

Skidmore, Owings & Merrill LLP
Performative Design Group



Reducing Carbon Impact in Singapore through On-Site Tri-Generation and Bio-Fuels

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06/09/2014

Project and Program Information

TOWER COMPETITION SINGAPORE

- **Singapore, China**
- Hotel Program
- 150 Floors
- 2,750 M² Floor Plates
- 100 M² per room
- One person per room
- 412,500 M² Total



Project and Program Information

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Design Day Information

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ASHRAE 99.6% Heating Design Conditions for Singapore CZ 1A

73°F (22.9°C) Design Dry-Bulb Temperature

73°F (22.9°C) Wet-Bulb at Max Dry Bulb

101133 Pa Barometric Pressure

2.1 m/s Wind Speed

340° Wind Direction {N=0, S=180}

ASHRAE 1% Cooling Design Conditions for Singapore CZ 1A

91°F (32.8°C) Design Dry-Bulb Temperature

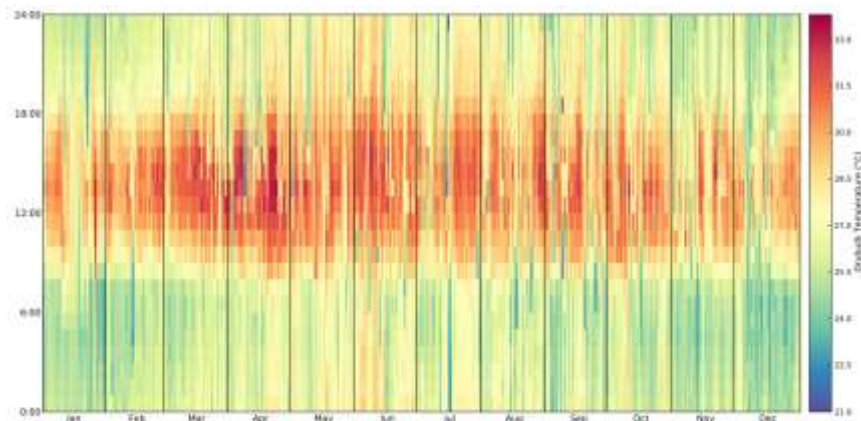
79°F (26.2°C) Wet-Bulb at Max Dry Bulb

10°F (5.6°C) Daily Temperature Range

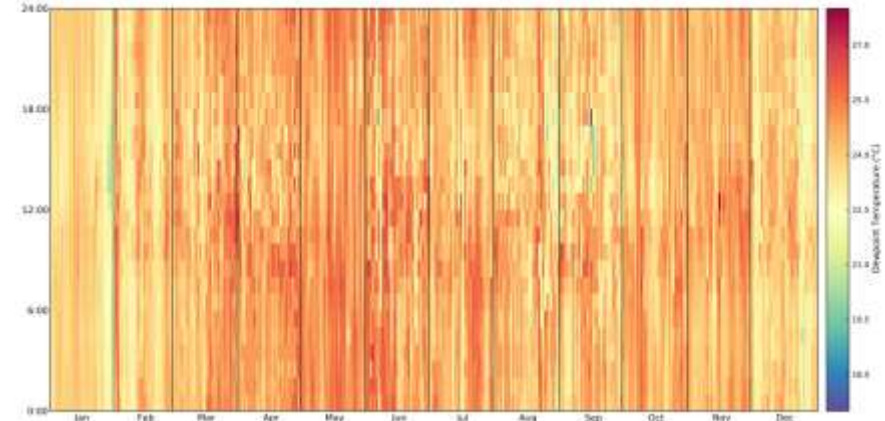
101133 Pa Barometric Pressure

4.3 m/s Wind Speed

30° Wind Direction {N=0, S=180}



Dry Bulb Temp [Scale: 21°C to 33°C]
Year round cooling requirement

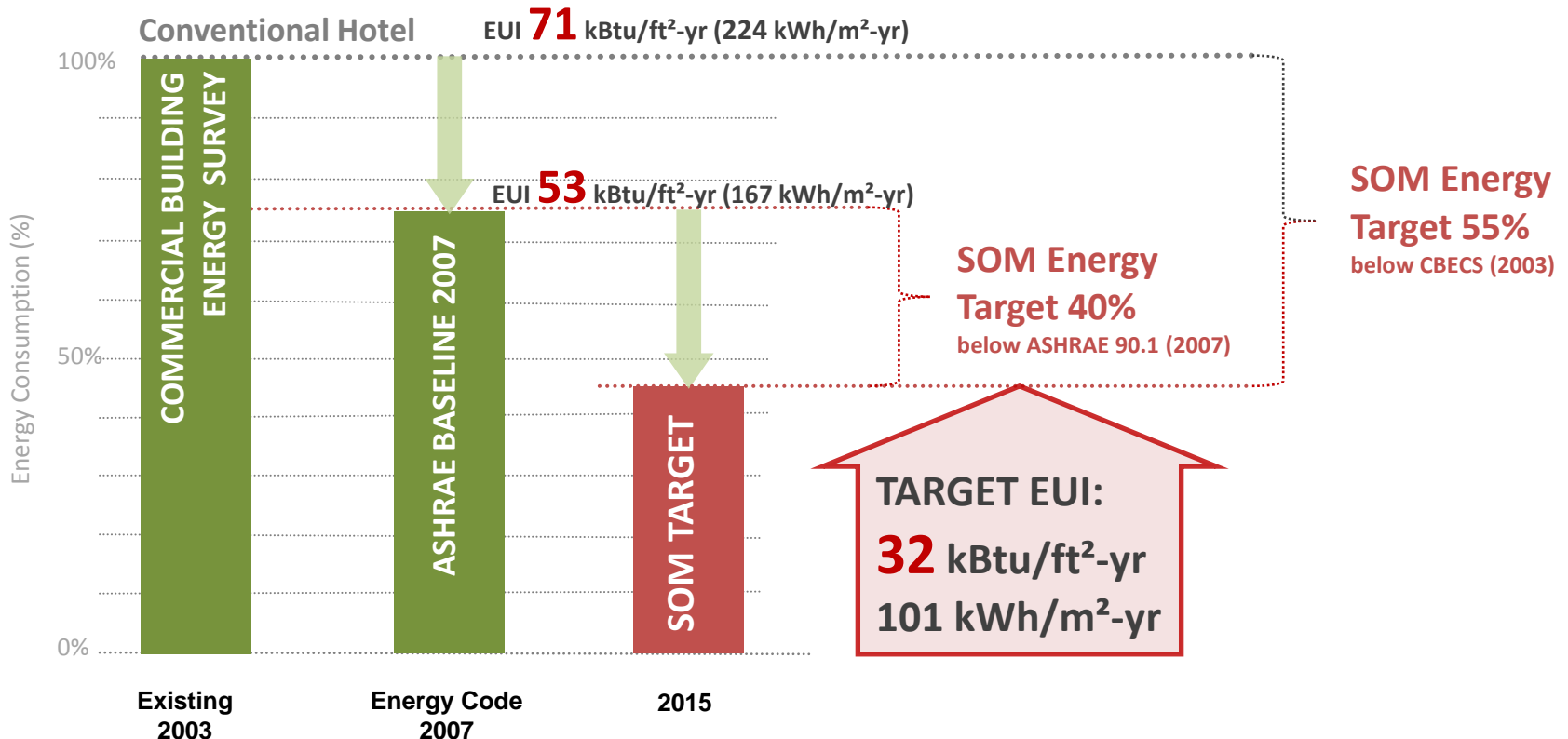


Dew-point Temp [Scale: 18°C to 27°C]
Year round dehumidification requirement

SOM High Performance Design Goals

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Fossil Fuel Sourced Energy Reduction Goal



