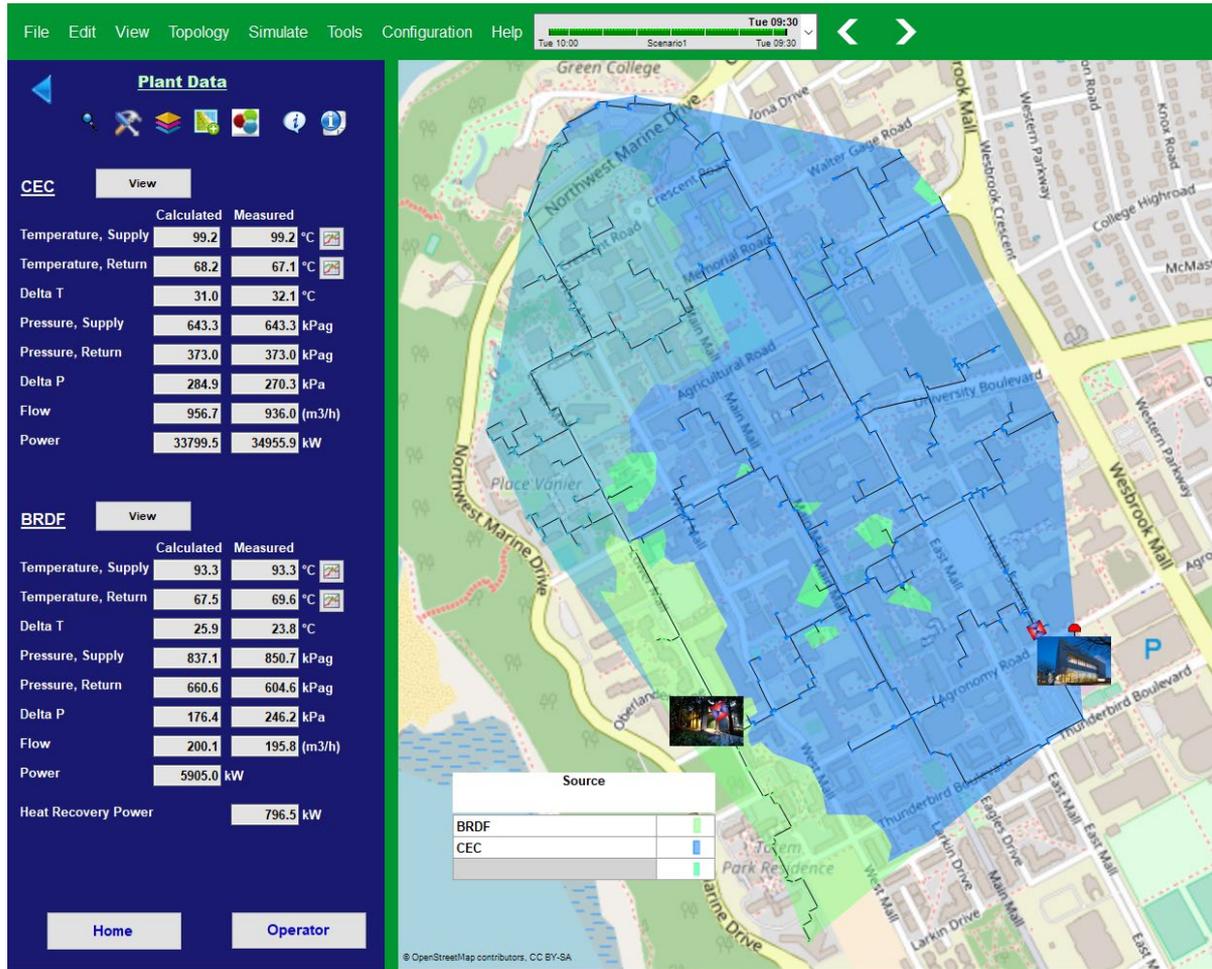
# “EYES ON OUR SYSTEM” AND ENGAGING WITH OUR COMMUNITY

