



# Differential Pressure Control

Hydronic College  
by IMI Hydronic Engineering Inc.

Engineering  
**GREAT**  
Solutions

 **IMI PNEUMATEX**

 **IMI TA**

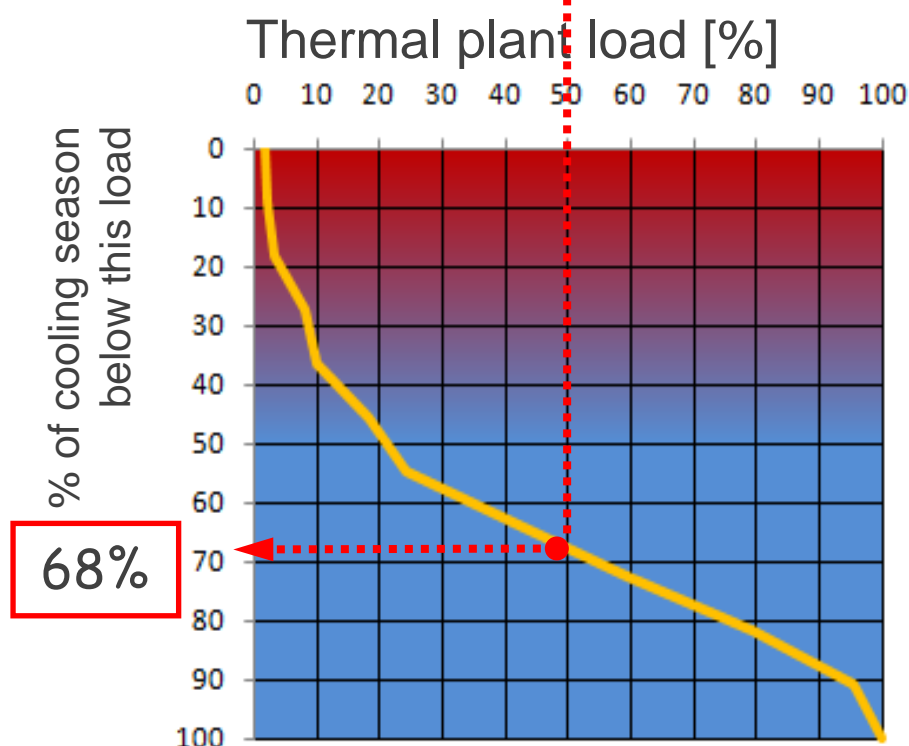
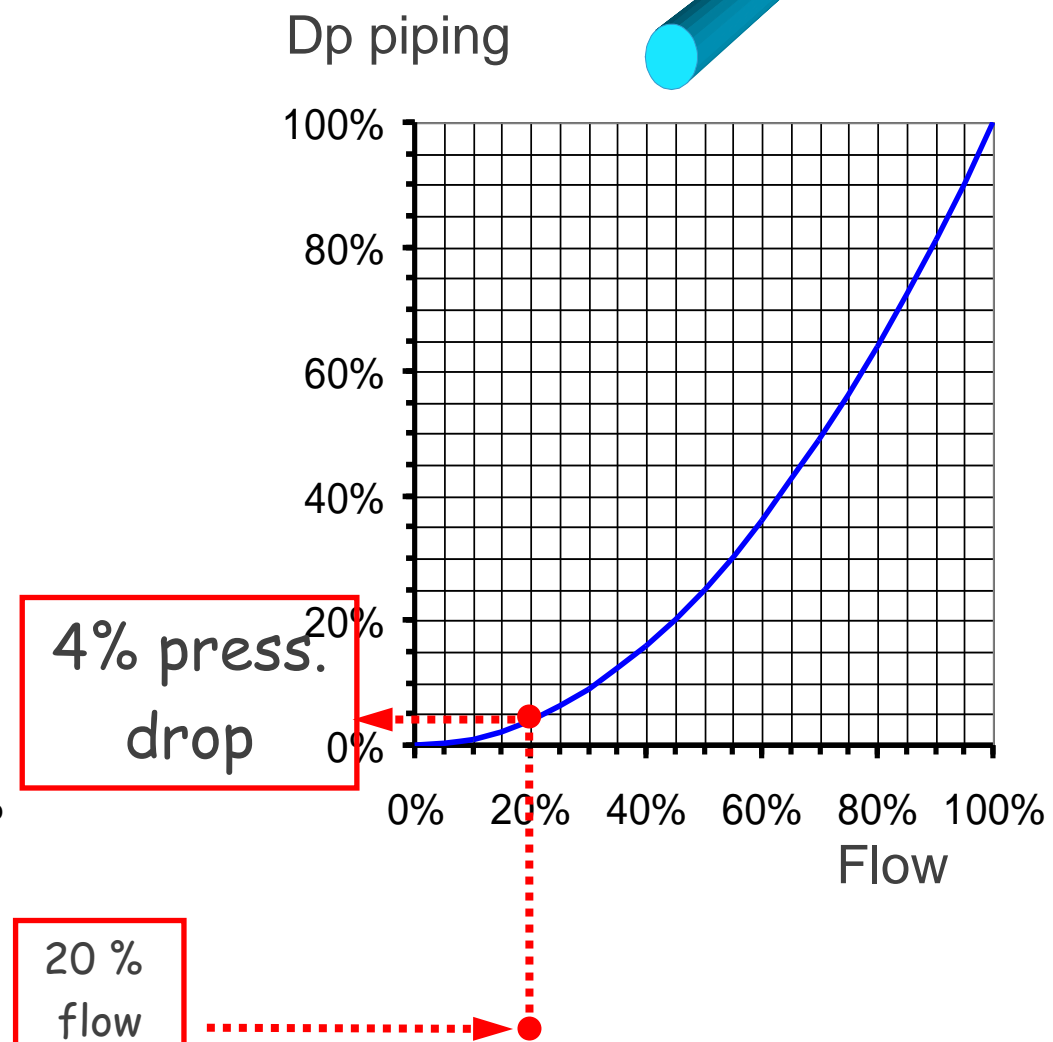
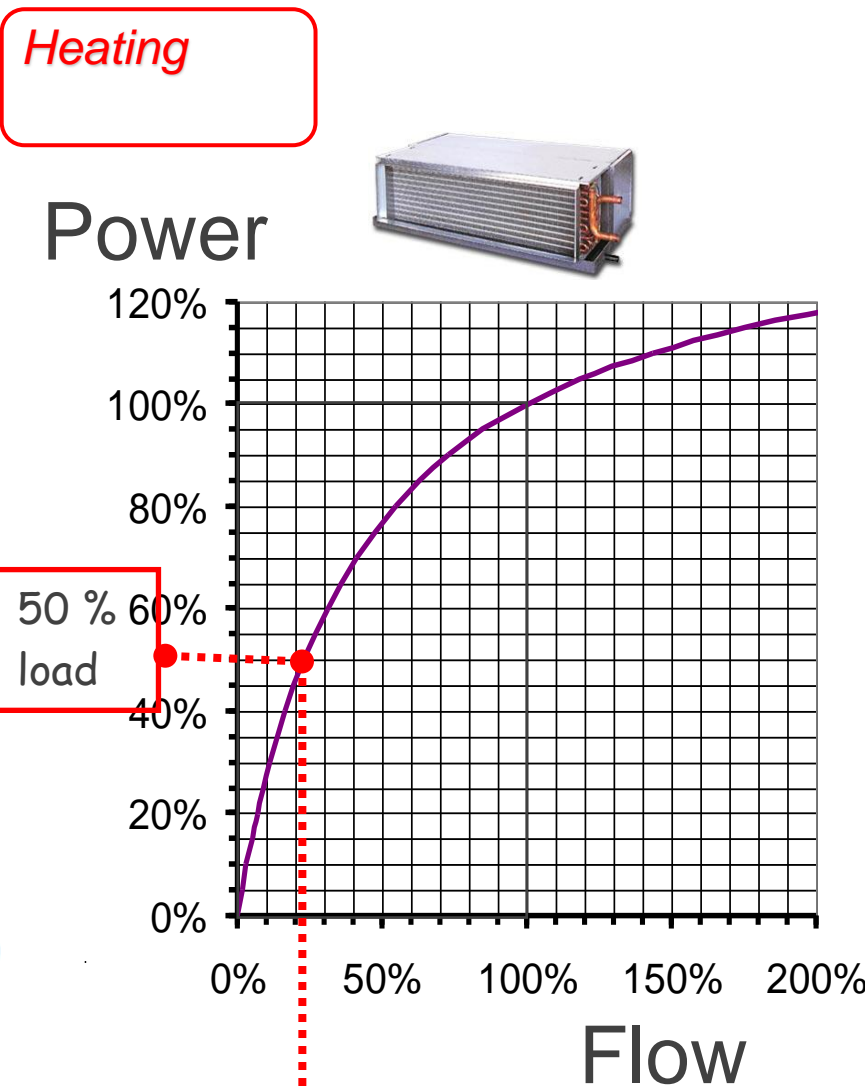
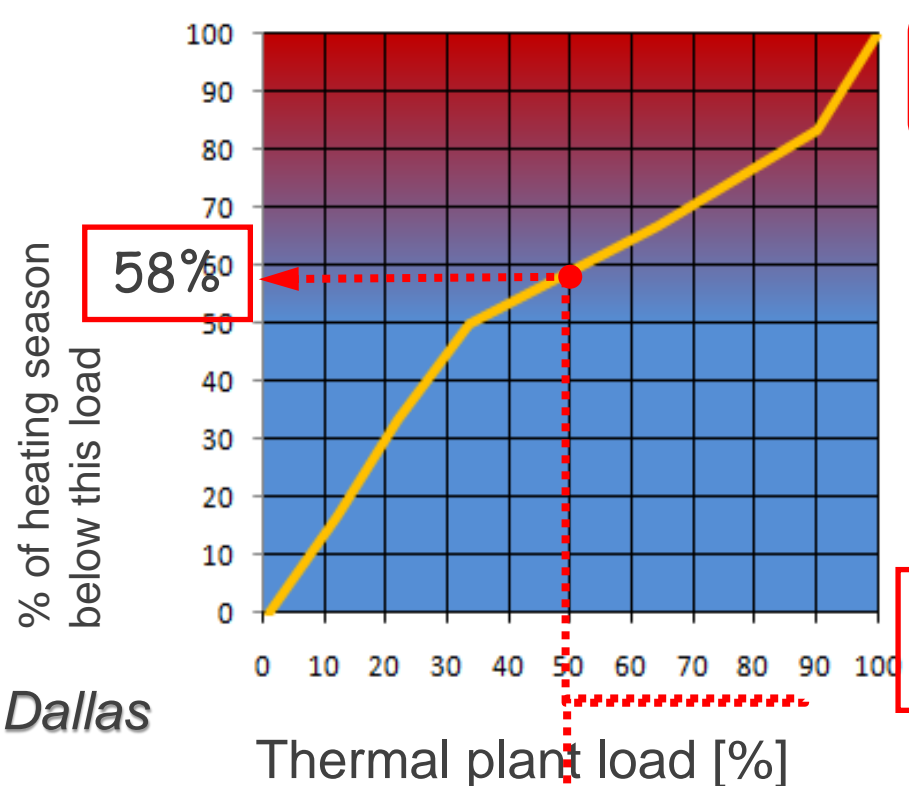
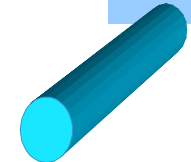
 **IMI HEIMEIER**

# Why differential pressure control?

- Control valves work with improved authority, therefore their performance is improved
- Reducing pump head and keep high controllability in the system
- Control valves are pressure relieved, so low force (= lower cost) actuators can be used
- Noise in control valves is reduced or removed completely
- Based on stabilized differential pressure across the circuit, the flow is limited.
- Circuits is a pressure independent modules. Which means:
  - *That the changes in other parts of the system do not affect the circuit*
  - *Large plants can be balanced module by module independently*
  - *New modules can be added to the system without rebalancing*