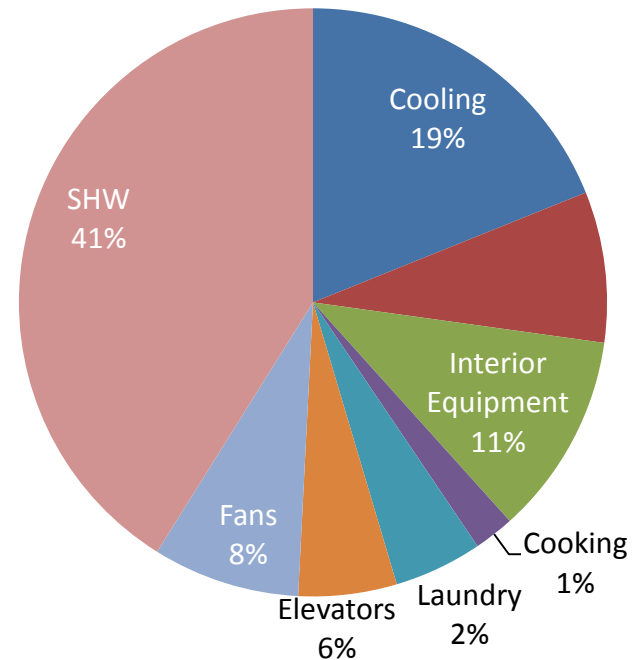
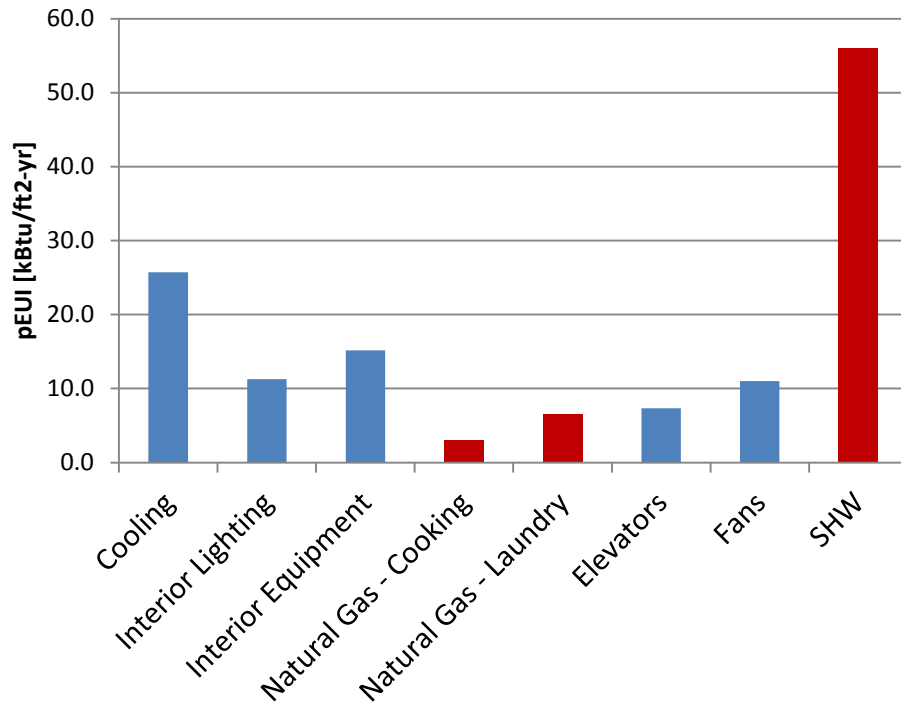
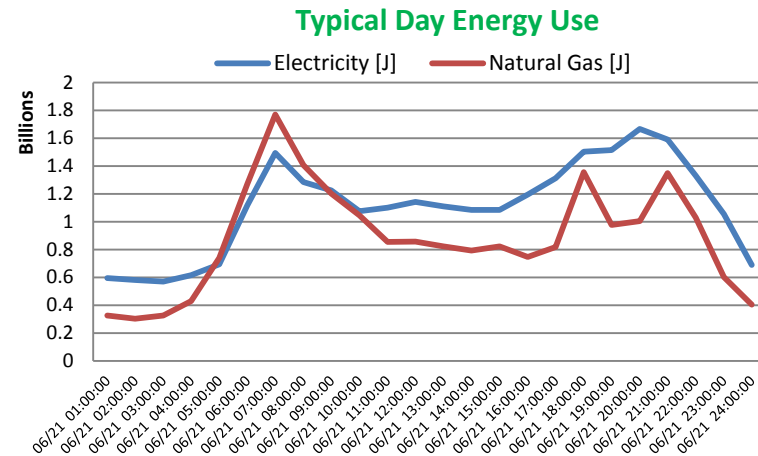
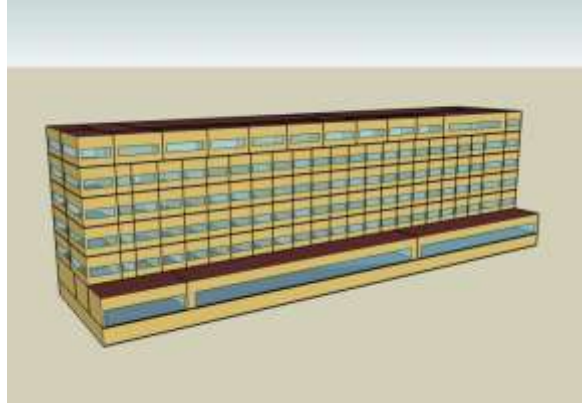
DoE Reference Hotel run in Singapore

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pEUI:

140 kBtu/ft²-yr

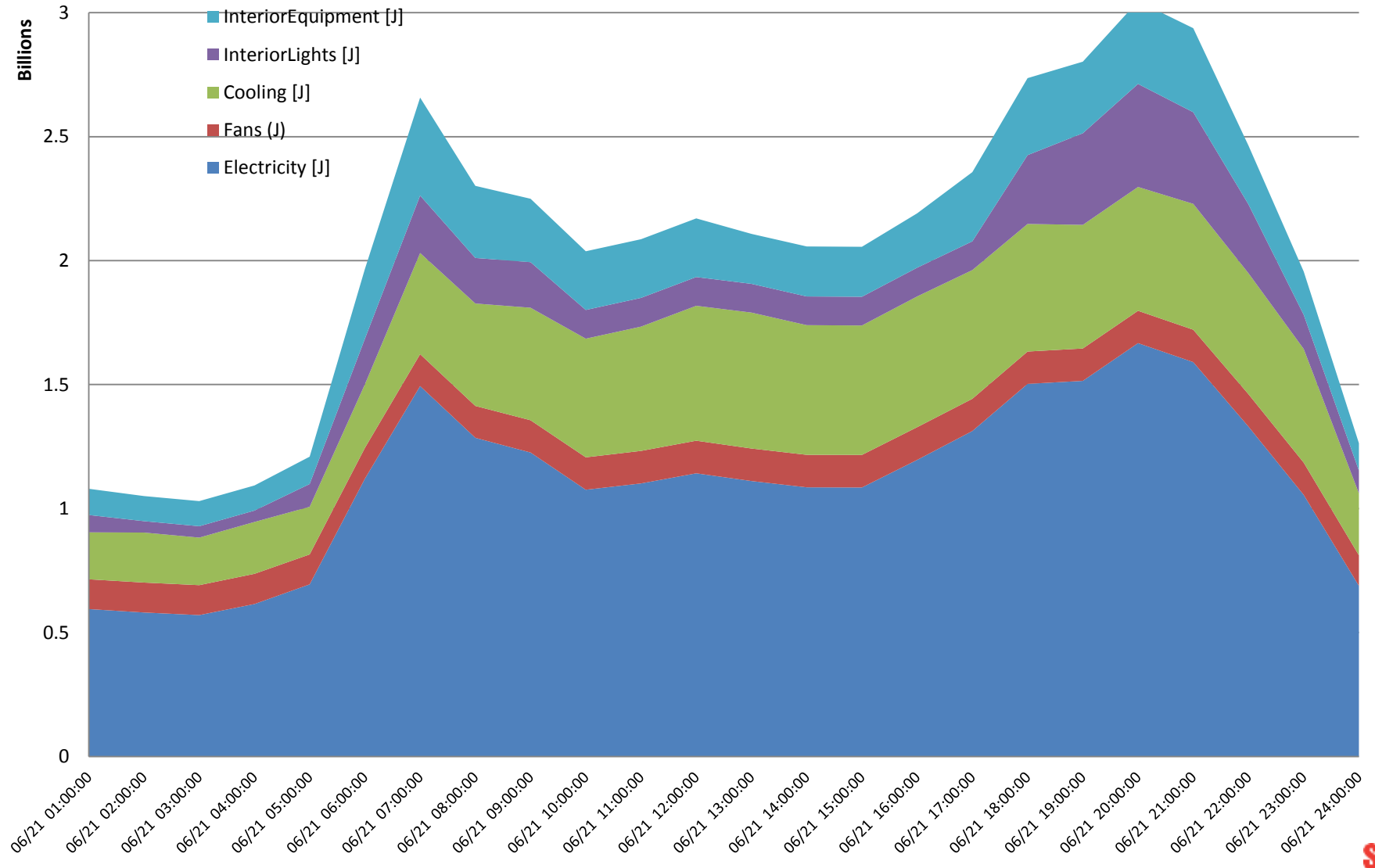
441 kWh/m²-yr



DoE Reference Hotel Load Profiles

TOWER COMPETITION SINGAPORE

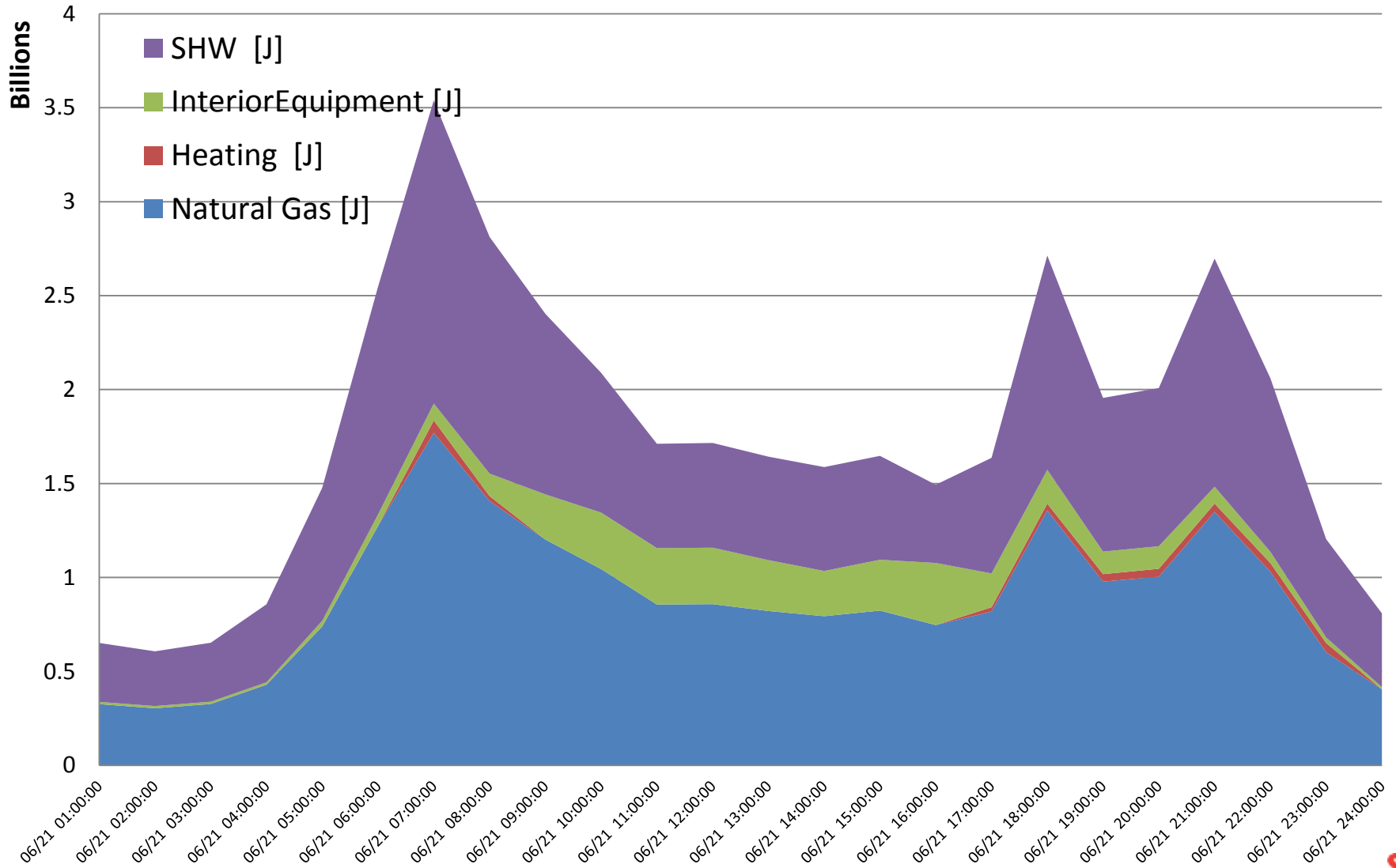
Electricity Load Profile



DoE Reference Hotel Use Profiles

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Natural Gas Consumption



Project Specific Concept Analysis Model Parameters

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Base Shape: Square

Length: 52.5 m

Width: 52.5 m

Floors: 150

Floor to Floor: 4.0 m

WWR – 40%

Envelope Properties: 90.1-2007 Climate Zone 1A Defaults

HVAC: Packaged Terminal Heat Pumps System 2

Lighting Power Density = 1 W/ft²

Miscellaneous Power Density = 1 W/ft²

Infiltration = 0.06 cfm/ft² ext wall area

Service Hot Water:

Peak flow of 3.0 GPM per Guest room

(2.5 GPM Shower, 0.5 GPM Faucet)

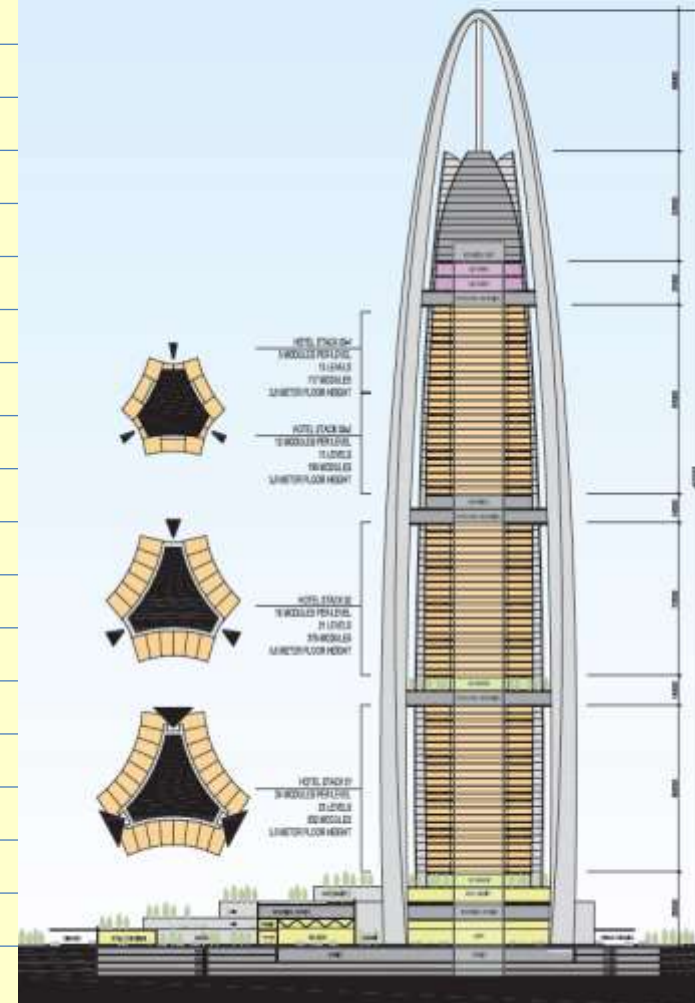
Peak flow of 90 GPM for all Kitchen SHW consumption

Peak flow of 90 GPM for all Laundry SHW consumption

Natural Gas Equipment:

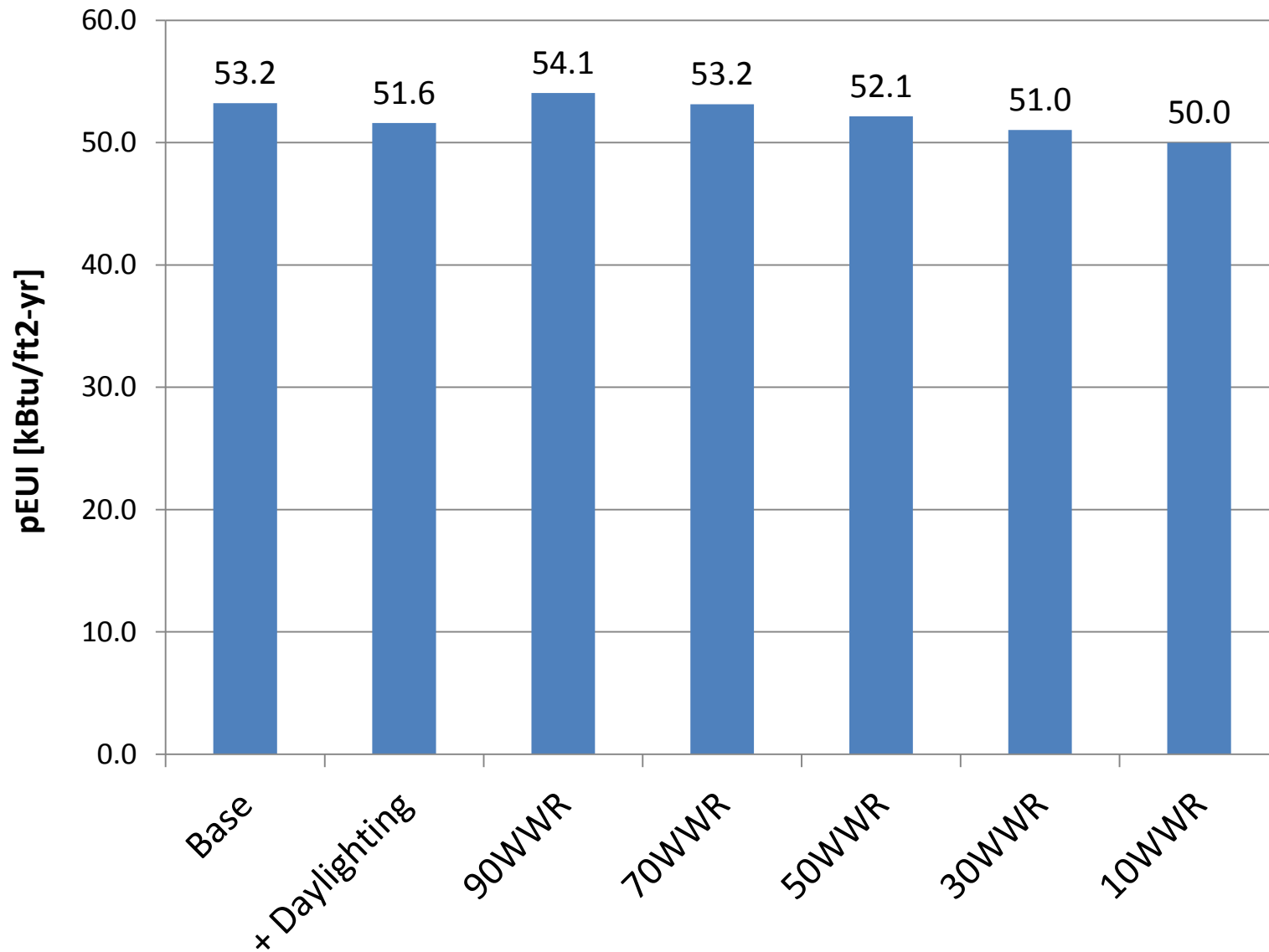
500 kW peak natural gas demand for cooking

500 kW peak natural gas demand for laundry



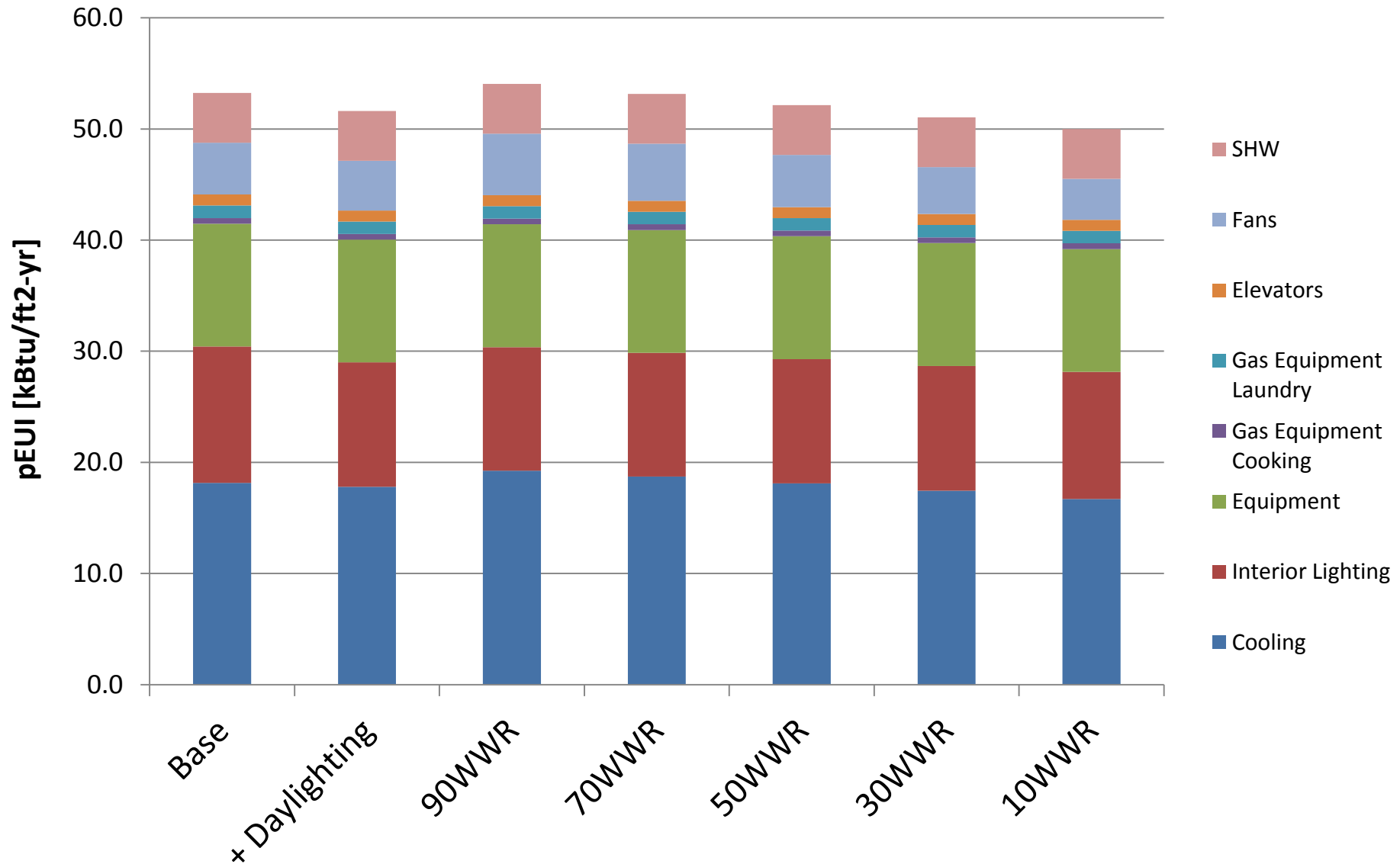
Parametric WWR Analysis of Square Floor Plate

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Parametric WWR Analysis of Square Floor Plate