- Telling UBC Steam to Hot Water and Bioenergy Plant story
- Shows UBC’s DES in real time
- Shows amount of energy supply with natural gas & biomass

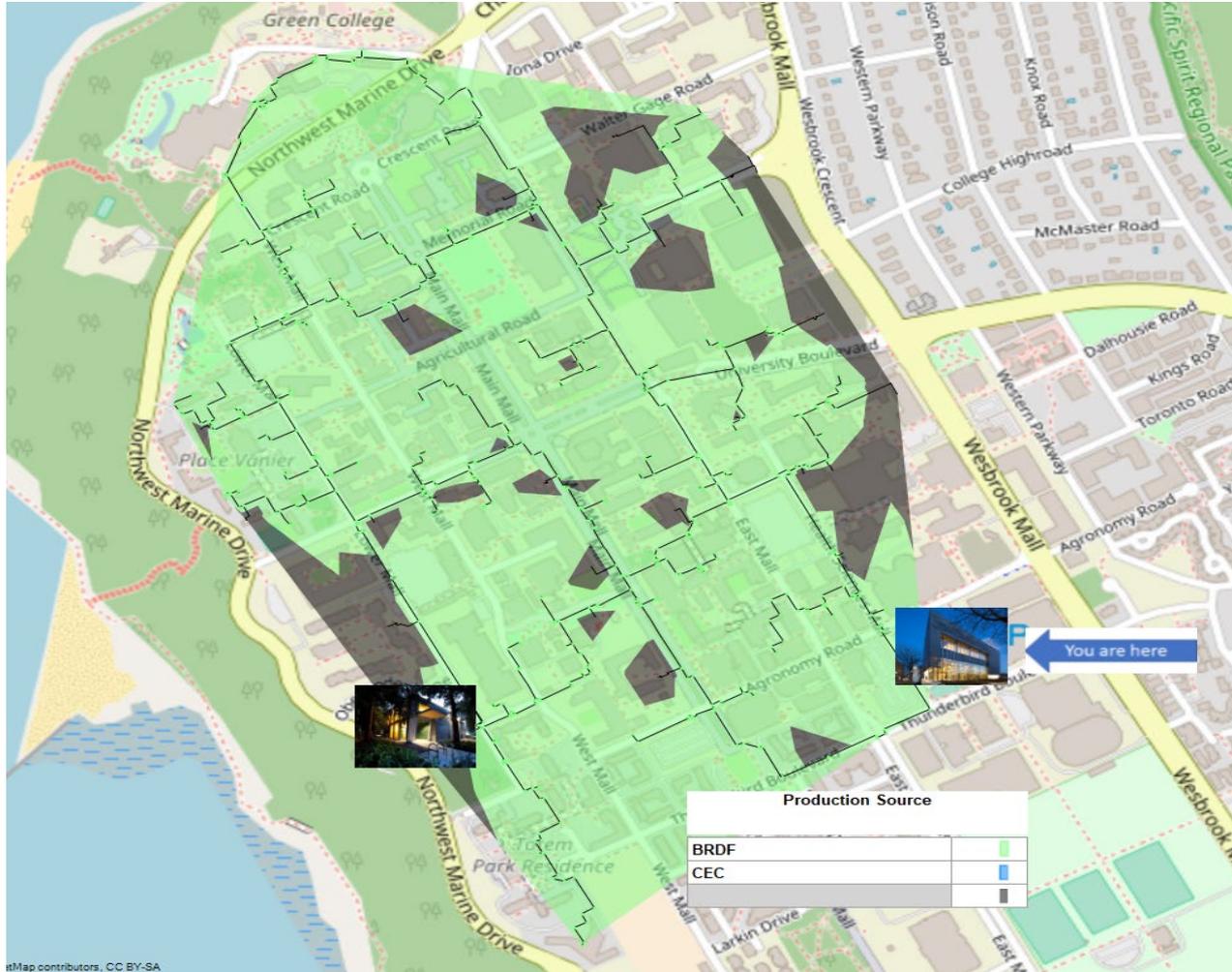


UBC's Hot Water	
Academic District Energy System	
Heating and Hot Water Supplied by:	
Natural Gas	0.0 kW
Clean Waste Wood	4564.4 kW
Recovered Waste Heat	358.0 kW
CEC - Campus Energy Centre	
Thermal Output (Gas)	0.0 kW
Temperature, Supply	84.5 °C
Temperature, Return	62.2 °C