# Differential pressure variations

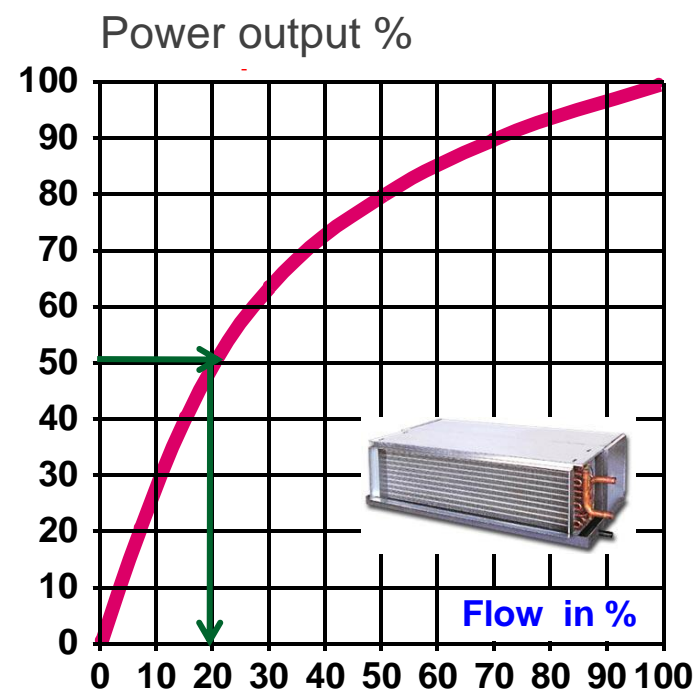
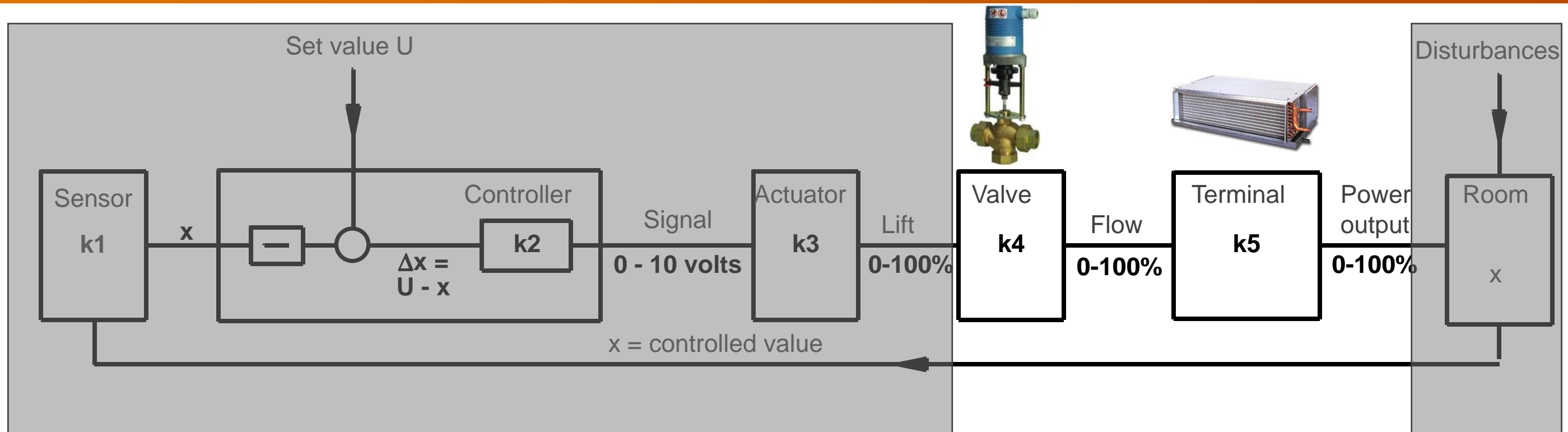
$$\Delta P \propto q^2$$



At constant supply water temperature

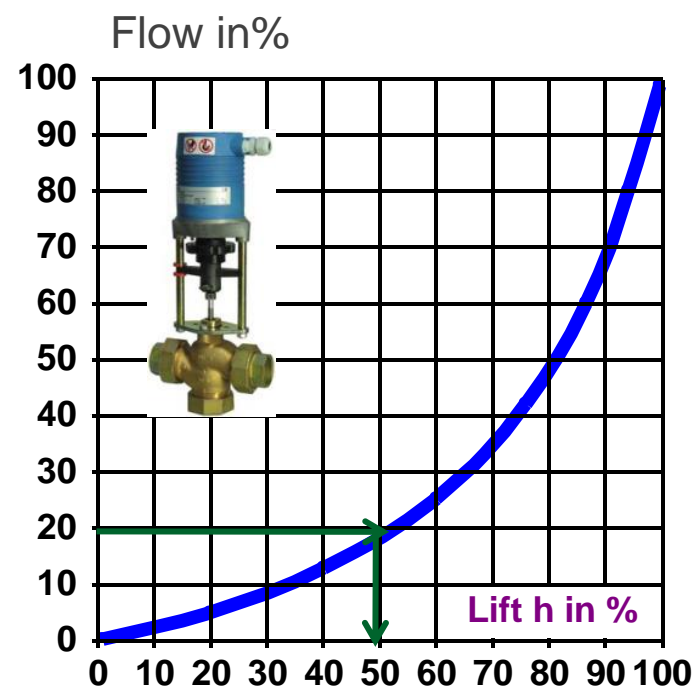
Pressure drops are reduced to 4% of their design value.

# Control loop



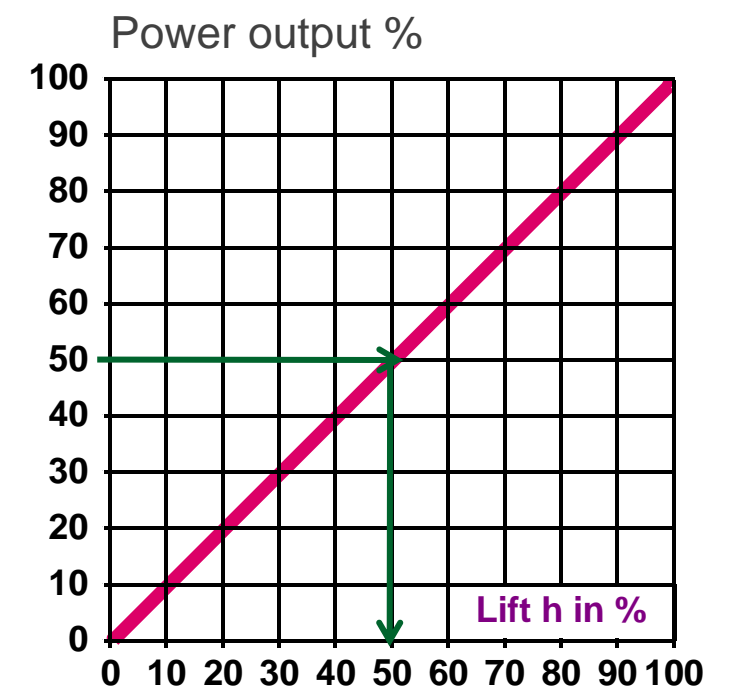
Terminal unit characteristic

+

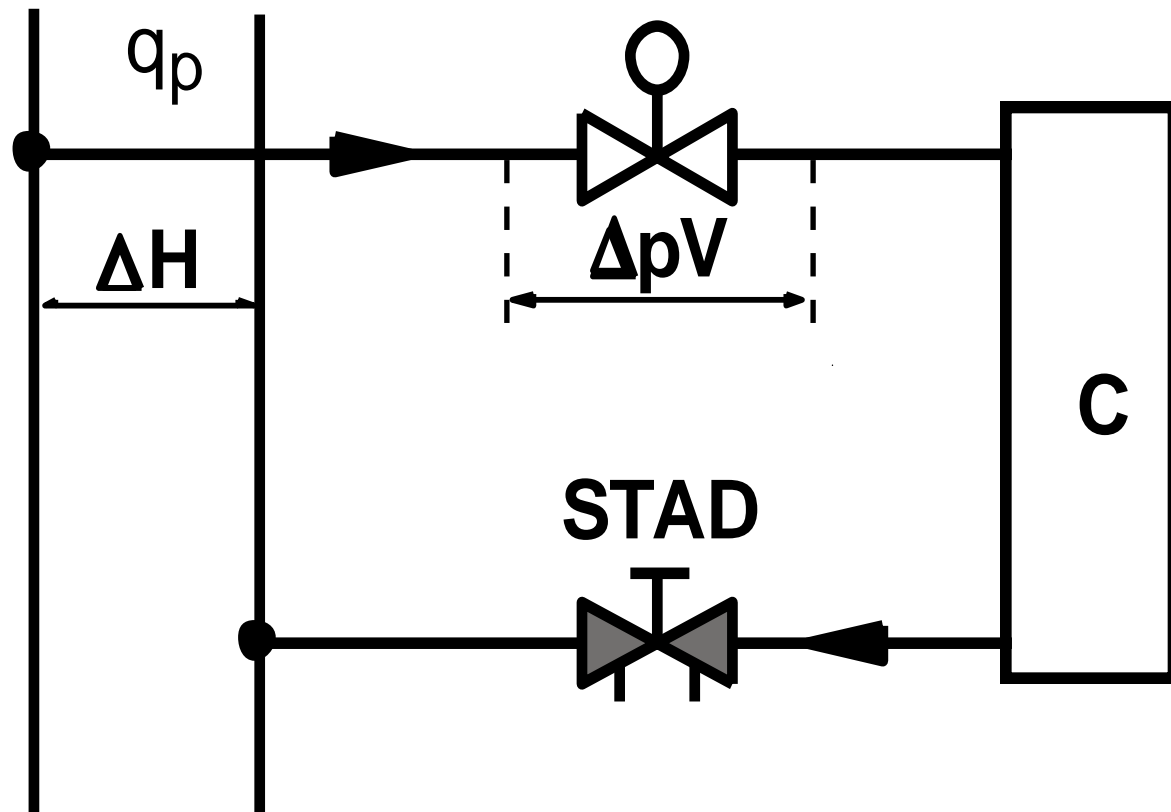


Control valve characteristic

=

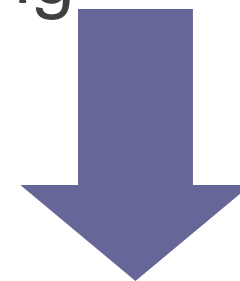


# Control valve authority



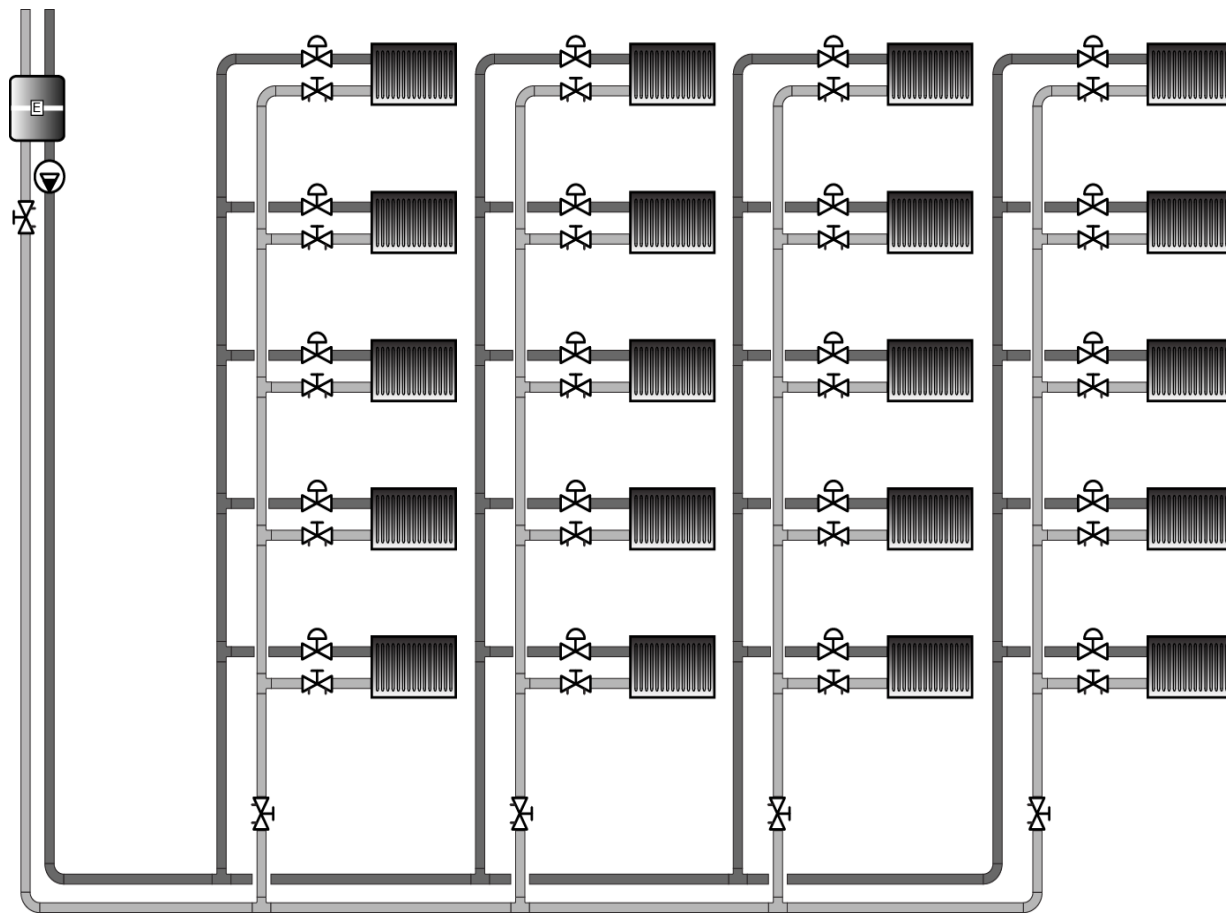
$$\beta = \frac{\Delta P_{\text{Control valve fully open and design flow}}}{\Delta P_{\text{Control valve fully shut}}}$$

The authority ( $\beta$ ) formulates how much the differential pressure builds up on the control orifice of a control valve when it is closing



Its value indicates how effectively the control valve can reduce the flow while it is closing.