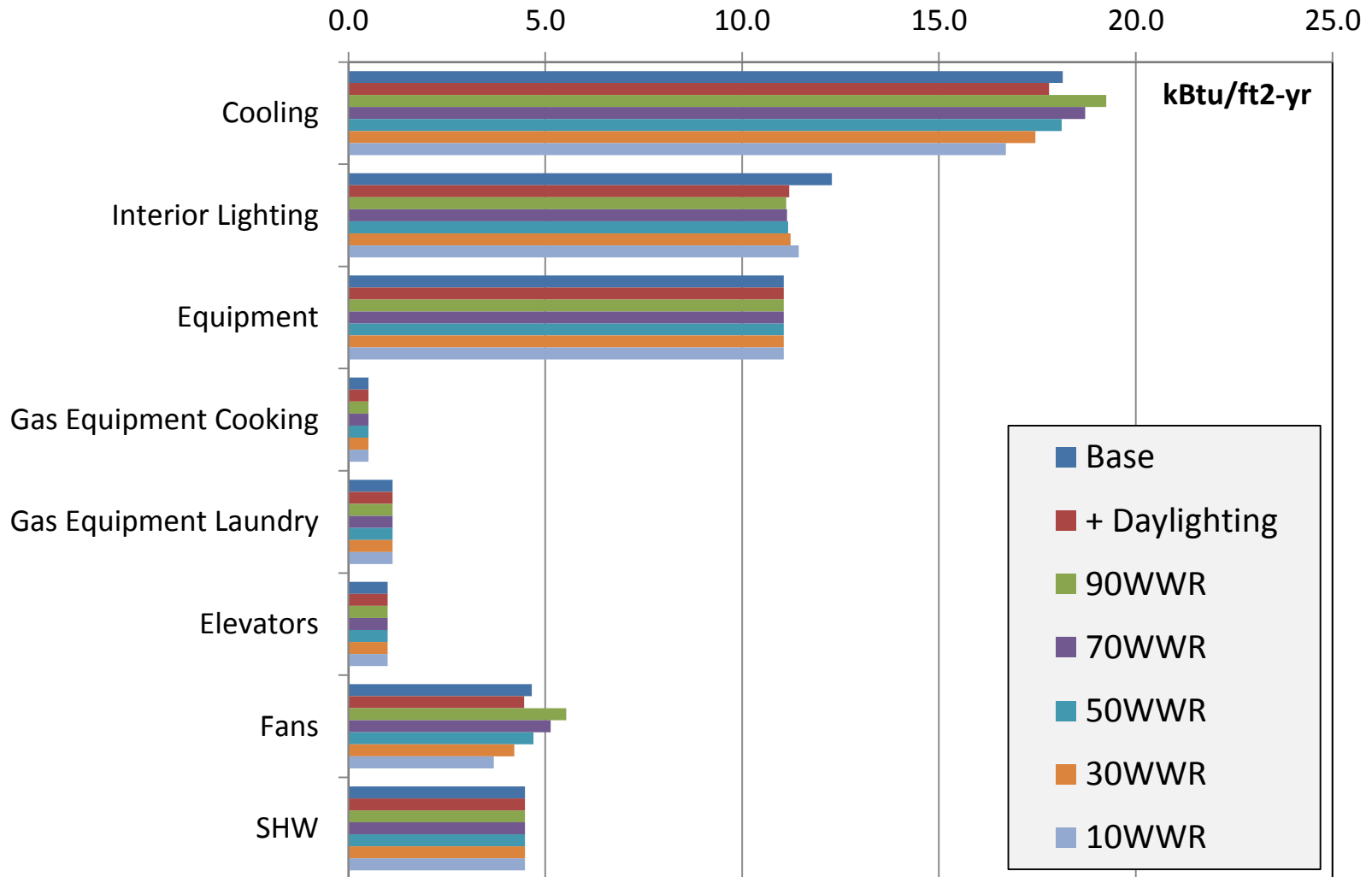
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Parametric WWR Analysis of Square Floor Plate

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Energy Consumption per End Use



Studies and Background Information

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CHP Studies Utilized as Basis of Analysis

http://www.epa.gov/chp/documents/wwtf_opportunities.pdf

<http://www.epa.gov/chp/markets/wastewater.html>

https://www.gov.uk/government/uploads/system/uploads/attachment_data/file/69400/anaerobic-digestion-strat-action-plan.pdf

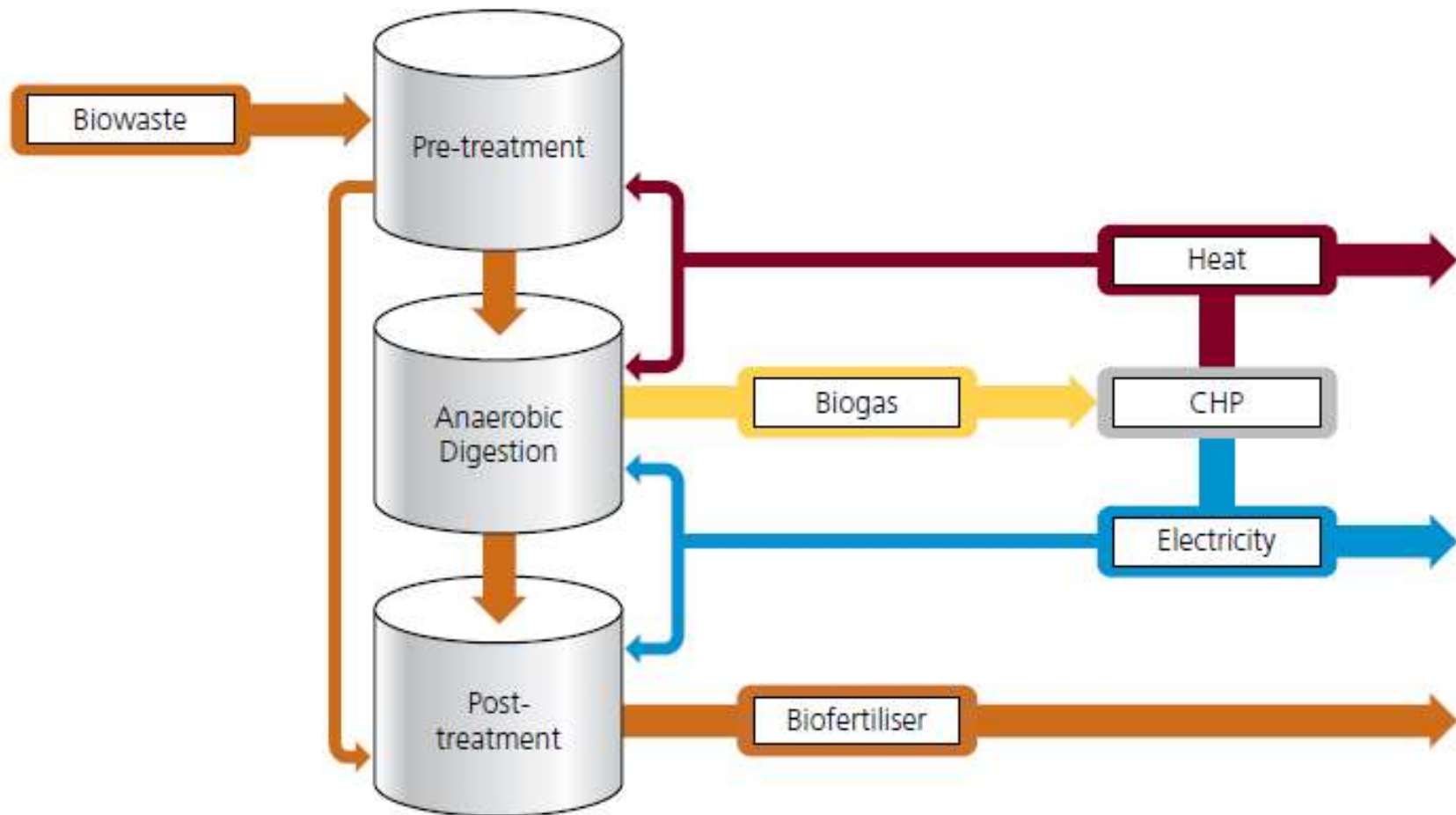
<http://www.diva-portal.org/smash/get/diva2:409206/FULLTEXT02>

<http://www.diva-portal.org/smash/get/diva2:324228/FULLTEXT01.pdf>

Anaerobic Digester Diagram

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Figure 1: Example of an AD plant configured to produce energy and biofertiliser from biowaste feedstock