Delta T	22.3 °C
Pressure, Supply	277.8 kPag
Pressure, Return	239.9 kPag
Delta P	37.9 kPa
Flow	0.0 (m3/h)
BRDF - Bioenergy Facility	
Waste Heat Recovery	358.0 kW
Thermal Output (Wood)	4564.4 kW
Temperature, Supply	91.8 °C
Temperature, Return	78.3 °C
Delta T	13.5 °C
Pressure, Supply	607.9 kPag
Pressure, Return	449.9 kPag
Delta P	158.0 kPa
Flow	161.2 (m3/h)

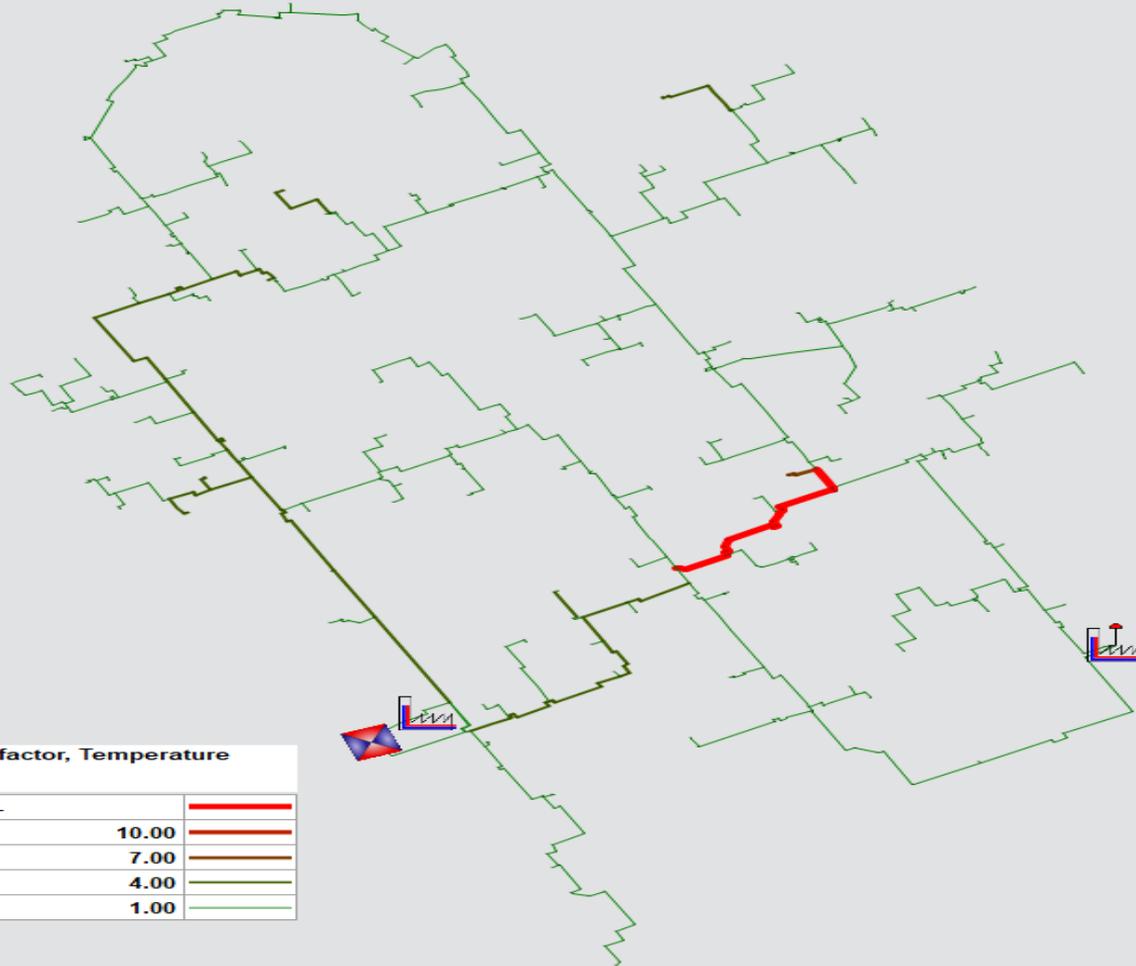
# VISUALIZATION & DASHBOARDS: TWO PLANTS IN OPERATION