# 2-way control valve authority (variable flow)



**Constant** as soon as the valve Cv is chosen ( $\Delta p_v$ ).

$$\beta = \frac{\Delta P_{\text{Control valve fully open and design flow}}}{\Delta P_{\text{Control valve fully shut}}}$$

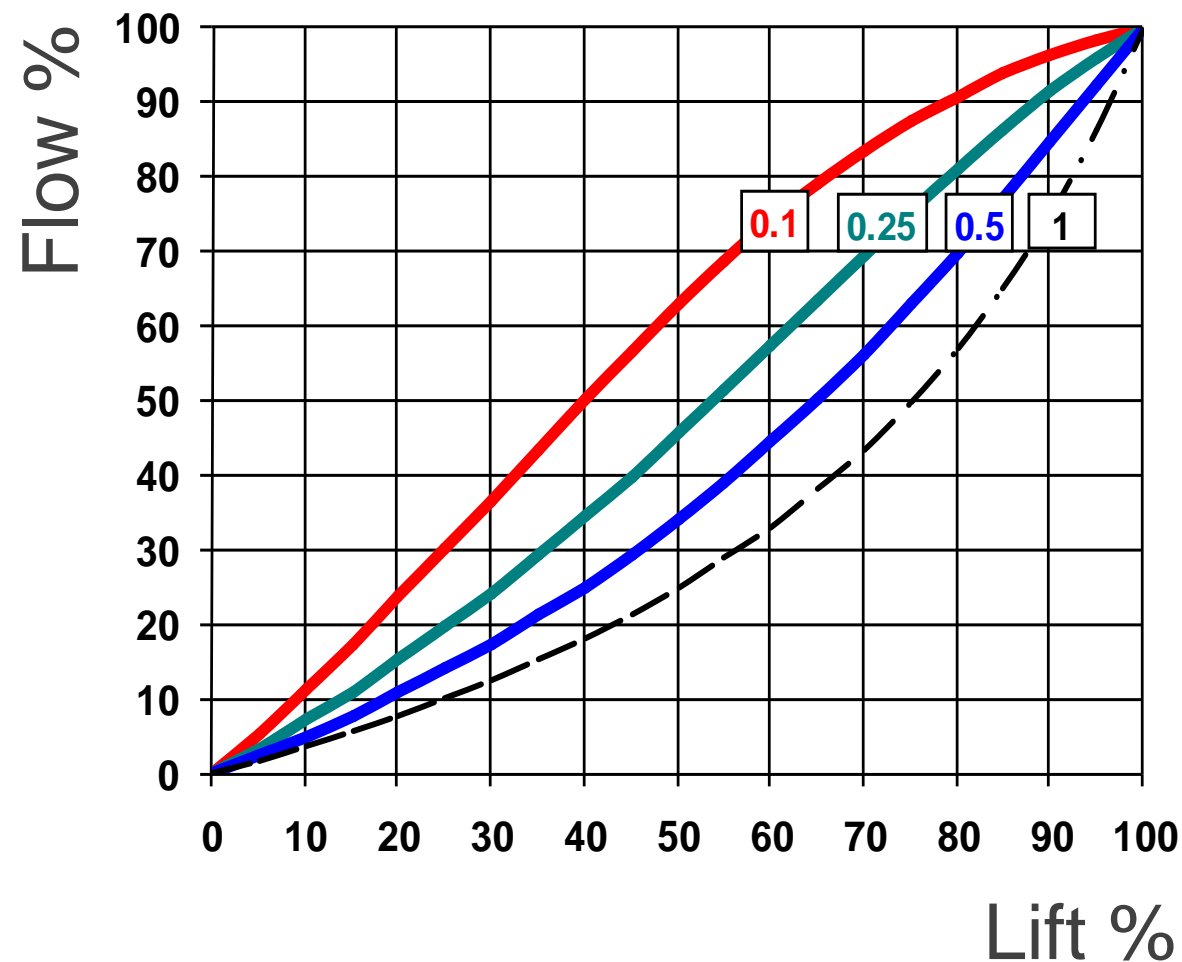
**Variable**, depends on flows in the piping,

thus also on the opening of all the other control valves.

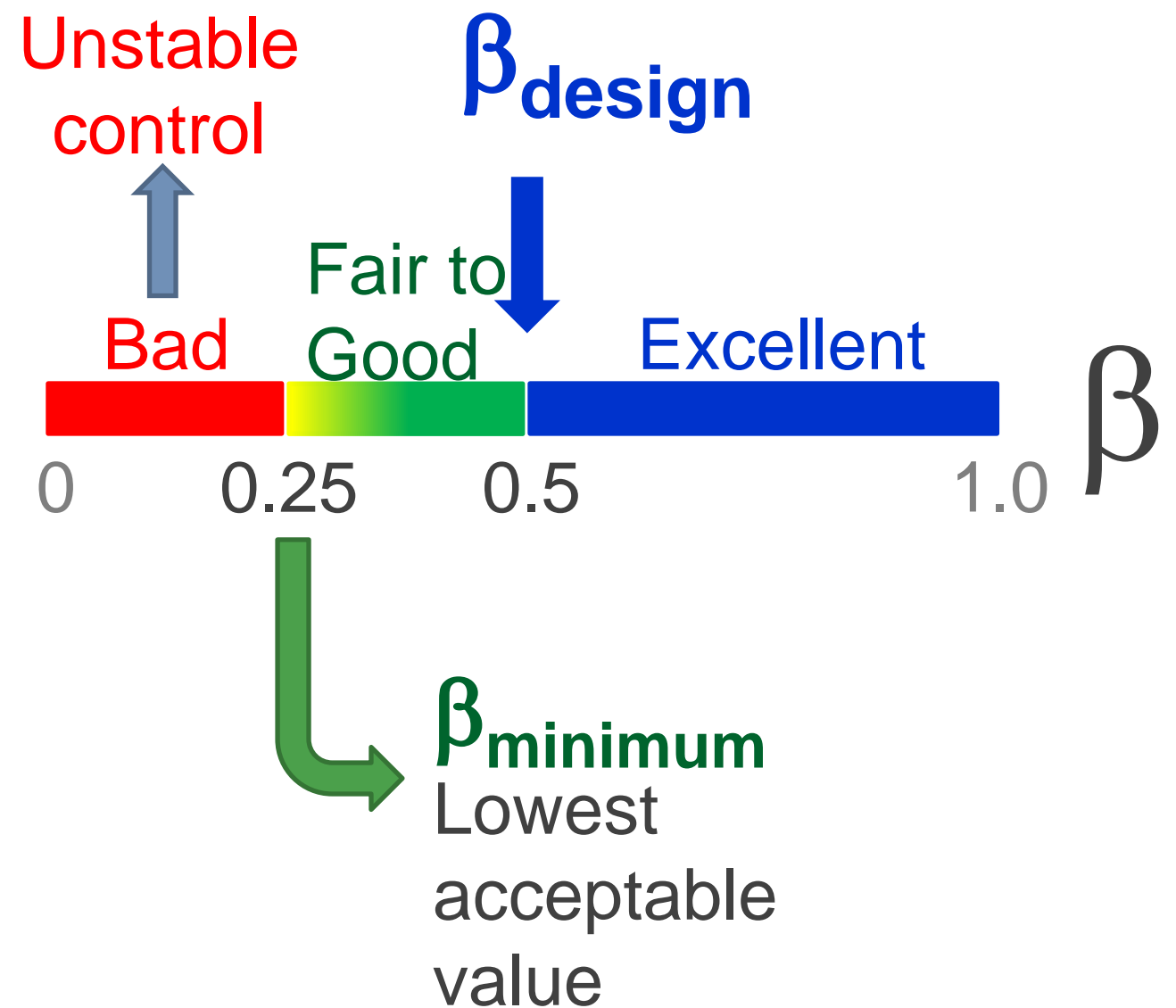
In a variable flow distribution,  
the authority of a control valve is  
variable.

# Distortion of valve characteristic

The lower the authority, the larger the  $\Delta p$  variations on the control valve, the larger distortion of the valve characteristic

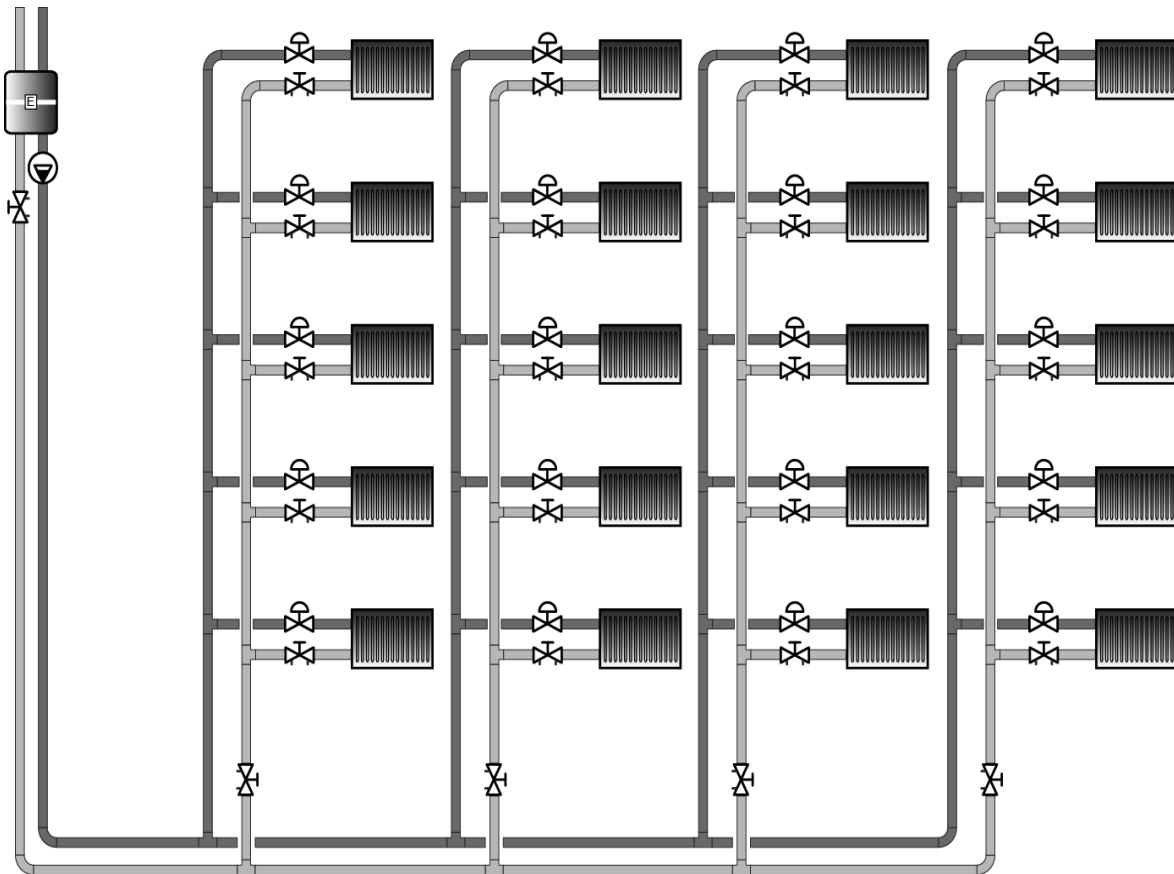


Control valve with  
**Equal-percentage  
characteristic (EQM)**





# Variable authority of 2-way control valves

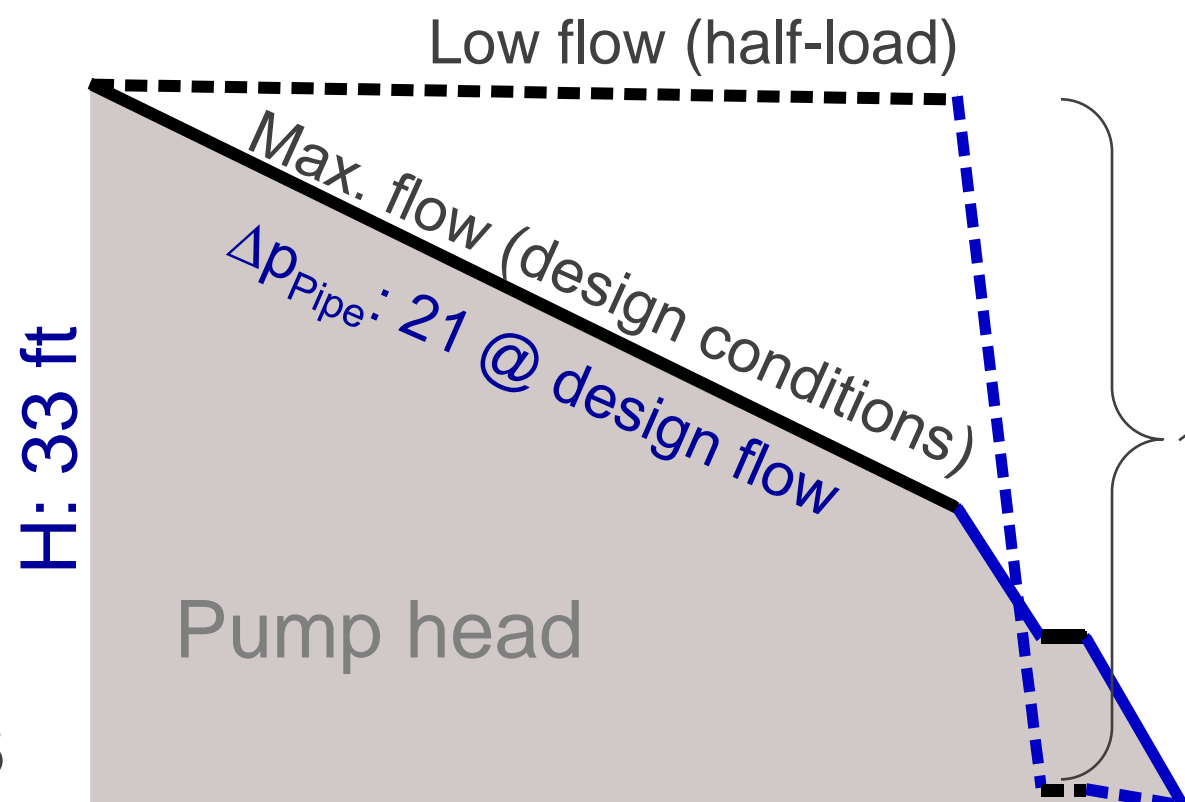


**Authority in design conditions:**

$$\beta \approx 5/(5+7) = \mathbf{0.42}$$

**Authority at half-load:**

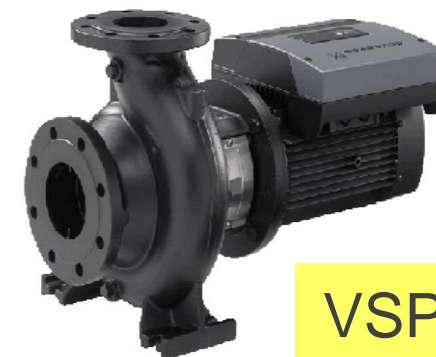
$$\beta = 5/(5+7+0.96*21) = \mathbf{0.15 !}$$