Contents lists available at ScienceDirect

Applied Energy

journal homepage: www.elsevier.com/locate/apenergy



Thermally driven cooling coupled with municipal solid waste-fired power plant: Application of combined heat, cooling and power in tropical urban areas

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ARTICLE INFO

Article history:

Received 16 July 2010

Received in revised form 15 November 2010

Accepted 3 December 2010

Available online 30 December 2010

Keywords:

MSW incineration

Absorption chillers

Thermally driven cooling

Economic evaluation

Greenhouse gas reduction

Tropical urban areas

ABSTRACT

Energy recovery from flue gases in thermal treatment plants is an integral part of municipal solid waste (MSW) management for many industrialized nations. Often cogeneration can be employed for both enhancing the plant profitability and increasing the overall energy yield. However, it is normally difficult to justify traditional cogeneration in tropical locations since there is little need for the heat produced. The main objective of this article is to investigate the opportunities and potentials for various types of absorption technologies driven by MSW power plants for providing both electricity and cooling. Results show that cogeneration coupling with thermally driven cooling is sustainably and economically attractive for both electricity and cooling production. The thermally driven cooling provides significant potential to replace electrically driven cooling: such systems are capable of providing cooling output and simultaneously increasing electricity yield (41%). The systems are also capable of reducing the fuel consumption per unit of cooling in comparison with conventional cooling technology: a reduction of more than $1 \text{ MW}_{\text{fuel}}/\text{MW}_{\text{cooling}}$ can be met in a small unit. MSW power plant coupled with thermally driven cooling can further reduce CO_2 emissions per unit of cooling of around 60% as compared to conventional compression chiller and has short payback period (less than 5 years).

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CHP Diagram

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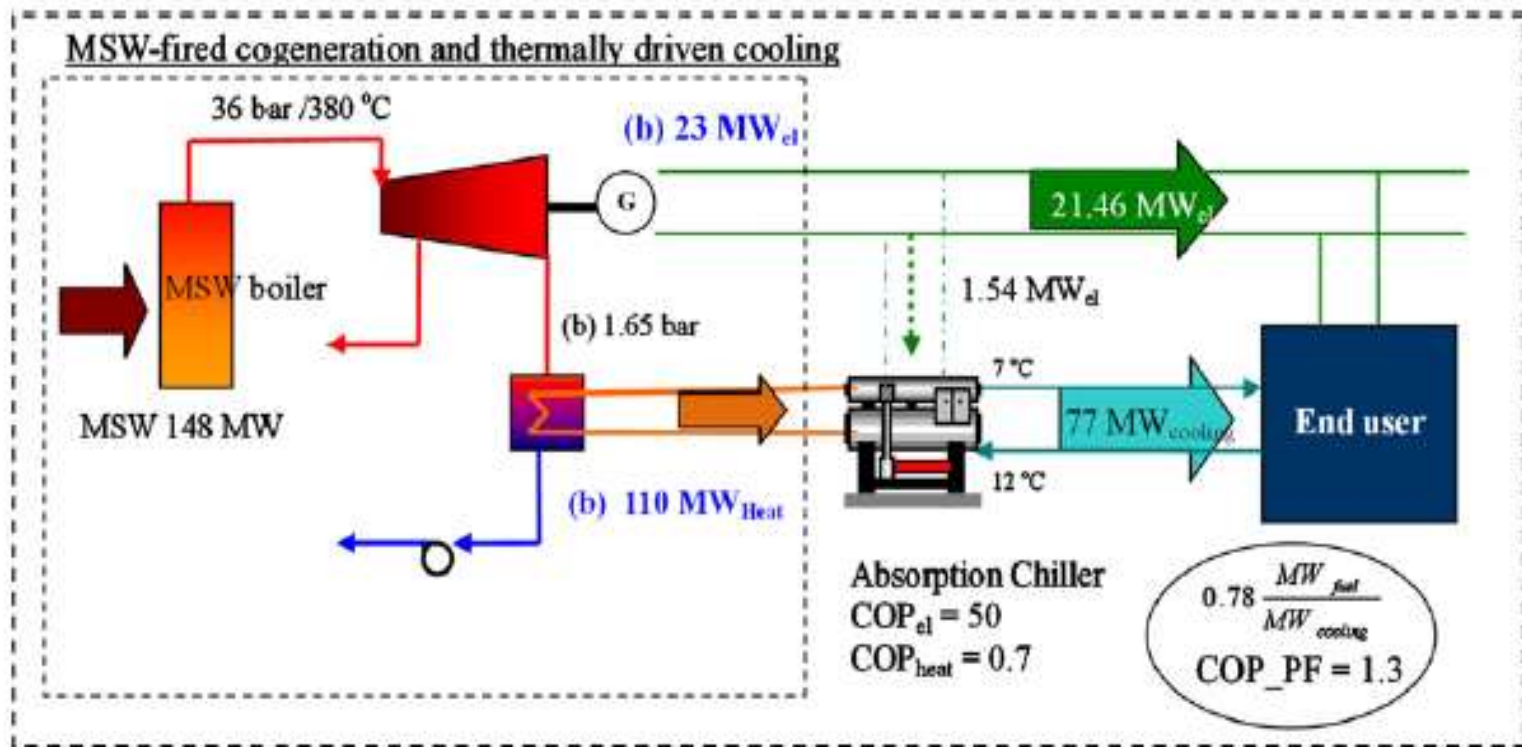


Fig. 3. Energy conversion chain from cogeneration of MSW power plant and thermally driven cooling from absorption chiller.

CHP Diagram

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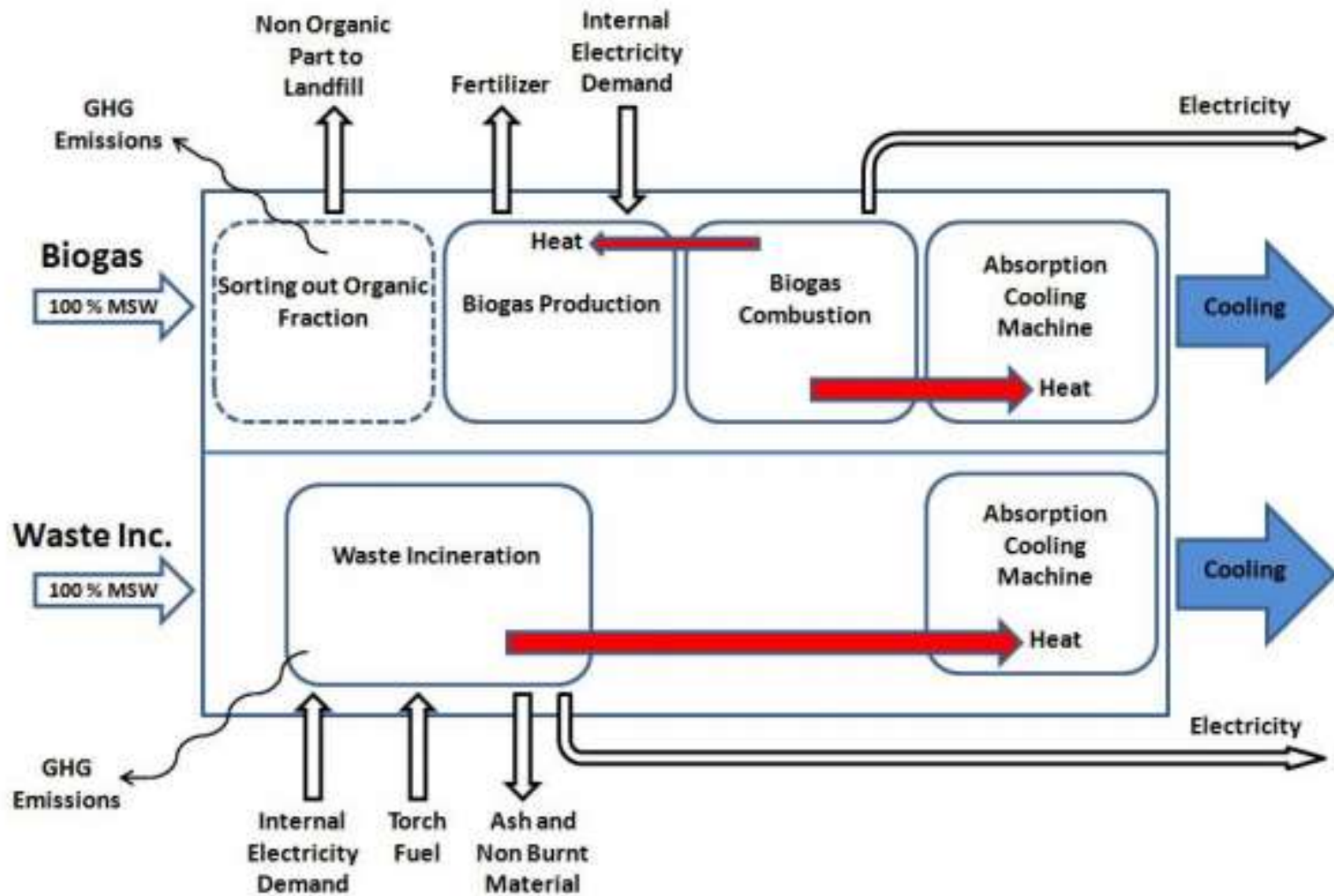