# SINGLE PLANT IN OPERATION



# TEMPERATURE MODE

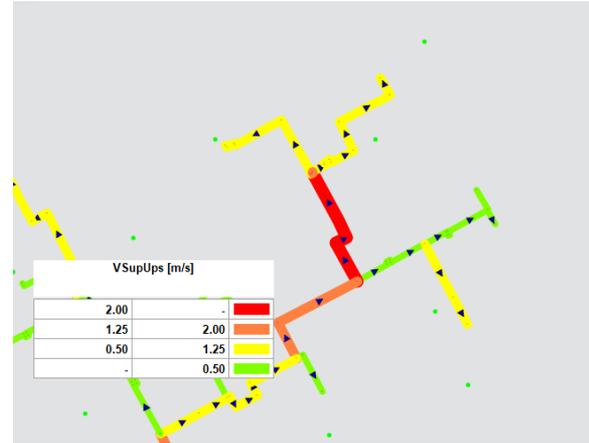
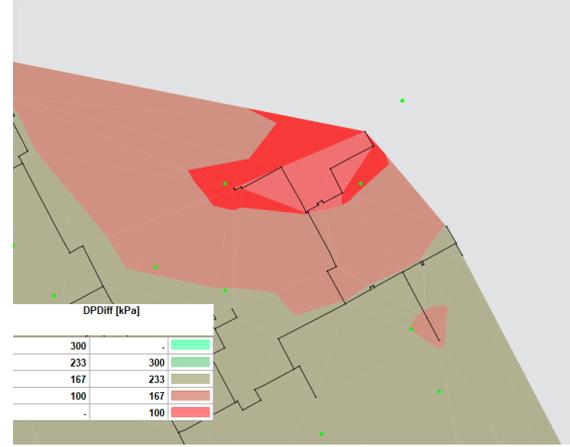
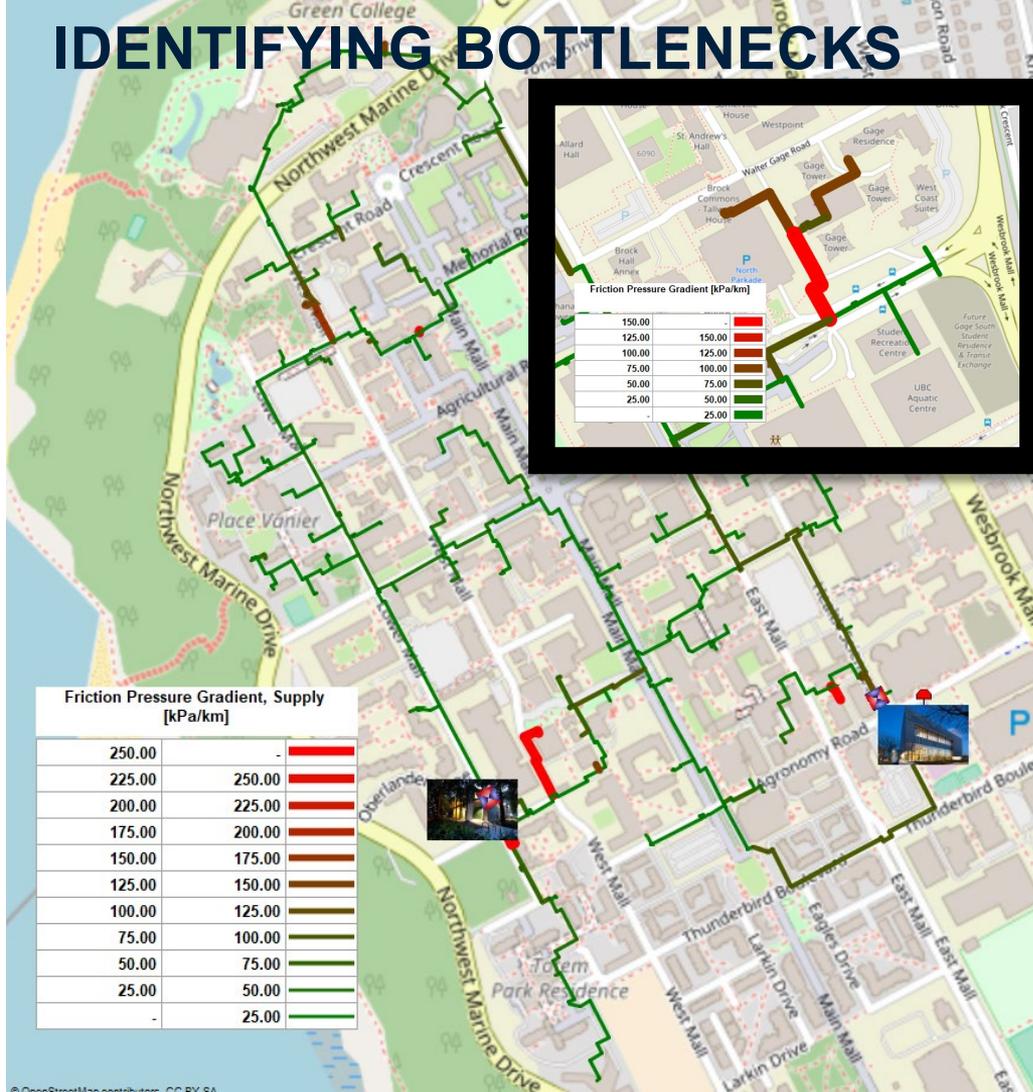