$0.96*21 \text{ ft} + 0.96*7 \text{ ft} \approx 26.9 \text{ ft}$  in excess in the valve at half-load

5 ft in the valve

7 ft in the circuit



VSP does not allow to compensate for all local  $D_p$  variations in the plant



# Control valve oversizing

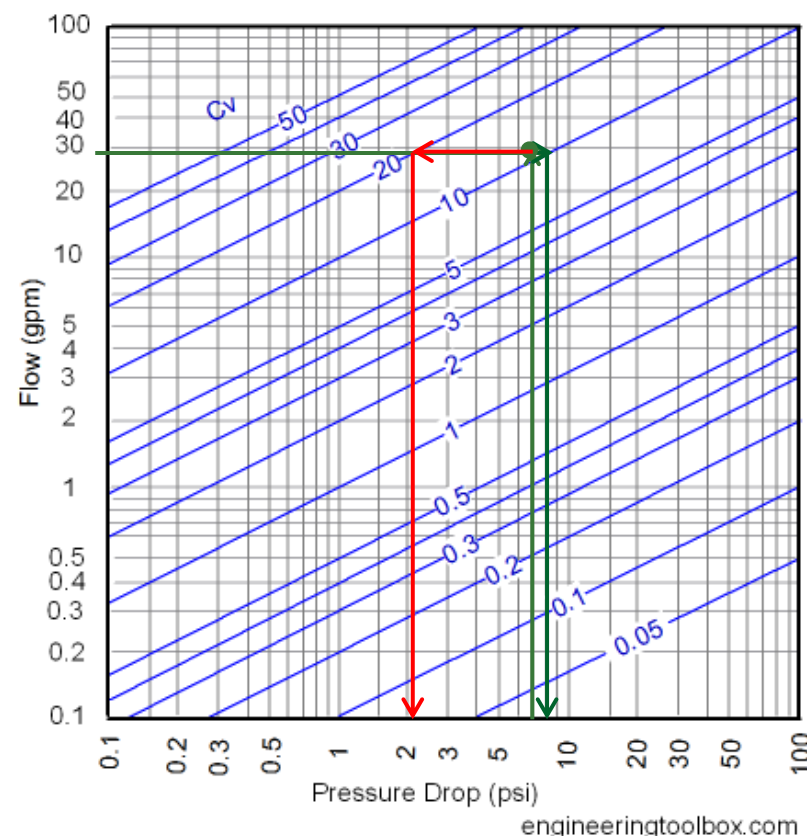
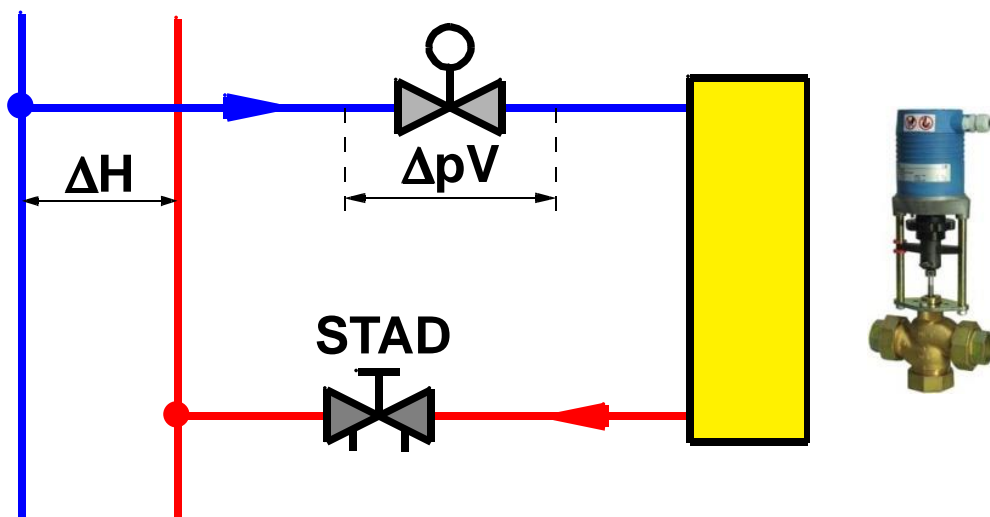
Control valves are commercially available with Cv values increasing according to the Reynard series: **Cv:..... 2.0 3.0 4.0 5.0 10 20 30**

Flow to a FCU of 29 gpm,  $\Delta p$  5 psi and 2 psi in connecting pipes. the commercially available control valves create a design  $\Delta pV$  of:

Cv:	11	20	10	
$\Delta pV$ [psi]	7	2. 12	8.4 9	NOTHING in between
$\beta_{\text{design}}$	0.5	0. 23	0.5 5	
$\Delta H$ [psi]	14	9. 12	15. 49	

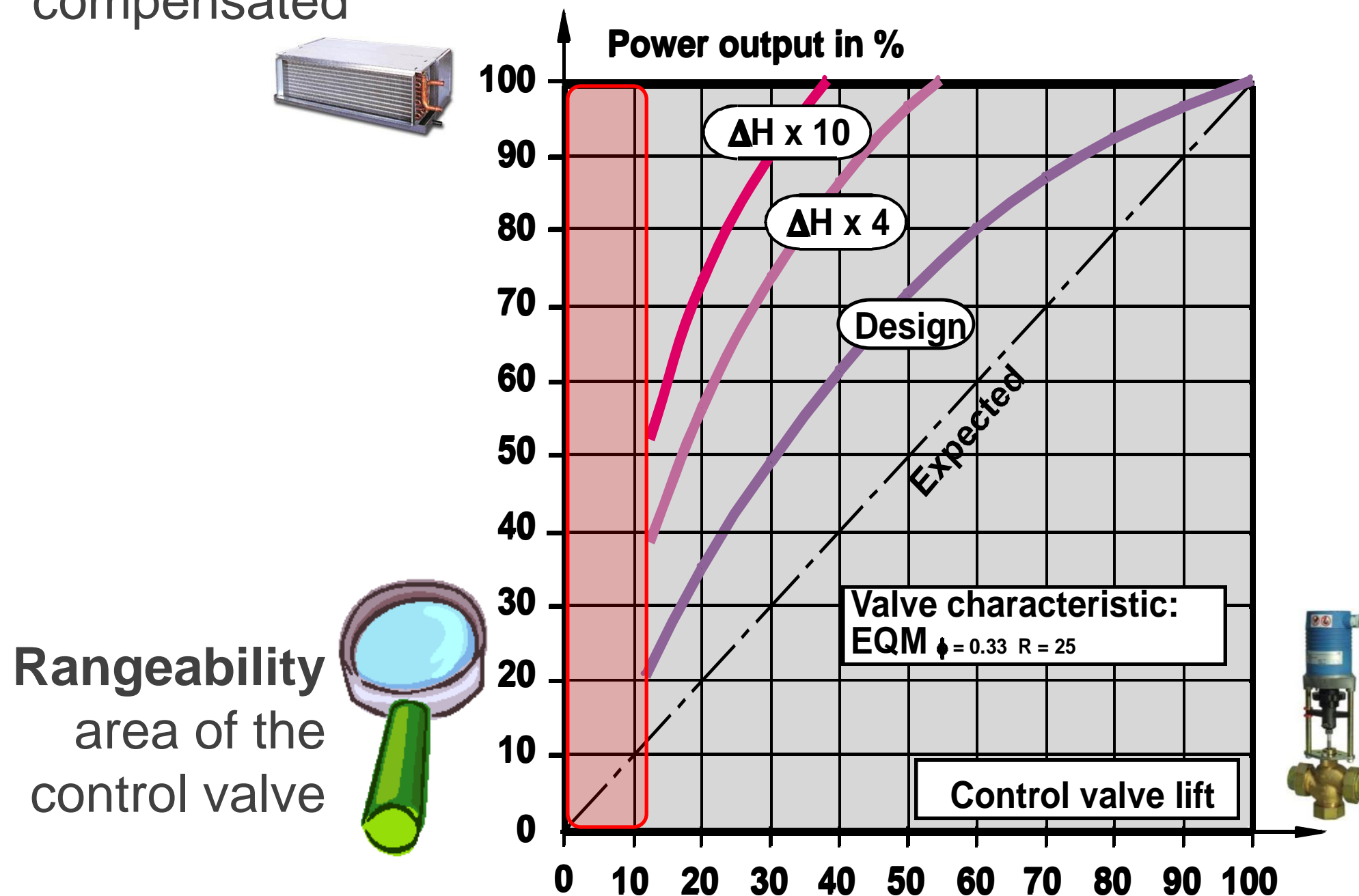
## Conclusion:

Control valves are generally oversized.



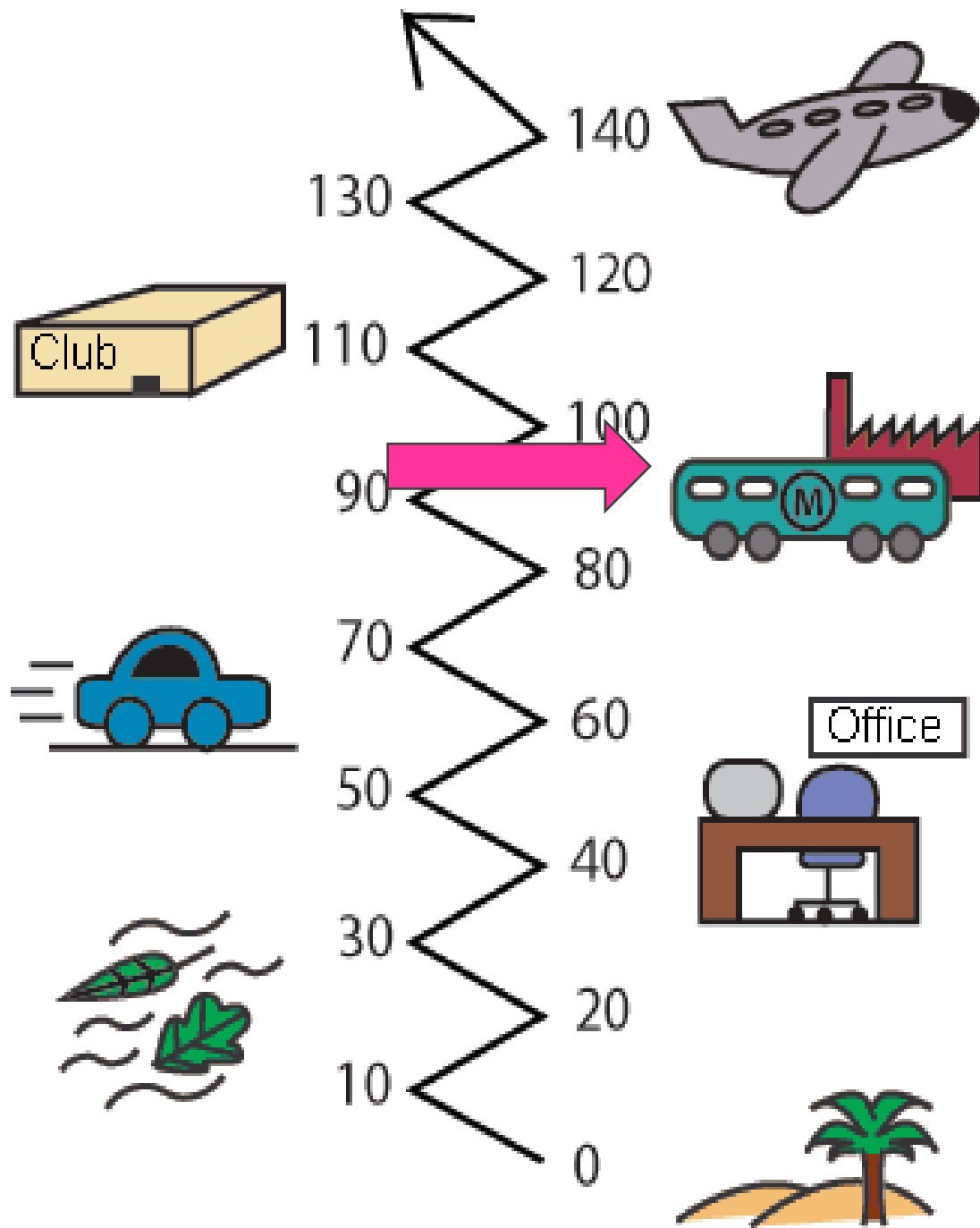
# Effect of $\Delta p$ variations on controlled heat output