Figure 5-1 – A schematic figure of the different flows in the model

Energy Potentials – Prime Movers

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Table 6: Electric and Thermal Energy Potential with CHP for Typically Sized Digester

	No CHP System	Reciprocating Engine CHP/ Rich-Burn	Reciprocating Engine CHP/ Lean-Burn	Microturbine CHP	Fuel Cell CHP
Total WWTF Flow (MGD)	9.1	9.1	9.1	9.1	9.1
Heat Requirement for Sludge (Btu/day)	6,693,375	6,693,375	6,693,375	6,693,375	6,693,375
Wall Heat Transfer (Btu/day)	591,725	591,725	591,725	591,725	591,725
Floor Heat Transfer (Btu/day)	1,109,484	1,109,484	1,109,484	1,109,484	1,109,484
Roof Heat Transfer (Btu/day)	741,013	741,013	741,013	741,013	741,013
Total Digester Heat Load (Btu/day)	9,135,597	9,135,597	9,135,597	9,135,597	9,135,597
Fuel Required for Digester Heat Load* (Btu/day) (HHV)	11,419,496				
Energy Potential of Gas (Btu/day) (HHV)	58,901,700	58,901,700	58,901,700	58,901,700	58,901,700
% of Gas Used for Digester Heat Load (Btu/day)	19.4%				
Excess Digester Gas** (Btu/day)	47,482,204				
Electric Efficiency (HHV)		29.1%	32.6%	26.0%	42.3%
Power-to-Heat Ratio		0.62	0.86	0.88	1.26
Total CHP Efficiency (HHV)		76%	71%	56%	76%
Electric Production (Btu/day)		17,140,395	19,201,954	15,314,442	24,915,419
Electric Production (kW)		209	234	187	304
Heat Recovery (Btu/day)		27,645,798	22,327,854	17,402,775	19,774,142
Digester Heat Load (Btu/day)		9,135,597	9,135,597	9,135,597	9,135,597
Additional Heat Available*** (Btu/day)		18,510,201	13,192,257	8,267,178	10,638,545

Note: Analysis assumes 50 percent summer and 50 percent winter digester operation.

*Assumes 80 percent efficient boiler.

**Assumes no other uses except boiler.

***Available for non-digester heating uses at the facility (e.g., space heating, hot water).

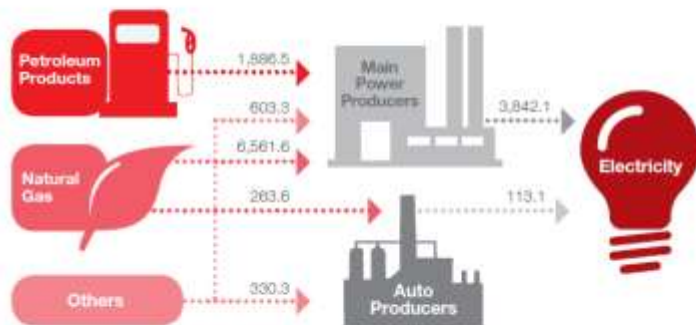
Energy Flow & Fuel Mix

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ENERGY FLOWS IN THE POWER GENERATION SECTOR

In 2011, a total of 3,955.2 ktoe of electricity was generated by the power generation sector in Singapore. Main Power Producers consumed 1,886.5 ktoe of petroleum products, 6,561.6 ktoe of natural gas and 603.3 ktoe of other energy products to produce 3,842.1 ktoe of electricity. Autoproducers consumed 14.9 ktoe of petroleum products, 263.6 ktoe of natural gas and 330.3 ktoe of other energy products to produce 113.1 ktoe of electricity, primarily for their own consumption.

	Petroleum products	Natural Gas	Others	Electricity
Total Transformation Sector	-1,901.4	-6,825.2	-933.6	3,955.2
Main Power Producers	-1,886.5	-6,561.6	-603.3	3,842.1
Autoproducers	-14.9	-263.6	-330.3	113.1



*The amount of fuel involved in electricity generation activity is indicated with a negative sign to represent consumption. The resulting amount of electricity produced is indicated in positive figures.

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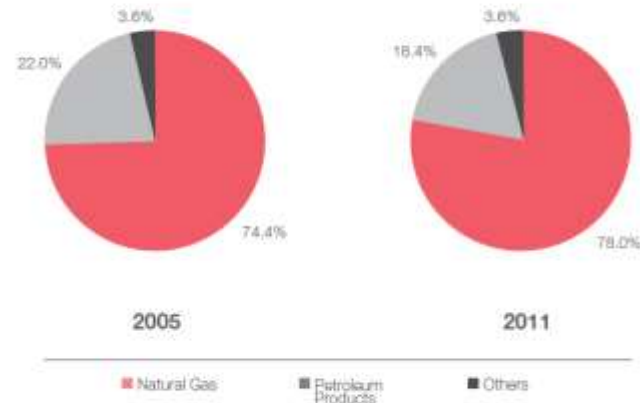
FUEL MIX FOR ELECTRICITY GENERATION

Singapore's fuel mix for electricity generation has been trending towards increasing usage of natural gas. In 2011, natural gas accounted for 78.0% of electricity generated, up from 74.4% in 2005. This was largely due to the greater role played by cleaner and more efficient Combined Cycle Gas Turbine (CCGT) plants in the Singapore power generation sector in recent years. CCGT plants primarily use natural gas as fuel to generate electricity.