Calibration factor, Temperature

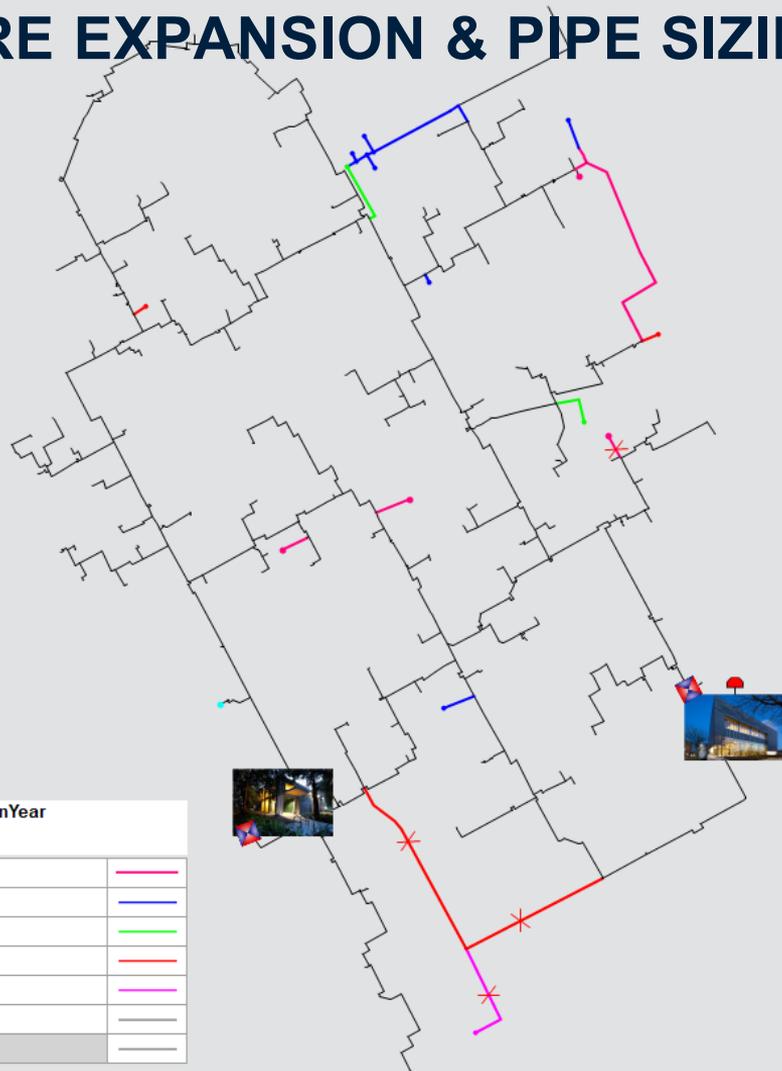
10.00	-	—————
7.00	10.00	—————
4.00	7.00	—————
1.00	4.00	—————
-	1.00	—————