$\Delta p$  variations distort the characteristic of the control valve  
 $\Rightarrow$  the nonlinear characteristic of the terminal unit is no longer compensated

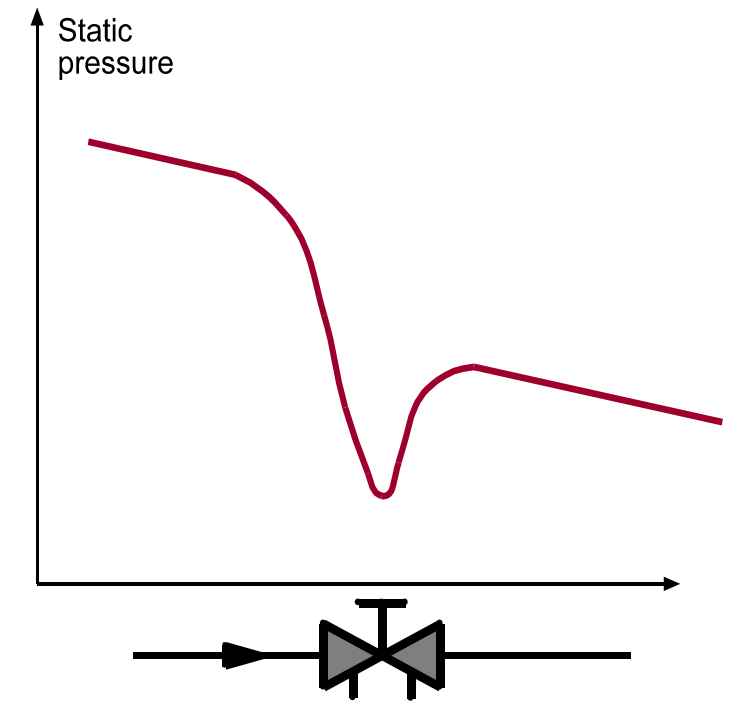


# Noise

Sound pressure level [dB]



**Cavitating valve**



**RULE OF THUMB :**  
Static pressure at the inlet of the valve should be at least twice the pressure drop in the valve.

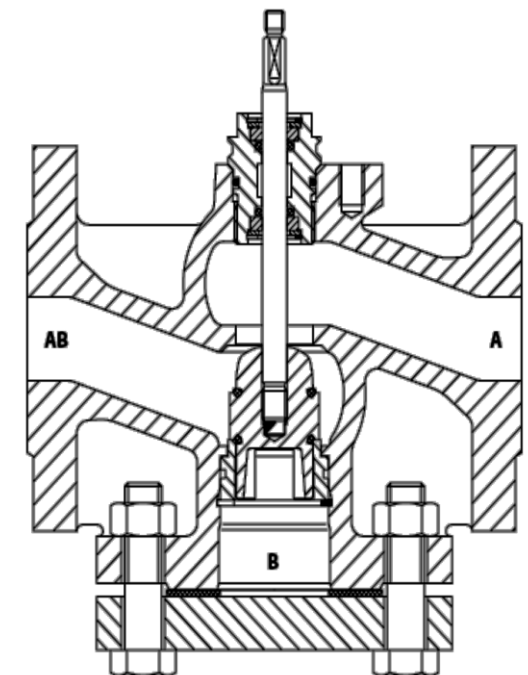
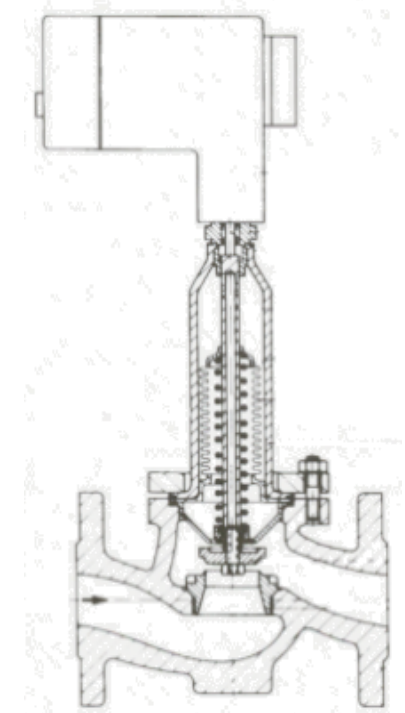
Engineering  
GREAT solutions

# Closing of control valves

According to its design, each valve has a required actuation **close-off force or torque** that depends on:

- Tension of the return spring, if any,
- Friction with o-rings and seals,
- Differential pressure applied on the plug.

Each control valve/actuator combination has a certain **close-off differential pressure**



Summary and Max. close-off differential pressure  $\Delta P_c$

Type	Conn. DN in.	Kv Cv		Kv Cv		MZ18L / 18A / 18B 180 N (40 lbf.) Max. $\Delta P_c$ kPa psi	MZ10T 96 N (22 lbf.) Max. $\Delta P_c$ kPa psi
		Kv	Cv	Kv	Cv	kPa	psi
VZ22	15 ½"	0.16	0.19			1600	232
VZ22	15 ½"	0.25	0.29			1600	232
VZ22	15 ½"	0.40	0.47			1600	232
VZ22	15 ½"	0.63	0.74			1600	232
VZ22	15 ½"	1.00	1.17			1200	174
VZ22	15 ½"	1.6	1.9			1200	174
VZ22	20 ¾"	2.5	2.9			400	58
VZ22	20 ¾"	4.0	4.7			400	58
		A-AB:		B-AB:			
VZ32	15 ½"	0.25	0.29	0.16	0.19	800	116
VZ32	15 ½"	0.40	0.47	0.25	0.29	800	116
						500	73



## Hydronic condition no. 2

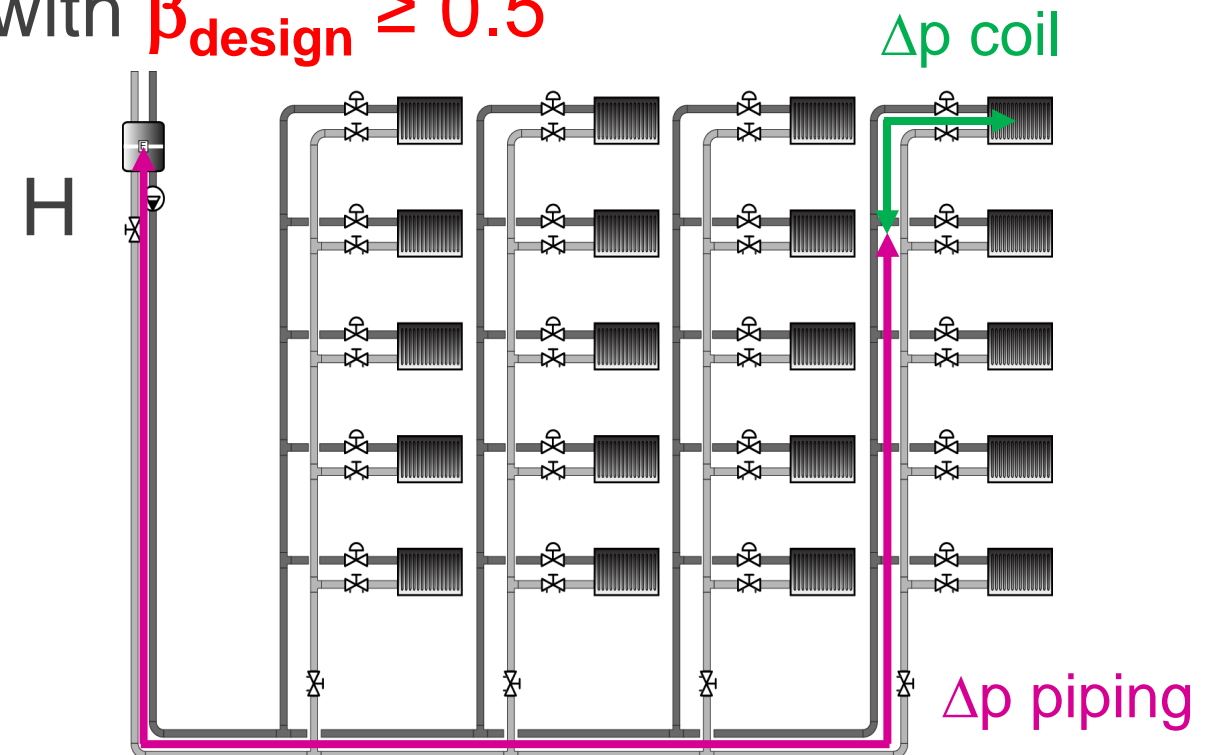
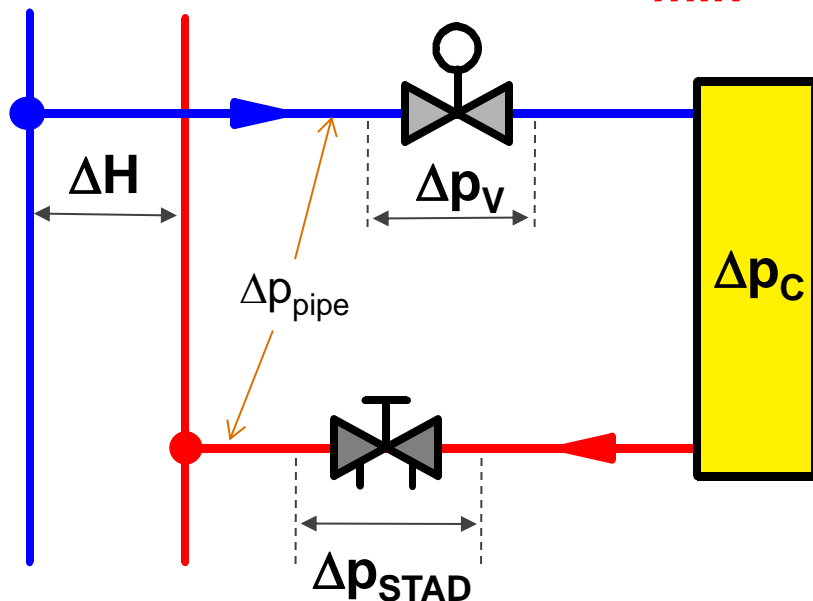


The differential pressure across control valves must not vary too much.

# Control valve authority

To achieve good control it's recommended to fulfill two rules on authority:

1. Size the control valve with a Cv with  $\beta_{\text{design}} \geq 0.5$
2. Ensure that  $\beta_{\text{min}} \geq 0.25$