Fuel Mix for Electricity Generation

Total Electricity Generated: 38.2 TWh

Total Electricity Generated: 46.0 TWh

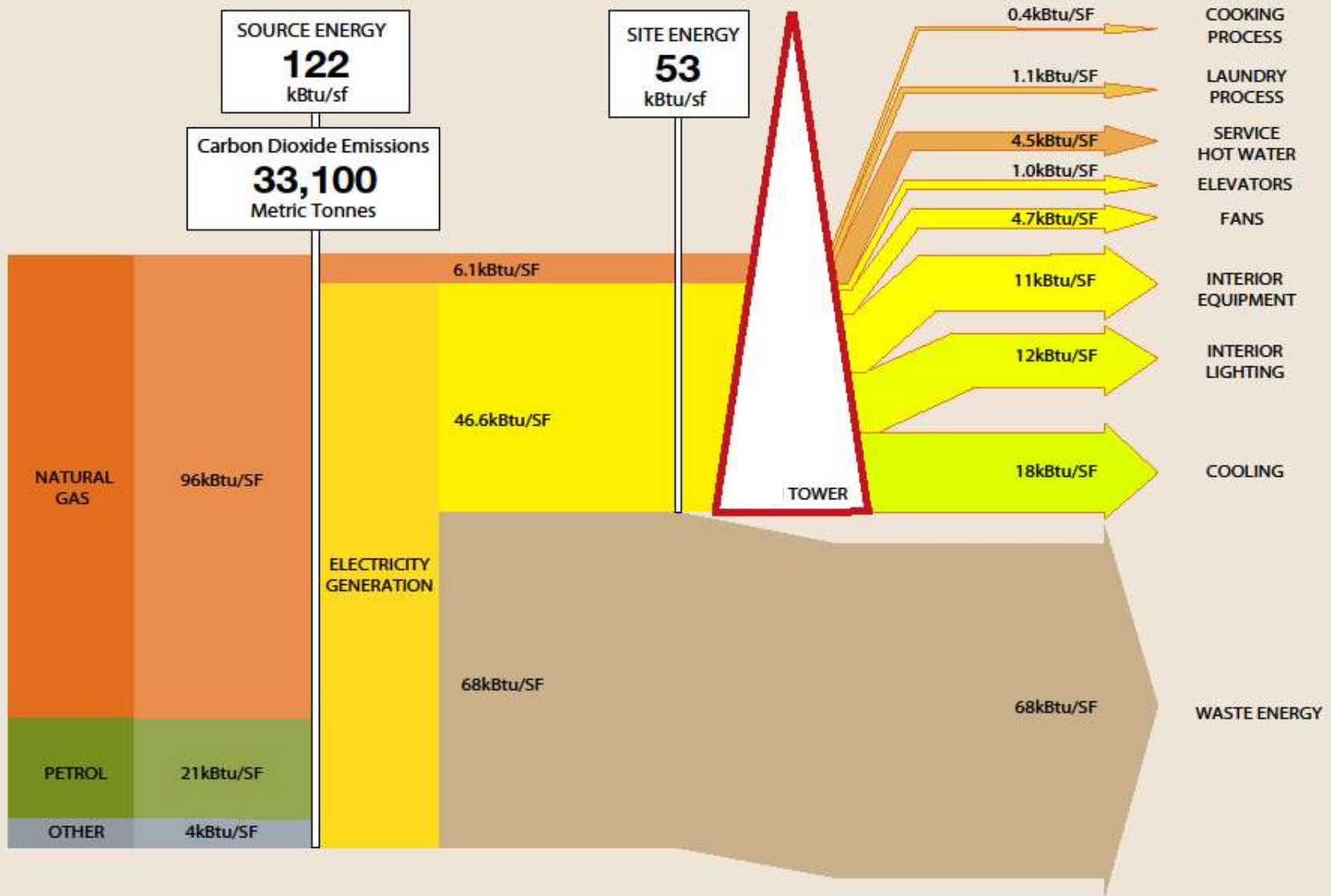


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http://www.ema.gov.sg/media/files/publications/EMA_SES_2012_Final.pdf

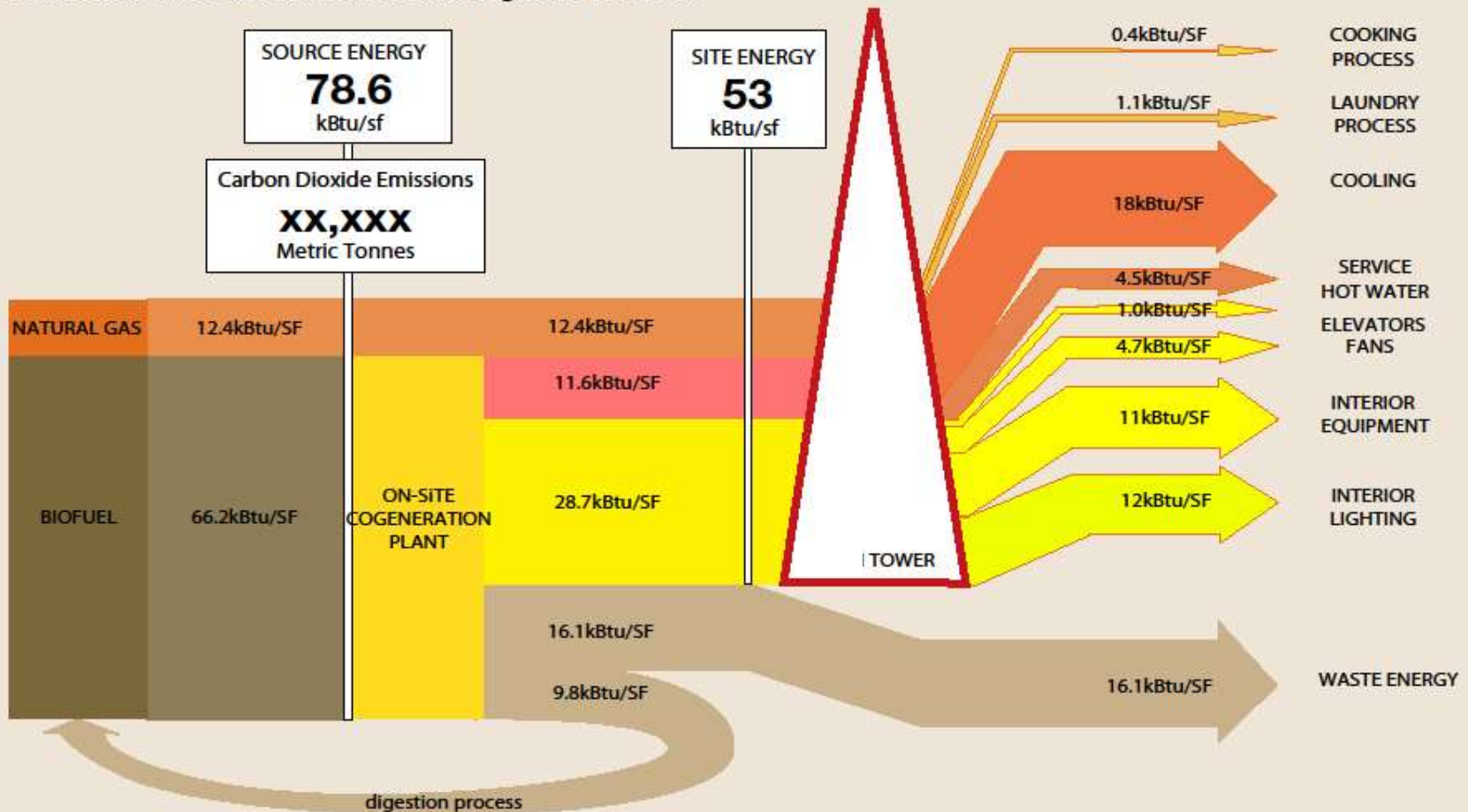
<http://www.ema.gov.sg/media/files/publications/SES%202013.pdf>

Energy Flow Diagram - ASHRAE 90.1 Code Compliant Building



Source to Site Energy Flows for a code compliant building in Singapore. Fuel use ratio determinations from Singapore Energy Statistics 2012. Based on the multiplier for this region, it takes 2.438 MBtu of energy to produce and deliver each 1.0 MBtu used at a building site. Based on Singapore's Electricity Grid Emission Factors, delivering 1.0 MBtu of electricity to the building site produces 150.8 kg Carbon Dioxide equivalent emissions. Note the amount of waste energy relative to the energy used on the site.

Energy Flow Diagram - On-site Tri-Generation with waste heat used in Anaerobic Digester Process



Source to Site Energy Flows for a code compliant building in Singapore. Fuel use ratio determinations from Singapore Energy Statistics 2012.

Based on the multiplier for this region, it takes 2.438 MBtu of energy to produce and deliver each 1.0 MBtu used at a building site.

Based on Singapore's Electricity Grid Emission Factors, delivering 1.0 MBtu of electricity to the building site produces 150.8 kg Carbon Dioxide equivalent emissions

Note the amount of waste energy relative to the energy used on the site.

Fuel from Waste Potentials

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Energy Densities of Various Waste Streams

Table 2

COD and methane emissions from various feedstock common in tropical regions

Feedstock Source	COD Range (g/L)	Average Methane Yield (m ³ /kg volatile solids)
Palm Oil Mill Effluent	50 – 150	0.39
Pig Manure	30 – 90	0.38
Dairy Manure	18 – 48	0.24
Sugar Beat	1.5 – 5.5	0.20
Municipal Solid Waste	15 – 50	0.35

Thank You!

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