# IDENTIFYING BOTTLENECKS



# FUTURE EXPANSION & PIPE SIZING MODELING

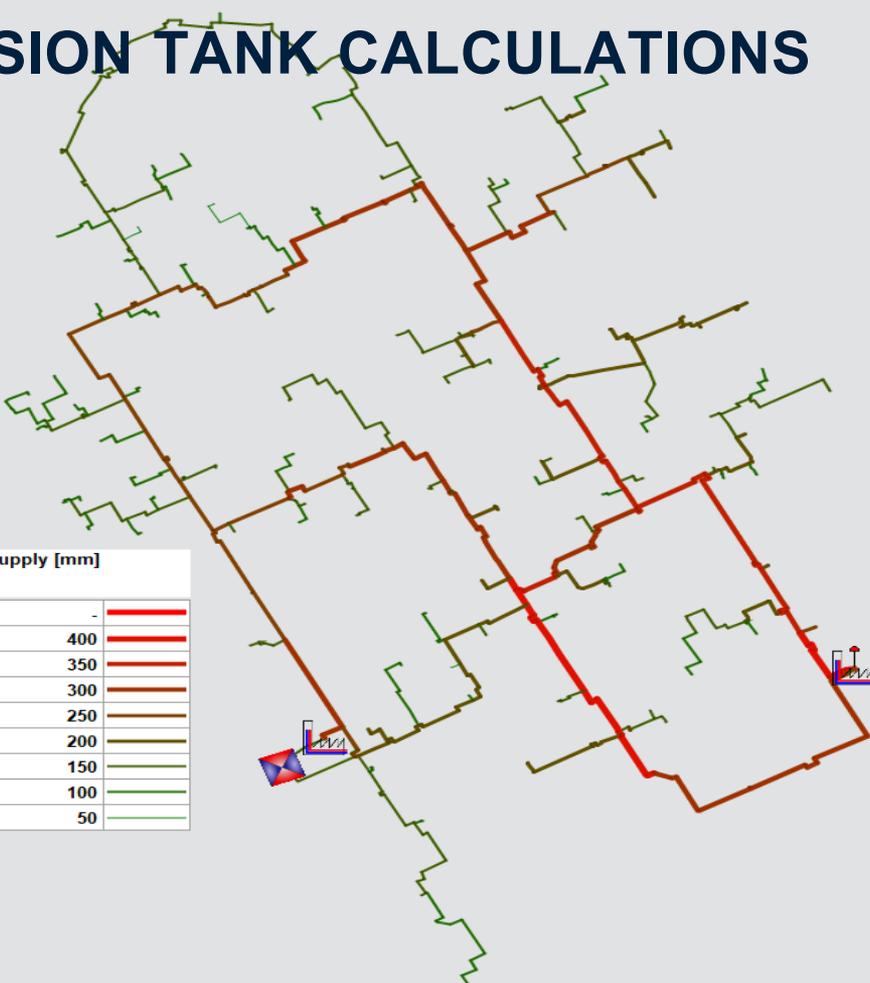


PlanYear

201920	
202122	
202223	
202324	
202425	
Existing	

	*	500	399	387	68
Pipe Type, Return		D70.3	D82.5	D160.3	D160.3
Pipe Length, Return [m]		1.4	1.9	12.7	9
Diameter, Return [mm]		70.3000	82.5000	160.3000	160.30
Roughness, Return [mm]		0.05	0.05	0.05	0.
Single Loss, Return		0	0	0	
Heat Transfer Coeff., Return [W/m/K]		0.26	0.27	0.39	0.
Pipe in return does not exists		<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
Pressure Drop Correction, Return		1	1	1	
Temperature Drop Correction, Return		1	1	1	
Auto dimension return		<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>