## Rule no 1:

$$\Delta p_v \geq \Delta p_C + \Delta p_{\text{pipe}} + \Delta p_{\text{STAD}}$$

or

$$\Delta p_v \geq 0.5 \times \Delta H$$



$$\beta_{\text{design}} \geq 0.5$$

## Rule no 2:

$$\Delta p_v \geq (\Delta p_{\text{piping}} + \Delta p_C)/3$$

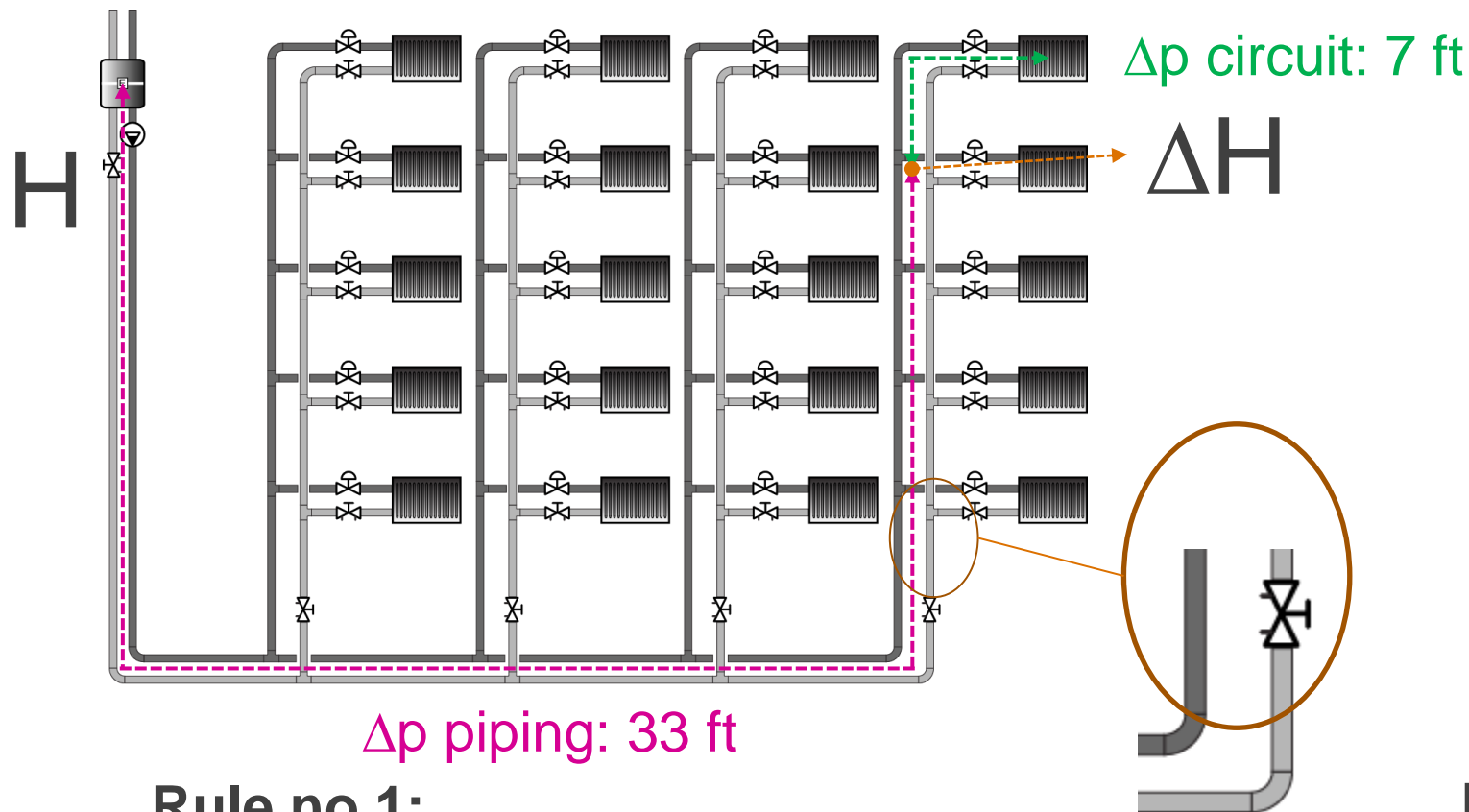
or

$$\Delta p_v \geq 0.25 \times H$$



$$\beta_{\text{min}} \geq 0.25$$

# Improved control by correct control valve sizing



## IDEA

Ensure **design** authority of **at least 0.5** and **minimum** on **0.25** in **all** control valves in the **worst** conditions.

$$\beta_{design} = \frac{\Delta P_{Control\ valve\ fully\ open\ and\ design\ flow}}{\Delta H}$$

$$\beta_{min} = \frac{\Delta P_{Control\ valve\ fully\ open\ and\ design\ flow}}{H}$$

### Rule no 1:

For obtaining a design authority of 0.5:

$\Delta p$  in control valve must be  $\geq 0.5 \times \Delta H$

Since  $\Delta p$  circuit = 7 ft,  
 $\Delta p$  in control valve must be  $\geq 7$  ft

Final pump head = 40 + 7 = **47 ft**

$\beta_{design} = 7/14 = 0.5$  but

$\beta_{min} = 7/47 = 0.15$



### Rule no 2:

For obtaining a minimum authority of 0.25:

$\Delta p$  in control valve must be  $\geq 0.25 \times H$

Since  $\Delta p$  piping + circuit = 33 + 7 = 40 ft,  
 $\Delta p$  in control valve must be  $\geq 13.3$  ft (40/3)

Final pump head = 40 + 13.3 = **53.3 ft**

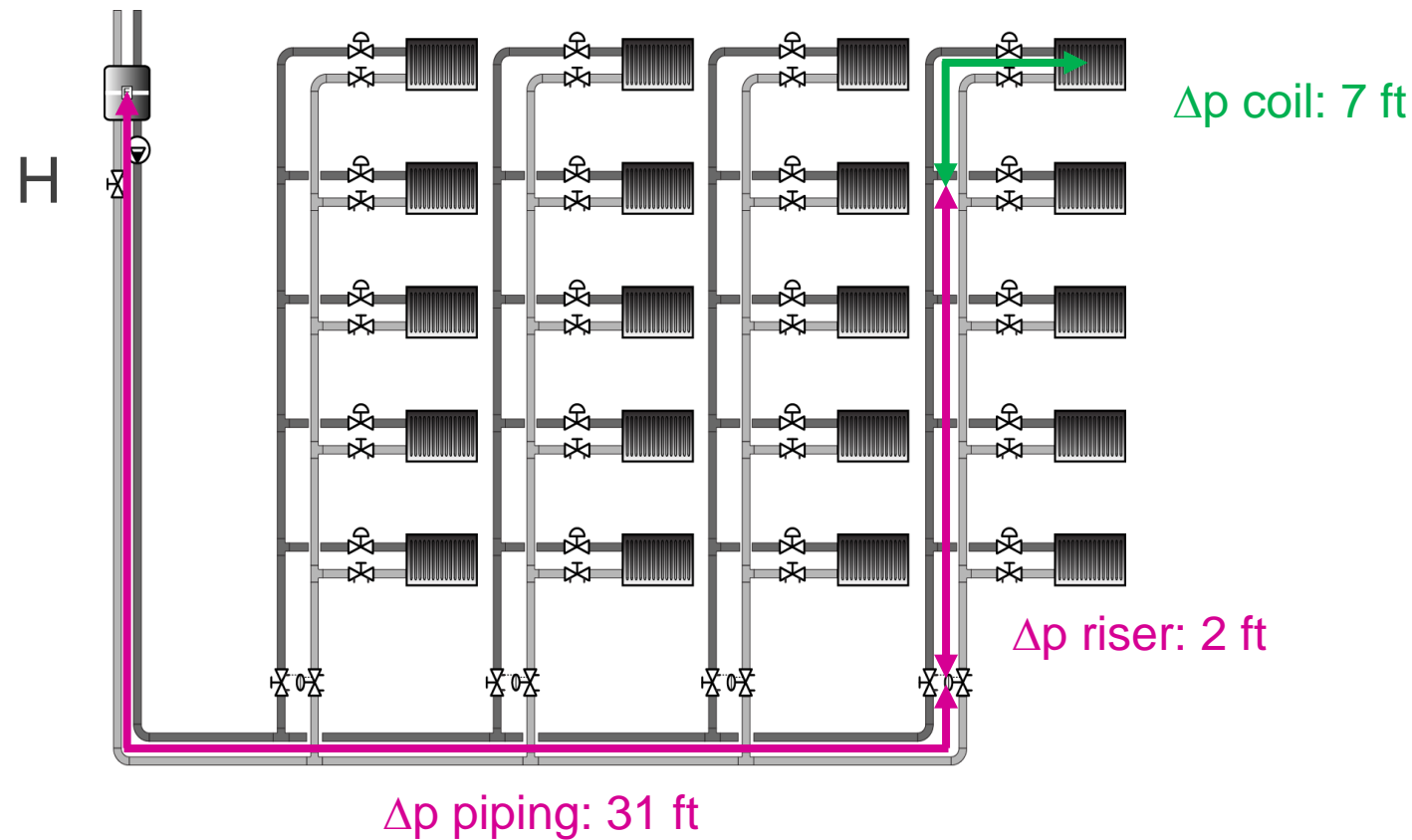
$\beta_{design} = 13.3/20.3 = 0.66$  and

$\beta_{min} = 13.3/53.3 = 0.25$





# Improved control with reduced pumping energy



Control valve sizing with Dp control:

For obtaining a design authority of 0.5 and min of 0.25:

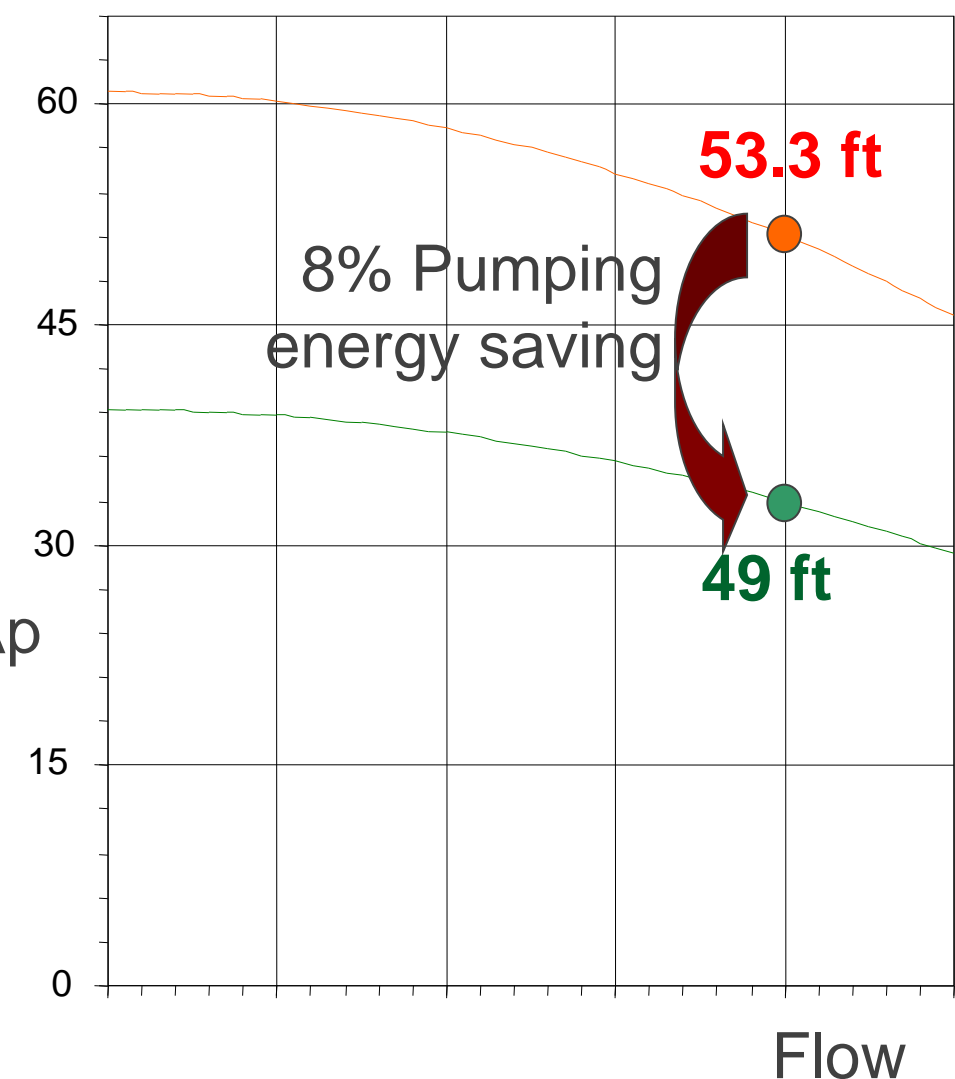
$\Delta p$  in control valve must be  $\geq 0.5 \times \Delta H$  and  $\geq 0.25$  of stabilized  $\Delta p$

Since  $\Delta p$  piping +  $\Delta p$  circuit = 7 ft,  
 $\Delta p$  in control valve must be  $\geq 7$  ft

Final stabilized  $\Delta p = 7 + 7 + 2 = 16$  ft

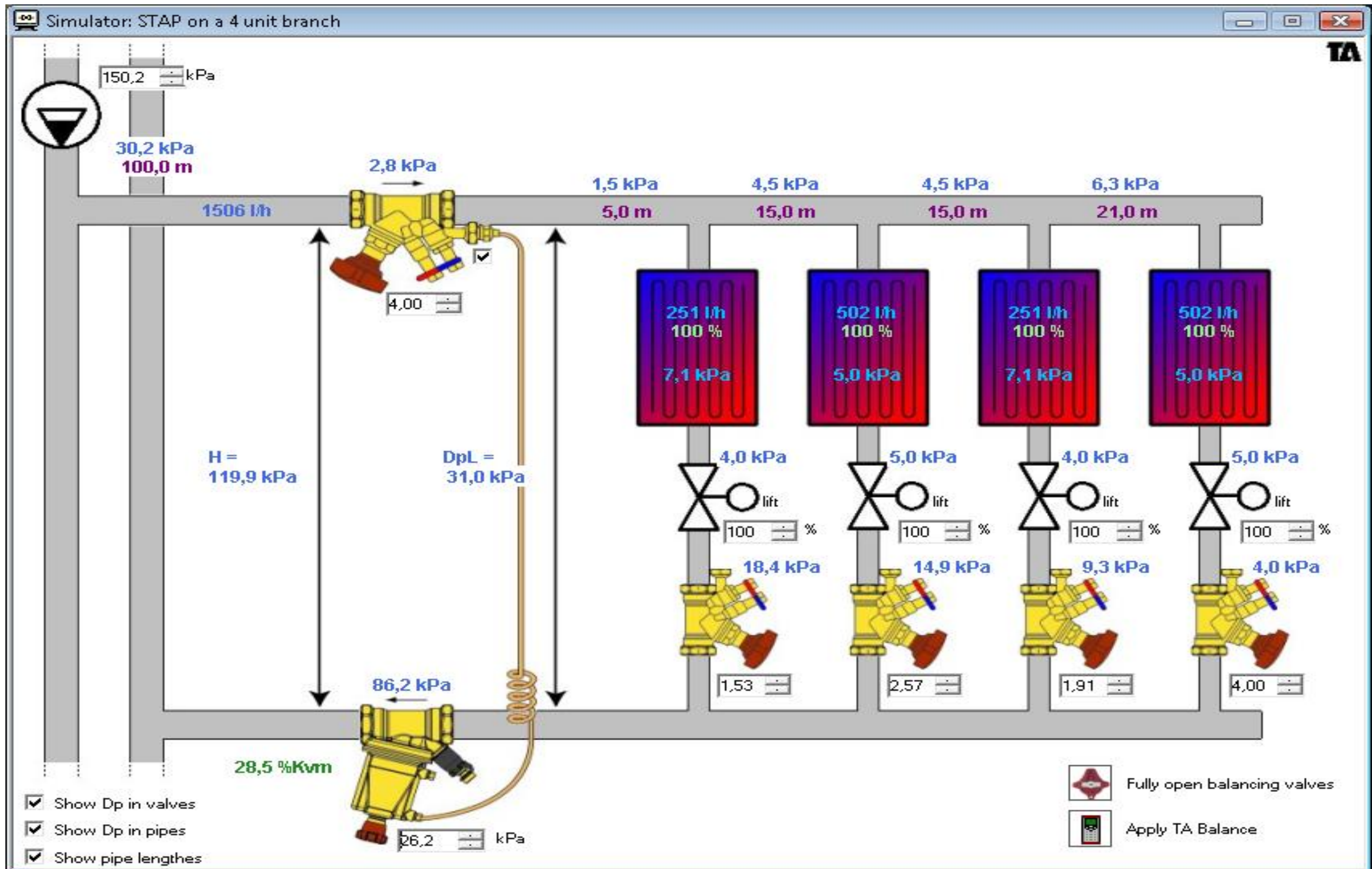
$\beta_{\text{design}} = 0.50$  and  $\beta_{\text{min}} = 0.44$

Head (ft)



16 Final pump head = 31 + min  $\Delta p$  of DpC (2 ft) + 2 + 7 + 7 = **49 ft**

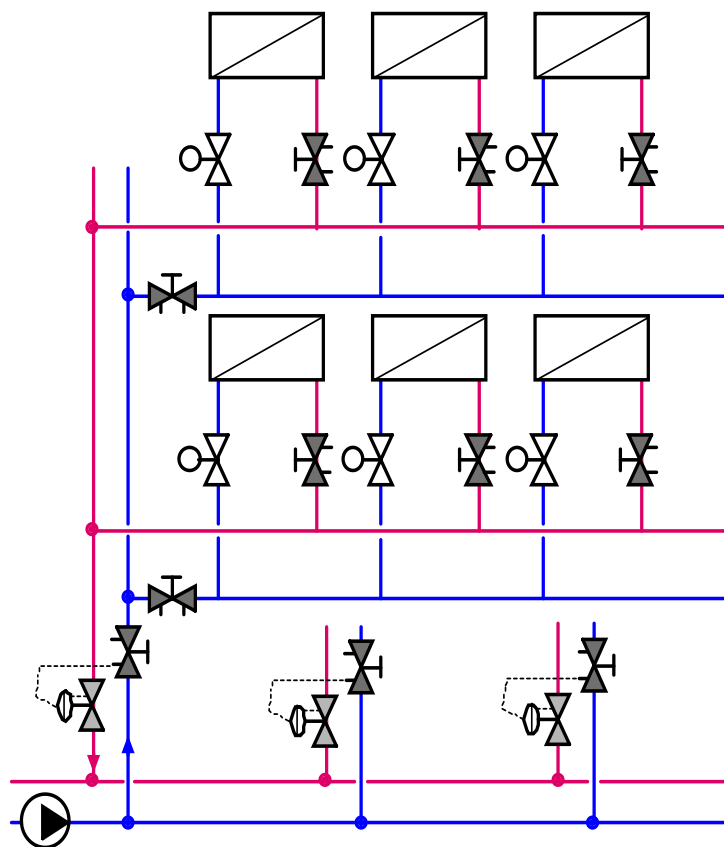
# Simulation



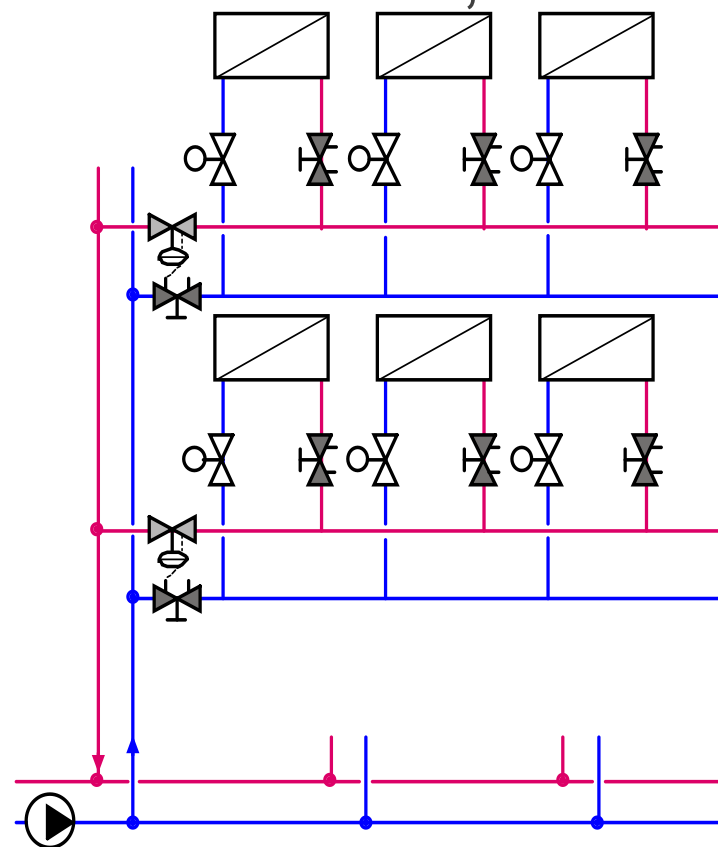
# Dp controller position

Depending on project structure, Dp control will be applied:

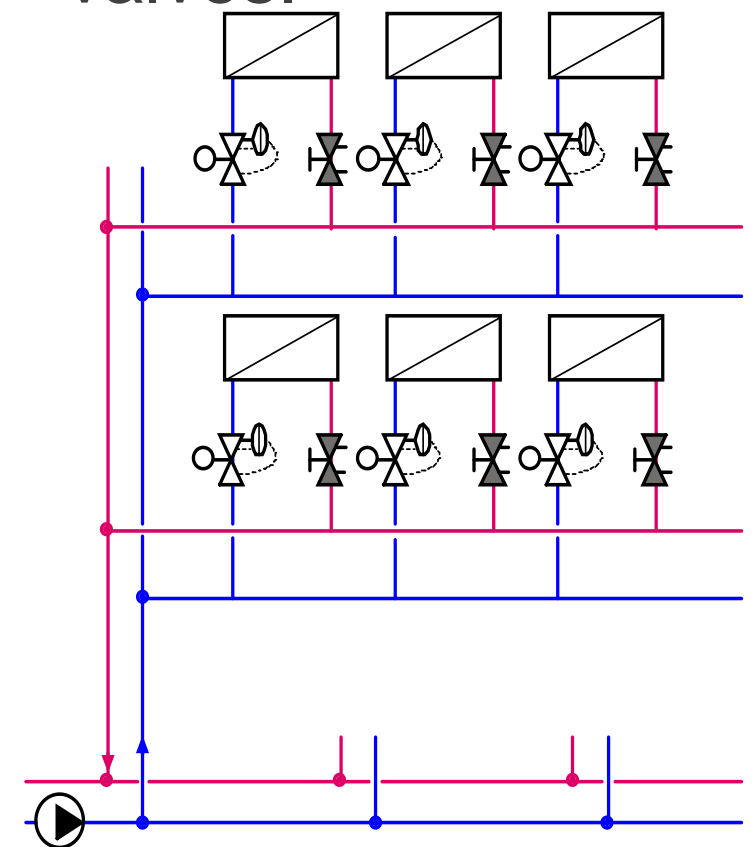
On risers,



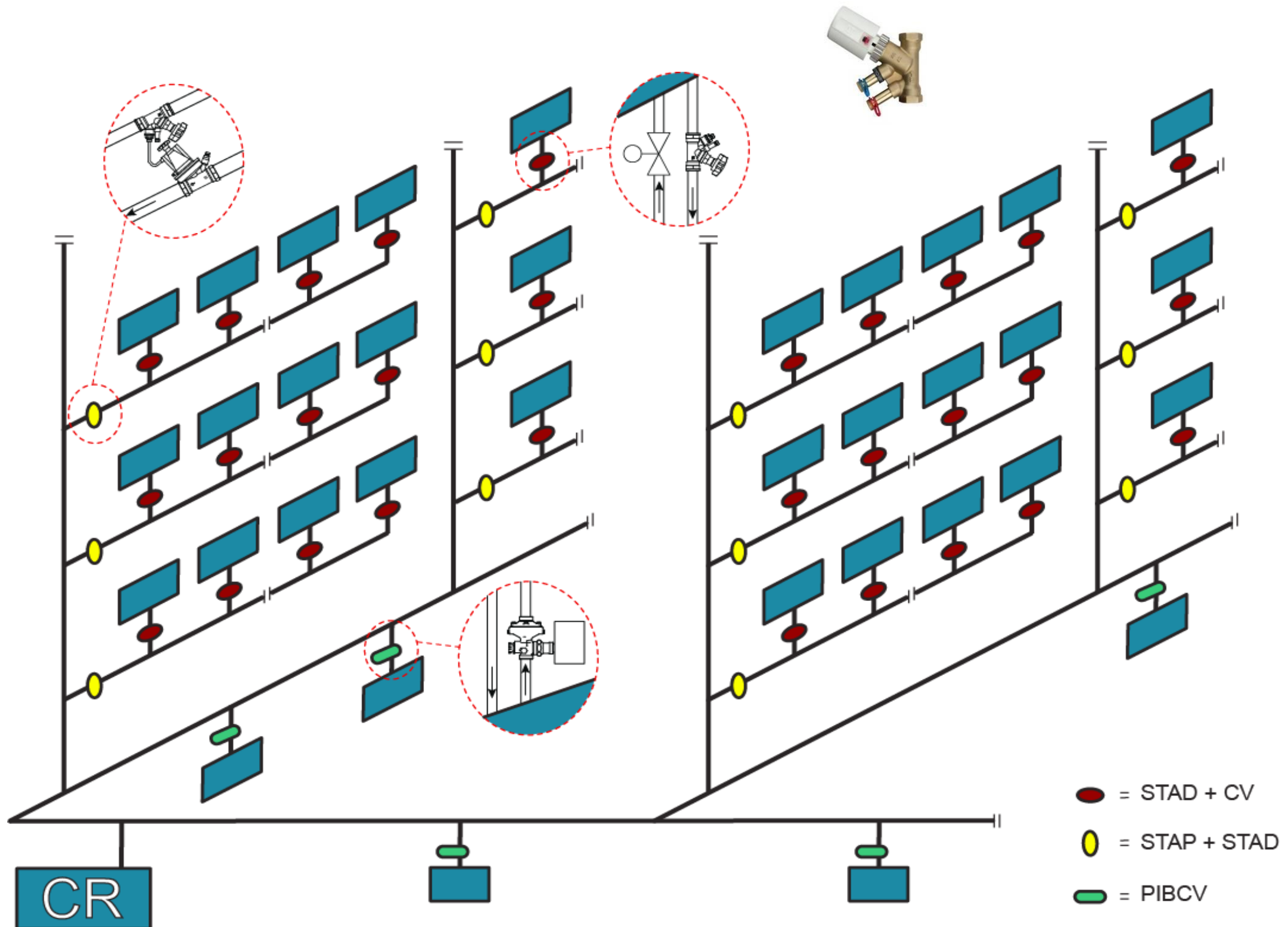
On branches,



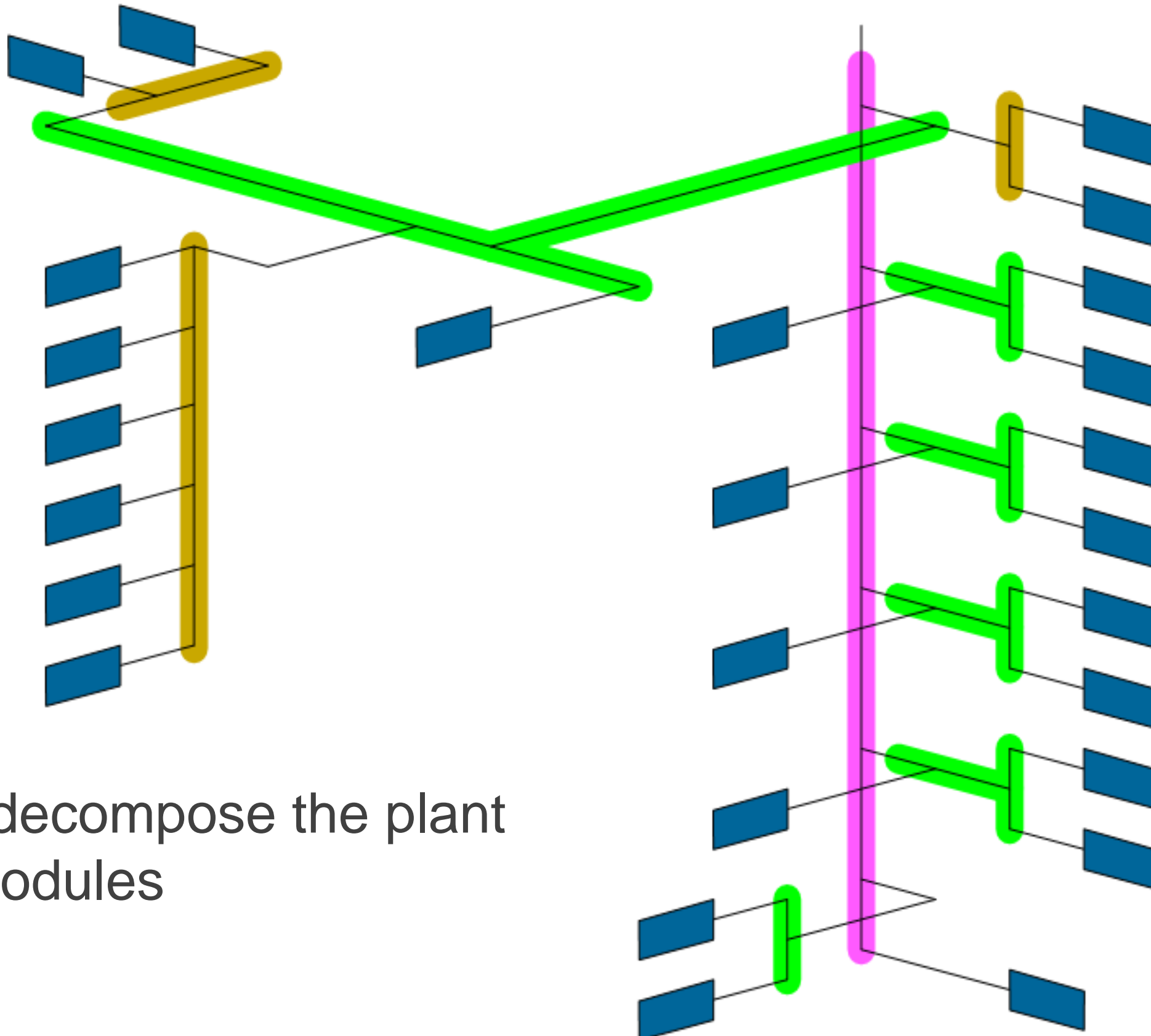
On control valves.



# Bigger plant with different Dp control configurations



# Find the best Dp control solution...



First, decompose the plant into modules



The savings are  
real!!

# Hong-Kong PolyTech University

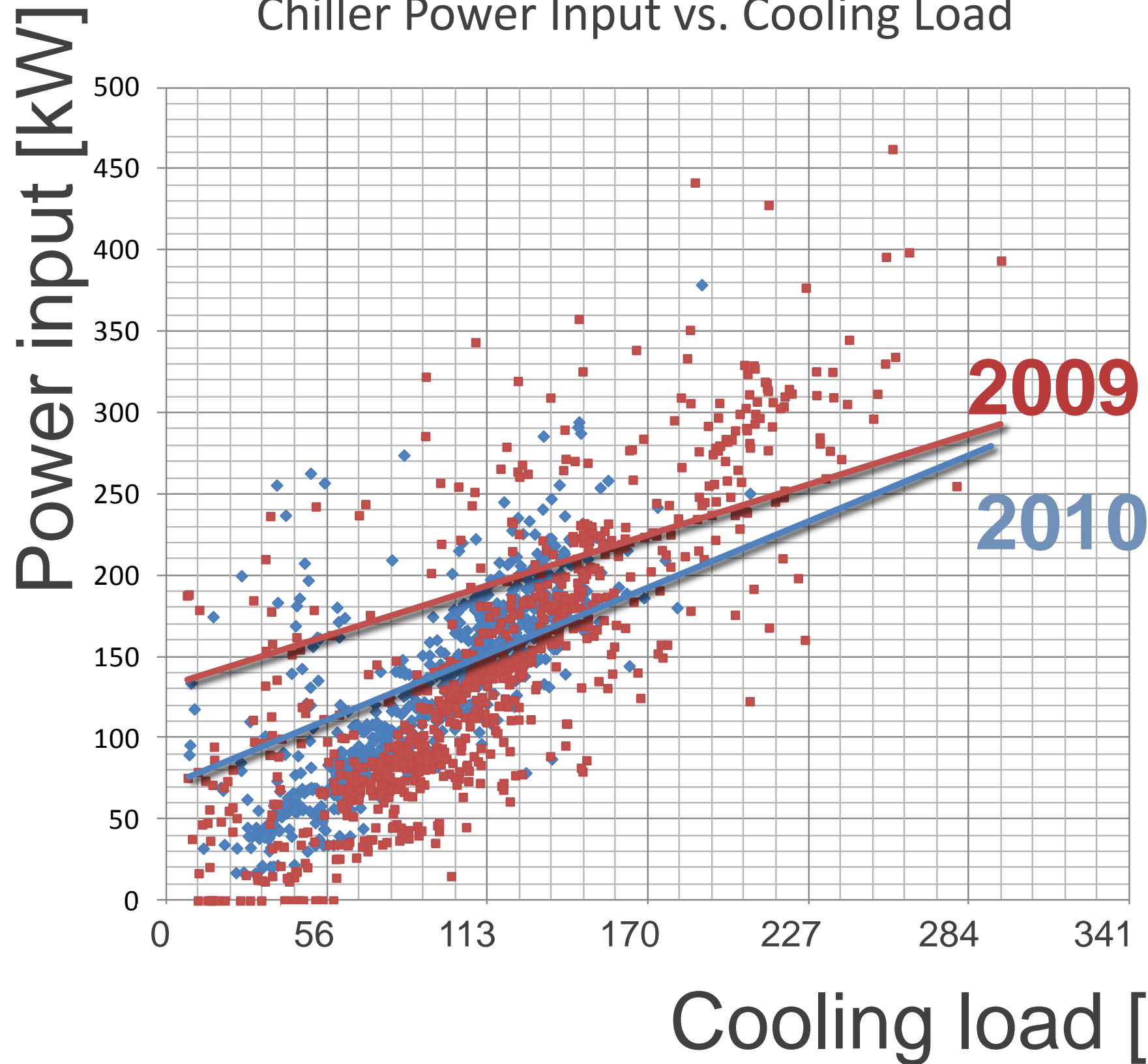


- › Renovation of 2 University buildings with a total of 106000 ft<sup>2</sup> (9840 m<sup>2</sup>)
- › Installed cooling capacity:
  - › Building 1 : 1452 tons refrigeration.
  - › Building 2 : 1730 tons refrigeration.

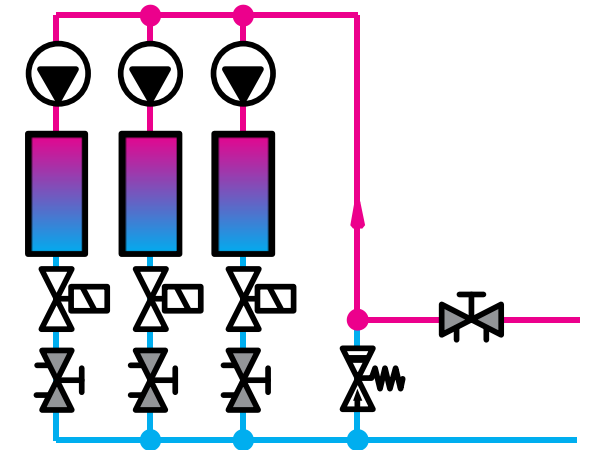


# Local University campus building 1 – chiller saving

Chiller Power Input vs. Cooling Load



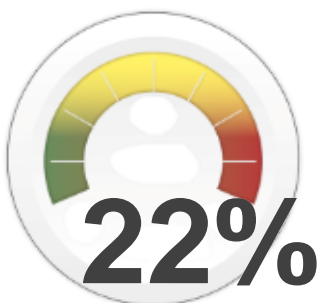
- Variable secondary flow with differential pressure bypass



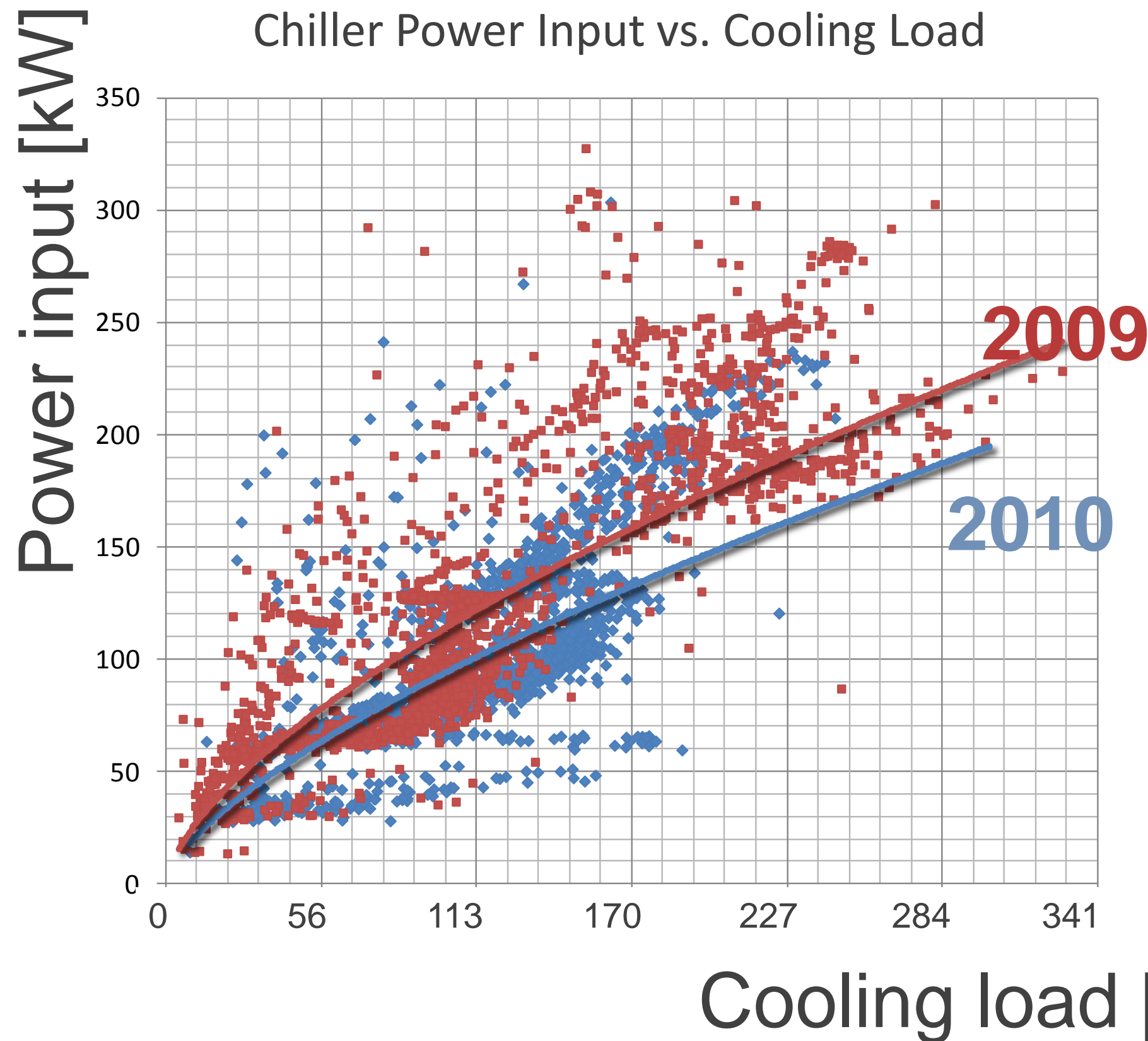
- Dp controllers at on-off control FCU groups and PAU/AHUs and re-balanced



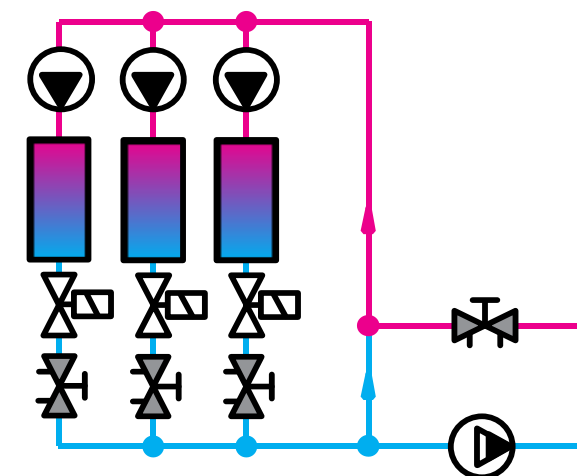
- Annualized 22% chiller energy savings



# Local University campus building 2 – chiller saving



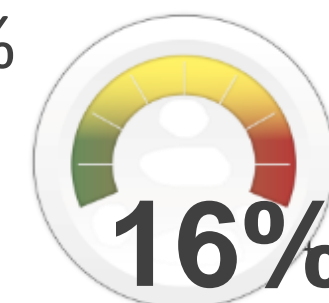
- Variable flow primary-secondary system



- Addition of Dp controllers at FCU groups zones and pressure independent control valves for PAU/ and re-balanced



- Annualized 16.5% chiller energy saving



## Questions?