# PIPE VOLUME, THERMAL STORAGE, & EXPANSION TANK CALCULATIONS



Diameter, Supply [mm]		
400	-	
350	400	
300	350	
250	300	
200	250	
150	200	
100	150	
50	100	
-	50	



# PIPE LINE VELOCITY & WATER FLOW DIRECTION

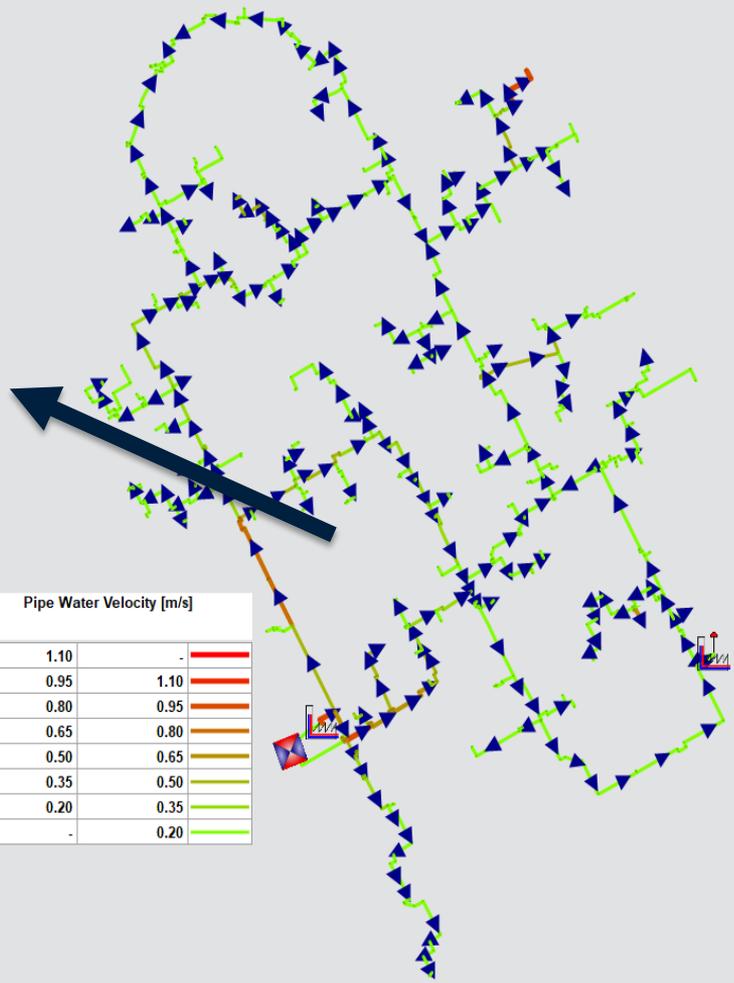
Scenario 1

- Pipe
- Results
- System
- Geometry
- Additional Info
- Data, Supply
- Data, Return
- Results, Supply
- Results, Return
- Show
- Adaption
- Measurements
- KPI

		154
▶ Pressure, Ups., Return [kPag]		466.6
Pressure, Dws., Return [kPag]		449.1
Friction Pressure Gradient, Return [kPa/km]		6.45
Mass Flow, Ups., Return [(m <sup>3</sup> /h)]		87.3
Volumetric Flow, Ups., Return [m <sup>3</sup> /h]		89.08
Velocity, Ups., Return [m/s]		0.46
Temperature, Ups., Return [°C]		65.0
Temperature, Dws., Return [°C]		65.1
Relative heat loss, Return [W/m]		-23.38

1 object

OK
Cancel
Apply



Pipe Water Velocity [m/s]		
1.10	-	[Red]
0.95	1.10	[Dark Orange]
0.80	0.95	[Orange]
0.65	0.80	[Light Orange]
0.50	0.65	[Yellow-Orange]
0.35	0.50	[Yellow]
0.20	0.35	[Light Green]
-	0.20	[Green]



# SAMPLE BUILDING & PLANT DATA

- Scenario 1
  - Node
    - Results
    - Control
    - Geometry
    - Additional Info
    - Update
    - Zone Definitions
    - Show
    - Measurements
    - KPI
    - System

		NO_PULPR
▶	dP [kPa]	12.16
	Pressure, Supply [kPag]	343.6
	Pressure, Return [kPag]	331.5
	Temperature, Supply, Consumer [°C]	78.1
	Temperature, Return, Consumer [°C]	52.6
	dT [°C]	-25.58
	Temperature, Supply [°C]	78.1
	Temperature, Return [°C]	52.6
	Volumetric Flow [m³/h]	0.31
	Load [kW]	8.91
	Mass Flow [m3/h]	0.3
	Source	BRDF: 1.00
	dT Consumer [°C]	25.64
	Transport Time [min]	644.87

1 object

OK Cancel Apply

		CEC	BRDF
▶	dP [kPa]	14.22	38.84
	dT [°C]	0.00	24.13
	Power [kW]	0.00	4530.85
	Pressure, Return [kPag]	239.9	455.4
	Production Units		
	Pressure, Supply [kPag]	254.1	494.2
	Mass Flow [m3/h]	0.0	161.2
	Actual Control Node	NO_754	
	Volumetric Flow [m³/h]	0.00	164.77
	Temperature, Supply, Plant [°C]	8.0	91.8
	Energy Costs [CU/s]	0.00	0.00
	Temperature, Return, Plant [°C]	8.0	67.7

2 objects

OK Cancel Apply



## EXAMPLES OF USE

1. What-If scenarios of plant capacity from 2019-2025 including DT impact,
2. What-If scenarios of Max and Min demand ( $T_{sup} = 75\text{ C}$ ),
3. What-If scenarios of pumping requirements for adding the BDRF 12 MWt plant,
4. What-If scenarios of use of booster pump,
5. What-If scenarios of use of control valves,
6. Initial assessment of plant supply temperature and pumping pressures.
7. Thermal storage
8. Early stages of modeling potential district cooling system nodes

DEMO



## LESSON LEARN/CHALLENGES

- Have a system like Termis to aid original design of the system to identify future scenarios and bottle necks.
- Suggest to have model during design stages of DES to use the offline model right away to check consultants work during implementation of new system
- Dedicated resources for daily check-in to ensure a healthy system.
- People communication is important: Receive plans, potential system upgrades, communication with IT (ie server upgrade = lost data)
- High level buy in



# CONCLUSIONS AND NEXT STEPS

**UBC is monitoring and managing the \$88 million energy transformation investment:**

- Improving planning, design, operational conditions by Dynamic Live Real-Time modeling
  - Real capacity and capability versus design
  - Improving / maintaining dT at a high level
  - Dispatch strategy to ensure low dP to minimize pumping
  - Management of piping losses, identify system bottlenecks
  - Measurements; accuracy watch-dog and location
  - Managing campus building expansions by applying loads from existing Building System
  - Managing valves and by-passes
  - Visual overview



# CONCLUSIONS AND NEXT STEPS

**UBC is monitoring and managing the \$88 million energy transformation investment:**

Next steps 2020-21:

## **Phase 6:**

Enable management, operational, and maintenance staff to use the Termis System Thin Client HMI (View Only) as well as tablet and smartphone devices.

## **Phase 7:**

Study of optimization and efficiency opportunities of dynamic supply pressure and supply temperature reset in real-time modeling advisory mode. In addition study the benefits and savings of load forecasting based production scheduling.

## **Phase 8:**

Potential implementation of the recommendations of Phase 7



# Thank you! Questions?



Thomas Lund-Hansen, REO



Joshua Wauthy, UBC



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